

108:025-08 FRONTIER REFINING CHEYENNE REFINERY (H CONSENT DECREE, SEMILANNUAL RPTS F3, AFS Folder #: 104717



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SEP 3 - 2014 ECEJ-AT

August 29, 2014

Chief
Environmental Enforcement Section
Environment and Natural Resources Division
U.S. Department of Justice
P.O. Box 7611, Ben Franklin Station
Washington, D.C. 20044-7611

Director, Air Enforcement Division Office of Civil Enforcement U.S. Environmental Protection Agency Mail Code 2242-A 1200 Pennsylvania Avenue, N.W. Washington, D.C. 20460-0001

Chief
Mail Code 8 ENF-T
Office of Enforcement, Compliance, and
Environmental Justice
U.S. EPA Region 8
1595 Wynkoop St.
Denver, CO 80202-1129

Wyoming Department of Environmental Quality Air Quality Division Herschler Building 122 W. 25th Street Cheyenne, WY 82002

RE: Frontier Refining LLC, Cheyenne Refinery
NPRI Consent Decree dated March 26, 2009
DOJ Case No. 90-5-2-1-08660
Civil Case No. 09-CV-1032-WEB-KMH
Submittal of Semi-annual Progress Report: January 1, 2014 through
June 30, 2014

To Whom It May Concern:

Pursuant to Section XI of the referenced Consent Decree, Frontier Refining LLC is hereby submitting the semi-annual progress report for January 1, 2014 through June 30, 2014 (see attached).

I certify under penalty of law that this information was prepared under my direction or supervision in accordance with a system designed to assure that qualified personnel properly gather and evaluate the information submitted. Based on my directions and my inquiry of the person(s) who manage the system, or the person(s) directly responsible for gathering the information, the information submitted is, to the best of my knowledge and belief, true, accurate, and complete.

Frontier Refining LLC

P.O. Box 1588 • Cheyenne, WY 82003-1588 (307) 634-3551 • Fax (307) 771-8794 http://www.hollyfrontier.com Please contact me at (307) 771-8706 if you have any questions.

Sincerely,

Glenn Travis

Environmental Manager Frontier Refining LLC

Attachments

cc: Director, Air Enforcement Division
Office of Civil Enforcement
U.S. Environmental Protection Agency
c/o Matrix New World Engineering, Inc.
26 Columbia TPKE STE 200
Florham Park, NJ 07932-2213

Electronic copy to csullivan@matrixnewworld.com foley.patrick@epa.gov

Introduction

In accordance with the requirements of Section XI of the NPRI Consent Decree dated March 26, 2009, Frontier Refining LLC (FR) is submitting the following "semi-annual report". This progress report lists the status of requirements with a completion deadline of June 30, 2014 or earlier. This report covers the time period from January 1, 2014 through June 30, 2014. A Report Cross Reference Table (Table 1) is provided to aid in the review process. Any attachments that are required to be submitted with this semi-annual report are provided behind the respective section.

(307) 634-3551 • Fax (307) 771-8794 http://www.hollyfrontier.com

Table 1 Report Cross Reference

Paragraph	Requirements	Comments	Attachment
216	FRI and FEDRC shall submit to EPA and the Applicable Intervenor, semi-annual reports due on August 31st (covering the prior period from January 1st to June 30th) and February 28th (covering the prior period from July 1st to December 31st), with the first such report due on August 31, 2009. The semi-annual reports shall contain the following information for each relevant Covered Refinery:		See below
216a	For the period covered by the report, a summary of the emissions data for the Covered Refinery that is specifically required by the reporting requirements of the Consent Decree;	Emissions reported per Paragraph 217 below	See below
216b	A description of any problems anticipated with respect to meeting the requirements of this Consent Decree at each Covered Refinery;	There are no problems anticipated. Some information on future plans is included in the summary of additional requirements.	н
216c	A description of all Supplemental Environmental Projects and Implementation activity in accordance with this Consent Decree;	SEPs are all completed.	F
216d	Any such additional matters as FRI or FEDRC believes should be brought to the attention of the Applicable Federal and State Agencies;	See summary of additional requirements.	н
216e	Any additional items required by any other Paragraph of this Consent Decree to be submitted with a semi- annual report including but not limited to reports required under Paragraphs 137, 152, 170, and 205.		137: A, 150 & 172: E, 205: F
217	In the semi-annual report required to be submitted on August 31st of each year, FRI and FEDRC shall provide a summary of annual emissions data for each Covered Refinery for the prior calendar year, to include:		See below
217a	NOx emissions in tons per year for each heater and boiler greater than 40 mmBTU/hr maximum fired duty;		D
217b	NOx emissions in tons per year as a sum for all heaters and bollers less than 40 mmBTU/hr maximum fired duty;		D
217c	SO2, CO and PM emissions in tons per year as a sum for all heaters and bollers;		D
217d	SO2 emissions from all Sulfur Recovery Plants in tons per year;		G
217e	SO2 emissions from all Acid Gas Flaring and Tail Gas Incidents by flare in tons per year;		C
217f	NOx, SO2, PM and CO emissions in tons per year as a sum at each Covered Refinery for all other emissions units for which emissions information is required to be included in the facilities' annual emissions summaries and that are not identified above;		н
217g	SO2, NOx, CO and PM emissions in tons per year for each FCCU,		8
217h	for each of the estimates or calculations in Subparagraphs 217.a. through 217.g. above, the basis for the emissions estimate or calculation (i.e. stack tests, CEMS, emission factor, etc.).	Included with each emission summary table.	N/A
217	To the extent that the required emissions summary data is available in other reports generated by FRI and/or FEDRC, as appropriate, such other reports can be attached or the appropriate information can be extracted from such other reports and attached to the semi-annual report to satisfy the requirement.	All of the necessary Information is included in this report unless noted otherwise.	N/A
218	In each semi-annual report required under Paragraph 216 for each Covered Refinery, FRI and FEDRC shall provide a summary of all exceedances of emission limits required or established by this Consent Decree, which shall include:		See below
218a	for operating units emissions limits that are required by this Consent Decree and monitored with CEMS, for each CEMS:	CEM monitoring data is contained in each applicable section.	FCCU: B, Heaters: D, SRP: G
218b	for any exceedance of an emissions limit required by this Consent Decree from an operating unit monitored through stack testing:	No exceedances of an emission limit from an operating unit monitored through stack testing occurred in this reporting period.	N/A
219	Each Covered Retinery's semi-annual report shall be certified by either the person responsible for environmental management and compliance for that Covered Refinery, or by a person responsible for overseeing implementation of this Consent Decree. The certification shall state: I certify under penalty of law that this information was prepared under my direction or supervision in accordance with a system designed to assure that qualified personnel properly gather and evaluate the information submitted. Based on my directions and my inquiry of the person(s) who manage the system, or the person(s) directly responsible for gathering the information, the information submitted is, to the best of my knowledge and belief, true, accurate, and complete.	Certification contained on the cover letter.	Cover Letter

Section A - BWON

Certificates

Quarterly Sampling

1st & 2nd Quarter Reports

Frontier Refining LLC
P.O. Box 1588 • Cheyenne, WY 82003-1588

Paragraph	Attachment A - BWON	Comments
137	Record Keeping and Reporting Requirements for this Section VI.L: As part of either the reports required under 40 C.F.R. § 61.357 or the progress report procedures of Part IX of this Consent Decree (Record Keeping and Reporting), for their respective Covered Refinery, FRI and FEDRC shall submit the following information as part of the quarterly report required pursuant to 40 C.F.R. § 61.357(d)(6) and (7) ("Section 61.357 Reports") (for FEDRC) or in the reports due pursuant to Paragraph 216 of this Decree:	The information is reported as described below.
137a	Sampling Results under Paragraphs 123, 124, and 125. The report shall include a list of all waste streams sampled, the results of the benzene analysis for each sample, and the computation of the quarterly and projected calendar year TAB (for the FRI Refinery) and the quarterly and projected calendar year uncontrolled benzene quantity (for the FEDRC Refinery);	This information is included in the reports under §61.357, which are also included in this section. Because Frontier has been determined to be >10 Mg/yr facility, the report includes the uncontrolled benzene quantity as opposed to the TAB.
123	The Sampling Plan shall commit FRI and/or FEDRC, as appropriate, to analyze, in each calendar quarter at least three representative samples from all waste streams identified in Paragraph 122.a and all locations identified in Paragraph 122.b.	Results from this sampling is included in the quarterly reports.
124	For Covered Refineries with a TAB greater than or equal to 10 Mg/yr, the Sampling Plans shall identify:	See below for sampling results details. As part of the recent audit and work following, Frontier has done a thorough review of the BWON Sampling Plan and is in the process of determining how the plan needs to be updated. After it is determined how to update the plan to properly reflect operations, it will be submitted and implemented.
124a	each uncontrolled waste stream that contains greater than 0.05 Mg/yr of benzene at the point of generation;	Results from this sampling is included in the quarterly reports.
3 7AF 1	the proposed End-of-Line sampling locations and methods for flow calculations to be used in calculating projected quarterly and annual uncontrolled benzene quantity calculations under the terms of Paragraph 129.	Results from EOL sampling is included in the quarterly reports.
	The Sampling Plan required under Paragraph 124 shall commit FRI and/or FEDRC, as appropriate, to analyze, in each calendar quarter, at least three representative samples from all waste streams identified in Subparagraphs 124.c.	Results from this sampling is included in the quarterly reports.
737b I	Training. Initial and/or subsequent training conducted by FRI and FEDRC in accordance with Paragraphs 115 - 117;	See below

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Paragraph	Attachment A - BWON	Comments
115	Benzene Waste Sample Training. By the later of the Date of Entry or March 31, 2009, FRI and FEDRC shall develop and begin annual (i.e., once each calendar year) training for all employees asked to draw BWON samples at either of the Covered Refineries.	Training completed as required. Training records are attached.
116	Standard Operating Procedures for BWON Equipment. By the later of the Date of Entry or March 31, 2009, FEDRC shall complete the development of standard operating procedures for all control equipment used to comply with the BWON at the Covered Refinery.	Frontier recently voluntarily disclosed audit findings that identified these procedures and training were deficient. Frontier is in the process of correcting those deficiencies.
1 <u>.</u> 16a	On or before June 1, 2009, FEDRC shall complete an initial training program regarding these procedures for all operators assigned to this equipment. FEDRC shall provide comparable training to any persons who subsequently become operators, prior to their assumption of this duty. Until termination of this Decree, "refresher" training in these procedures shall be performed at a minimum on a three (3) year cycle.	Not Applicable
116b	The FRI Refinery shall comply with the provisions of Paragraph 116 if and when its TAB reaches 10 Mg/yr. FRI shall propose a schedule for training at the same time that FRI proposes a plan, pursuant to Paragraph 94, that identifies the compliance strategy and schedule that FRI shall implement to maintain compliance with the waste benzene NESHAP.	Frontier recently voluntarily disclosed audit findings that identified these procedures and training were deficient. Frontier is in the process of correcting those deficiencies.
117	Training: Contractors. As part of their training program, FRI and FEDRC must ensure that the employees of any contractors hired to perform the requirements of Paragraphs 115 and 116 are properly trained to implement all applicable provisions of this Section VI.L.	Frontier recently voluntarily disclosed audit findings that identified these procedures and training were deficient. Training was completed as required. Training records are attached.
137c	Laboratory Audits. Initial and subsequent audits conducted by FRI and FEDRC pursuant to Paragraphs 110 - 113, through the calendar quarter for which the quarterly report is due, including in each such report, at a minimum, the identification of each laboratory audited, a description of the methods used in the audit, and the results of the audit.	See below
110	Laboratory Audits. FRI and FEDRC shall conduct audits as required by Paragraphs 111 - 112, below, of all laboratories that perform analyses of their respective BWON samples to ensure that proper analytical and quality assurance/quality control procedures are followed.	BWON lab audits were conducted on 8/13/2013 and 8/17/2013. Results of both audits are attached. A subsequent audit is required at least once every two years.
111	Within one year from the Date of Entry, FRI and FEDRC shall complete audits of all of the laboratories they each use to perform analyses of BWON samples. Thereafter, FRI and FEDRC shall audit any new laboratory to be used for analyses of BWON samples prior to such use.	Completed previously.

Paragraph	Attachment A - BWON	Comments
112	Until this Consent Decree is terminated, FRI and FEDRC shall conduct subsequent audits of each of their respective laboratories used for BWON analyses at least once every two years.	BWON lab audits were conducted on 8/13/2013 and 8/17/2013. Results of both audits are attached. A subsequent audit is required at least once every two years.
113	sole responsibility and obligation of FRI and FEDRC to ensure that the Covered Refineries comply with this Consent Decree and Subpart FF.	Frontier utilizes a third party to conduct the audits.
130	In making the calculations required under Paragraph 129, FRI and FEDRC shall use the average of the three (3)	The calculations are submitted in the required reports and included in the quarterly reports.

2014 Q2 UNCONTROLLED QUANTITY BASED ON QUARTERLY END OF LINE CONSENT DECREE SAMPLING RESULTS FRONTIER REFINING LLC, CHEYENNE REFINERY, CHEYENNE, WYOMING

Quarter	Equipment Description	Percent Aqueous	Percent Organic	Hydrocarbon Density (lbs/ft²)	Benzene Concentration Aqueous (mg/L)	Benzene Concentration Organic (mg/kg)	Total Benzene in Waste (ppmw)	Flow (gal/min)	Quarterly Estimated Uncontrolled BQ (Mg/yr)	Total Annual Estimated Uncontrolled BQ (Mg/yr)
1Q 2014	API Effluent (Total)	99.73	0.27	55.44	2.76	371.59	3.66	583.92	0.4742	1.8969
	Desalter Effluent (Controlled)	99.22	0.78	55.44	19.27	1926.67	32.54	28.63	= #v	
	Coker API Effluent (Controlled)	99.00	1.00	55.44	1.09	108.77	2.05	107.40	χτ	
	Groundwater (Controlled)	99.95	0.05	55.44	1.09	109.00	1.14	30.00		
2Q 2014	API Effluent (Total)	99.18	0.82	57.09	2.00	213.22	3.59	587.2	→ 0.2445	1.4374
	Desalter Effluent (Controlled)	99.22	0.78	57.09	16.37	1636.67	27.98	43.53		
	Coker API Effluent (Controlled)	99.00	1.00	57.09	1.23	123.07	2,35	106,14	*2.=	
	Groundwater (Controlled)	99.95	0.05	57.09	4.73	473.10	4.95	30.00		

quarterly limit = 1.5 Mg

2014 Q1 UNCONTROLLED WASTE STREAMS >0.05 MG FRONTIER REFINING LLC, CHEYENNE REFINERY, CHEYENNE, WYOMING

Quarter	Equipment Description	Percent Aqueous	Percent Organic	Hydrocarbon Density (lbs/ft³)	Benzene Concentration Aqueous (mg/L)	Benzene Concentration Organic (mg/kg)	Total Benzene in Waste (ppmw)	Flow (gal/min)	Total Annual Estimated Uncontrolled BQ (Mg/yr)
1Q 2014	Tank 34	95.00	5.00	48.69	95.30	9530.00	467.50	0.00008	0.00007
	Flare Knockout	80.00	20.00	51.04	3.50	350.33	62.38	0.00	0.00000
	P-528A/B	0.00	100.00	45.04	19.82	1982.00	1982.01	0.00	0.0000

2014 Q2 UNCONTROLLED WASTE STREAMS >0.05 MG FRONTIER REFINING LLC, CHEYENNE REFINERY, CHEYENNE, WYOMING

Quarter	Equipment Description	Percent Aqueous	Percent Organic	Hydrocarbon Density (lbs/ft³)	Benzene Concentration Aqueous (mg/L)	Benzene Concentration Organic (mg/kg)	Total Benzene in Waste (ppmw)	Flow (gal/min)	Total Annual Estimated Uncontrolled BQ (Mg/yr)
2Q 2014	Tank 34	95.00	5.00	48.69	53.60	5360.00	262.94	0.00008	0.00004
	Flare Knockout	80.00	20.00	47.77	17.31	1731.27	292.62	0.00	0.00000
	P-528A/B	0.00	100.00	43.99	32.59	3259.00	3259.01	0.00	0.00000



Certificate of Completion

This document certifies that Calvin Williams

has completed Trihydro's training program for **Method 25D**

Awarded: 4/4/2014



This document certifies that Will Scaggari

has completed Trihydro's training program for **Method 25D**

Awarded: 4/15/2013



This document certifies that Korey Kennedy

has completed Trihydro's training program for **Method 25D**

Awarded: 4/16/2013



This document certifies that Jacob Berreth

has completed Trihydro's training program for **Method 25D**

Awarded: 12/2/2013

Section B – FCCU

CEMS Data

Frontier Refining LLC
P.O. Box 1588 • Cheyenne, WY 82003-1588

Report Period January 1 – July 31, 2014

Paragraph	Attachment B - FCCU	Comments
247-	CO3 NO. CO and DNA amingtons in tone persons for each ECCU	Emissions information contained in
217g	SO2, NOx, CO and PM emissions in tons per year for each FCCU,	this section.
	for each of the estimates or calculations in Subparagraphs 217.a. through 217.g. above, the basis for the emissions estimate or calculation (i.e. stack tests, CEMS, emission factor, etc.).	Basis for the emission estimate or
f 717M		calculation is included with the
l		emission information.
3100	for operating units emissions limits that are required by this Consent Decree and monitored with CEMS, for	CEM monitoring data is included in
218a	each CEMS:	this section.

1Q14

DEPARTMENT OF ENVIRONMENTAL QUALITY AIR QUALITY DIVISION CONTINUOUS EMISSION MONITORING REPORT

FORM A

I. GENERAL INFORMATION

- A. Facility Name: FRONTIER REFINING LLC
- B. Process Unit/Pollutant Monitored: NO_x MONITORING SYSTEM FLUIDIZED CATALYTIC CRACKING UNIT (FCCU) REGENERATOR
- C. Applicable Permit Number or Regulation: Consent Decree, MD-9640
 - D. Applicable Emission Limit: 21.9 lb/hr (7-day rolling average); 10.9 lb/hr (365-day rolling average); 120 ppmvd @ 0% 0, (7-day rolling average); 60ppmvd @ 0% 0, (365-day rolling average)

II. MONITOR INFORMATION

- A. Date of Original Monitor Installation: 6/5/2012
- B. Date of Latest Monitor Certification: 7/17/2012
- C. Pollutant/Opacity Monitor
 - 1. Manufacturer: Teledyne/API
 - 2. Model Number: Model 200H
 - 3. Serial Number Main Chassis: 82
 - 4. Basis of Measurement (If Applicable Wet or Dry): Dry
 - 5. Instrument Span, Range Value (Specify Units): 0-600 ppm and 0-150 lb/hr

D. Diluent Monitor NONE

- 1. Type of Monitor: O₂ or CO₂ (circle one)
- 2. Manufacturer:
- 3. Model Number:
- 4. Serial Number Main Chassis
- 5. Basis of Measurement (If Applicable Wet or Dry):
- 6. Instrument Span, Range Value (Specify Units):___

E. Flow Monitor

- 1. Type of Instrument (i.e. S-type Pitot Tube): S-Type Pitot Tube
- 2. Manufacturer: Dieterich Standard
- 3. Model Number: PSF-S4H HSVH FADH0 FADC
- 4. Serial Number Main Chassis: <u>DFCII CEM 1MN 2XX #MN 4MN P1 ES RB TR AR YX ZS DB</u>
- F. Quality Assurance Data
 - 1. QA Plan Date: 10/15/2012
 - 2. QA Plan Approval Date: 4/22/2013

III. Operating/Monitoring Data

A. Quarter: 1 Year: 2014

B Total Hours in Reporting Period: 2160

C. Hours Unit Operated During the Reporting Period: 1902

Note: Include <u>all</u> unit operating time for the quarter including operating time associated with Startup/Shutdown and Chapter 1 Section 5 (Emergency/Abnormal) Operations. Report time in hours to one decimal place, i.e. 1902.8.

IV. Quarterly Audits/Monitoring System Modifications

A. Quarterly Audits
Type Audit: CGA

Pollutant/Opacity Monitor: Date Conducted Pass
3/20/2014 YES

Note: A copy of the quarterly audits shall be included with the corresponding quarterly excess emission report.

Equipment Replaced During Reporting Period: <u>Changed out Filters: Changed out NO. Span</u>
<u>Calibration Bottle: Replaced Sample Line Temperature Transmitter.</u>

Note: Only equipment replacements or modifications to the system that could affect the ability of the continuous monitoring system to comply with the associated Performance Specification shall be reported.

V. Report Contact

A. Name: David Weeks, Environmental Engineer

B. Phone Number: (307) 771-8827

EXCESS EMISSION SUMMARY REPORT FCCU NOx (lb/hr) CEMS 7-day rolling average = 21.9 lb/hr

FORM B

Emission Data Summary		CMS Performance Report				
I. Duration of Excess Emission in Reporting Peri	od Due to:	I. CMS Downtime in Reporting Period Due to:				
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	12.0			
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	4.0			
C. Process Problem	0.0	C. Quality Assurance Calibration	1.0			
D. Other Known Causes	0.0	D. Other Known Causes	2.0			
E. Unknown Causes	0.0	E. Unknown Causes	0.0			
II. Total Duration of Excess Emission	0.0	II. Total CMS Downtime	19.0			
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.0%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	1.0%			

Total time of excess emission events due to emergency/abnormal operations: _______. NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2 Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)
- 4. Rolling 7-day and 365-day averages are calculated for each day the emission source is operating, including days when the analyzer has downtime. A null value is used for days in a rolling average period where the unit is not operating or the CEMS downtime causes insufficient data for a valid daily average. This can result in a day where the data is considered to be both an excess emission and analyzer downtime.

1Q14 FCCU CEMS

NOx lb/hr 7-Day Rolling Average

Form C – Excess Emission Summary

FCCU Excess Emissions Summary Frontier Refining LLC NOx lbs 7-Day Rolling Excess Emissions for 1/1/2014 thru 3/31/2014

Reason	Duration
There are no excess emissions for this report.	
Total duration of NOx lbs 7-Day Rolling excess emissions	0
Total operating time	1902 hours
Operating time with excess emissions	0.0%

FCCU NOx (lb/hr) CEMS 365-day rolling average = 10.9 lb/hr

FORM B

Emission Data Summary		CMS Performance Report				
I. Duration of Excess Emission in Reporting Per	riod Due to:	I. CMS Downtime in Reporting Period Due to:				
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	12.0			
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	4.0			
C. Process Problem	0.0	C. Quality Assurance Calibration	1.0			
D. Other Known Causes	0.0	D. Other Known Causes	2.0			
E. Unknown Causes	0.0	E. Unknown Causes	0.0			
II. Total Duration of Excess Emission	0.0	II. Total CMS Downtime	19.0			
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.0%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	1.0%			

Total time of excess emission events due to emergency/abnormal operations: _______.

NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2 Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)
- 4. Rolling 7-day and 365-day averages are calculated for each day the emission source is operating, including days when the analyzer has downtime. A null value is used for days in a rolling average period where the unit is not operating or the CEMS downtime causes insufficient data for a valid daily average. This can result in a day where the data is considered to be both an excess emission and analyzer downtime.

1Q14 FCCU CEMS

NOx lb/hr 365-Day Rolling Average

Form C – Excess Emission Summary

FCCU Excess Emissions Summary

Frontier Refining LLC NOx lbs 365-Day Rolling Excess Emissions for 1/1/2014 thru 3/31/2014

Reason	Duration	
There are no excess emissions for this report.		
Total duration of NOx ibs 365-Day Rolling excess emissions	0	
Total operating time	1902 hours	
Operating time with excess emissions	0.0%	

1Q14 FCCU CEMS

NOx Lb/Hr

Form D – Downtime Summary

FCCU CEMS Downtime Summary Frontier Refining LLC NOx ibs CEMS Downtime for 1/1/2014 thru 3/31/2014

Reason	Duration	
CiSCO Technician inadvertantly triggered a calibration on the FCCU CEMS while working on the Crude Charge Heater CEMS causing the data to go OOC	1 hour	
Cylinder Gas Audit (CGA)	1 hour	
Maintenance - High Stack Vacuum	1 hour	
NOx and SO2 Lb/Hr Data Invalid - Formula Input Out of Range	3 hours	
NOx ib/hr & SO2 ib/hr Invalid Data - Low Excess O2 - Formula Input Out of Range	1 hour	
Unit Start-up - Analyzer Calibration Checks Falled	12 hours	
Total duration of NOx lbs CEMS downtime	19 hours	
Total operating time	1902 hours	
Operating time with CEMS downtime	1.0%	

FCCU CEMS Downtime

Frontier Refining LLC NOx lbs CEMS Downtime for 1/1/2014 thru 3/31/2014

Parameter	Start	End	Duration	Reason	Action
NOx ibs	1/4/2014 8:00 AM	10:59 AM	3 hours	NOx and SO2 Lb/Hr Data Invalid - Formula Input Out of Range	Adjusted Excess O2
NOx ibs	1/6/2014 9:00 AM	9:59 AM	1 hour	NOx lb/hr & SO2 lb/hr Invalid Data - Low Excess O2 - Formula Input Out of Range	Adjusted Excess O2
NOx ibs	1/8/2014 9:00 AM	9:59 AM	1 hour	Maintenance - High Stack Vacuum	Changed out sample filters both at the probe and the cabinet. Blow out sample line.
NOx lbs	1/21/2014 1:00 PM	1:59 PM	1 hour	CISCO Technician inadvertantly triggered a calibration on the FCCU CEMS white working on the Crude Charge Heater CEMS causing the data to go OOC	Ran Manual Celibration
NOx ibs	2/16/2014 12:00 AM	11:59 AM	12 hours	Unit Start-up - Analyzer Calibration Checks Falled	Ran Manual Calibration
NOx lbs	3/20/2014 9:00 AM	9:59 AM	1 hour	Cylinder Gas Audit (CGA)	Performed NOx, SO2, CO & O2 CGA
	Total duration		19 hours		

EXCESS EMISSION SUMMARY REPORT FCCU NOx (ppm) CEMS 7-day Rolling Average = 120 ppmvd @ 0% 02

FORM B

Emission Data Summary		CMS Performance Report	
I. Duration of Excess Emission in Reporting Per	iod Due to:	I. CMS Downtime in Reporting Period Due to:	
A. Startup/Shutdown	48.0	A. Monitor Equipment Malfunction	0.0
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	11.0
C. Process Problem	0.0	C. Quality Assurance Calibration	1.0
D. Other Known Causes	0.0	D. Other Known Causes	1.0
E. Unknown Causes	0.0	E. Unknown Causes	0.0
II. Total Duration of Excess Emission	48.0	II. Total CMS Downtime	13.0
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	2.5%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	0.7%

Total time of excess emission events due to emergency/abnormal operations: $\underline{0}$. NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2 Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)
- 4. Rolling 7-day and 365-day averages are calculated for each day the emission source is operating, including days when the analyzer has downtime. A null value is used for days in a rolling average period where the unit is not operating or the CEMS downtime causes insufficient data for a valid daily average. This can result in a day where the data is considered to be both an excess emission and analyzer downtime.

1Q14 FCCU CEMS

NOx ppm @ 0% O2 7-Day Rolling Average

Form C – Excess Emission Summary

FCCU Excess Emissions Summary

Frontier Refining LLC
NOx ppm @0% O2 7-Day Rolling Excess Emissions for 1/1/2014 thru 3/31/2014

Reason	Duration	
Emission Exceedence - NOx ppm @ 0% O2 7-Day Rolling Average	48 hours	
Total duration of NOx ppm @0% O2 7-Day Rolling excess emissions	48 hours	
Total operating time	1902 hours	
Operating time with excess emissions	2.5%	

FCCU Excess Emissions

Frontier Refining LLC
NOx ppm @0% O2 7-Day Rolling Excess Emissions for 1/1/2014 thru 3/31/2014

Parameter	Start	End	Duration	Value	Min	Max	Limit	Reason	Action
NOx ppm @0% O2 7-Day Rolling	2/16/2014	11:59 PM	24 hours	81.0	81.0	81.0	120	Emission Exceedence - NOx ppm @ 0% O2 7-Day Rolling Average	Lowered Excess O2 Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx pprn @0% O2 7-Day Rolling	2/17/2014	11:59 PM	24 hours	86.8	86.8	86.8	120	Emission Exceedence - NOx ppm @ 0% O2 7-Day Rolling Average	Lowered Excess O2 Added DeNOx Additive; increased Stripping Steam; Added CGO to Feed

FCCU NOx (ppm) CEMS 365-day rolling average = 60 ppmvd @ 0% 02

FORM B

Emission Data Summary		CMS Performance Report	
I. Duration of Excess Emission in Reporting Per	riod Due to:	I. CMS Downtime in Reporting Period Due to:	
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	0.0
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	11.0
C. Process Problem	1015.0	C. Quality Assurance Calibration	1.0
D. Other Known Causes	0.0	D. Other Known Causes	1.0
E. Unknown Causes	0.0	E. Unknown Causes	0.0
II. Total Duration of Excess Emission	1015.0	II. Total CMS Downtime	13.0
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	53.4%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	0.7%

Total time of excess emission events due to emergency/abnormal operations: _______.

NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2 Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)
- 4. Rolling 7-day and 365-day averages are calculated for each day the emission source is operating, including days when the analyzer has downtime. A null value is used for days in a rolling average period where the unit is not operating or the CEMS downtime causes insufficient data for a valid daily average. This can result in a day where the data is considered to be both an excess emission and analyzer downtime.

1Q14 FCCU CEMS

NOx ppm @ 0% O2 365-Day Rolling Average

Form C – Excess Emission Summary

FCCU Excess Emissions Summary

Frontier Refining LLC
NOx ppm @0% O2 365-Day Rolling Excess Emissions for 1/1/2014 thru 3/31/2014

Reason	Duration	
Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	1015 hours	
Total duration of NOx ppm @0% O2 365-Day Rolling excess emissions	1015 hours	
Total operating time	1902 hours	
Operating time with excess emissions	53.4%	

FCCU Excess Emissions

Frontier Refining LLC
NOx ppm @0% O2 365-Day Rolling Excess Emissions for 1/1/2014 thru 3/31/2014

Parameter	Start	End	Duration	Value	Min	Max	Limit	Reason	Action
NOx ppm @0% O2 365-Day Roiling	1/1/2014	11:59 PM	24 hours	64.0	64.0	64.0	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @ 0% O2 365-Day Rolling	1/2/2014	11:59 PM	24 hours	63.9	63.9	63.9	60	Emission Exceedence - NOx ppm @ 0% O2 385-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/3/2014	11:59 PM	24 hours	63.9	63.9	63.9	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/4/2014	11:59 PM	24 hours	63.7	63.7	63.7	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/5/2014	11:59 PM	24 hours	63.5	63.5	63.5	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess C2; Added DeNOx Additive; increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/6/2014	11:59 PM	24 hours	63.4	63.4	63.4	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/7/2014	11:59 PM	24 hours	63.3	63.3	63.3	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed

Parameter	Start	End	Duration	Value	Min	Max	Limit	Reason	Action
NOx ppm @0% O2 365-Day Rolling	1/8/2014	11:59 PM	24 hours	63.2	63.2	63.2	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/9/2014	11:59 PM	24 hours	63.1	63.1	63.1	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/10/2014	11:59 PM	24 hours	63.0	63.0	63.0	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/11/2014	11:59 PM	24 hours	62.9	62.9	62.9	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/12/2014	11:59 PM	24 hours	62.8	62.8	62.8	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/13/2014	11:59 PM	24 hours	62.9	62.9	62. 9	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/14/2014	11:59 PM	24 hours	62.9	62.9	82.9	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/15/2014	11:59 PM	24 hours	62.8	62.6	62.8	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; increased Stripping Steam; Added CGO to Feed

Parameter	Start	End	Duration	Value	Min	Max	Limit	Reason	Action
NOx ppm @0% O2 365-Day Rolling	1/16/2014	11:59 PM	24 hours	62.8	62.8	62.8	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 385-Day Rolling	1/17/2014	11:59 PM	24 hours	62.7	62.7	62.7	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/18/2014	11:59 PM	24 hours	62.6	62.6	62.6	60	Emission Exceedence - NOx ppm @ 0% 02 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/19/2014	11:59 PM	24 hours	62.5	62.5	62.5	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/20/2014	11:59 PM	24 hours	62.6	62.6	62.6	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/21/2014	11:59 PM	24 hours	62.5	62.5	62.5	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/22/2014	11: 59 PM	24 hours	62.5	62.5	62.5	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/23/2014	11:59 PM	24 hours	62.5	62.5	62.5	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; increased Stripping Steam; Added CGO to Feed

Parameter	Start	End	Duration	Value	Min	Max	Llmit	Reason	Action
NOx ppm @0% O2 365-Day Rolling	1/24/2014	11:59 PM	24 hours	62.5	62.5	62.5	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/25/2014	11:59 PM	24 hours	62.5	62.5	62.5	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/26/2014	11:59 PM	24 hours	62.4	62.4	62.4	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/27/2014	11:59 PM	24 hours	62.3	62.3	62.3	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/28/2014	11:59 PM	24 hours	62.3	62.3	62.3	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/29/2014	11:59 PM	24 hours	62.2	62.2	62.2	60	Emission Exceedence - NOx ppm @ 0% O2 385-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/30/2014	11:59 PM	24 hours	62.2	62.2	62.2	60	Emission Exceedence - NOx ppm @ 0% O2 385-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	1/31/2014	11:59 PM	24 hours	62.1	62.1	62.1	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed

Parameter	Start	End	Duration	Value	Min	Max	Limit	Reason	Action
NOx ppm @0% O2 385-Day Rolling	2/1/2014	11:59 PM	24 hours	62.1	62.1	62.1	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	2/2/2014	11:59 PM	24 hours	62.0	62.0	62.0	60	Emission Exceedence - NOx ppm @ 0% O2 385-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	2/3/2014	11:59 PM	24 hours	61.8	61.8	61.8	60	Emission Exceedence - NOx ppm @ 0% O2 385-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	2/4/2014	11:59 PM	24 hours	61.8	61.8	61.8	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	2/5/2014	7:59 AM	8 hours	61.8	61.8	61.8	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	2/18/2014	11:59 PM	24 hours	61.8	61.8	61.8	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	2/19/2014	11:59 PM	24 hours	61.6	61.6	61.6	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	2/20/2014	11:59 PM	24 hours	61.3	61.3	61.3	60 ,	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; increased Stripping Steam; Added CGO to Feed

Parameter	Start	End	Duration	Value	Min	Max	Limit	Reason	Action
NOx ppm @0% O2 365-Day Rolling	2/21/2014	11:59 PM	24 hours	61.0	61.0	61.0	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	2/22/2014	11:59 PM	24 hours	60,7	60.7	60.7	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 365-Day Rolling	2/23/2014	11:59 PM	24 hours	60.5	60.5	60.5	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed
NOx ppm @0% O2 385-Day Rolling	2/24/2014	10:59 PM	23 hours	60.2	60.2	60.2	60	Emission Exceedence - NOx ppm @ 0% O2 365-Day Rolling Average	Lowered Excess O2; Added DeNOx Additive; Increased Stripping Steam; Added CGO to Feed

Total duration

1015 hours

NOx ppm @ 0% O2

Form D – Downtime Summary

FCCU CEMS Downtime Summary Frontier Refining LLC NOx ppm @0% O2 CEMS Downtime for 1/1/2014 thru 3/31/2014

Reason	Duration
CISCO Technician inadvertantly triggered a calibration on the FCCU CEMS while working on the Crude Charge Heater CEMS causing the data to go OOC	1 hour
Cylinder Gas Audit (CGA)	1 hour
Unit Start-up - Analyzer Calibration Checks Feiled	11 hours
Total duration of NOx ppm @0% O2 CEMS downtime	13 hours
Total operating time	1902 hours
Operating time with CEMS downtime	0.7%

FCCU CEMS Downtime

Frontier Refining LLC NOx ppm @0% O2 CEMS Downtime for 1/1/2014 thru 3/31/2014

Parameter	Start	End	Duration	Reason	Action
NOx ppm @0% O2	1/21/2014 1:00 PM	1:59 PM	1 hour	CISCO Technician inadvertantly triggered a calibration on the FCCU CEMS while working on the Crude Charge Heater CEMS causing the data to go OOC	Ran Manual Celibration
NOx ppm @0% O2	2/16/2014 12:00 AM	10:59 AM	11 hours	Unit Start-up - Analyzer Calibration Checks Failed	Ran Manual Calibration
NOx ppm @0% O2	3/20/2014 9:00 AM	9:59 AM	1 hour	Cylinder Gas Audit (CGA)	Performed NOx, SO2, CO & O2 CGA
To	otal duration		13 hours		

1Q14

DEPARTMENT OF ENVIRONMENTAL QUALITY AIR QUALITY DIVISION CONTINUOUS EMISSION MONITORING REPORT

FORM A

I. GENERAL INFORMATION

- A. Facility Name: FRONTIER REFINING LLC
- B. Process Unit/Pollutant Monitored: <u>SO₂ MONITORING SYSTEM FLUIDIZED</u>
 CATALYTIC CRACKING UNIT (FCCU) REGENERATOR
- C. Applicable Permit Number or Regulation: MD-946
- D. Applicable Emission Limit: 320 lb/hr SQ, (1-hr average); 1401.6 tpv (calendar year)

II. MONITOR INFORMATION

- A. Date of Original Monitor Installation: 6/5/2012
- B. Date of Latest Monitor Certification: 7/17/2012
- C. Pollutant/Opacity Monitor
 - 1. Manufacturer: Teledyne/API
 - 2. Model Number: Model 100H
 - 3. Serial Number Main Chassis: 71
 - 4. Basis of Measurement (If Applicable Wet or Dry): Dry
 - 5. Instrument Span, Range Value (Specify Units): 0-1800 ppm and 0-600 lb/hr

D. Diluent Monitor NONE

- 1. Type of Monitor: O₂ or CO₂ (circle one)
- 2. Manufacturer:
- 3. Model Number:
- 4. Serial Number Main Chassis
- 5. Basis of Measurement (If Applicable Wet or Dry):
- 6. Instrument Span, Range Value (Specify Units):__

E. Flow Monitor

- 1. Type of Instrument (i.e. S-type Pitot Tube): S-Type Pitot Tube
- 2. Manufacturer: Dieterich Standard
- 3. Model Number: PSF-S4H HSVH FADH0 FADC
- 4. Serial Number Main Chassis: DFCII CEM 1MN 2XX #MN 4MN P1 ES RB TR AR YX ZS DB

F. Quality Assurance Data

- 1. QA Plan Date: 10/15/2012
- 2. QA Plan Approval Date: 4/22/2013

III. Operating/Monitoring Data

A. Quarter: 1 Year: 2014

B Total Hours in Reporting Period: 2160

C. Hours Unit Operated During the Reporting Period: 1902

Note: Include <u>all</u> unit operating time for the quarter including operating time associated with Startup/Shutdown and Chapter 1 Section 5 (Emergency/Abnormal) Operations. Report time in hours to one decimal place, i.e. 1902.8.

- IV. Quarterly Audits/Monitoring System Modifications
 - A. Quarterly Audits
 Type Audit: <u>CGA</u>

Pollutant/Opacity Monitor: 3/20/2014 Pass
YES

Note: A copy of the quarterly audits shall be included with the corresponding quarterly excess emission report.

Equipment Replaced During Reporting Period: <u>Changed out Filters: Changed out SO, Span Calibration Bottle: Replaced Sample Line Temperature Transmitter: Changed out SO, Analyzer Sample Pump.</u>

Note: Only equipment replacements or modifications to the system that could affect the ability of the continuous monitoring system to comply with the associated Performance Specification shall be reported.

V. Report Contact

A. Name: David Weeks, Environmental Engineer

B. Phone Number: (307) 771-8827

EMISSION SUMMARY REPORT FCCU SO2 (lb/hr) CEMS 1-hr average = 320 lb/hr

FORM B

Emission Data Summary		CMS Performance Report				
I. Duration of Excess Emission in Reporting Per	iod Due to:	I. CMS Downtime in Reporting Period Due to:				
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	14.0			
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	4.0			
C. Process Problem	0.0	C. Quality Assurance Calibration	1.0			
D. Other Known Causes	0.0	D. Other Known Causes	2.0			
E. Unknown Causes	0.0	E. Unknown Causes	0.0			
II. Total Duration of Excess Emission	0.0	II. Total CMS Downtime	21.0			
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.0%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	1.1%			

Total time of excess emission events due to emergency/abnormal operations: ____0__. NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2. Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)

1Q14 FCCU CEMS SO2 Lb/Hr

Form C – Excess Emission Summary

FCCU Excess Emissions Summary

Frontier Refining LLC SO2 lbs 1-Hr Excess Emissions for 1/1/2014 thru 3/31/2014

Reason	Duration
There are no excess emissions for this report.	
Total duration of SO2 lbs 1-Hr excess emissions	0
Total operating time	1902 hours
Operating time with excess emissions	0.0%

SO2 Lb/Hr

Form D – Downtime Summary

FCCU CEMS Downtime Summary Frontier Refining LLC SO2 lbs CEMS Downtime for 1/1/2014 thru 3/31/2014

Reason	Duration
CiSCO Technician inadvertantly triggered a calibration on the FCCU CEMS while working on the Crude Charge Heater CEMS causing the data to go COC	1 hour
Cylinder Gas Audit (CGA)	1 hour
Falled Morning SO2 Span Calibration Check	2 hours
Maintenance - High Stack Vacuum	1 hour
NOx and SO2 Lb/Hr Data invalid - Formula input Out of Range	3 hours
NOx tb/hr & SO2 tb/hr Invalid Data - Low Excess O2 - Formula Input Out of Range	1 hour
Unit Start-up - Analyzer Calibration Checks Failed	12 hours
Total duration of SO2 lbs CEMS downtime	21 hours
Total operating time	1902 hours
Operating time with CEMS downtime	1.1%

FCCU CEMS Downtime

Frontier Refining LLC SO2 lbs CEMS Downtime for 1/1/2014 thru 3/31/2014

Parameter	Start	End	Duration	Reason	Action
SO2 ibs	1/4/2014 8:00 AM	10:59 AM	3 hours	NOx and SO2 Lb/Hr Data Invalid - Formula Input Out of Range	Adjusted Excess O2
SO2 lbs	1/6/2014 9:00 AM	9:59 AM	1 hour	NOx Ib/hr & SO2 Ib/hr Invalid Data - Low Excess O2 - Formula Input Out of Range	Adjusted Excess O2
SO2 ibs	1/8/2014 9:00 AM	9:59 AM	1 hour	Maintenance - High Stack Vacuum	Changed out sample filters both at the probe and the cabinet, Blew out sample line.
SO2 lbs	1/21/2014 1:00 PM	1:59 PM	1 hour	CISCO Technician inadvertantly triggered a calibration on the FCCU CEMS while working on the Crude Charge Heater CEMS causing the data to go OOC	Ran Manual Calibration
SO2 ibs	2/16/2014 12:00 AM	11:59 AM	12 hours	Unit Start-up - Analyzer Calibration Checks Failed	Ran Manual Calibration
SO2 lbs	2/17/2014 6:00 AM	7:59 AM	2 hours	Falled Morning SO2 Span Calibration Check	Adjusted SO2 Span, Ran Manual Calibration
SO2 lbs	3/20/2014 9:00 AM	9:59 AM	1 hour	Cylinder Gas Audit (CGA)	Performed NOx, SO2, CO & O2 CGA
	Total duration		24 hours		

Total duration

21 hours

4Q13

DEPARTMENT OF ENVIRONMENTAL QUALITY AIR QUALITY DIVISION CONTINUOUS EMISSION MONITORING REPORT

FORM A

I. GENERAL INFORMATION

- A. Facility Name: FRONTIER REFINING LLC
- B. Process Unit/Pollutant Monitored: <u>CO MONITORING SYSTEM FLUIDIZED</u> CATALYTIC CRACKING UNIT (FCCU) REGENERATOR
- C. Applicable Permit Number or Regulation: <u>3-0-149-2; MACT Subpart UUU; Consent Decree; MD-9640</u>
- D. Applicable Emission Limit: 500 ppm (1-hr); 500 ppmvd @ 0% 02 (1-hr); 100 ppmvd @ 0% 02 (365 day rolling average); 30 lb/hr (1-hr); 18.2 lb/hr (365 day rolling average)

II. MONITOR INFORMATION

- A. Date of Original Monitor Installation: 6/5/2012
- B. Date of Latest Monitor Certification: 7/17/2012
- C. Pollutant/Opacity Monitor
 - 1. Manufacturer: Teledyne/API
 - 2. Model Number: Model 300H
 - 3. Serial Number Main Chassis: 186
 - 4. Basis of Measurement (If Applicable Wet or Dry): Dry
 - 5. Instrument Span, Range Value (Specify Units): 0-1000 ppm
- D. Diluent Monitor NONE
 - 1. Type of Monitor: O₂ or CO₂ (circle one)
 - 2. Manufacturer:
 - 3. Model Number:
 - 4. Serial Number Main Chassis
 - 5. Basis of Measurement (If Applicable Wet or Dry):
 - 6. Instrument Span, Range Value (Specify Units):
- **E.** Flow Monitor
 - 1. Type of Instrument (i.e. S-type Pitot Tube); S-Type Pitot Tube
 - 2. Manufacturer: Dieterich Standard
 - 3. Model Number: PSF-S4H HSVH FADH0 FADC
 - 4. Serial Number Main Chassis: DFCII CEM 1MN 2XX #MN 4MN P1 ES RB TR AR YX ZS DB
- F. Quality Assurance Data
 - 1. QA Plan Date: 10/15/2012
 - 2. QA Plan Approval Date: 4/22/2013

III. Operating/Monitoring Data

A. Quarter: 1 Year: 2014

B Total Hours in Reporting Period: 2160

C. Hours Unit Operated During the Reporting Period: 1902

Note: Include <u>all</u> unit operating time for the quarter including operating time associated with Startup/Shutdown and Chapter 1 Section 5 (Emergency/Abnormal) Operations. Report time in hours to one decimal place, i.e. 1902.8.

- IV. Quarterly Audits/Monitoring System Modifications
 - A. Quarterly Audits
 Type Audit: CGA

Date Conducted

<u>Pass</u>

Pollutant/Opacity Monitor:

3/20/2014

YES

Note: A copy of the quarterly audits shall be included with the corresponding quarterly excess emission report.

B. Equipment Replaced During Reporting Period: <u>Changed out Filters</u>; <u>Changed out CO Span Calibration Bottle</u>; <u>Replaced Sample Line Temperature Transmitter 1.</u>

Note: Only equipment replacements or modifications to the system that could affect the ability of the continuous monitoring system to comply with the associated Performance Specification shall be reported.

V. Report Contact

A. Name: David Weeks, Environmental Engineer

B. Phone Number: (307) 771-8827

FCCU CO (ppm) (1-hr average) CEMS 1-hr average limit = 500 ppm

FORM B

Emission Data Summary		CMS Performance Report				
I. Duration of Excess Emission in Reporting Peri	od Due to:	I. CMS Downtime in Reporting Period Due to:				
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	12.0			
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	8.0			
C. Process Problem	10.0	C. Quality Assurance Calibration	1.0			
D. Other Known Causes	0.0	D. Other Known Causes	1.0			
E. Unknown Causes	0.0	E. Unknown Causes	0.0			
II. Total Duration of Excess Emission	10.0	II. Total CMS Downtime	22.0			
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.5%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	1.2%			

Total time of excess emission events due to emergency/abnormal operations: ______. NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Porm C).
- 2. Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)

CO ppm

Form C – Excess Emission Summary

FCCU Excess Emissions Summary

Frontier Refining LLC CO ppm 1-Hr Excess Emissions for 1/1/2014 thru 3/31/2014

Reason	Duration
CO ppm, CO ppm @ 0% O2, & CO lb/hr Emission Exceedance - Decreased total charge 1000 BPD due to unit pressure. Making adjustments for vacuum, on WGC surface condenser - Low Excess O2	2 hours
CO ppm, ppm @ 0% O2, & Lb/Hr Emission Exceedance - increasing Rates - Low Excess O2	7 hours
Process Upset - Indeck Ballers #1 & #2 Shutdown	1 hour
Total duration of CO ppm 1-Hr excess emissions	10 hours
Total operating time	1902 hours
Operating time with excess emissions	0.5%

FCCU Excess Emissions

Frontier Refining LLC CO ppm 1-Hr Excess Emissions for 1/1/2014 thru 3/31/2014

Parameter	Start	End	Duration	Value	Min	Max	Limit	Reason	Action
CO ppm 1-Hr	1/3/2014 10:00 AM	11:59 AM	2 hours	915.00	828.70	1001.40	500	CO ppm, CO ppm @ 0% O2, & CO lb/hr Emission Exceedance - Decreased total charge 1000 BPD due to unit pressure. Making adjustments for vacuum, on WGC surface condenser - Low Excess O2	Adjusted Excess O2
CO ppm 1-Hr	1/10/2014 11:00 AM	5:59 PM	7 hours	786.40	536.50	999.20	500	CO ppm, ppm @ 0% O2, & Lb/Hr Emission Exceedance - Increasing Rates - Low Excess O2	Adjusted Excess O2
CO ppm 1-Hr	3/2/2014 3:00 AM	3:59 AM	1 hour	906.10	906.10	906.10	500	Process Upset - Indeck Boilers #1 & #2 Shutdown	Stabilized Unit and Restarted Bollers

Total duration

10 hours

CO ppm

Form D – Downtime Summary

FCCU CEMS Downtime Summary

Frontier Refining LLC CO ppm CEMS Downtime for 1/1/2014 thru 3/31/2014

Reason	Duration
CISCO Technician inadvertantly triggered a calibration on the FCCU CEMS while working on the Crude Charge Heater CEMS causing the data to go OOC	1 hour
CO Analyzer Maifunction - Data Invalid - Formula Input Out of Range - Low Excess O2	1 hour
CO Analyzer Malfunction - Low Excess O2	7 hours
Cylinder Gas Audit (CGA)	1 hour
FCCU Down - Lost all Boilers	1 hour
Unit Start-up - Analyzer Celibration Checks Failed	11 hours
Total duration of CO ppm CEMS downtime	22 hours
Total operating time	1902 hours
Operating time with CEMS downtime	1.2%

FCCU CEMS Downtime

Frontier Refining LLC CO ppm CEMS Downtime for 1/1/2014 thru 3/31/2014

Parameter	Start	End	Duration	Reason	Action
СО ррт	1/3/2014 12:00 PM	12:59 PM	1 hour	CO Analyzer Malfunction - Data Invalid - Formula Input Out of Range - Low Excess O2	Adjusted Excess O2
CO ppm	1/4/2014 7:00 AM	11:59 AM	5 hours	CO Analyzer Malfunction - Low Excess 02	Adjusted Excess O2
CO ppm	1/5/2014 10:00 AM	10:59 AM	1 hour	CO Analyzer Malfunction - Low Excess O2	Adjusted Excess O2
CO ppm	1/6/2014 9:00 AM	9:59 AM	1 hour	CO Analyzer Malfunction - Low Excess O2	Adjusted Excess O2
CO ppm	1/21/2014 1:00 PM	1:69 PM	1 hour	CISCO Technician inadvertantly triggered a calibration on the FCCU CEMS while working on the Crude Charge Heater CEMS causing the data to go OOC	Ran Manual Calibration
CO ppm	2/5/2014 7:00 AM	7:59 AM	1 hour	FCCU Down - Lost all Boilers	Insufficient Data - <0.5 Hours of Valid Data - Restarted Unit
CO ppm	2/16/2014 12:00 AM	10:59 AM	11 hours	Unit Start-up - Analyzer Celibration Checks Failed	Ran Manual Calibration
CO ppm	3/20/2014 9:00 AM	9:59 AM	1 hour	Cylinder Gas Audit (CGA)	Performed NOx, SO2, CO & O2 CGA

Total duration

22 hours

EXCESS EMISSION SUMMARY REPORT FCCU CO (ppmvd) @ 0% 02 (1-hr average) CEMS 1-hr average limit = 500 ppmvd @ 0% 02

FORM B

Emission Data Summary		CMS Performance Report				
I. Duration of Excess Emission in Reporting Peri	iod Due to:	I. CMS Downtime in Reporting Period Due to:				
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	12.0			
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	8.0			
C. Process Problem	10.0	C. Quality Assurance Calibration	1.0			
D. Other Known Causes	0.0	D. Other Known Causes	1.0			
E. Unknown Causes	0.0	E. Unknown Causes	0.0			
II. Total Duration of Excess Emission	10.0	II. Total CMS Downtime	22.0			
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.5%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	1.2%			

Total time of excess emission events due to emergency/abnormal operations: ____0__. NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2. Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)

EXCESS EMISSION SUMMARY REPORT FCCU CO (ppmvd) @ 0% 02 (365-day rolling average) CEMS 365-day rolling average = 100 ppmvd @ 0% 02

FORM B

Emission Data Summary		CMS Performance Report			
I. Duration of Excess Emission in Reporting Pe	riod Due to:	I. CMS Downtime in Reporting Period Due to:			
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	12.0		
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	8.0		
C. Process Problem	0.0	C. Quality Assurance Calibration	1.0		
D. Other Known Causes	0.0	D. Other Known Causes	1.0		
E. Unknown Causes	0.0	E. Unknown Causes	0.0		
II. Total Duration of Excess Emission	0.0	II. Total CMS Downtime	22.0		
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.0%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	1.2%		

Total time of excess emission events due to emergency/abnormal operations: ______. NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2 Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)
- 4. Rolling 7-day and 365-day averages are calculated for each day the emission source is operating, including days when the analyzer has downtime. A null value is used for days in a rolling average period where the unit is not operating or the CEMS downtime causes insufficient data for a valid daily average. This can result in a day where the data is considered to be both an excess emission and analyzer downtime.

CO ppm @ 0% O2

Form C – Excess Emission Summary

FCCU Excess Emissions Summary Frontier Refining LLC CO ppm @0% O2 1-Hr Excess Emissions for 1/1/2014 thru 3/31/2014

Reason	Duration
CO ppm, CO ppm @ 0% O2, & CO lb/hr Emission Exceedance - Decreased total charge 1000 BPD due to unit pressure. Making adjustments for vacuum, on WGC surface condenser - Low Excess O2	2 hours
CO ppm, ppm @ 0% O2, & Lb/Hr Emission Exceedance - Increasing Retes - Low Excess O2	7 hours
Process Upset - Indeck Boilers #1 & #2 Shutdown	1 hour
Total duration of CO ppm @0% O2 1-Hr excess emissions	10 hours
Total operating time	1902 hours
Operating time with excess emissions	0.5%

FCCU Excess Emissions

Frontier Refining LLC
CO ppm @0% O2 1-Hr Excess Emissions for 1/1/2014 thru 3/31/2014

Parameter	Start	End	Duration	Value	Min	Max	Limit	Reason	Action
CO ppm @0% O2 1-Hr	1/3/2014 10:00 AM	11:59 AM	2 hours	924.40	838.30	1010.50	500	CO ppm, CO ppm @ 0% O2, & CO fb/hr Emission Exceedance - Decreased total charge 1000 BPD due to unit pressure. Making adjustments for vacuum, on WGC surface condenser - Low Excess O2	Adjusted Excess O2
CO ppm @0% O2 1-Hr	1/10/2014 11:00 AM	5:59 PM	7 hours	797.20	548.70	1009.40	500	CO ppm, ppm @ 0% O2, & Lb/Hr Emission Exceedance - Increasing Rates - Low Excess O2	Adjusted Excess O2
CO ppm @0% O2 1-Hr	3/2/2014 3:00 AM	3:59 AM	1 hour	1549.60	1549.60	1549.60	500	Process Upset - Indeck Boilers #1 & #2 Shutdown	Stabilized Unit and Restarted Bollers

Total duration

10 hours

CO ppm @ 0% O2 365-Day Rolling Average

Form C – Excess Emission Summary

FCCU Excess Emissions Summary

Frontier Refining LLC CO ppm @0% O2 365-Day Rolling Excess Emissions for 1/1/2014 thru 3/31/2014

Reason	Duration
There are no excess emissions for this report.	
Total duration of CO ppm @0% O2 385-Day Rolling excess emissions	0
Total operating time	1902 hour
Operating time with excess emissions	0.0%

CO ppm @ 0% O2

Form D – Downtime Summary

FCCU CEMS Downtime Summary Frontier Refining LLC CO ppm @0% O2 CEMS Downtime for 1/1/2014 thru 3/31/2014

Reason	Duration
CISCO Technician inadvertantly triggered a calibration on the FCCU CEMS while working on the Crude Charge Heater CEMS causing the data to go OOC	1 hour
CO Analyzer Malfunction - Data invalid - Formula Input Out of Range - Low Excess O2	1 hour
CO Analyzer Melfunction - Low Excess O2	7 hours
Cylinder Gas Audit (CGA)	1 hour
FCCU Down - Lost all Bollers	1 hour
Unit Start-up - Analyzer Calibration Checks Falled	11 hours
Total duration of CO ppm @0% O2 CEMS downtime	22 hours
Total operating time	1902 hours
Operating time with CEMS downtime	1.2%

FCCU CEMS Downtime

Frontier Refining LLC CO ppm @0% O2 CEMS Downtime for 1/1/2014 thru 3/31/2014

Parameter	Start	End	Duration	Reason	Action
CO ppm @0% O2	1/3/2014 12:00 PM	12:59 PM	1 hour	CO Analyzer Mailunction - Data Invalid - Formula Input Out of Range - Low Excess O2	Adjusted Excess O2
CO ppm @0% O2	1/4/2014 7:00 AM	11:59 AM	5 hours	CO Analyzer Malfunction - Low Excess O2	Adjusted Excess O2
CO ppm @0% O2	1/5/2014 10:00 AM	10:59 AM	1 hour	CO Analyzer Mailtunction - Low Excess O2	Adjusted Excess O2
CO ppm @0% O2	1/6/2014 9:00 AM	9:59 AM	1 hour	CO Analyzer Maifunction - Low Excess O2	Adjusted Excess O2
CO ppm @0% O2	1/21/2014 1:00 PM	1:59 PM	1 hour	CISCO Technician inadvertantly triggered a calibration on the FCCU CEMS while working on the Crude Charge Heater CEMS causing the data to go OOC	Ran Manual Calibration
CO ppm @0% O2	2/5/2014 7:00 AM	7:59 AM	1 hour	FCCU Down - Lost all Boilers	insufficient Data - <0.5 Hours of Valid Data - Restarted Unit
CO ppm @0% O2	2/16/2014 12:00 AM	10:59 AM	11 hours	Unit Start-up - Analyzer Calibration Checks Failed	Ran Manual Calibration
CO ppm @0% O2	3/20/2014 9:00 AM	9:59 AM	1 hour	Cylinder Gas Audit (CGA)	Performed NOx, SO2, CO & O2 CGA

Total duration

22 hours

EXCESS EMISSION SUMMARY REPORT FCCU CO (ib/hr) CEMS 1-hr average limit = 30 lb/hr

FORM B

Emission Data Summary		CMS Performance Report			
I. Duration of Excess Emission in Reporting Peri	od Due to:	I. CMS Downtime in Reporting Period Due to:			
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	13.0		
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	8.0		
C. Process Problem	9.0	C. Quality Assurance Calibration	1.0		
D. Other Known Causes	0.0	D. Other Known Causes	2.0		
E. Unknown Causes	0.0	B. Unknown Causes	0.0		
II. Total Duration of Excess Emission	9.0	II. Total CMS Downtime	24.0		
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.5%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	1.3%		

Total time of excess emission events due to emergency/abnormal operations: __0_. NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2 Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)

FCCU CO (lb/hr) CEMS 365-day rolling average = 18.2 lb/hr

FORM B

	Emission Data Summary		CMS Performance Report				
I.	I. Duration of Excess Emission in Reporting Period Due to		I. CMS Downtime in Reporting Period Due to:				
	A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	13.0			
	B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	8.0			
	C. Process Problem	0.0	C. Quality Assurance Calibration	1.0			
	D. Other Known Causes	0.0	D. Other Known Causes	2.0			
	E. Unknown Causes	0.0	B. Unknown Causes	0.0			
II.	. Total Duration of Excess Emission	0.0	II. Total CMS Downtime	24.0			
п	I. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.0%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	1.3%			

Total time of excess emission events due to emergency/abnormal operations: _______.

NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2 Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)
- 4. Rolling 7-day and 365-day averages are calculated for each day the emission source is operating, including days when the analyzer has downtime. A null value is used for days in a rolling average period where the unit is not operating or the CEMS downtime causes insufficient data for a valid daily average. This can result in a day where the data is considered to be both an excess emission and analyzer downtime.

1Q14 FCCU CEMS

CO Lb/Hr

Form C – Excess Emission Summary

FCCU Excess Emissions Summary Frontier Refining LLC CO lbs 1-Hr Excess Emissions for 1/1/2014 thru 3/31/2014

Reason	Duration
CO Lb/Hr Emission Exceedance - Low Excess O2	1 hour
CO ppm, CO ppm @ 0% O2, & CO lb/hr Emission Exceedance - Decreased total charge 1000 BPD due to unit pressure. Making adjustments for vacuum, on WGC surface condenser - Low Excess O2	2 hours
CO ppm, ppm @ 0% O2, & Lb/Hr Emission Exceedance - Increasing Rates - Low Excess O2	5 hours
Process Upset - indeck Boilers #1 & #2 Shutdown	1 hour
Total duration of CO lbs 1-Hr excess emissions	9 hours
Total operating time	1902 hours
Operating time with excess emissions	0.5%

FCCU Excess Emissions

Frontier Refining LLC CO lbs 1-Hr Excess Emissions for 1/1/2014 thru 3/31/2014

Parameter	Start	End	Duration	Value	Min	Max	Limit	Reason	Action
CO lbs 1-Hr	1/3/2014 9:00 AM	10:59 AM	2 hours	35.3	32.4	38.1	30	CO ppm, CO ppm @ 0% O2, & CO lb/hr Emission Exceedance - Decreased total charge 1000 BPD due to unit pressure. Making adjustments for vacuum, on WGC surface condenser - Low Excess O2	Adjusted Excess O2
CO lbs 1-Hr	1/10/2014 11:00 AM	12:59 PM	2 hours	38.0	36.2	39,7	30	CO ppm, ppm @ 0% O2, & Lb/Hr Emission Exceedance - Increasing Rates - Low Excess O2	Adjusted Excess O2
CO ibs 1-Hr	1/10/2014 3:00 PM	5:59 PM	3 hours	41.0	39.3	42.2	30	CO ppm, ppm @ 0% O2, & Lb/Hr Emission Exceedance - Increasing Rates - Low Excess O2	Adjusted Excess O2
CO ibs 1-Hr	1/22/2014 2:00 PM	2:59 PM	1 hour	35.9	35.9	35.9	30	CO Lb/Hr Emission Exceedance - Low Excess O2	Adjusted Excess O2
CO lbs 1-Hr	3/2/2014 3:00 AM	3:59 AM	1 hour	103.2	103.2	103.2	30	Process Upset - Indeck Boilers #1 & #2 Shutdown	Stabilized Unit and Restarted Bollers

Total duration

9 hours

1Q14 FCCU CEMS

CO lb/hr 365-Day Rolling Average

Form C – Excess Emission Summary

FCCU Excess Emissions Summary

Frontier Refining LLC CO lbs/hr 365-Day Rolling Excess Emissions for 1/1/2014 thru 3/31/2014

Reason	Duration
There are no excess emissions for this report.	
Total duration of CO lbs/hr 365-Day Rolling excess emissions	0
Total operating time	1902 hours
Operating time with excess emissions	0.0%

1Q14 FCCU CEMS

CO Lb/Hr

Form D – Downtime Summary

FCCU CEMS Downtime Summary Frontier Refining LLC CO lbs CEMS Downtime for 1/1/2014 thru 3/31/2014

Reason	Duration
CISCO Technician inadvertantly triggered a calibration on the FCCU CEMS while working on the Crude Charge Heater CEMS causing the data to go OOC	1 hour
CO Analyzer Malfunction - Data Invalid - Formula Input Out of Range - Low Excess O2	1 hour
CO Analyzer Malfunction - Low Excess O2	7 hours
Cylinder Gas Audit (CGA)	1 hour
FCCU Down - Lost all Boilers	1 hour
Maintenance - High Stack Vacuum	1 hour
Unit Start-up - Analyzer Calibration Checks Falled	12 hours
Total duration of CO lbs CEMS downtime	24 hours
Total operating time	1902 hours
Operating time with CEMS downtime	1.3%

FCCU CEMS Downtime

Frontier Refining LLC CO lbs CEMS Downtime for 1/1/2014 thru 3/31/2014

Parameter	Start	End	Duration	Reason	Action
CO ibs	1/3/2014 12:00 PM	12:59 PM	1 hour	CO Analyzer Matfunction - Data Invalid - Formula Input Out of Range - Low Excess O2	Adjusted Excess O2
CO lbs	1/4/2014 7:00 AM	11:59 AM	5 hours	CO Analyzer Malfunction - Low Excess O2	Adjusted Excess O2
CO lbs	1/5/2014 10:00 AM	10:59 AM	1 hour	CO Analyzer Maifunction - Low Excess O2	Adjusted Excess O2
CO lbs	1/6/2014 9:00 AM	9:59 AM	1 hour	CO Analyzer Malfunction - Low Excess 02	Adjusted Excess O2
CO lbs	1/8/2014 9:00 AM	9:59 AM	1 hour	Maintenance - High Stack Vacuum	Changed out sample filters both at the probe and the cabinet. Blew out sample line.
CO ibs	1/21/2014 1:00 PM	1:59 PM	1 hour	CISCO Technician inadvertantly triggered a calibration on the FCCU CEMS while working on the Crude Charge Heater CEMS causing the data to go OOC	Rain Manual Calibration
CO lbs	2/5/2014 7:00 AM	7:59 AM	1 hour	FCCU Down - Lost all Boilers	Insufficient Data - <0.5 Hours of Valid Data - Restarted Unit
CO lbs	2/16/2014 12:00 AM	11:59 AM	12 hours	Unit Start-up - Analyzer Calibration Checks Failed	Ran Manual Calibration
CØ lbs	3/20/2014 9:00 AM	9:59 AM	1 hour	Cylinder Gas Audit (CGA)	Performed NOx, SO2, CO & O2 CGA

Total duration

24 hours

1014

DEPARTMENT OF ENVIRONMENTAL QUALITY AIR QUALITY DIVISION CONTINUOUS EMISSION MONITORING REPORT

FORM A

I. GENERAL INFORMATION

- A. Facility Name: FRONTIER REFINING LLC
- B. Process Unit/Pollutant Monitored: <u>PM MONITORING SYSTEM FLUIDIZED</u>

 <u>CATALYTIC CRACKING UNIT (FCCU) REGENERATOR</u>
- C. Applicable Permit Number or Regulation: Consent Decree, MD-9640, and MACT Subpart UUU
- D. Applicable Emission Limit: 70.8 lb/hr (3-hr average); 0.029 lb Ni/hr (1-hr average)

II. MONITOR INFORMATION Laser Hawk PM Monitor

- A. Date of Original Monitor Installation: May 2011
- B. Date of Latest Monitor Certification: December 2012 (Approved 4/22/2013)
- C. Pollutant/Opacity Monitor
 - 1. Manufacturer: Teledyne Instruments
 - 2. Model Number: 360 PM Laser Hawk
 - 3. Serial Number Main Chassis: 360085
 - 4. Basis of Measurement (If Applicable Wet or Dry): NA
 - 5. Instrument Span, Range Value (Specify Units): NA

D. Diluent Monitor NONE

- 1. Type of Monitor: O₂ or CO₂ (circle one)
- 2. Manufacturer:
- 3. Model Number:
- 4. Serial Number Main Chassis
- 5. Basis of Measurement (If Applicable Wet or Drv):
- 6. Instrument Span, Range Value (Specify Units):

E. Flow Monitor NONE

- 1. Type of Instrument (i.e. S-type Pitot Tube):
- 2. Manufacturer:
- 3. Model Number:
- 4. Serial Number Main Chassis:

F. Quality Assurance Data

- 1. QA Plan Date: 2/15/2013
- 2. QA Plan Approval Date: 4/22/2013

III. Operating/Monitoring Data

A. Quarter: 1 Year: 2014

B Total Hours in Reporting Period: 2160

C. Hours Unit Operated During the Reporting Period: 1902

Note: Include <u>all</u> unit operating time for the quarter including operating time associated with Startup/Shutdown and Chapter 1 Section 5 (Emergency/Abnormal) Operations. Report time in hours to one decimal place, i.e. 1902.8.

- IV. Quarterly Audits/Monitoring System Modifications
 - A. Quarterly Audits
 Type Audit: ACA

<u>Date Conducted</u> 3/19/2014

Pass

Yes

Pollutant/Opacity Monitor: 3/1

Equipment Replaced During Reporting Period: None.

Note: Only equipment replacements or modifications to the system that could affect the ability of the continuous monitoring system to comply with the associated Performance Specification shall be reported.

V. Report Contact

A. Name: David Weeks, Environmental Engineer

B. Phone Number: (307) 771-8827

EXCESS EMISSION SUMMARY REPORT FCCU PM (lb/hr) CEMS 3-hr average limit = 70.8 lb/hr

FORM B

Emission Data Summary		CMS Performance Report		
I. Duration of Excess Emission in Reporting Period Due to:		I. CMS Downtime in Reporting Period Due to:		
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	28.0	
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	0.0	
C. Process Problem	0.0	C. Quality Assurance Calibration	0.0	
D. Other Known Causes	0.0	D. Other Known Causes	0.0	
E. Unknown Causes	0.0	E. Unknown Causes	0.0	
II. Total Duration of Excess Emission	0.0	II. Total CMS Downtime	28.0	
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.0%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	1.5%	

Total time of excess emission events due to emergency/abnormal operations: ______. NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2. Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)

1Q14 FCCU CEMS

PM Lb/Hr
3-Hour Rolling Average

Form C – Excess Emission Summary

FCCU Excess Emissions Summary Frontier Refining LLC PM lbs 3-Hr Rolling Excess Emissions for 1/1/2014 thru 3/31/2014

Reason	Duration
There are no excess emissions for this report.	
Total duration of PM lbs 3-Hr Rolling excess emissions	0
Total operating time	1902 hours
Operating time with excess emissions	0.0%

1Q14 FCCU CEMS

PM Lb/Hr

Form D – Downtime Summary

FCCU CEMS Downtime Summary Frontier Refining LLC PM lbs CEMS Downtime for 1/1/2014 thru 3/31/2014

Reason	Ouration
Particulate Analyzer Fault	18 hours
Unit Start-up - Analyzer Calibration Checks Failed	12 hours
Total duration of PM ibs CEMS downtime	28 hours
Total operating time	1902 hours
Operating time with CEMS downtime	1.5%

FCCU CEMS Downtime

Frontier Refining LLC PM lbs CEMS Downtime for 1/1/2014 thru 3/31/2014

Parameter	Start	End	Duration	Reason	Action
PM lbs	1/8/2014 7:00 AM	8:59 AM	2 hours	Particulate Analyzer Fault	Cleaned Lens and Ran Cal to Clear Alarm
PM lbs	1/10/2014 8:00 AM	8:59 AM	1 hour	Particulate Analyzer Fault	Cleaned Lens and Ran Cal to Clear Alarm
PM lbs	1/11/2014 7:00 AM	9:59 AM	3 hours	Particulate Analyzer Fault	Cleaned Lens and Ran Cal to Clear Alarm
PM ibs	1/16/2014 7:00 AM	7:59 AM	1 hour	Particulate Analyzer Fault	Cleaned Lens and Ran Cal to Clear Alarm
PM lbs	1/17/2014 7:00 AM	8:59 AM	2 hours	Particulate Analyzer Fault	Cleaned Lens and Ran Cal to Clear Alarm
PM ibs	1/18/2014 7:00 AM	7:59 AM	1 hour	Particulate Analyzer Fault	Cleaned Lens and Ran Cal to Clear Alarm
PM lbs	1/20/2014 7:00 AM	8:59 AM	2 hours	Particulate Analyzer Fault	Cleaned Lens and Ran Cal to Clear Alarm
PM lbs	2/16/2014 12:00 AM	11:59 AM	12 hours	Unit Start-up - Analyzer Calibration Checks Failed	Ran Manual Calibration
PM ibs	3/10/2014 7:00 AM	8:59 AM	2 hours	Particulate Analyzer Fault	Cleaned Lens and Ran Cal to Clear Alarm
PM (bs	3/25/2014 7:00 AM	7:59 AM	1 hour	Particulate Analyzer Fault	Cleaned Lens and Ran Cal to Clear Alarm
PM ibs	3/26/2014 7:00 AM	7:59 AM	1 hour	Particulate Analyzer Fault	Cleaned Lens and Ran Cal to Clear Alarm

Total duration

28 hours

FCCU PM (Ni lb/hr) CEMS 1-hr average limit = 0.029 lb/hr

FORM B

Emission Data Summary		CMS Performance Report		
I. Duration of Excess Emission in Reporting Per	iod Due to:	I. CMS Downtime in Reporting Period Due to:		
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	28.0	
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	0.0	
C. Process Problem	0.0	C. Quality Assurance Calibration	0.0	
D. Other Known Causes	0.0	D. Other Known Causes	0.0	
E. Unknown Causes	0.0	E. Unknown Causes	0.0	
II. Total Duration of Excess Emission	0.0	II. Total CMS Downtime	28.0	
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.0%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	1.5%	

Total time of excess emission events due to emergency/abnormal operations: _______. NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2. Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)

1Q14 FCCU CEMS

Ni Lb/Hr

Form C – Excess Emission Summary

FCCU Excess Emissions Summary

Frontier Refining LLC Nickle Ibs 1-Hr Excess Emissions for 1/1/2014 thru 3/31/2014

Reason	Duration
There are no excess emissions for this report.	
Total duration of Nickle lbs 1-Hr excess emissions	0
Total operating time	1902 hours
Operating time with excess emissions	0.0%

1Q14 FCCU CEMS

Ni Lb/Hr

Form D – Downtime Summary

FCCU CEMS Downtime Summary Frontier Refining LLC Nickel ibs CEMS Downtime for 1/1/2014 thru 3/31/2014

Reason	Duration
Particulate Analyzer Fault	16 hours
Unit Start-up - Analyzer Calibration Checks Failed	12 hours
Total duration of Nickel Ibs CEMS downtime	28 hours
Total operating time	1902 hours
Operating time with CEMS downtime	1.5%

FCCU CEMS Downtime

Frontier Refining LLC Nickel lbs CEMS Downtime for 1/1/2014 thru 3/31/2014

Parameter	Start	End	Duration	Reason	Action
Nickel (bs	1/8/2014 7:00 AM	8:59 AM	2 hours	Particulate Analyzer Fault	Cleaned Lens and Ran Cal to Clear Alarm
Nickel ibs	1/10/2014 8:00 AM	8:59 AM	1 hour	Particulate Analyzer Fault	Cleaned Lens and Ran Cal to Clear Alarm
Nickel Ibs	1/11/2014 7:00 AM	9:59 AM	3 hours	Particulate Analyzer Fault	Cleaned Lens and Ran Cal to Clear Alarm
Nickel (bs	1/16/2014 7:00 AM	7:59 AM	1 hour	Particulate Analyzer Fault	Cleaned Lens and Ran Cal to Clear Alarm
Nickel (bs	1/17/2014 7:00 AM	8:59 AM	2 hours	Particulate Analyzer Fault	Cleaned Lens and Ran Cal to Clear Alarm
Nickel (bs	1/18/2014 7:00 AM	7:59 AM	1 hour	Particulate Analyzer Fault	Cleaned Lens and Ran Cal to Clear Alarm
Nickel lbs	1/20/2014 7:00 AM	8:59 AM	2 hours	Particulate Analyzer Fault	Cleaned Lens and Ran Cal to Clear Alarm
Nickel ibs	2/16/2014 12:00 AM	11:59 AM	12 hours	Unit Start-up - Analyzer Calibration Checks Failed	Ran Manual Calibration
Nickel Ibs	3/10/2014 7:00 AM	8:59 AM	2 hours	Particulate Analyzer Fault	Cleaned Lens and Ran Cal to Clear Alarm
Nicket (bs	3/25/2014 7:00 AM	7:59 AM	1 hour	Particulate Analyzer Fault	Cleaned Lens and Ran Cal to Clear Alarm
Nickel (bs	3/26/2014 7:00 AM	7:59 AM	1 hour	Particulate Analyzer Fault	Cleaned Lens and Ran Cal to Clear Alarm

Total duration 28 hours

Data Sheet for FCCU PM CEM System Absolute Correlation Audit (ACA)

Date: March 19, 2014 Time: 9:50 A.M. **Zero %** 100% Low Mid Analyzer Analyzer Analyzer Analyzer Run 1 0.02 57.37 78.57 100.30 Run 2 0.01 57.93 79.21 101.10 Run 3 0.04 58.40 79.67 101.40 CCEM, RCEM (1.15)57.90 79.15 100.93 CRV, RV 0.00 58.00 79.30 100.00 ACA 1.63 0.17 0.19 0.93 Accuracy

Yes

Signature of Technician(s) performing ACA:

Yes

Matt Hobbs, Keyin Marschner and/or Tad Milliken

Yes

Calculation of ACA Accuracy:

For Low, Mid & 100%:

Eq. 2-1a ACA = $(R_{CEM} - R_V) / R_V \times 100$

ACA must be +/-10% to pass.

Yes

where:

ACA = accuracy of CEM, %

R_{CEM} = average of reponses

R_V = certified audit value of gas

For Zero:

Pass?

Eq. 2-1b ACA = $(C_{CEM} - C_{RV}) / C_S \times 100$

ACA must be +/-7.5% to pass.

where:

ACA = accuracy of CEM, %

 C_{CEM} = average of reponses $Y (mg/m^3) =$

 $Y (mg/m^3) = 6.4 * X (backscatter in %) - 1.3$

C_{RV}= certified audit value of gas

Data Sheet for FCCU CEM System Cylinder Gas Audit

1. Date Audit Commenced:	2014.03.20	Time Audit Commenced:	0930 thru 1125

2. Audit Gases Used for CGA (All gases to be Protocol 1 Certified):

Acceptable Audit Gas Ranges	Cylinder Number and Expiration Date	Audit Gas Concentrations		+/- of Audit Gas Range
NO _x Low:	CC420619	100.7	ppm	25.18%
80 - 120 ppm	20-Feb-21	100.7	ppni	25.10%
NO _x Mid:	CC363979	223	ppm	55.75%
200 - 240 ppm	28-Feb-21	223	ppiii	33.73%
SO _x Low:	CC420619	300.7	nnm	25.06%
240 - 360 ppm	28-Feb-21	300.7	ppm	25.00%
SO _x Mid:	CC363979	655.9	nnm	54.66%
600 - 720 ppm	25-Feb-21	000.0	ppm	34.00%
CO Low:	CC420619	251.2		25.12%
200 - 300 ppm	28-Feb-21	201.2	ppm	25.1276
CO Mid:	CC363979	553.9	222	55.39%
500 - 600 ppm	28-Feb-21	000.8	ppm	23.3976
O ₂ Low:	CC94180	6,22	%	24.88%
4 - 6% by volume	16-Feb-21	0.22	70	24.00%
O₂ Mid:	CC234478	13.67	%	54.68%
8 - 12% by volume	27-Feb-21	13.07	70	54.0676
CO ₂ Low:	CC94180		0/	24.00%
5 - 8% by volume	- 4 Mh	4.90	%	24.80%
CO ₂ Mid:	CC234478	40.07	64	P. () P. ()
10 - 14% by volume	27-Feb-21	10.97	%	54.85%

Data Sheet for FCCU CEM System Cylinder Gas Audit

Date: 2014.03.20

3. CEM System Response:

	Low-Sp	an No _x	Mid-Sp	an No _x	Low-Sp	an SO₂	Mid-Sp	an SO ₂
	Analyzer	CISCO	Analyzer	CISCO	Analyzer	CISCO	Analyzer	CISCO
Run 1	108.58	108.43	241.40	241.59	292.41	292.19	653.40	653.12
Run 2	108.57	108.42	241.88	242.06	293.83	293.66	658.51	657.77
Run 3	109.05	108.95	241.85	242.13	297.96	297.75	664.49	663.78
Avg. (d _m)	108.73	108.60	241.71	241.93	294.73	294.53	658.80	658.22
Α	7.98	7.85	8.39	8.49	1.98	2.05	0.44	0.35
Pass?	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes

	Low-Sp	oan CO	Mid-Sp	an CO
	Analyzer	nalyzer CiSCO Analy		CISCO
Run 1	257.35	257.35	540.13	539.61
Run 2	257.29	257.04	540.63	539.86
Run 3	257.22	257.08	540.57	539.84
Avg. (d _m)	257.29	257.16	540.44	539.77
Α	2.42	2.37	2.43	2.55
Pass?	Yes	Yes	Yes	Yes

4. Signature of Technician(s) performing CGA:

Matt Hobbs, Kevin Marschner and/or Tad Milliken

Calculation of A:

 $A = (d_m - c_a) / c_a \times 100$

A must be +/-15% to pass.

where:

A = accuracy of CEM

d_m = average of reponses

c_a = certified audit value of gas

Data Sheet for FCCU CEM System Cylinder Gas Audit

Date: 2014.03.20

3. CEM System Response:

	Low-Sp	oan O ₂	Mid-Sp	oan O ₂	Low-Sp	an CO ₂	Mid-Sp	an CO ₂
	Analyzer	CISCO	Analyzer	CISCO	Analyzer	CISCO	Analyzer	CISCO
Run 1	6.41	6.42	13.95	13.96	5.14	5.13	10.67	10.64
Run 2	6.42	6.44	13.95	13.97	5.14	5.13	10.70	10.65
Run 3	6.43	6.44	13.97	13.99	5.11	5.10	10.68	10.65
Avg. (d _m)	6.42	6.43	13.96	13.97	5.13	5.12	10.68	10.65
Α	3.22	3.43	2.10	2.22	3.43	3.23	2.61	2.95
Pass?	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes

4. Signature of Technician(s) performing CGA:

Matt Hobbs, Kevin Marschner and/or Tad Milliken

Calculation of A:

 $A = (d_m - c_a) / c_a \times 100$

A must be +/-15% to pass.

where:

A = accuracy of CEM

d_m = average of reponses

c_a = certified audit value of gas

2014

DEPARTMENT OF ENVIRONMENTAL QUALITY AIR QUALITY DIVISION CONTINUOUS EMISSION MONITORING REPORT

FORM A

I. GENERAL INFORMATION

- A. Facility Name: FRONTIER REFINING LLC
- B. Process Unit/Pollutant Monitored: NO_x MONITORING SYSTEM FLUIDIZED CATALYTIC CRACKING UNIT (FCCU) REGENERATOR
- C. Applicable Permit Number or Regulation: Consent Decree, MD-9640
 - D. Applicable Emission Limit: 21.9 lb/hr (7-day rolling average); 10.9 lb/hr (365-day rolling average); 120 ppmvd @ 0% 0, (7-day rolling average); 60ppmvd @ 0% 0, (365-day rolling average)

II. MONITOR INFORMATION

- A. Date of Original Monitor Installation: 6/5/2012
- B. Date of Latest Monitor Certification: 7/17/2012
- C. Pollutant/Opacity Monitor
 - 1. Manufacturer: Teledyne/API
 - 2. Model Number: Model 200H
 - 3. Serial Number Main Chassis: 82
 - 4. Basis of Measurement (If Applicable Wet or Dry): Dry
 - 5. Instrument Span, Range Value (Specify Units): 0-600 ppm and 0-150 lb/hr

D. Diluent Monitor NONE

- 1. Type of Monitor: O₂ or CO₂ (circle one)
- 2. Manufacturer:
- 3. Model Number:
- 4. Serial Number Main Chassis
- 5. Basis of Measurement (If Applicable Wet or Dry):
- 6. Instrument Span, Range Value (Specify Units):

E. Flow Monitor

- 1. Type of Instrument (i.e. S-type Pitot Tube): S-Type Pitot Tube
- 2. Manufacturer: Dieterich Standard
- 3. Model Number: PSF-S4H HSVH FADH0 FADC
- 4. Serial Number Main Chassis: DFCII CEM 1MN 2XX #MN 4MN P1 ES RB TR AR YX ZS DB
- F. Quality Assurance Data
 - 1. QA Plan Date: 10/15/2012
 - 2. QA Plan Approval Date: 4/22/2013

III. Operating/Monitoring Data

A. Ouarter:

2 Year: 2014

B Total Hours in Reporting Period:

2184

C. Hours Unit Operated During the Reporting Period: 2015

Note: Include <u>all</u> unit operating time for the quarter including operating time associated with Startup/Shutdown and Chapter 1 Section 5 (Emergency/Abnormal) Operations. Report time in hours to one decimal place, i.e. 1902.8.

- IV. Quarterly Audits/Monitoring System Modifications
 - A. Quarterly Audits

Type Audit: RATA

Date Conducted

Pass

Pollutant/Opacity Monitor:

5/13/2014

YES

Note: A copy of the quarterly audits shall be included with the corresponding quarterly excess emission report.

Equipment Replaced During Reporting Period: Changed out Filters; Replaced Flow Pressure Transducer.

Note: Only equipment replacements or modifications to the system that could affect the ability of the continuous monitoring system to comply with the associated Performance Specification shall be reported.

- V. Report Contact
 - A. Name: David Weeks. Environmental Engineer
 - B. Phone Number: (307) 771-8827

EXCESS EMISSION SUMMARY REPORT FCCU NOx (lb/hr) CEMS 7-day rolling average = 21.9 lb/hr

FORM B

Emission Data Summary I. Duration of Excess Emission in Reporting Period Due to:		CMS Performance Report I. CMS Downtime in Reporting Period Due to:		
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	8.0	
C. Process Problem	0.0	C. Quality Assurance Calibration	0.0	
D. Other Known Causes	0.0	D. Other Known Causes	0.0	
E. Unknown Causes	0.0	E. Unknown Causes	0.0	
II. Total Duration of Excess Emission	0.0	II. Total CMS Downtime	22.0	
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.0%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	1.1%	

Total time of excess emission events due to emergency/abnormal operations: __0_. NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2 Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)
- 4. Rolling 7-day and 365-day averages are calculated for each day the emission source is operating, including days when the analyzer has downtime. A null value is used for days in a rolling average period where the unit is not operating or the CEMS downtime causes insufficient data for a valid daily average. This can result in a day where the data is considered to be both an excess emission and analyzer downtime.

FCCU NOx (lb/hr) CEMS 365-day rolling average = 10.9 lb/hr

FORM B

Emission Data Summary I. Duration of Excess Emission in Reporting Period Due to:		CMS Performance Report I. CMS Downtime in Reporting Period Due to:		
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	8.0	
C. Process Problem	0.0	C. Quality Assurance Calibration	0.0	
D. Other Known Causes	0.0	D. Other Known Causes	0.0	
E. Unknown Causes	0.0	E. Unknown Causes	0.0	
II. Total Duration of Excess Emission	0.0	II. Total CMS Downtime	22.0	
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.0%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	1.1%	

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2 Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)
- 4. Rolling 7-day and 365-day averages are calculated for each day the emission source is operating, including days when the analyzer has downtime. A null value is used for days in a rolling average period where the unit is not operating or the CEMS downtime causes insufficient data for a valid daily average. This can result in a day where the data is considered to be both an excess emission and analyzer downtime.

FCCU Excess Emissions Summary

Frontier Refining LLC
NOx Ibs 7-Day Rolling Excess Emissions for 4/1/2014 thru 6/30/2014

Reason	Duration
There are no excess emissions for this report.	
Total duration of NOx lbs 7-Day Rolling excess emissions	0
Total operating time	2015 hours
Operating time with excess emissions	0.0%

Comment: Form C - Excess Emissions Summary

FCCU Excess Emissions Summary

Frontier Refining LLC
NOx ibs 365-Day Rolling Excess Emissions for 4/1/2014 thru 6/30/2014

Reason	Duration
There are no excess emissions for this report.	
Total duration of NOx Ibs 365-Day Rolling excess emissions	0
Total operating time	2015 hours
Operating time with excess emissions	0.0%

Comment: Form C - Excess Emissions Summary

FCCU CEMS Downtime Summary

Frontier Refining LLC NOx lbs CEMS Downtime for 4/1/2014 thru 6/30/2014

Reason	Duration	
Maintenance - Following Upset of FCCU due to Boiler #1 & #2 Shutdown - Sample System	13 hours	
Maintenance - Sample System	1 hour 7 hours 1 hour	
Process - Ran Low Excess O2 - Wet O2 > Dry O2 causing % Moisture and Lb/Hr to be invalid		
Process - Ran Low Excess O2 - Wet O2 > Dry O2 causing % Moisture, Dry Stack Flow and Lb/Hr to be invalid		
Total duration of NOx ibs CEMS downtime	22 hours	
Total operating time	2015 hours	
Operating time with CEMS downtime	1.1%	

Comment: Form D - Downtime Summary

FCCU CEMS Downtime

Frontier Refining LLC NOx lbs CEMS Downtime for 4/1/2014 thru 6/30/2014

4/11/2014 7:00 AM				
11 11 11 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	7:59 AM	1 hour	Maintenance - Sample System	Took stack out of service to clean and change filters and service sample dryer. Passed Manual Calibration.
6/13/2014 10:00 AM	10:59 PM	13 hours	Maintenance - Following Upset of FCCU due to Boiler #1 & #2 Shutdown - Sample System	Cleaned sample probe filter
6/13/2014 11:00 PM	11:59 PM	1 hour	Process - Ran Low Excess O2 - Wet O2 > Dry O2 causing % Moisture and Lb/Hr to be Invalid	Adjusted Excess O2. Morning Calibration Check Corrected Discrepancy.
6/14/2014 12:00 AM	5:59 AM	6 hours	Process - Ran Low Excess O2 - Wet O2 > Dry O2 causing % Moisture and Lb/Hr to be Invalid	Adjusted Excess O2. Morning Calibration Check Corrected Discrepancy.
6/23/2014 10:00 PM	10:59 PM	1 hour	Process - Ran Low Excess O2 - Wet O2 > Dry O2 causing % Moisture, Dry Stack Flow and Lb/Hr to be invalid	FCCU Shutdown
	6/13/2014 11:00 PM 6/14/2014 12:00 AM	6/13/2014 11:00 PM 11:59 PM 6/14/2014 12:00 AM 5:59 AM	6/13/2014 11:00 PM 11:59 PM 1 hour 6/14/2014 12:00 AM 5:59 AM 6 hours	of FCCU due to Boiler #1 & #2 Shutdown - Sample System 6/13/2014 11:00 PM 11:59 PM 1 hour Process - Ran Low Excess O2 - Wet O2 > Dry O2 causing % Moisture and Lb/Hr to be invalid 6/14/2014 12:00 AM 5:59 AM 6 hours Process - Ran Low Excess O2 - Wet O2 > Dry O2 causing % Moisture and Lb/Hr to be invalid 6/23/2014 10:00 PM 10:59 PM 1 hour Process - Ran Low Excess O2 - Wet O2 > Dry O2 causing % Moisture, Dry Stack Flow and

Total duration 22 hours

Comment: Form D - Downtime Summary

FCCU NOx (ppm) CEMS 7-day Rolling Average = 120 pnmvd @ 0% 02

FORM B

Emission Data Summary		CMS Performance Report		
I. Duration of Excess Emission in Reporting Period Due to:		I. CMS Downtime in Reporting Period Due to:		
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	14.0	
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	0.0	
C. Process Problem	0.0	C. Quality Assurance Calibration	0.0	
D. Other Known Causes	0.0	D. Other Known Causes	0.0	
E. Unknown Causes	0.0	E. Unknown Causes	0.0	
II. Total Duration of Excess Emission	0.0	II. Total CMS Downtime	14.0	
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.0%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	0.7%	

Total time of excess emission events due to emergency/abnormal operations: ______. NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2 Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)
- 4. Rolling 7-day and 365-day averages are calculated for each day the emission source is operating, including days when the analyzer has downtime. A null value is used for days in a rolling average period where the unit is not operating or the CEMS downtime causes insufficient data for a valid daily average. This can result in a day where the data is considered to be both an excess emission and analyzer downtime.

EXCESS EMISSION SUMMARY REPORT FCCU NOx (ppm) CEMS 365-day rolling average = 60 ppmyd @ 0% 02

FORM B

Emission Data Summary		CMS Performance Report		
I. Duration of Excess Emission in Reporting Period Due to:		I. CMS Downtime in Reporting Period Due to:		
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	14.0	
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	0.0	
C. Process Problem	0.0	C. Quality Assurance Calibration	0.0	
D. Other Known Causes	0.0	D. Other Known Causes	0.0	
E. Unknown Causes	0.0	E. Unknown Causes	0.0	
II. Total Duration of Excess Emission	0.0	II. Total CMS Downtime	14.0	
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.0%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	0.7%	

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2 Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)
- 4. Rolling 7-day and 365-day averages are calculated for each day the emission source is operating, including days when the analyzer has downtime. A null value is used for days in a rolling average period where the unit is not operating or the CEMS downtime causes insufficient data for a valid daily average. This can result in a day where the data is considered to be both an excess emission and analyzer downtime.

FCCU Excess Emissions Summary

Frontier Refining LLC NOx ppm @0% O2 7-Day Rolling Excess Emissions for 4/1/2014 thru 6/30/2014

Reason	Duration
There are no excess emissions for this report.	
Total duration of NOx ppm @0% O2 7-Day Rolling excess emissions	0
Total operating time	2015 hour
Operating time with excess emissions	0.0%

FCCU Excess Emissions Summary Frontier Refining LLC

Lighter Vermin fro						
NOx ppm @0% O2 365-Da	y Rolling Excess En	nissions for	4/1/2014 thru	6/30/2014		

Reason	Duration
There are no excess emissions for this report.	
Total duration of NOx ppm @0% O2 365-Day Rolling excess emissions	0
Total operating time	2015 hours
Operating time with excess emissions	0.0%

FCCU CEMS Downtime Summary

Frontier Refining LLC NOx ppm @0% O2 CEMS Downtime for 4/1/2014 thru 6/30/2014

Reason	Duration
Maintenance - Following Upset of FCCU due to Boiler #1 & #2 Shutdown - Sample System	13 hours
Maintenance - Sample System	1 hour
Total duration of NOx ppm @0% O2 CEMS downtime	14 hours
Total operating time	2015 hours
Operating time with CEMS downtime	0.7%

FCCU CEMS Downtime

Frontier Refining LLC NOx ppm @0% O2 CEMS Downtime for 4/1/2014 thru 6/30/2014

Parameter	Start	End	Duration	Reason	Action
NOx ppm @0% O2	4/11/2014 7:00 AM	7:59 AM	1 hour	Maintenance - Sample System	Took stack out of service to clean and change filters and service sample dryer. Passed Manual Calibration.
NOx ppm @0% O2	6/13/2014 10:00 AM	10:59 PM	13 hours	Maintenance - Following Upset of FCCU due to Boller #1 & #2 Shutdown - Sample System	Cleaned sample probe filter
To	otal duration		14 hours		

2Q14

DEPARTMENT OF ENVIRONMENTAL QUALITY AIR QUALITY DIVISION CONTINUOUS EMISSION MONITORING REPORT

FORM A

I. GENERAL INFORMATION

- A. Facility Name: FRONTIER REFINING LLC
- B. Process Unit/Pollutant Monitored: <u>SO, MONITORING SYSTEM FLUIDIZED</u>

 <u>CATALYTIC CRACKING UNIT (FCCU) REGENERATOR</u>
- C. Applicable Permit Number or Regulation: MD-946
- D. Applicable Emission Limit: 320 lb/hr SO, (1-hr average); 1401.6 tpy (calendar year)

II. MONITOR INFORMATION

- A. Date of Original Monitor Installation: 6/5/2012
- B. Date of Latest Monitor Certification: 7/17/2012
- C. Pollutant/Opacity Monitor
 - 1. Manufacturer: Teledyne/API
 - 2. Model Number: Model 100H
 - 3. Serial Number Main Chassis: 71
 - 4. Basis of Measurement (If Applicable Wet or Dry): Dry
 - 5. Instrument Span, Range Value (Specify Units): 0-1800 ppm and 0-600 lb/hr

D. Diluent Monitor NONE

- 1. Type of Monitor: O₂ or CO₂ (circle one)
- 2. Manufacturer:
- 3. Model Number:
- 4. Serial Number Main Chassis
- 5. Basis of Measurement (If Applicable Wet or Dry):
- 6. Instrument Span, Range Value (Specify Units):

E. Flow Monitor

- 1. Type of Instrument (i.e. S-type Pitot Tube): S-Type Pitot Tube
- 2. Manufacturer: Dieterich Standard
- 3. Model Number: PSF-S4H HSVH FADH0 FADC
- 4. Serial Number Main Chassis: <u>DFCII CEM 1MN 2XX #MN 4MN P1 ES RB TR AR</u> YX ZS DB

F. Quality Assurance Data

- 1. QA Plan Date: 10/15/2012
- 2. QA Plan Approval Date: 4/22/2013

III. Operating/Monitoring Data

A. Quarter: 2 Year: 2014

B Total Hours in Reporting Period: 2184

C. Hours Unit Operated During the Reporting Period: 2015

Note: Include <u>all</u> unit operating time for the quarter including operating time associated with Startup/Shutdown and Chapter 1 Section 5 (Emergency/Abnormal) Operations. Report time in hours to one decimal place, i.e. 1902.8.

IV. Quarterly Audits/Monitoring System Modifications

A. Quarterly Audits
Type Audit: RATA

Date Conducted

Pass

Pollutant/Opacity Monitor:

5/13/2014

YES

Note: A copy of the quarterly audits shall be included with the corresponding quarterly excess emission report.

Equipment Replaced During Reporting Period: <u>Changed out Filters: Replaced SO2 Flow</u>

Pressure Transducer Sensor.

Note: Only equipment replacements or modifications to the system that could affect the ability of the continuous monitoring system to comply with the associated Performance Specification shall be reported.

V. Report Contact

A. Name: David Weeks, Environmental Engineer

B. Phone Number: (307) 771-8827

EMISSION SUMMARY REPORT FCCU SO2 (lb/hr) CEMS 1-hr average = 320 lb/hr

FORM B

Emission Data Summary		CMS Performance Report		
I. Duration of Excess Emission in Reporting Peri	iod Due to:	I. CMS Downtime in Reporting Period Due to:		
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	41.0	
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	8.0	
C. Process Problem	0.0	C. Quality Assurance Calibration	0.0	
D. Other Known Causes	0.0	D. Other Known Causes	0.0	
E. Unknown Causes	0.0	E. Unknown Causes	0.0	
II. Total Duration of Excess Emission	0.0	II. Total CMS Downtime	49.0	
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.0%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	2.4%	

Total time of excess emission events due to emergency/abnormal operations: $\underline{0}$. NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2. Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)

FCCU Excess Emissions Summary

Frontier Refining LLC SO2 lbs 1-Hr Excess Emissions for 4/1/2014 thru 6/30/2014

Reason	Ouration
There are no excess emissions for this report.	
Total duration of SO2 lbs 1-Hr excess emissions	0
Total operating time	2015 hours
Operating time with excess emissions	0.0%

FCCU CEMS Downtime Summary

Frontier Refining LLC SO2 lbs CEMS Downtime for 4/1/2014 thru 6/30/2014

Reason	Duration
Maintenance - Following Upset of FCCU due to Boiler #1 & #2 Shutdown - Sample System	13 hours
Maintenance - Sample System	1 hour
Process - Ran Low Excess O2 - Wet O2 > Dry O2 causing % Moisture and Lb/Hr to be invalid	7 hours
Process - Ran Low Excess O2 - Wet O2 > Dry O2 causing % Moisture, Dry Stack Flow and Lb/Hr to be Invalid	1 hour
SO2 Analyzer Malfunction	3 hours
SO2 Analyzer Melfunction - Flow Pressure Transducer	24 hours
Total duration of SO2 (bs CEMS downtime	49 hours
Total operating time	2015 hours
Operating time with CEMS downtime	2.4%

FCCU CEMS Downtime

Frontier Refining LLC SO2 lbs CEMS Downtime for 4/1/2014 thru 6/30/2014

Parameter	Start	End	Duration	Reason	Action
SO2 lbs	4/11/2014 7:00 AM	7:59 AM	1 hour	Maintenance - Sample System	Took stack out of service to clean and change filters and service sample dryer. Passed Manual Calibration.
SO2 ibs	4/22/2014 10:00 PM	10:59 PM	1 hour	SO2 Analyzer Malfunction	Cleared fault and troubleshot issue. Found flow reading on SO2 instrument wasn't reading correctly and was reading low. Adjusted flow to nominal.
SO2 lbs	5/3/2014 9:00 AM	9:59 AM	1 hour	SO2 Analyzer Malfunction - Flow Pressure Transducer	Replaced transducer and ran calibration & validation.
SO2 lbs	5/3/2014 12:00 PM	2:59 PM	3 hours	SO2 Analyzer Maifunction - Flow Pressure Transducer	Replaced transducer and ran calibration & validation.
SO2 bs	5/3/2014 4:00 PM	6:59 PM	3 hours	SO2 Analyzer Malfunction - Flow Pressure Transducer	Replaced transducer and ran calibration & validation.
SO2 ibs	5/3/2014 9:00 PM	9:59 PM	1 hour	SO2 Analyzer Malfunction - Flow Pressure Transducer	Replaced transducer and ran calibration & validation.
SO2 lbs	5/4/2014 7:00 AM	7:59 AM	1 hour	SO2 Analyzer Malfunction - Flow Pressure Transducer	Replaced transducer and ran calibration & validation.
SO2 ibs	5/4/2014 11:00 AM	12:59 PM	2 hours	SO2 Analyzer Malfunction - Flow Pressure Transducer	Replaced transducer and ran calibration & validation.
SO2 lbs	5/4/2014 2:00 PM	2:59 PM	1 hour	SO2 Analyzer Malfunction - Flow Pressure Transducer	Replaced transducer and ran calibration & validation.
SO2 ibs	5/4/2014 5:00 PM	11:59 PM	7 hours	SO2 Analyzer Malfunction - Flow Pressure Transducer	Replaced transducer and ran calibration & validation.
SO2 ibs	5/5/2014 12:00 AM	4:59 AM	5 hours	SO2 Analyzer Matfunction - Flow Pressure Transducer	Replaced transducer and ran calibration & validation.
SO2 lbs	5/11/2014 12:00 AM	12:59 AM	1 hour	SO2 Analyzer Malfunction	Self Corrected
SO2 lbs	6/8/2014 6:00 AM	6:59 AM	1 hour	SO2 Analyzer Maifunction	Self Corrected
SO2 ibs	6/13/2014 10:00 AM	10:59 PM	13 hours	Maintenance - Following Upset of FCCU due to Boller #1 & #2 Shutdown - Sample System	Cleaned sample probe filter
SO2 lbs	6/13/2014 11:00 PM	11:59 PM	1 hour	Process - Ran Low Excess O2 - Wet O2 > Dry O2 causing % Moisture and Lb/Hr to be invalid	Adjusted Excess O2. Morning Calibration Check Corrected Discrepancy.

Parameter	Start	End	Duration	Reason	Action
SO2 lbs	6/14/2014 12:00 AM	5:59 AM	6 hours	Process - Ran Low Excess O2 - Wat O2 > Dry O2 causing % Moisture and Lb/Hr to be Invalid	Adjusted Excess O2. Morning Calibration Check Corrected Discrepancy.
SO2 lbs	6/23/2014 10:00 PM	10:59 PM	1 hour	Process - Ran Low Excess O2 - Wet O2 > Dry O2 causing % Moisture, Dry Stack Flow and Lb/Hr to be Invalid	FCCU Shutdown
	Total duration		49 hours		

DEPARTMENT OF ENVIRONMENTAL QUALITY AIR QUALITY DIVISION CONTINUOUS EMISSION MONITORING REPORT

FORM A

I. GENERAL INFORMATION

- A. Facility Name: FRONTIER REFINING LLC
- B. Process Unit/Pollutant Monitored: <u>CO MONITORING SYSTEM FLUIDIZED</u> CATALYTIC CRACKING UNIT (FCCU) REGENERATOR
- C. Applicable Permit Number or Regulation: 3-0-149-2; MACT Subpart UUU; Consent Decree; MD-9640
- D. Applicable Emission Limit: 500 ppm (1-hr); 500 ppmvd @ 0% 02 (1-hr); 100 ppmvd @ 0% 02 (365 day rolling average); 30 lb/hr (1-hr); 18.2 lb/hr (365 day rolling average)

II. MONITOR INFORMATION

- A. Date of Original Monitor Installation: 6/5/2012
- B. Date of Latest Monitor Certification: 7/17/2012
- C. Pollutant/Opacity Monitor
 - 1. Manufacturer: Teledyne/API
 - 2. Model Number: Model 300H
 - 3. Serial Number Main Chassis: 186
 - 4. Basis of Measurement (If Applicable Wet or Dry): Dry
 - 5. Instrument Span, Range Value (Specify Units): 0-1000 ppm

D. Diluent Monitor NONE

- 1. Type of Monitor: O₂ or CO₂ (circle one)
- 2. Manufacturer:
- 3. Model Number:
- 4. Serial Number Main Chassis
- 5. Basis of Measurement (If Applicable Wet or Dry):
- 6. Instrument Span, Range Value (Specify Units):

E. Flow Monitor

- 1. Type of Instrument (i.e. S-type Pitot Tube): S-Type Pitot Tube
- 2. Manufacturer: Dieterich Standard
- 3. Model Number: PSF-S4H HSVH FADH0 FADC
- 4. Serial Number Main Chassis: DFCII CEM 1MN 2XX #MN 4MN P1 ES RB TR AR YX ZS DB
- F. Quality Assurance Data
 - 1. QA Plan Date: 10/15/2012
 - 2. QA Plan Approval Date: 4/22/2013

III. Operating/Monitoring Data

A. Quarter:

2 Year: 2014

B Total Hours in Reporting Period: 2184

C. Hours Unit Operated During the Reporting Period: 2015

Note: Include <u>all</u> unit operating time for the quarter including operating time associated with Startup/Shutdown and Chapter 1 Section 5 (Emergency/Abnormal) Operations. Report time in hours to one decimal place, i.e. 1902.8.

IV. Quarterly Audits/Monitoring System Modifications

A. Quarterly Audits

Type Audit: RATA

Date Conducted

Pass

Pollutant/Opacity Monitor:

5/13/2014

YES

Note: A copy of the quarterly audits shall be included with the corresponding quarterly excess emission report.

B. Equipment Replaced During Reporting Period: <u>Changed out Filters; Replaced Flow</u>
Pressure Transducer.

Note: Only equipment replacements or modifications to the system that could affect the ability of the continuous monitoring system to comply with the associated Performance Specification shall be reported.

V. Report Contact

A. Name: David Weeks, Environmental Engineer

B. Phone Number: (307) 771-8827

EXCESS EMISSION SUMMARY REPORT FCCU CO (ppm) (1-hr average) CEMS 1-hr average limit = 500 ppm

FORM B

Emission Data Summary		CMS Performance Report			
I. Duration of Excess Emission in Reporting Peri	od Due to:	I. CMS Downtime in Reporting Period Due to:			
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	14.0		
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	2.0		
C. Process Problem	4.0	C. Quality Assurance Calibration	0.0		
D. Other Known Causes	0.0	D. Other Known Causes	0.0		
E. Unknown Causes	0.0	E. Unknown Causes	0.0		
II. Total Duration of Excess Emission	4.0	II. Total CMS Downtime	16.0		
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.2%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	0.8%		

Total time of excess emission events due to emergency/abnormal operations: _______. NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2. Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)

FCCU Excess Emissions Summary Frontier Refining LLC CO ppm 1-Hr Excess Emissions for 4/1/2014 thru 6/30/2014

Reason	Duration
Emission Exceedance - CO ppm @ 0% O2 and CO Lb/Hr - Rate Change - Low Excess O2	1 hour
Emission Exceedance - CO ppm, CO ppm @ 0% O2 and CO Lb/Hr - Low Excess O2	1 hour
Process Upset - Low Excess O2 from Raising LCO Rate	1 hour
Process Upset - Low Excess O2 from Rate Increase and LCO Rate Increase - Ran Out of Blower Capacity	1 hour
Total duration of CO ppm 1-Hr excess emissions	4 hours
Total operating time	2015 hours
Operating time with excess emissions	0.2%

FCCU Excess Emissions

Frontier Refining LLC
CO ppm 1-Hr Excess Emissions for 4/1/2014 thru 6/30/2014

Parameter	Start	End	Duration	Value	Min	Max	Limit	Reason	Action
CO ppm 1-Hr	5/2/2014 6:00 AM	6:59 AM	1 hour	533.10	533.10	533.10	500	Process Upset - Low Excess O2 from Raising LCO Rate	Adjusted Excess O2
CO ppm 1-Hr	5/2/2014 2:00 PM	2:59 PM	1 hour	514.10	514.10	514.10	500	Process Upset - Low Excess O2 from Rate Increase and LCO Rate Increase - Ran Out of Blower Capacity	Adjusted Rate to meet Blower Capacity and Adjusted Excess O2
CO ppm 1-Hr	5/28/2014 1:00 PM	1:59 PM	1 hour	638.80	638.80	638.80	500	Emission Exceedance - CO ppm @ 0% O2 and CO Lb/Hr - Rate Change - Low Excess O2	Adjusted Unit Operation and Excess O2
CO ppm 1-Hr	6/16/2014 1:00 PM	1:59 PM	1 hour	522.30	522.30	522.30	500	Emission Exceedance - CO ppm, CO ppm @ 0% O2 and CO Lb/Hr- Low Excess O2	Raised Excess O2 and Trimmed Rate 400 BPD

Total duration

4 hours

FCCU CEMS Downtime Summary

Frontier Refining LLC CO ppm CEMS Downtime for 4/1/2014 thru 6/30/2014

Reason	Duration
Maintenance - Following Upset of FCCU due to Boller #1 & #2 Shutdown - Sample System	13 hours
Maintenance - Sample System	1 hour
Process - Ran Low Excess O2 - Wet O2 > Dry O2 causing % Moisture, Dry Stack Flow and Lb/Hr to be Invalid	2 hours
Total duration of CO ppm CEMS downtime	16 hours
Total operating time	2015 hours
Operating time with CEMS downtime	0.8%

FCCU CEMS Downtime

Frontier Refining LLC CO ppm CEMS Downtime for 4/1/2014 thru 6/30/2014

Parameter	Start	End	Duration	Reason	Action
CO ppm	4/11/2014 7:00 AM	7:59 AM	1 hour	Maintenance - Sample System	Took stack out of service to clean and change filters and service sample dryer. Passed Manual Calibration.
CO ppm	6/13/2014 10:00 AM	10:59 PM	13 hours	Maintenance - Following Upset of FCCU due to Boiler #1 & #2 Shutdown - Sample System	Cleaned sample probe filter
CO ppm	6/23/2014 9:00 PM	10:59 PM	2 hours	Process - Ran Low Excess O2 - Wet O2 > Dry O2 causing % Moisture, Dry Stack Flow and Lb/Hr to be invalid	FCCU Shutdown
	Total duration		16 hours		

EXCESS EMISSION SUMMARY REPORT FCCU CO (ppmvd) @ 0% 02 (1-hr average) CEMS 1-hr average limit = 500 ppmvd @ 0% 02

FORM B

Emission Data Summary		CMS Performance Report				
I. Duration of Excess Emission in Reporting Peri	od Due to:	I. CMS Downtime in Reporting Period Due to:				
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	14.0			
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	2.0			
C. Process Problem	4.0	C. Quality Assurance Calibration	0.0			
D. Other Known Causes	0.0	D. Other Known Causes	0.0			
E. Unknown Causes	0.0	E. Unknown Causes	0.0			
II. Total Duration of Excess Emission	4.0	II. Total CMS Downtime	16.0			
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.2%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	0.8%			

Total time of excess emission events due to emergency/abnormal operations: ______.

NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2. Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)

EXCESS EMISSION SUMMARY REPORT FCCU CO (ppmvd) @ 0% 02 (365-day rolling average) CEMS

365-day rolling average = 100 ppmvd @ 0% 02

FORM B

Emission Data Summary		CMS Performance Report				
I. Duration of Excess Emission in Reporting Per	riod Due to:	I. CMS Downtime in Reporting Period Due to:				
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	14.0			
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	2.0			
C. Process Problem	0.0	C. Quality Assurance Calibration	0.0			
D. Other Known Causes	0.0	D. Other Known Causes	0.0			
E. Unknown Causes	0.0	E. Unknown Causes	0.0			
II. Total Duration of Excess Emission	0.0	II. Total CMS Downtime	16.0			
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.0%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	0.8%			

Total time of excess emission events due to emergency/abnormal operations: __0_. NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2 Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)
- 4. Rolling 7-day and 365-day averages are calculated for each day the emission source is operating, including days when the analyzer has downtime. A null value is used for days in a rolling average period where the unit is not operating or the CEMS downtime causes insufficient data for a valid daily average. This can result in a day where the data is considered to be both an excess emission and analyzer downtime.

FCCU Excess Emissions Summary

Frontier Refining LLC
CO ppm @0% O2 1-Hr Excess Emissions for 4/1/2014 thru 6/30/2014

Reason	Duration
Emission Exceedance - CO ppm @ 0% O2 and CO Lb/Hr - Rate Change - Low Excess O2	1 hour
Emission Exceedance - CO ppm, CO ppm @ 0% O2 and CO Lb/Hr - Low Excess O2	1 hour
Process Upset - Low Excess O2 from Reising LCO Rate	1 hour
Process Upset - Low Excess O2 from Rate Increase and LCO Rate Increase - Ran Out of Blower Capacity	1 hour
Total duration of CO ppm @0% O2 1-Hr excess emissions	4 hours
Total operating time	2015 hours
Operating time with excess emissions	0.2%

FCCU Excess Emissions

Frontier Refining LLC
CO ppm @0% O2 1-Hr Excess Emissions for 4/1/2014 thru 6/30/2014

Parameter	Start	End	Duration	Value	Min	Max	Limit	Reason	Action
CO ppm @0% O2 1-Hr	5/2/2014 6:00 AM	6:59 AM	1 hour	542.20	542.20	542.20	500	Process Upset - Low Excess O2 from Raising LCO Rate	Adjusted Excess O2
CO ppm @0% O2 1-Hr	5/2/2014 2:00 PM	2:59 PM	1 hour	520.30	520.30	520.30	500	Process Upset - Low Excess O2 from Rate Increase and LCO Rate Increase - Ran Out of Blower Capacity	Adjusted Rate to meet Blower Capacity and Adjusted Excess O2
CO ppm @0% O2 1-Hr	5/28/2014 1:00 PM	1:59 PM	1 hour	647.20	647.20	647.20	500	Emission Exceedance - CO ppm @ 0% O2 and CO Lb/Hr - Rate Change - Low Excess O2	Adjusted Unit Operation and Excess O2
CO ppm @0% O2 1-Hr	6/16/2014 1:00 PM	1:59 PM	1 hour	635.10	535.10	535.10	500	Emission Exceedance - CO ppm, CO ppm @ 0% O2 and CO Lb/Hr - Low Excess O2	Raised Excess O2 and Trimmed Rate 400 8PD

Total duration

4 hours

FCCU Excess Emissions Summary

Frontier Refining LLC
CO ppm @0% O2 365-Day Rolling Excess Emissions for 4/1/2014 thru 6/30/2014

Reason	Duration
There are no excess emissions for this report.	
Total duration of CO ppm @0% O2 365-Day Rolling excess emissions	0
Total operating time	2015 hours
Operating time with excess emissions	0.0%

FCCU CEMS Downtime Summary

Frontier Refining LLC CO ppm @0% O2 CEMS Downtime for 4/1/2014 thru 6/30/2014

Reason	Duration
Maintenance - Following Upset of FCCU due to Boiler #1 & #2 Shutdown - Sample System	13 hours
Maintenance - Sample System	1 hour
Process - Ran Low Excess O2 - Wet O2 > Dry O2 causing % Moisture, Dry Stack Flow and Lb/Hr to be Invalid	2 hours
Total duration of CO ppm @0% O2 CEMS downtime	16 hours
Total operating time	2015 hours
Operating time with CEMS downtime	0.8%

FCCU CEMS Downtime

Frontier Refining LLC CO ppm @0% O2 CEMS Downtime for 4/1/2014 thru 6/30/2014

Parameter	Start	End	Duration	Reason	Action
СО ррт @0% О2	4/11/2014 7:00 AM	7:59 AM	1 hour	Maintenance - Sample System	Took stack out of service to clean and change filters and service sample dryer, Passed Manual Calibration.
CO ppm @0% O2	6/13/2014 10:00 AM	10:59 PM	13 hours	Maintenance - Following Upset of FCCU due to Boiler#1 & #2 Shutdown - Sample System	Cleaned sample probe filter
СО ррт @0% О2	6/23/2014 9:00 PM	10:59 PM	2 hours	Process - Ran Low Excess O2 - Wet O2 > Dry O2 causing % Moisture, Dry Stack Flow and Lb/Hr to be invalid	FCCU Shutdown
T	otal duration		16 hours		<u> </u>

EXCESS EMISSION SUMMARY REPORT FCCU CO (lb/hr) CEMS 1-hr average limit = 30 lb/hr

FORM B

Emission Data Summary		CMS Performance Report I. CMS Downtime in Reporting Period Due to:			
I. Duration of Excess Emission in Reporting Pe	riod Due to:				
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	14.0		
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	9.0		
C. Process Problem	4.0	C. Quality Assurance Calibration	0.0		
D. Other Known Causes	0.0	D. Other Known Causes	0.0		
E. Unknown Causes	0.0	E. Unknown Causes	0.0		
II. Total Duration of Excess Emission	4.0	II. Total CMS Downtime	23.0		
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.2%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	1.1%		

Total time of excess emission events due to emergency/abnormal operations: __0_. NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2 Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)

EXCESS EMISSION SUMMARY REPORT FCCU CO (lb/hr) CEMS 365-day rolling average = 18.2 lb/hr

FORM B

Emission Data Summary		CMS Performance Report I. CMS Downtime in Reporting Period Due to:			
I. Duration of Excess Emission in Reporting Per	iod Due to:				
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	14.0		
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	9.0		
C. Process Problem	0.0	C. Quality Assurance Calibration	0.0		
D. Other Known Causes	0.0	D. Other Known Causes	0.0		
E. Unknown Causes	0.0	E. Unknown Causes	0.0		
II. Total Duration of Excess Emission	0.0	II. Total CMS Downtime	23.0		
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.0%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	1.1%		

Total time of excess emission events due to emergency/abnormal operations: ___0_. NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2 Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)
- 4. Rolling 7-day and 365-day averages are calculated for each day the emission source is operating, including days when the analyzer has downtime. A null value is used for days in a rolling average period where the unit is not operating or the CEMS downtime causes insufficient data for a valid daily average. This can result in a day where the data is considered to be both an excess emission and analyzer downtime.

FCCU Excess Emissions Summary

Frontier Refining LLC CO lbs 1-Hr Excess Emissions for 4/1/2014 thru 6/30/2014

Reason	Duration	
Emission Exceedance - CO ppm @ 0% O2 and CO Lb/Hr - Rate Change - Low Excess O2	1 hour	
Emission Exceedance - CO ppm, CO ppm @ 0% O2 and CO Lb/Hr - Low Excess O2	2 hours	
Process Upset - Low Excess O2 from Raising LCO Rate	1 hour	
Total duration of CO lbs 1-Hr excess emissions	4 hours	
Total operating time	2015 hours	
Operating time with excess emissions	0.2%	

FCCU Excess Emissions

Frontier Refining LLC
CO lbs 1-Hr Excess Emissions for 4/1/2014 thru 6/30/2014

Parameter	Start	End	Duration	Value	Min	Max	Limit	Reason	Action
CO lbs 1-Hr	5/2/2014 6:00 AM	6:59 AM	1 hour	32.1	32.1	32.1	30	Process Upset - Low Excess O2 from Raising LCO Rate	Adjusted Excess O2
CO lbs 1-Hr	5/28/2014 1:00 PM	1:59 PM	1 hour	42.1	42.1	42.1	30	Emission Exceedance - CO ppm @ 0% O2 and CO Lb/Hr - Rate Change - Low Excess O2	Adjusted Unit Operation and Excess O2
CO lbs 1-Hr	6/16/2014 12:00 PM	1:59 PM	2 hours	43.5	35.3	51.7	30	Emission Exceedance - CO ppm, CO ppm @ 0% O2 and CO Lb/Hr- Low Excess O2	Raised Excess O2 and Trimmed Rate 400 BPD

Total duration

4 hours

FCCU Excess Emissions Summary

Frontier Refining LLC
CO lbs/hr 365-Day Rolling Excess Emissions for 4/1/2014 thru 6/30/2014

Reason	Duration	
There are no excess emissions for this report.		
Total duration of CO lbs/hr 365-Day Rolling excess emissions	0	
Total operating time	2015 hours	
Operating time with excess emissions	0.0%	

FCCU CEMS Downtime Summary

Frontier Refining LLC CO lbs CEMS Downtime for 4/1/2014 thru 6/30/2014

Reason	Duration
Maintenance - Following Upset of FCCU due to Boller #1 & #2 Shutdown - Sample System	13 hours
Maintenance - Semple System	1 hour
Process - Ran Low Excess O2 - Wet O2 > Dry O2 causing % Moisture and Lb/Hr to be invalid	7 hours
Process - Ran Low Excess O2 - Wet O2 > Dry O2 causing % Moisture, Dry Stack Flow and Lb/Hr to be Invalid	2 hours
Total duration of CO lbs CEMS downtime	23 hours
Total operating time	2015 hours
Operating time with CEMS downtime	1.1%

FCCU CEMS Downtime

Frontier Refining LLC CO lbs CEMS Downtime for 4/1/2014 thru 6/30/2014

Parameter	Start	End	Duration	Reason	Action
CO lbs	4/11/2014 7:00 AM	7:59 AM	1 hour	Maintenance - Sample System	Took stack out of service to clean and change filters and service sample dryer. Passed Manuel Calibration.
CO lbs	6/13/2014 10:00 AM	10:59 PM	13 hours	Maintenance - Following Upset of FCCU due to Boiler#1 & #2 Shutdown - Sample System	Cleaned sample probe filter
CO lbs	6/13/2014 11:00 PM	11:59 PM	1 hour	Process - Ran Low Excess O2 - Wet O2 > Dry O2 causing % Moisture and Lb/Hr to be Invalid	Adjusted Excess O2. Morning Calibration Check Corrected Discrepancy.
CO lbs	6/14/2014 12:00 AM	5:59 AM	6 hours	Process - Ran Low Excess O2 - Wet O2 > Dry O2 causing % Moisture and Lb/Hr to be Invalid	Adjusted Excess O2. Morning Calibration Check Corrected Discrepancy.
CO ibs	6/23/2014 9:00 PM	10:59 PM	2 hours	Process - Ran Low Excess O2 - Wet O2 > Dry O2 causing % Moisture, Dry Stack Flow and Lb/Hr to be invalid	FCCU Shutdown
	Total duration		23 hours		

2014

DEPARTMENT OF ENVIRONMENTAL QUALITY AIR QUALITY DIVISION CONTINUOUS EMISSION MONITORING REPORT

FORM A

I. GENERAL INFORMATION

- A. Facility Name: FRONTIER REFINING LLC
- B. Process Unit/Pollutant Monitored: <u>PM MONITORING SYSTEM FLUIDIZED</u>

 <u>CATALYTIC CRACKING UNIT (FCCU) REGENERATOR</u>
- C. Applicable Permit Number or Regulation: <u>Consent Decree, MD-9640, and MACT</u>
 Subpart UUU
- D. Applicable Emission Limit: 70.8 lb/hr (3-hr average); 0.029 lb Ni/hr (1-hr average)

II. MONITOR INFORMATION Laser Hawk PM Monitor

- A. Date of Original Monitor Installation: May 2011
- B. Date of Latest Monitor Certification: December 2012 (Approved 4/22/2013)
- C. Pollutant/Opacity Monitor
 - 1. Manufacturer: Teledyne Instruments
 - 2. Model Number: 360 PM Laser Hawk
 - 3. Serial Number Main Chassis: 360085
 - 4. Basis of Measurement (If Applicable Wet or Dry): NA
 - 5. Instrument Span, Range Value (Specify Units): NA

D. Diluent Monitor NONE

- 1. Type of Monitor: O₂ or CO₂ (circle one)
- 2. Manufacturer:
- 3. Model Number:
- 4. Serial Number Main Chassis
- 5. Basis of Measurement (If Applicable Wet or Dry):
- 6. Instrument Span, Range Value (Specify Units):___

E. Flow Monitor NONE

- 1. Type of Instrument (i.e. S-type Pitot Tube):
- 2. Manufacturer:
- 3. Model Number:
- 4. Serial Number Main Chassis:

F. Quality Assurance Data

- 1. QA Plan Date: 2/15/2013
- 2. QA Plan Approval Date: <u>4/22/2013</u>

III. Operating/Monitoring Data

A. Quarter: 2 Year: 2014

B Total Hours in Reporting Period: 2184

C. Hours Unit Operated During the Reporting Period: 2015

Note: Include <u>all</u> unit operating time for the quarter including operating time associated with Startup/Shutdown and Chapter 1 Section 5 (Emergency/Abnormal) Operations. Report time in hours to one decimal place, i.e. 1902.8.

- IV. Quarterly Audits/Monitoring System Modifications
 - A. Quarterly Audits
 Type Audit: ACA

Pollutant/Opacity Monitor:

Date Conducted Pass
6/9/2014 Yes

Equipment Replaced During Reporting Period: None.

Note: Only equipment replacements or modifications to the system that could affect the ability of the continuous monitoring system to comply with the associated Performance Specification shall be reported.

V. Report Contact

A. Name: David Weeks, Environmental Engineer

B. Phone Number: <u>(307) 771-8827</u>

EXCESS EMISSION SUMMARY REPORT FCCU PM (ib/hr) CEMS 3-hr average limit = 70.8 lb/hr

FORM B

Emission Data Summary		CMS Performance Report		
I. Duration of Excess Emission in Reporting Peri	od Due to:	I. CMS Downtime in Reporting Period Due to:		
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	2.0	
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	0.0	
C. Process Problem	0.0	C. Quality Assurance Calibration	0.0	
D. Other Known Causes	0.0	D. Other Known Causes	0.0	
E. Unknown Causes	0.0	E. Unknown Causes	0.0	
II. Total Duration of Excess Emission	0.0	II. Total CMS Downtime	2.0	
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.0%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	0.1%	

Total time of excess emission events due to emergency/abnormal operations: ______. NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2. Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)

FCCU Excess Emissions Summary

Frontier Refining LLC PM lbs 3-Hr Rolling Excess Emissions for 4/1/2014 thru 6/30/2014

Reason	Duration
There are no excess emissions for this report.	
Total duration of PM lbs 3-Hr Rolling excess emissions	0
Total operating time	2015 hours
Operating time with excess emissions	0.0%

Comment: Form C - Excess Emissions Summary

FCCU CEMS Downtime Summary

Frontier Refining LLC PM lbs CEMS Downtime for 4/1/2014 thru 6/30/2014

Reason	Duration
Particulate Analyzer Fault	2 hours
Total duration of PM lbs CEMS downtime	2 hours
Total operating time	2015 hours
Operating time with CEMS downtime	0.1%

Comment: Form D - Downtime Summary

FCCU CEMS Downtime

Frontier Refining LLC PM lbs CEMS Downtime for 4/1/2014 thru 6/30/2014

Parameter	Start	End	Duration	Reason	Action
PM lbs	4/5/2014 6:00 AM	6:59 AM	1 hour	Particulate Analyzer Fault	Cleaned Lens and Ran Cal to Clear Alarm
PM lbs	5/5/2014 6:00 AM	6:59 AM	1 hour	Particulate Analyzer Fault	Cleaned Lens and Ran Cal to Clear Alarm
	Total duration		2 hours		

Comment: Form D - Downtime Summary

EXCESS EMISSION SUMMARY REPORT FCCU PM (Ni lb/hr) CEMS 1-hr average limit = 0.029 lb/hr

FORM B

Emission Data Summary		CMS Performance Report	
I. Duration of Excess Emission in Reporting Per	riod Due to:	I. CMS Downtime in Reporting Period Due to:	
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	2.0
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	0.0
C. Process Problem	0.0	C. Quality Assurance Calibration	0.0
D. Other Known Causes	0.0	D. Other Known Causes	2.0
E. Unknown Causes	0.0	E. Unknown Causes	0.0
II. Total Duration of Excess Emission	0.0	II. Total CMS Downtime	2.0
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.0%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	0.2%

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2. Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)

FCCU Excess Emissions Summary

Frontier Refining LLC Nickie ibs 1-Hr Excess Emissions for 4/1/2014 thru 6/30/2014

Reason	Duration
There are no excess emissions for this report.	
Total duration of Nickle Ibs 1-Hr excess emissions	0
Total operating time	2015 hours
Operating time with excess emissions	0.0%

FCCU CEMS Downtime Summary

Frontier Refining LLC Nickel ibs CEMS Downtime for 4/1/2014 thru 6/30/2014

Reason	Duration
Particulate Analyzer Fault	2 hours
Total duration of Nickel Ibs CEMS downtime	2 hours
Total operating time	2015 hours
Operating time with CEMS downtime	0.1%

Comment: Form D - Downtime Summary

FCCU CEMS Downtime

Frontier Refining LLC Nickel lbs CEMS Downtime for 4/1/2014 thru 6/30/2014

Parameter	Start	End	Duration	Reason	Action
Nickel Ibs	4/5/2014 6:00 AM	6:59 AM	1 hour	Particulate Analyzer Fault	Cleaned Lens and Ran Cel to Clear Alarm
Nickel ibs	5/5/2014 6:00 AM	6:59 AM	1 hour	Particulate Analyzer Fault	Cleaned Lens and Ran Cal to Clear Alarm
، میں بنے بین بناء طولان کی بادرک نے بنی بنا	Total duration		2 hours		

Comment: Form D - Downtime Summary

Data Sheet for FCCU PM CEM System Absolute Correlation Audit (ACA)

Date:	June 9, 201	June 9, 2014		9:50 AM	
	Zero % Low		Mid	100%	
	Analyzer	Analyzer	Analyzer	Analyzer	
Run 1	0.00	57.15	77.88	98.86	
Run 2	(0.03)	57.78	`77.95	99.02	
Run 3	0.00	57.56	77.68	99.02	
C _{CEM} , R _{CEM}	(1.36)	57.50	77.78	98.97	
C _{RV} , R _V	0.00	58.00	79.30	100.00	
ACA Accuracy	1.93	0.87	1.92	1.03	
Pass?	Yes	Yes	Yes	Yes	

Signature of Technician(s) performing ACA:

Matt Hobbs, Keyin Marschner and/or Tad Milliken

Calculation of ACA Accuracy:

For Low, Mid & 100%:

Eq. 2-1a ACA = $(R_{CEM} - R_V) / R_V \times 100$

ACA must be +/-10% to pass.

where:

ACA = accuracy of CEM, %

R_{CEM} = average of reponses

R_V = certified audit value of gas

For Zero:

Eq. 2-1b ACA = $(C_{CEM} - C_{RV}) / C_8 \times 100$

ACA must be +/-7.5% to pass.

where:

ACA = accuracy of CEM, %

C_{CEM} = average of reponses

 $Y (mg/m^3) = 6.4 * X (backscatter in %) - 1.3$

C_{RV}= certified audit value of gas

Attachment B - FCCU

Paragaph 217g Emission Summary

FCCU SOURCE EMISSIONS DATA FOR 2013

	Actual Emissions	Method of Determination
	tons/yr	
PM	82.2	PM CEMS data
SO2	68.5	SO2 CEMS data
NOx	42.5	NOx CEMS data
CO	17.3	CO CEMS data

Section C - FLARING

RCFA Reports

Reports pulled and placed in Floring Sile

Frontier Refining LLC
P.O. Box 1588 • Cheyenne, WY 82003-1588

Paragraph	Attachment C - Flaring	Comments
84	Semi-Annual Reporting. Within thirty (30) calendar days after the end of the first semi-annual period after the Date of Entry of this Consent Decree (i.e., January 31st or July 31st), and on each subsequent January 31st and July 31st thereafter, FRI and FEDRC shall submit to EPA and the Applicable Intervenor a Semi-Annual report that includes copies of each and every report of all Acid Gas Flaring Incidents and Tail Gas Incidents that FRI and FEDRC was required to prepare under Paragraphs 71 and 82 during the previous six month period (e.g., July to December). FRI and/or FEDRC may elect to submit the Semi-Annual report required by this Paragraph with the Semi-Annual progress report required by Paragraph 216. Each Semi-Annual report shall also include a summary of the Incidents including the following:	A table summarizing all of the incidents is included in this section. The report for each incident is also included.
84a	a. Date;	See table.
84b	b. Summary of root cause(s);	See table.
84c	c. Duration;	See table.
84d	d. Amount of SO2 released;	See table.
84e	e. Any associated penalties for each Incident;	See table.
84f	f. Corrective Action completed; and	See table.
84g	g. A list of all Acid Gas Flaring Incidents, Tail Gas Incidents, and Hydrocarbon Flaring Incidents for which corrective actions are still outstanding.	See table.
84	Such Semi-Annual report shall also include a summary analysis of any trends identified by FRI and/or FEDRC, as appropriate, in the number, Root Cause, types of corrective action, or other relevant information regarding Acid Gas and Tail Gas Incidents during the previous six-month period.	After reviewing the incidents, there were no trends identified in the number, root cause, types of corrective actions, or other relevant information during the previous six months.
85	85. For Hydrocarbon Flaring Incidents occurring more than 180 days after the Date of Entry, at their respective Covered Refineries, FRI and FEDRC shall follow the same investigative, reporting, and corrective action procedures as those set forth in Section VI.J., Paragraphs 71 through 72 for Acid Gas Flaring Incidents; provided however, that in lieu of analyzing possible corrective actions under Paragraph 71.e and taking interim and/or long-term corrective action under Paragraph 72 for a Hydrocarbon Flaring Incident attributable to the Startup or Shutdown of a unit that FRI and/or FEDRC has previously analyzed under this Paragraph, FRI and/or FEDRC, as applicable, may identify such prior analysis when submitting the report required under this Paragraph. At their respective Covered Refineries, FRI and FEDRC shall submit the Hydrocarbon Flaring Incident(s) reports as part of the Semi-Annual Reports required pursuant to Paragraph 84. Stipulated penalties under Paragraphs 74 through 76 shall not apply to Hydrocarbon Flaring Incident(s). The formulas at Paragraph 80, used for calculating the quantity and rate of sulfur dioxide emissions during AG Flaring Incidents, shall be used to calculate the quantity and rate of sulfur dioxide emissions during Hydrocarbon Flaring Incidents.	The table summarizing all incidents includes hydrocarbon flaring events is attached. All incident reports have been completed and are included here.

Paragraph	Attachment C - Flaring	Comments
217e	SO2 emissions from all Acid Gas Flaring and Tail Gas Incidents by flare in tons per year;	Summary of emissions is attached.

P84 & P85 Summary of Acid Gas, Tail Gas, and Hydrocarbon Flaring Incidents

Date of Event	Type of Event	Duration (hrs)	SO2 Released (tons)	Root Cause	Corrective Actions Completed?	Corrective Actions Outstanding?	Associated Penalties
				Level indicator for liquid in the naphtha splitter overhead receiver			
				stuck causing too much liquid into the crude compressor knock			
1/23/2014	Hydrocarbon	0.75	0.6	out drum	Yes	No	N/A
1/26/2014	Acid Gas	1.0	4.9	The SRU #2 flow transmitter froze due to extreme cold weather	Yes	No	See Report
a /00 /00 a				Too many water booots were draining hydrocarbons due to cold			
1/29/2014	Hydrocarbon	8.9	0.3	weather	Partial	Yes	N/A
1/31/2014	Acid Gas	1.6	7.8	The SRU #1 coarse air transmitter froze due to extreme temperatures	Yes	No	See Report
1,01,201	700 003		7.0	The board operator did not properly address the low level alarm	163	140	see neport
2/3/2014	Tail Gas	1.1	0.3	on the boiler feed water	Yes	No	See Report
2/4/2014	Acid Gas	0.2	1.3	The panel view for the Boiler Manangement System (BMS) failed	Yes	No	See Report
				The flame scanner of SRU #1 malfunctioned. If the system does			
	Acid Gas &	2.2		not see a flame on SRU #1, it automatically shuts off the air			
2/5/2014	Hydrocarbon 3.7 12.1 demand to the unit and then the acid gas into the unit.		demand to the unit and then the acid gas into the unit.	Yes	No	See Report	
				Crude VRU Compressor, C-401, was not online when the Crude			
2/11/2014	Hydrocarbon	14.8	0.5	unit was started.	Yes	No	N/A
	Acid Gas &		7.1	The jumper for the SRU #2 was removed and pilot caused the			
2/13/2014	Hydrocarbon	2.2	0.7	shut down.	Yes	No	See Report
				Excess hydrocarbon in the Amine unit caused by carryover from			
2/14/2014	Acid Gas	10.0	73.4	upsets in the other units upstream	Yes	No	See Report
				The electric lube oil turbine was not turned on prior to strating			
2/16/2014	Hydrocarbon	43.9	23.5	the wet gas compressor	Yes	No	N/A
				Operations did not adequately monitor the boiler feed water of			
2/17/2014	Acid Gas	0.6	1.9	SRU #2.	Yes	No	See Report
2/26/2014	Hydrocarbon	0.6	0.5	The glycol system for C-407 failed.	Partial	Yes	N/A
2/28/2014	Hydrocarbon	0.6	1.0	Improper operation of overhead fin fan controls	Yes	No	N/A
3/1/2014	Hydrocarbon	7.8	0.7	Water boots were stuck open and drained to the degassing drum.	Yes	No	N/A
2/2/2014	Lhulmandon	2.5	1.5	The air dryer line for the instrument air feeding the boilers was frozen.	Yes		A1 (A
3/2/2014	Hydrocarbon	2.3	1.3	III V4561.	Yes	No	N/A
3/2/2014	Hydrocarbon	41.3	1.5	The seal of C-402A failed due to the extreme cold temperatures.	Yes	No	N/A
3/3/2014	Hydrocarbon	29.2	1.7	Water boots were stuck open and drained to the degassing drum.	Yes	No	N/A
3/5/2014	Hydrocarbon	17.0	1.9	The cooling water in the service water cooler was fouled.	Yes	No	N/A
3/19/2014	Hydrocarbon	0.8	3.6	Condensate pluggage in the Reboiler	Yes	No	N/A

3/20/2014	Hydrocarbon	0.3	0.5	The repairs made to C-408 did not fix the compressor.	Yes	No	N/A
3/28/2014	Hydrocarbon	9.0	4.9	The seal on the cooling water pump for C-407 falled.	Yes	No	N/A
3/30/2014	Hydrocarbon	0.7	0.5	Replacement oil filters for C-407 were not readily available.	Yes	No	N/A
3/31/2014	Hydrocarbon	2.3	0.6	The FGRU compressor needed a solenoid valve replacement.	Yes	No	N/A
4/5/2014	Hydrocarbon	4.9	2.8	A bolt on the compressor crosshead needed to be blinded from service to properly repair the leak.	Yes	No	N/A
4/25/2014	Acid Gas	0.1	0.4	SRU#1 flame scanner malfunction.	Partial	Yes	See Report
5/29/2014	Acid Gas	1.2	8.0	The condensate valve from the overhead line from the SCOT was not closed properly and allowed condensate into the K.O. Drum.	Yes	No	See Report
6/10/2014	Hydrocarbon	0.9	0.7	C-407 compressor fan blades are missing, which causes improper cooling of the compressor.	Partial	Yes	N/A
6/13/2014	Hydrocarbon	3.0	0.9	the reduction of Annulus and Reactor Riser steam at a point in time when cold feed at low rates was being introduced to the Reactor Riser with a marginal Regenerator differential pressure and high temperatures in the Regenerator caused the FCCU catalyst reversal.	Partial	Yes	N/A
6/16/2014	The tube leak on exchanger £-7 damaged the float level indic		The tube leak on exchanger E-7 damaged the float level indicator on the sweet gas knockout drum.	Yes	No	N/A	
6/27/2014	Hydrocarbon	The crude unit was placed into circulation which caused Hydrocarbon 35.7 1.2 inadequate gas supply		I .	Yes	No	N/A
4/3/2013	Hydrocarbon	Reported 1H2013	Reported 1H2013	Blisters were found on the reactor riser causing an emergency shutdown of the FCCU	Yes 6/2013	Yes	N/A

Attachment C - Flaring

P217e Emission Summary

Flare Emission Data (All Acid Gas and Tail Gas Incidents for 2013)

Flare Identification	Pollutant	Actual Emissions	Method of Determination				
	1	tons/yr	-				
Main Plant Flare	SO2	12.1	calculations for each exceedance based on engineering estimates				
Coker Flare	Coker flare does	not flare Acid Gas or Tall	Gas.				
The Old Plant Flare temporarily operated from October 9, 2013 to October 29, 2013 while the Main Plant Flare was taken out-of-service for the 201 Turnaround. During this time there were no Acid Gas or Tail Gas flaring Old Plant Flare Incidents.							

Section D - HEATERS AND BOILERS

NOx Control Plan

Frontier Refining LLC

P.O. Box 1588 • Cheyenne, WY 82003-1588

Paragraph	Attachment D - Heaters and Boilers	Comments
44	For their respective Covered Refineries, FRI and FEDRC shall each submit a detailed NOx control plan ("Control Plan") to EPA and the Applicable Intervenor for review by no later than one hundred and eighty (180) days after Date of Entry, with annual updates, covering the prior calendar year, on August 31st of each year thereafter until implementation of the Control Plan is complete. The Control Plan and its updates shall describe the achieved and anticipated progress of the NOx emissions reductions program for heaters and boilers and shall contain the following information for each heater and boiler greater than 40 mmBTU/hr that FRI and FEDRC plan to use to satisfy the requirements of Paragraphs 42, 45 and 46:	As required for the August 31 submissions, the updated Nox Control Plan is included in this section.
44a	All of the information in Appendix A;	See NOx Control Plan.
44b	Identification of the type of Qualifying Controls installed or planned with date installed or planned (including identification of the heaters and boilers to be permanently shut down);	See NOx Control Plan.
44c	To the extent limits exist or are planned, the allowable NOx emission rates (in lbs/mmBTU (HHV), with averaging period) and allowable heat input rate (in mmBTU/hr (HHV)) obtained or planned with dates obtained or planned;	See NOx Control Plan.
44d	The results of emissions tests and annual average CEMS or PEMs data (in ppmvd at 3% O2, lbs/mmBTU) conducted pursuant to Paragraph 47 and tons per year; and	No annual emission tests or CEMs or PEMs data was required in this reporting period.
44e	The amount in tons per year applied or to be applied toward satisfying Paragraph 42.	See NOx Control Plan.
217a	NOx emissions in tons per year for each heater and boiler greater than 40 mmBTU/hr maximum fired duty;	See emission summary included in this section.
217b	NOx emissions in tons per year as a sum for all heaters and boilers less than 40 mmBTU/hr maximum fired duty;	See emission summary included in this section.
217c	SO2, CO and PM emissions in tons per year as a sum for all heaters and boilers;	See emission summary included in this section.
218a	for operating units emissions limits that are required by this Consent Decree and monitored with CEMS, for each CEMS:	The NOx CEMS was certified 3/6/2014. The CEM data for Nox analyzer and the H2S analyzer on the fuel gas are attached.

FR NOx Control Plan - 2013 Update

Source	Maximum or Allowable Annual Heat Input Capacity	2003 Utilization Rate	2903 NOx Emission Rate	2003 NOx Emissions	2004 Utilization Rate	2004 NOx Emission Rate	2004 NOx Emissions	2003 - 2004 Average NOx Emissions	Type of data used to derive emission estimate	Qualifying	y Controls	Amount Applie to Paragraph 4 Requirement
	mm8TUffer (HHV)	mmSTUffer (146V)	DimmBTU	tons/yr	mmBTUfter (HHV)	th/mmBTU	tons/yr	tons/yr		Туре	date	
R												
21	200	148.5	0.031	23.4	162.7	0.031	21.43	22.4	stack test	ULNB*	Pre-2003	0
23	40.1	33.6	0.043	14.39	32.6	0.043	5.42	9.9	stack test			
34a	186.9	119.5	0.22	113.02	107.1	0.22	138.01	125.5	stack test	Shutdown	12/17/13	125.5
50	61.7	35.7	0.03	4.88	53.4	0.03	6.62	5.7	stack test			
58	177.6	138.7	0.078	44.41	148.9	0.078	52.8	48.6	CEMS			
59	177.6	140,3	0,081	53,79	149.0	0.081	58,24	58.0	CEMS			
Total	843.9			253.69			282.52	268.1				125.5
EDRC		400										
B-105	361.00	121.2	0.2359	125.2	133.1	0,2488	143.9	134.6	AP-42			
B-107	233.00	114.6	0.2000	100.4	107.3	0.2000	94.0	97.2	Stack Test	, transcription and discounter		
B-2306	184.00	136.8	0.0530	31.8	145.9	0.0530	33.9	32.8	Stack Test			
B-301	175.10	169.9	0.3090	229.9	163.0	0.3090	220.6	225.3	Stack Test	Shutdown	03/31/08	225.3
B-304	170.40	147.5	0.3090	199.6	153.9	0.3090	208.3	204.0	Stack Test	Shutdown	03/31/08	204.0
B-109	148.40	85.4	0.0720	26.9	85.5	0.0720	27.0	26.9	Stack Test			
B-2601	97.00	68.2	0.1200	35.8	72.9	0.1200	38.3	37.1	Permit Limit	Shutdown	12/31/12	
B-2104	86.53	31.8	0.0841	11.7	43.4	0.0879	16.7	14.2	AP-42			
8-2901	79.00	25.7	0.0855	9.6	23.6	0.0889	9.2	9.4	AP-42			
8-2401	74.70	74.2	0.3090	100.4	85.9	0.3090	116.3	108.3	Stack Test	Shutdown	03/31/08	108.3
B-3501	73.70	60.7	0.0100	2.7	65.9	0.0100	2.9	28	Permit Limit	SCR	02/28/11	
B-1002	72.50	37.1	0.0830	13.5	34.8	0.0878	13.4	13.4	AP-42	ULNB**	11/12/09	0.0
B-2106	72.50	56.6	0.0842	20.9	55.3	0.0878	21.3	21.1	AP-42			
B-1001	70.00	45.9	0.0829	16.7	48.5	0.0879	18.7	17.7	AP-42			
B-140	69.00	29.0	0.0851	10.8	21.7	0.0880	8.4	9.6	AP-42			
8-2105	59.27	29.4	0.0841	10.8	34.8	0.0877	13.4	12.1	AP-42			
B-2607	57.50	25.6	0.0841	9.4	23.2	0 0885	9.0	9.2	AP-42	Shutdown	12/31/12	
B-2503	43.00	28.8	0.0839	10.6	26.9	0.0881	10.4	10.5	AP-42			
B-2001	54.00	31.7	0.0840	11.7	35.2	0.0885	13.6	12.7	AP-42			
B-3401	50.00	34.0	0.0669	10.0	33.1	0.0689	9.7	9.8	Stack Test			
B-2304	48.00	10.4	0.0823	3.8	10.2	0.0893	4.0	3.9	AP-42			
B-2006	46.50	33.3	0.0841	12.3	32.7	0.0885	12.7	12.5	AP-42			
B-2802	45.40	38.3	0.0849	14.2	39.2	0.0889	15.3	14.7	AP-42			
otal	2,370,50			1,018.7		The second secon	1,060.7	1,039,7		-	The same of the sa	537.6

Paragraph 42 NOx Reductions - FEDRC & FRI Combined							
Total Required NOx Reductions by December 31, 2013	649 tpy	Reduction achieved by December 31, 2009	537.6 tpy				
Two-Thirds Reduction by December 31, 2009	432 tpy	Reduction planned by December 31, 2013	663.1 tpy				
	Paragraph 48 NOx Control Requ	rements - FR8					
30% of meximum heat capacity	253.17 mmBTU/hr						
Control already schieved or planned	386.9 mmBTU/hr						
Amount left to achieve (undefined)	0 mmBTU/hr						

Attachment D - HEATERS & BOILERS

P217a - Emission Summary Each Heaters & Bollers >40 MMBTU/hr

Unit	Size	NOx Emissions	Method of Determination
	MMBtu/hr	tons/yr	
21	202	18.45	Source Test
23	54	2.91	Source Test
34A	187	79.22	Source Test
50	62	12.62	Source Test
58	178	29.58	CEMS Data
59	178	35.56	CEMS Data
83*	200	9.83	CEMS Data

^{*}Boiler 83 was is not included in the CD Appendix C, but is a heater at the source >40 MMBTU/hr

P217b - Emission Summary All Heaters & Boilers <40 MM BTU/hr

	2012 Actual Emissions	Method of
1	tons/yr	Determination
NOx	96.26	Emission Factor

P217C - Emission Summary All Heaters & Bollers

	2012 Actual	Method of
	Emissions	Determination
	tons/yr	
PM	11.05	Emission Factors
SO2	14.27	H2S CEM
СО	156.03	Emission Factors

DEPARTMENT OF ENVIRONMENTAL QUALITY AIR QUALITY DIVISION CONTINUOUS EMISSION MONITORING REPORT

FORM A

I. GENERAL INFORMATION

- A. Facility Name: FRONTIER REFINING LLC
- B. Process Unit/Pollutant Monitored: H₂S MONITOR #3 AMINE TREATER (ALL FUEL GAS PROCESSING UNITS)
- C. Applicable Permit Number or Regulation: 3-0-149-2
- D. Applicable Emission Limit: 162 ppm H.S (0.1 gr/scf) 3-hour average

II. MONITOR INFORMATION

- A. Date of Original Monitor Installation: December 1978 (Replaced October 29, 2013)
- B. Date of Latest Monitor Certification: December 31, 2013
- C. Pollutant/Opacity Monitor
 - 1. Manufacturer: ABB Inc.
 - 2. Model Number: PGC5000
 - 3. Serial Number Main Chassis: 867521
 - 4. Basis of Measurement (If Applicable Wet or Dry): Wet
 - 5. Instrument Span, Range Value (Specify Units): 0 320 ppm H.S

D. Diluent Monitor

- 1. Type of Monitor: O₂ or CO₂ (circle one): NONE
- 2 Manufacturer:
- 3. Model Number:
- 4. Serial Number Main Chassis
- 5. Basis of Measurement (If Applicable Wet or Dry):
- 6. Instrument Span, Range Value (Specify Units):

E. Flow Monitor

- 1. Type of Instrument (i.e. S-type Pitot Tube): NONE
- 2. Manufacturer:
- 3. Model Number:__
- 4. Serial Number Main Chassis:

F. Quality Assurance Data

- 1. QA Plan Date: January 18, 2013
- 2. QA Plan Approval Date: August 29, 2013

III. Operating/Monitoring Data

A. Quarter: 1 Year: 2014

B Total Hours in Reporting Period: 2160

C. Hours Unit Operated During the Reporting Period: 2160

Note: Include <u>all</u> unit operating time for the quarter including operating time associated with Startup/Shutdown and Chapter 1 Section 5 (Emergency/Abnormal) Operations. Report time in hours to one decimal place, i.e. 1902.8.

IV. Quarterly Audits/Monitoring System Modifications

A. Quarterly Audits
Type Audit: CGA

Date Conducted Pass 3/24/2014 YES

Diluent Monitor

Pollutant/Opacity Monitor:

B. Equipment Replaced During Reporting Period: Replaced Compressed Air Bottle.

Note: Only equipment replacements or modifications to the system that could affect the ability of the continuous monitoring system to comply with the associated Performance Specification shall be reported.

V. Report Contact

A. Name: David Weeks, Environmental Engineer

B. Phone Number: (307) 771-8827

EXCESS EMISSION SUMMARY REPORT Fuel Gas H2S CEMS 3-hr average ppm = 162 ppm

FORM B

Emission Data Summary		CMS Performance Report			
I. Duration of Excess Emission in Reporting Perk	od Due to:	I. CMS Downtime in Reporting Period Due to:			
A. Startup/Shutdown	25.0	A. Monitor Equipment Malfunction	2.0		
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	0.0		
C. Process Problem	11.0	C. Quality Assurance Calibration	1.0		
D. Other Known Causes	0.0	D. Other Known Causes	190.0		
E. Unknown Causes	0.0	E. Unknown Causes	0.0		
II. Total Duration of Excess Emission	36.0	II. Total CMS Downtime	193.0		
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	1.7%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	8.9%		

Total time of excess emission events due to emergency/abnormal operations: ______. NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2. Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)

1Q14 Fuel Gas CEMS

H₂S ppm 3-Hour Rolling Average

Form C - Excess Summary

Fuel Gas H2S Excess Emissions Summary

Frontier Refining LLC
H2S ppm 3-Hr Rolling Excess Emissions for 1/1/2014 thru 3/31/2014

Resson	Duration
H2S ppm 3-Hour Rolling Average Emission Exceedance - Lost all Bollers - All Units Shutdown	9 hours
H2S PPM 3-Hour Rolling Average Exceedance - Start-Up Issues	16 hours
Process Upset - Amine Unit - High Regen level and slumped Reboiler	3 hours
Sour Water Stripper (SWS) shutdown due to the loss of Boller #3	2 hours
SRU #2 shut down three times during the shift, the last shutdown lasted three hours due to the stackmatch would not light. This resulted in high H2S in the fuel gas.	6 hours
Total duration of H2S ppm 3-Hr Rolling excess emissions	36 hours
Total operating time	2160 hours
Operating time with excess emissions	1.7%

Fuel Gas H2S Excess Emissions

Frontier Refining LLC H2S ppm 3-Hr Rolling Excess Emissions for 1/1/2014 thru 3/31/2014

Parameter	Start	End	Duration	Value	Min	Max	Limit	Reason	Action
H2S ppm 3-Hr Rolling	1/23/2014 8:00 PM	9:59 PM	2 hours	180.0	174.5	185.4	163	Sour Water Stripper (SWS) shutdown due to the loss of Boiler #3	Restarted SWS.
H2S ppm 3-Hr Rolling	1/31/2014 10:00 AM	3:59 PM	6 hours	291.7	234.9	320.0	163	SRU #2 shut down three times during the shift, the last shutdown lasted three hours due to the stackmatch would not light. This resulted in high H2S in the fuel gas.	Reduced rate in the plant for sulfur containment, I&E worked on the stackmatch.
H2S ppm 3-Hr Rolling	2/5/2014 10:00 AM	6:59 PM	9 hours	299.8	200.2	320,0	163	H2S ppm 3-Hour Rolling Average Emission Exceedance - Lost all Boilers - All Units Shutdown	Units Shutdown
H2S ppm 3-Hr Rolling	2/8/2014 12:00 AM	11:59 AM	12 hours	298.0	226.6	320.0	163	H2S PPM 3-Hour Rolling Average Exceedance - Start-Up issues	Adjusted Unit Operations
H2S ppm 3-Hr Rolling	2/8/2014 3:00 PM	6:59 PM	4 hours	258.9	245.7	269.5	163	H2S PPM 3-Hour Rolling Average Exceedance - Start-Up Issues	Adjusted Unit Operations
H2S ppm 3-Hr Rolling	3/19/2014 4:00 AM	6:59 AM	3 hours	217.7	191.9	259.5	163	Process Upset - Amine Unit - High Regen lével and slumped Reboiler	Regained control of Regen level and Reboiler

Total duration

36 hours

1Q14 Fuel Gas CEMS

 H_2Sppm

Form D - Downtime Summary

Fuel Gas H2S CEMS Downtime Summary

Frontier Refining LLC H2S ppm CEMS Downtime for 1/1/2014 thru 3/31/2014

Reason	Duration
Cylinder Ges Audit (CGA)	1 hour
Failed Morning H2S Span Calibration Check - Low Instrument Air Pressure	25 hours
Failed Morning H2S Span Calibration Check - Low instrument air pressure had caused analyzer to shut down	3 hours
Falled Morning H2S Span Calibration Check; Falled Manual Calibration	2 hours
H2S Analyzer Malfunction - Low Instrument Air Pressure	15 hours
Maintenance - Analyzer	1 hour
Sample System Maifunction - Low Instrument Air Pressure	146 hours
Total duration of H2S ppm CEMS downtime	193 hours
Total operating time	2160 hours
Operating time with CEMS downtime	8.9%

Fuel Gas H2S CEMS Downtime

Frontier Refining LLC H2S ppm CEMS Downtime for 1/1/2014 thru 3/31/2014

Parameter Parame	Start	End	Duration	Reason	Action
H2S ppm	1/17/2014 10:00 AM	10:59 AM	1 hour	Maintenance - Analyzer	Ran validations and calibrations on fuel gas analyzer
H2S ppm	2/5/2014 7:00 AM	7:59 AM	1 hour	Sample System Malfunction - Low instrument Air Pressure	Self Corrected - instrument Air Pressure increased
H2S ppm	2/5/2014 9:00 PM	9:59 PM	1 hour	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/8/2014 12:00 PM	12:59 PM	1 hour	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/12/2014 4:00 PM	4:59 PM	1 hour	Sample System Melfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/13/2014 10:00 AM	10:59 AM	1 hour	Semple System Maifunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/13/2014 2:00 PM	2:59 PM	1 hour	Sample System Malfunction - Low instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/13/2014 5:00 PM	7:59 PM	3 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - instrument Air Pressure Increased
H2S ppm	2/13/2014 9:00 PM	11:59 PM	3 hours	Sample System Maifunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/14/2014 1:00 AM	1:59 AM	1 hour	Sample System Maifunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/14/2014 8:00 AM	10:59 AM	3 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/17/2014 2:00 PM	2:59 PM	1 hour	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/18/2014 3:00 AM	4: 59 AM	2 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/18/2014 8:00 AM	8:59 AM	1 hour	Sample System Melfunction - Low instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/18/2014 6:00 PM	10:59 PM	5 hours	Sample System Matfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/19/2014 2:00 AM	5:59 AM	4 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/19/2014 6:00 AM	8:59 AM	3 hours	Failed Morning H2S Span Calibration Check - Low instrument air pressure had caused analyzer to shut down	When instrument air pressure had returned to normal, another validation check was ran. Analyzer passed span check.

Parameter	Start	End	Duration	Reason	Action
H2S ppm	2/21/2014 11:00 AM	1:59 PM	3 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/22/2014 4:00 PM	4:59 PM	1 hour	Sample System Mailunction - Low instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/23/2014 9:00 PM	10:59 PM	2 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/25/2014 2:00 AM	5:59 AM	4 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure increased
H2S ppm	2/25/2014 7:00 AM	8:59 AM	2 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure increased
H2S ppm	2/25/2014 3:00 PM	11:59 PM	9 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/26/2014 12:00 AM	12:59 AM	1 hour	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/26/2014 2:00 AM	3:59 AM	2 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/26/2014 7:00 AM	7:59 AM	1 hour	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/26/2014 2:00 PM	10:59 PM	9 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/27/2014 9:00 AM	9:59 AM	1 hour	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure increased
H2S ppm	2/27/2014 11:00 AM	11:59 AM	1 hour	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/27/2014 4:00 PM	4:59 PM	1 hour	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/27/2014 6:00 PM	8:59 PM	3 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/27/2014 11:00 PM	11:59 PM	1 hour	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/28/2014 7:00 AM	4:59 PM	10 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/28/2014 7:00 PM	8:59 PM	2 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	2/28/2014 10:00 PM	11:59 PM	2 hours	Sample System Maifunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	3/1/2014 12:00 AM	1:59 AM	2 hours	Sample System Matfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	3/1/2014 3:00 AM	5:59 AM	3 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased

Parameter	Start	End	Duration	Reason	Action
H2S ppm	3/1/2014 6:00 AM	12:59 PM	7 hours	Failed Morning H2S Span Calibration Check - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	3/1/2014 1:00 PM	1:59 PM	1 hour	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	3/1/2014 2:00 PM	11:59 PM	10 hours	H2S Analyzer Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure increased
H2S ppm	3/2/2014 12:00 AM	1:59 AM	2 hours	H2S Analyzer Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	3/2/2014 2:00 AM	2:59 AM	1 hour	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	3/2/2014 3:00 AM	5: 59 AM	3 hours	H2S Analyzer Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	3/5/2014 5:00 AM	5:59 AM	1 hour	Sample System Malfunction - Low instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	3/5/2014 8:00 AM	9:59 AM	2 hours	Failed Morning H2S Span Calibration Check; Failed Manual Calibration	Ran an Additional Manual Calibration
H2S ppm	3/7/2014 6:00 AM	6:59 AM	1 hour	Failed Morning H2S Span Calibration Check - Low Instrument Air Pressure	Ran Manual Calibration
H2S ppm	3/7/2014 3:00 PM	8:59 PM	6 hours	Sample System Malfunction - Low instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	3/7/2014 10:00 PM	11:59 PM	2 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	3/8/2014 12:00 AM	5:59 AM	6 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	3/8/2014 7:00 AM	8:59 AM	2 hours	Failed Morning H2S Span Calibration Check - Low Instrument Air Pressure	Ran Manual Celibration
H2S ppm	3/8/2014 12:00 PM	2:59 PM	3 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	3/8/2014 7:00 PM	11:59 PM	5 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	3/9/2014 12:00 AM	3:59 AM	4 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	3/9/2014 6:00 AM	5:59 PM	12 hours	Falled Morning H2S Span Calibration Check - Low Instrument Air Pressure	Ran Manual Calibration
H2S ppm	3/9/2014 6:00 PM	11:59 PM	6 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased

Parameter	Start	End	Duration	Reason	Action
H2S ppm	3/10/2014 2:00 AM	5:59 AM	4 hours	Sample System Maifunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	3/10/2014 8:00 AM	3:59 PM	8 hours	Sample System Matfunction - Low instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	3/10/2014 6:00 PM	7:59 PM	2 hours	Sample System Maifunction - Low Instrument Air Pressure	Self Corrected - instrument Air Pressure Increased
H2S ppm	3/10/2014 10:00 PM	11:59 PM	2 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	3/11/2014 12:00 AM	5:59 AM	6 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	3/11/2014 6:00 AM	8:59 AM	3 hours	Failed Moming H2S Span Calibration Check - Low Instrument Air Pressure	Ran Manual Calibration
H2S ppm	3/24/2014 12:00 PM	12:59 PM	1 hour	Cylinder Gas Audit (CGA)	Performed H2S CGA

1Q14 Fuel Gas

 H_2Sppm

Monthly Average Summary

Frontier Refining LLC Cheyenne, WY Fuel Gas H2S Monthly Average - Summary 2014 Q1

Month	H2S ppm Monthly
January 2014	20.2
February 2014	25.9
March 2014	8.2

Data Sheet for Fuel Gas CEM System Cylinder Gas Audit

1. Date Audit Commenced: 24-Mar-14 Time Audit Commenced: 12:45PM

2. Audit Gases Used for CGA (All gases to be Protocol 1 Certified):

Acceptable Audit Gas Ranges	Cylinder Number and Expiration Date			+/- of Audit Gas Range
H ₂ S Low:	SG9200120	70.00	DDM	45.000
100 - 150 PPM	26-Oct-14	76.38 PPM	15.28%	
H₂S Mid:	CC3831	450.00	-	24 2224
250 - 300 PPM	23-Mar-13	159.30 PPM		31.86%

3. CEM System Response:

	Low-Span	H ₂ S PPM	Mid-Span H₂S PPM		
	Analyzer	CISCO	Analyzer	Cisco	
Run 1	69.21	N/A	155.90	N/A	
Run 2	70.07	N/A	156.94	N/A	
Run 3	70.20	N/A	157.93	N/A	
Avg. (d _m)	69.83	#DIV/0!	156.92	#DIV/0!	
A	8.58	#DIV/01	1.49	#DIV/01	
Pass?	Yes	#DIV/0!	Yes	#DIV/01	

4. Signature of Technician(s) performing CGA:

Vatt Hobbs, Kevin Marschner and/or Tad Milliken

Calculation of A:

 $A = (d_m - c_a) / c_a \times 100$

A must be +/-15% to pass.

where:

A = accuracy of CEM d_m = average of reponses c_a = certified audit value of gas

DEPARTMENT OF ENVIRONMENTAL QUALITY AIR QUALITY DIVISION CONTINUOUS EMISSION MONITORING REPORT

FORM A

I. GENERAL INFORMATION

- A. Facility Name: FRONTIER REFINING LLC
- B. Process Unit/Pollutant Monitored: H₂S MONITOR #3 AMINE TREATER (ALL FUEL GAS PROCESSING UNITS)
- C. Applicable Permit Number or Regulation: 3-0-149-2
- D. Applicable Emission Limit: 162 ppm H.S (0.1 gr/scf) 3-hour average

II. MONITOR INFORMATION

- A. Date of Original Monitor Installation: December 1978 (Replaced October 29, 2013)
- B. Date of Latest Monitor Certification: December 31, 2013
- C. Pollutant/Opacity Monitor
 - 1. Manufacturer: ABB Inc.
 - 2. Model Number: PGC5000
 - 3. Serial Number Main Chassis: 867521
 - 4. Basis of Measurement (If Applicable Wet or Dry): Wet
 - 5. Instrument Span, Range Value (Specify Units): 0 320 ppm H₂S

D. Diluent Monitor

- 1. Type of Monitor: O₂ or CO₂ (circle one): NONE
- 2 Manufacturer:
- 3. Model Number:
- 4. Serial Number Main Chassis
- 5. Basis of Measurement (If Applicable Wet or Dry):
- 6. Instrument Span, Range Value (Specify Units):

B. Flow Monitor

- 1. Type of Instrument (i.e. S-type Pitot Tube): NONE
- 2. Manufacturer:
- 3. Model Number:
- 4. Serial Number Main Chassis:

F. Quality Assurance Data

- 1. OA Plan Date: January 18, 2013
- 2. OA Plan Approval Date: August 29, 2013

III. Operating/Monitoring Data

A. Quarter: 2

Year: 2014

B Total Hours in Reporting Period: 2184

C. Hours Unit Operated During the Reporting Period: 2184

Note: Include <u>all</u> unit operating time for the quarter including operating time associated with Startup/Shutdown and Chapter 1 Section 5 (Emergency/Abnormal) Operations. Report time in hours to one decimal place, i.e. 1902.8.

IV. Quarterly Audits/Monitoring System Modifications

A. Quarterly Audits
Type Audit: CGA

Date Conducted

Pass

Pollutant/Opacity Monitor:

6/3/2014

YES

Diluent Monitor

B. Equipment Replaced During Reporting Period: <u>Installed new dedicated Instrument Air</u> line.

Note: Only equipment replacements or modifications to the system that could affect the ability of the continuous monitoring system to comply with the associated Performance Specification shall be reported.

V. Report Contact

A. Name: <u>David Weeks, Environmental Engineer</u>

B. Phone Number: (307) 771-8827

EXCESS EMISSION SUMMARY REPORT Fuel Gas H2S CEMS 3-hr average ppm = 162 ppm

FORM B

Emission Data Summary	-	CMS Performance Report		
I. Duration of Excess Emission in Reporting Perio	d Due to:	I. CMS Downtime in Reporting Period Due to:		
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	2.0	
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	18.0	
C. Process Problem	11.0	C. Quality Assurance Calibration	0.0	
D. Other Known Causes	0.0	D. Other Known Causes	2.0	
E. Unknown Causes	0.0	E. Unknown Causes	0.0	
II. Total Duration of Excess Emission	11.0	II. Total CMS Downtime	22.0	
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.5%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	1.0%	

Total time of excess emission events due to emergency/abnormal operations: _______.

NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2. Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)

Fuel Gas H2S Excess Emissions Summary

Frontier Refining LLC
H2S ppm 3-Hr Rolling Excess Emissions for 4/1/2014 thru 6/30/2014

Reason	Duration
Amine treater had a couple upsets during the day which resulted in high H2S in the fuel gas.	2 hours
High H2S in fuel gas. There was low level in #3 amine. The regenerator lost flow from #3 amine.	3 hours
Process Upset - Result of Prior Upsets caused by Boilers #1 & #2 Shutdown	4 hours
Treater bounced causing high H2S levels in the fuel gas.	2 hours
Total duration of H2S ppm 3-Hr Rolling excess emissions	11 hours
Total operating time	2184 hours
Operating time with excess emissions	0.5%

Comment: Form C - Excess Emissions Summary

Fuel Gas H2S Excess Emissions

Frontier Refining LLC
H2S ppm 3-Hr Rolling Excess Emissions for 4/1/2014 thru 6/30/2014

Parameter	Start	End	Duration	Value	Min	Max	Limit	Reason	Action
H2S ppm 3-Hr Rolling	4/1/2014 8:00 AM	10:59 AM	3 hours	183.9	171.3	207.2	163	High H2S in fuel gas. There was low level in #3 amine. The regenerator lost flow from #3 amine.	Operators transferred amine from #4 amine sump to #3 amine to get the level back.
H2S ppm 3-Hr Rolling	4/1/2014 7:00 PM	8:59 PM	2 hours	187.8	179.4	195.8	163	Treater bounced causing high H2S levels in the fuel gas.	Adjusted Process.
H2S ppm 3-Hr Rolling	4/2/2014 1:00 PM	2:59 PM	2 hours	214.7	206.9	222.4	163	Amine treater had a couple upsets during the day which resulted in high H2S in the fuel gas.	Operators back flushed coolers, steam was added, and the flow increased.
H2S ppm 3-Hr Rolling	6/14/2014 12:00 AM	3:59 AM	4 hours	220.0	167.9	269.3	163	Process Upset - Result of Prior Upsets caused by Boilers #1 & #2 Shutdown	Adjusted Unit Operation

Total duration

11 hours

Comment: Form C - Excess Emissions Summary

Fuel Gas H2S CEMS Downtime Summary Frontier Refining LLC H2S ppm CEMS Downtime for 4/1/2014 thru 6/30/2014

Reason	Duration
Fuel gas analyzer failed validation due to low instrument air pressure.	2 hours
Maintenance - Shut down H2S analyzer to Install a new dedicated air line.	2 hours
Sample System Malfunction - Low instrument Air Pressure	18 hours
Total duration of H2S ppm CEMS downtime	22 hours
Total operating time	2184 hours
Operating time with CEMS downtime	1.0%

Comment: Form D - Downtime Summary

Fuel Gas H2S CEMS Downtime

Frontier Refining LLC H2S ppm CEMS Downtime for 4/1/2014 thru 6/30/2014

Parameter	Start	End	Duration	Reason	Action
H2S ppm	4/7/2014 6:00 AM	9:59 AM	4 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	4/11/2014 9:00 AM	10:59 AM	2 hours	Sample System Malfunction - Low instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	4/14/2014 3:00 AM	4:59 AM	2 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	4/17/2014 4:00 AM	4:59 AM	1 hour	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air pressure increased.
H2S ppm	4/17/2014 5:00 AM	8:59 AM	2 hours	Fuel gas analyzer failed validation due to low instrument air pressure.	Ran calibration check. Instrument Air pressure increased.
H2S ppm	4/23/2014 11:00 AM	11:59 AM	1 hour	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	5/3/2014 5:00 PM	5:59 PM	1 hour	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	5/22/2014 6:00 AM	7:59 AM	2 hours	Maintenance - Shut down H2S analyzer to install a new dedicated air line.	New dedicated instrument Air line installed to help redure Low instrument Air pressure issues.
H2S ppm	6/3/2014 12:00 PM	12:59 PM	1 hour	Semple System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	6/10/2014 2:00 PM	3:59 PM	2 hours	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	6/20/2014 1:00 PM	1:59 PM	1 hour	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	6/21/2014 1:00 PM	1:59 PM	1 hour	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	6/21/2014 3:00 PM	3:59 PM	1 hour	Sample System Malfunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased
H2S ppm	6/22/2014 1:00 AM	1:59 AM	1 hour	Sample System Mailunction - Low Instrument Air Pressure	Self Corrected - Instrument Air Pressure Increased

Total duration 22 hours

Comment: Form D - Downtime Summary

Data Sheet for Fuel Gas CEM System Cylinder Gas Audit

1. Date Audit Commenced: 3-Jun-14 Time Audit Commenced: 1:00 PM

2. Audit Gases Used for CGA (All gases to be Protocol 1 Certified):

Acceptable Audit Gas Ranges	Cylinder Number and Expiration Date	Audit Gas Concentration	+/- of Audit Gas Range	
H ₂ S Low:	SG9200120	70.00	0014	45.0004
4 00 - 150 PPM	26-Oct-14	76.38	PPM	15.28%
H ₂ S Mid:	CC3831	450.00	5554	24 900
250 300 PPM	29-Apr-15	159.00	PPM	31.80%

3. CEM System Response:

	Low-Span	H ₂ S PPM	Mid-Span H₂S PPM		
	Analyzer	Cisco	Analyzer	Cisco	
Run 1	67.89		151.03		
Run 2	68.81		151.38		
Run 3	68.48		151.58		
Avg. (d _m)	68.39	#DIV/0I	151.32	#DIV/0!	
Α	10.46	#DIV/0!	4.83	#DIV/0!	
Pass?	Yes	#DIV/0!	Yes	#DIV/0!	

4.	Signature	of Technician(s)	performing CGA:
----	-----------	------------------	-----------------

Matt Hobbs, Kevin Marschner and/or Tad Milliken

Calculation of A:

 $A = (d_m - c_a) / c_a \times 100$

A must be +/-15% to pass.

where:

A = accuracy of CEM

d_m = average of reponses

c_a = certified audit value of gas



CERTIFICATE OF ANALYSIS Grade of Product: EPA Protocol

Airgas, Inc. 800 Union Landing Road Chinaminson, NJ 08077 (856) 829-7878 Fax: (856) 829-6576 www.airgas.com

Part Number:

E02NI99E15A0160

CC3831

Cylinder Volume:

Reference Number: 82-124432208-1

Cylinder Number

144.4 CF

Laboratory.

ASG - Riverton - NJ

Cylinder Pressure:

2015 PSIG

PGVP Number:

B52014

Valve Outlet:

330

Gas Code:

H2S.BALN

Certification Date:

Apr 29, 2014

Expiration Date: Apr 29, 2015

Certification performed in accordance with "EPA Traceability Protocol for Assay and Certification of Geseous Celibration Standards (May 2012)" document EPA 600/R-12/531, using the assay procedures listed. Analytical Methodology does not require correction for analytical interference. This cylinder has a total analytical uncertainty as stated below with a confidence level of 95%. There are no significant impurities which affect the use of this celibration mixture. All concentrations are on a volume/volume basis unless otherwise noted.

Do Not Use This Cylinder below 100 paig, i.e. 0,7 megapascals **ANALYTICAL RESULTS** Component Actual Requested Protocol **Total Relative** Assay Concentration Concentration Method Uncertainty Dates HYDROGEN SULFIDE 165.0 PPM 159.0 PPM +/-2.0% 04/29/2014 G1 **NITROGEN** Balance CALIBRATION STANDARDS

Туре	Lot ID	Cylinder No	Concentration	Uncertainty	Expiration Date				
GMIS	12319	CC158744	199.2 PPM HYDROGEN SULFIDE/NITROGEN	+4 1.1%	Jan 25, 2016				
PRM	12323	D249639	300.4 PPM HYDROGEN SULFIDE/NITROGEN	+/- 1.0%	Jul 18, 2016				
The SRM	. PRM or RGM	noted above is only in refer	rence to the GMIS used in the assay and not part of the analy:	sis.					

ANALYTICAL EQUIPMENT

Instrument/Make/Model

Analytical Principle

Last Multipoint Calibration

Ametek 9000 RM

Notes:

NDUV

Apr 29, 2014

Triad Data Available Upon Request

proved for Release

1014

DEPARTMENT OF ENVIRONMENTAL QUALITY AIR QUALITY DIVISION CONTINUOUS EMISSION MONITORING REPORT

FORM A

I. GENERAL INFORMATION

- A. Facility Name: FRONTIER REFINING LLC
- B. Process Unit/Pollutant Monitored: NOx MONITOR CRUDE CHARGE HEATER
- C. Applicable Permit Number or Regulation: Consent Decree
- D. Applicable Emission Limit: 0.031 lb/mmbtu (1-hr average): 6.3 lb/hr (1-hr average)

II. MONITOR INFORMATION

- A. Date of Original Monitor Installation: <u>December 20, 2013 (New Installation)</u>
- B. Date of Latest Monitor Certification: March 6, 2014
- C. Pollutant/Opacity Monitor
 - 1. Manufacturer: Teledyne Advanced Pollution Instrumentation
 - 2. Model Number: T200H/M
 - 3. Serial Number Main Chassis: 154
 - 4. Basis of Measurement (If Applicable Wet or Dry): Dry
 - 5. Instrument Span, Range Value (Specify Units): <u>0 100 ppm NO</u>,

D. Diluent Monitor

- 1. Type of Monitor: O2
- 2. Manufacturer: Teledyne Advanced Pollution Instrumentation
- 3. Model Number: T200H/M
- 4. Serial Number Main Chassis: 154
- 5. Basis of Measurement (If Applicable Wet or Dry): Dry
- 6. Instrument Span, Range Value (Specify Units): 0-25 percent (%)

E. Flow Monitor

- 1. Type of Instrument: Microprocessor Based Delta P Pressure "Smart" Transmitter
- 2. Manufacturer: Air Monitor Corporation
- 3. Model Number: Veltron II
- 4. Serial Number Main Chassis: 81983A

Flow Monitor Probe

- 1. Type of Instrument (i.e. S-type Pitot Tube): Pitot Traverse
- 2. Manufacturer: Air Monitor Corporation
- 3. Model Number: Drawing No. W81983AA
- 4. Serial Number Main Chassis: 81983

F. Quality Assurance Data

- 1. QA Plan Date: To be Submitted
- 2. OA Plan Approval Date:

III. Operating/Monitoring Data

A. Quarter: 1 Year: 2014

B Total Hours in Reporting Period: 2160

C. Hours Unit Operated During the Reporting Period: 612 (Hours of Operation after Linearity Testing completed)

Note: Include <u>all</u> unit operating time for the quarter including operating time associated with Startup/Shutdown and Chapter 1 Section 5 (Emergency/Abnormal) Operations. Report time in hours to one decimal place, i.e. 1902.8.

IV. Quarterly Audits/Monitoring System Modifications

A. Quarterly Audits

Type Audit: RATA (Including 7-Day Drift Test (January 21, 2014 - January 27, 2014))

		Date Conducted	Pass	
	Pollutant/Opacity Monitor:	3/4/2014	Yes	
	Diluent Monitor	3/4/2014	Yes	
В.	Quarterly Audits			
	Type Audit: Linearity Test			
		Date Conducted	Pass	
	Pollutant/Opacity Monitor:	3/6/2014	Yes	
	Diluent Monitor	3/6/2014	Yes	

Note: A copy of the quarterly audits shall be included with the corresponding quarterly excess emission report.

B. Equipment Replaced During Reporting Period: New Flow, NO₂ and O₃ CEMS installation on December 20, 2013; Changed O₂ Calibration Bottle.

Note: Only equipment replacements or modifications to the system that could affect the ability of the continuous monitoring system to comply with the associated Performance Specification shall be reported.

V. Report Contact

A. Name: David Weeks, Environmental Engineer

B. Phone Number: (307) 771-8827

EXCESS EMISSION SUMMARY REPORT Crude Charge Heater NO_x (lb/mmbtu) CEMS 1-hr average = 0.031 lb/mmbtu

FORM B

Emission Data Summary (12-hour average ppm)		CMS Performance Report		
I. Duration of Excess Emission in Reporting Per	iod Due to:	I. CMS Downtime in Reporting Period Due to:	7	
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	1.0	
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	0.0	
C. Process Problem	1.0	C. Quality Assurance Calibration	0.0	
D. Other Known Causes	0.0	D. Other Known Causes	0.0	
B. Unknown Causes	0.0	E. Unknown Causes	0.0	
II. Total Duration of Excess Emission	1.0	II. Total CMS Downtime	1.0	
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.2%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	0.2%	

Total time of excess emission events due to emergency/abnormal operations: __0_. NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2. Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)
- 4. New CEMS installation on December 20, 2013. Data not valid until March 6, 2014 after 7-Day Drift Test, RATA and Linearity Test was successfully completed.

1Q14 Crude Charge Heater CEMS

NOx lb/mmbtu (1-Hour)

Form C - Excess Emissions Summary

_	No.	Start Time	End Time	Hours	Reason	Action	
	1	3/22/2014 11:00:00 AM	3/22/2014 12:00:00 PM	1	Emission Exceedance - NO _x lb/mmbtu - High Excess O ₂	Adjusted Excess O ₂	
Total Periods Excess Emissions			1				

1Q14 Crude Charge Heater CEMS Form D - Monitor Downtime Summary

NOx lb/mmbtu (1-Hour)

No.	Start Time	End Time	Hours	Reason	Action
1	3/21/2014 6:00:00 AM	3/21/2014 7:00:00 AM	1	Failed Morning O2 Span Calibration Check	Ran Manual Calibration
	Total House 1	Amitor I Ingvailable	à		

EXCESS EMISSION SUMMARY REPORT Crude Charge Heater NO_X (lb/hr) CEMS 1-hr average = 6.3 lb/hr

FORM B

Emission Data Summary (lb/	hr)	CMS Performance Report			
I. Duration of Excess Emission in Reporting 1	Period Due to:	I. CMS Downtime in Reporting Period Due to:			
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	51.0		
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	0.0		
C. Process Problem	0.0	C. Quality Assurance Calibration	0.0		
D. Other Known Causes	0.0	D. Other Known Causes	0.0		
E. Unknown Causes	0.0	E. Unknown Causes	0.0		
II. Total Duration of Excess Emission	0.0	II. Total CMS Downtime	51.0		
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.0%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	8.3%		

Total time of excess emission events due to emergency/abnormal operations: 0. NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2. Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)
- 4. New CEMS installation on December 20, 2013. Data not valid until March 6, 2014 after 7-Day Drift Test, RATA and Linearity Test was successfully completed.

1Q14 Crude Charge Heater CEMS Form C - Excess Emissions Summary

NOx lb/hr (1-Hour)

No.

Start Time

End Time

Hours

Reason

Action

There are no excess emissions for this report.

Total Periods Excess Emissions

n

1Q14 Crude Charge Heater CEMS

NOx lb/hr (1-Hour)

Form D - Monitor Downtime Summary

No.	Start Time	End Time	Hours	Reason	Action
1	3/12/2014 6:00:00 AM	3/13/2014 6:00:00 AM	24	Failed Morning Stack Flow Delta P Span Calibration Check and Subsequent Manual Calibrations	Morning Calibration Check Cleared the Alarm
2	3/21/2014 6:00:00 AM	3/21/2014 8:00:00 AM	2	Failed Morning Stack Flow Delta P Span Calibration Check	Ran Manual Calibration
3	3/23/2014 6:00:00 AM	3/24/2014 6:00:00 AM	24	Failed Morning Stack Flow Delta P Span Calibration Check	Morning Calibration Check Cleared the Alarm
4	3/31/2014 6:00:00 AM	3/31/2014 7:00:00 AM	1	Failed Morning Stack Flow Delta P Span Calibration Check	Ran Manual Calibration
	Total Hours M	onitor Unavailable	:51		



April 8, 2014

Mr. Fred DiLella
Stationary Source Compliance Program Manager
Air-Quality Division,-Wyoming-DEQ
122 West 25th Street
Chevenne, WY 82002

Subject:

Crude Charge Heater Initial RATA and Compliance Test, 7-Day Drift Test, and Linearity Test Reports

Frontier Refining LLC (Frontier) installed a Continuous Emissions Monitoring System (CEMS) on the Crude Charge Heater (Source ID 21) to meet the requirements of the Consent Decree. The CEMS was put into operation on December 26, 2013, and the initial testing was performed per the protocol submitted on November 1, 2013.

Attached please find the reports of the Relative Accuracy Test Audit (RATA) and Compliance Test conducted on March 4, 2014, the 7-Day Drift Test from January 21, 2014 through January 27, 2014, and Linearity Test conducted on March 6, 2014. These initial stack tests were conducted to demonstrate compliance with Operating Permit 3-0-149-2.

The testing showed the unit to be in compliance with all of the performance standards.

If you have any questions or comments, please contact me at (307) 634-3551.

Sincerely,

David Weeks

Environmental Engineer

Attachment

cc. Glenn Spangler, WDEQ District 1 Engineer
Mark Gagen, WDEQ CEMS Coordinator
Mike Achacoso, Frontier Refining LLC
Glenn Travis, Frontier Refining LLC

I certify that the information contained in this report is true, accurate, and complete to the best of my knowledge based upon my reasonable inquiry of the person(s) responsible for preparing this report.

Mike Achacoso

Vice President & Refinery Manager

Mike Shawn

Frontier Refining LLC
300 Morrie Ave. • Cheyenne, WY 82007
(307) 634-3551 • http://www.hollyfrontier.com



Source Emissions Test Report Frontier Refining LLC

Relative Accuracy Test Audit
Crude Charge Heater
Relative Accuracy Test Audit and Compliance Testing - NO_X
Cheyenne, Wyoming

Test Date: March 4, 2014

Report prepared for: Frontier Refining LLC 300 Morrie Avenue Cheyenne, Wyoming 82007

Report prepared by: Air Pollution Testing, Inc. 5530 Marshall Street Arvada, Colorado 80002

APT Project: FRO3331



Certification

Team Leader Certification:

I certify that all of the sampling and analytical procedures and data presented in this report are authentic and accurate.

Adam Loes

Field Team Leader / Project Manager

Reviewer Certification:

I certify that all of the testing details and conclusions are accurate and valid.

Karl Breuer

MARIA

Reviewer / Senior Technical Writer



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1. Introduction

Air Pollution Testing, Inc. (APT) was contracted by Frontier Refining LLC (Frontier) to conduct a Relative Accuracy Test Audit (RATA) at the Cheyenne Wyoming Refinery. The Frontier Cheyenne Refinery processes crude oil to produce a variety of products and is located in Cheyenne, Laramie County, Wyoming.

The purpose of the testing program was to determine the Relative Accuracy (RA) of the oxygen (O_2) and nitrogen oxides (NO_X) Continuous Emission Monitoring Systems (CEMS) currently in place on the Crude Charge Heater (Source 21) at the Cheyenne Refinery. Additionally, each set of three RATA runs were combined into a single compliance run (for a total of 3 compliance runs) to determine compliance with the permitted emission restrictions. Concurrent stack gas volumetric flow measurements were collected for the determination of mass emission rates. The testing program was conducted with the Crude Charge Heater and all associated processes operating under normal operating conditions.

The data collected during the testing program are being used to determine the compliance status with respect to applicable Wyoming Department of Environmental Quality (WDEQ) permit requirements.

Key contact personnel involved in the test program are provided in Table 1.1. Source identification and emission limit summaries are provided in Table 1.2 on the following page.

Frontier Refining LLC : Cheyenne, Wyoming – Crude Charge Heater Test Program Contact Personnel						
Name, Title	Company, Address	Telephone, Facsimile				
Mr. David Weeks, Environmental Engineer	Frontier Refining LLC 300 Morrie Street Cheyenne, Wyoming 82007	(307) 771 8827, (307) 771 8794				
Mr. Mark Gagen, Air Quality CEMS Coordinator	WDEQ	(307) 777 7334, (307) 777 5616				
Mr. Glenn Spangler, Air Quality District 1 Engineer	122 West 25th Street Cheyenne, Wyoming 82002	(307) 777 3787, (307) 777 5616				
Mr. Dave Maiers, Operations Director	Air Pollution Testing, Inc. 5530 Marshall Street Arvada, Colorado 80002	(303) 420 5949 ext. 33, (303) 420 5920				

Table 1.1: Test Program Contact Personnel

Frontier Refining LLC : Cr Source Identification Sum						
Source Identification	Testing Parameter	Emission Limits				
Cauda Charna Master	O ₂	PS 3 – average d ≤ 1.0% (%vd)				
Crude Charge Heater Capacity: 202 MMBtu/hr Source ID: 21	NO _X	PS 2 - RA: 20% RM or 10% ES (ppmvd) PS 6 - RA: 20% RM or 10% ES (lb/MMBtu)				
NO _x Emission Standard - 0.031 lb/MMBtu, 6.3 lb/hr						

Table 1.2: Source Identification Summary

2. Methods

Air Pollution Testing, Inc. (APT) tested in accordance with the following U.S. Environmental Protection Agency (EPA) source emissions test methods referenced in 40 CFR Part 60. Appendix A.

EPA Method 1 - Sample and Velocity Traverses for Stationary Sources

EPA Method 2 – Determination of Stack Gas Velocity and Volumetric Flow Rate (Type S Pitot Tube)

EPA Method 3A – Determination of Oxygen and Carbon Dioxide Concentrations in Emissions from Stationary Sources (Instrumental Analyzer Procedure)

EPA Method 4 - Determination of Moisture Content in Stack Gases

EPA Method 7E - Determination of Nitrogen Oxides Emissions from Stationary Sources (Instrumental Analyzer Procedure)

The test methods were used to demonstrate compliance with the following Performance Specifications referenced in <u>40 CFR Part 60</u>, <u>Appendix B</u>.

Performance Specification 2 – Specifications and Test Procedures for SO₂ and NO_x Continuous Emission Monitoring Systems in Stationary Sources

Performance Specification 3 – Specifications and Test Procedures for O₂ and CO₂ Continuous Emission Monitoring Systems in Stationary Sources

Performance Specifications 6 - Specifications and Test Procedures for Continuous Emission Rate Monitoring Systems in Stationary Sources

3. Test Program Summary

The testing performed by APT determined all emissions parameters detailed in Table 3.1.

On-site gas analyzers, housed in a temperature-controlled analytical trailer, were used to determine the emission concentrations of oxygen (O_2) , carbon dioxide (CO_2) and NO_X from the Crude Charge Heater. Concurrent gas velocity and moisture content measurements were conducted to calculate NO_X mass emission rates.

Ten sampling runs conducted for a minimum of 21 minutes were performed for the RATA with nine runs used to determine relative accuracy. A velocity traverse was conducted at the beginning of each sampling period. A total of 3 moisture runs were conducted. The emission data from each sampling period was compared with CEMS data to calculate the RA of the system. The NO $_{\rm X}$ RA was calculated in units of parts per million, dry volume basis (ppmvd) and pounds per million British thermal units (lb/MMBtu). The O $_{\rm Z}$ RA was calculated in percent, dry volume basis (%vd).

Prior to the RATA test periods, the more stringent 12-point stratification test requirements described in <u>40 CFR Part 75</u>, <u>Appendix A. Section 6.5.6.1</u> were performed to determine appropriate pollutant and diluent sampling points. The number and location of the velocity traverse points were selected in accordance with EPA Method 1.

Emission Parameter Sampling Method Analytical Method						
gas flow	Methods 1, 2	draft gauge				
oxygen (O₂)	Method 3A	paramagnetic analyzer				
carbon dioxide (CO ₂)	Method 3A	non-dispersive infrared analyzer	APT on-site			
moisture (H₂O)	Method 4	gravimetric				
NO _X	Method 7E	chemiluminescent analyzer				

Table 3.1: Sampling and Analytical Methods Summary

4. Test Method Details

4.1. Stack Gas Flow, Oxygen, Carbon Dioxide, Moisture

Stack gas velocity, volumetric flow rate, O_2 , CO_2 , and moisture (H_2O) content were measured in accordance with EPA Methods 1, 2, 3A, and 4.

Each sampling period consisted of conducting a temperature and differential pressure traverse of the stack using a K-type thermocouple and an S-type pitot tube. Concurrent with each traverse, a sample of gas for moisture determination was extracted from the stack at a constant flow rate of no greater than 0.75 cubic feet per minute. The gas sample passed through a stainless steel probe, through a series of 4 chilled glass impingers, and through a calibrated dry gas meter. Please see Appendix 5 – Schematics for a diagram of the EPA Method 1, 2 and 4 sampling train.

Concurrently, a sample of stack gas was extracted through a heated Teflon line, passed through a refrigeration-type gas conditioner to remove moisture, and directed to a Servomex Series 1400 paramagnetic O₂ analyzer and a Servomex Series 1400 non-dispersive infrared (NDIR) CO₂ analyzer connected in series. The O₂ and CO₂ concentrations were displayed on the analyzer front panels in units of dry volume percent (%vd) and logged to a computerized data acquisition system (CDAS).

Prior to sampling, the first two impingers were each seeded with 100 milliliters of water. The third impinger was empty. The fourth impinger was seeded with 250 grams of silica gel. Before and after each sampling period, the analyzers were challenged with calibration gases to calibrate the instruments, to verify linearity of response, and to quantify span and zero drift for the previous sampling period. The calibration gases were certified in accordance with EPA Protocol 1. To ensure no system bias, the analyzer calibrations were conducted by introducing all gases to the analyzers at the sampling probe tip at stack pressure.

Following sampling, the moisture gain in the impingers was measured gravimetrically to determine the moisture content of the stack gas. The CDAS data were averaged in one-minute increments, corrected for instrumental drift, and reported as average concentrations for each sampling period in units of %vd.

All of the above data were combined to calculate the stack gas velocity and volumetric flow rate in units of feet per second (ft/sec), actual cubic feet per minute (acfm), dry standard (1 atmosphere and 68°F) cubic feet per minute (dscfm), and pounds per hour (lb/hr).

4.2. Nitrogen Oxides

NO_x emissions were measured in accordance with EPA Method 7E.

Each sampling period consisted of extracting a gas sample from the stack at a constant flow rate of approximately two (2) liters per minute. The sample passed through a refrigeration-type gas conditioner to remove moisture and into the sampling port of a Thermo Environmental Instruments (TECO) Model 42CHL chemiluminescent NO_X analyzer. The NO_X concentrations were displayed on the analyzer front panels in units of ppmvd and logged to a CDAS.

Before and after each sampling period, the analyzer was challenged with calibration gases to calibrate the instruments, to verify linearity of response, and to quantify zero and span drift for the previous sampling period. The calibration gases were prepared and certified in accordance with EPA Protocol 1. To ensure no system bias, the analyzer calibrations were conducted by introducing all gases to the analyzer at the sampling probe tip at stack pressure. Please see Appendix 5 — Schematics for a diagram of the EPA Methods 3A and 7E sampling train.

Following sampling, the CDAS data were averaged in one-minute increments, corrected for instrumental drift, and reported as average NO_X emission concentrations for each sampling period in units of ppmvd. The concentration data were combined with concurrently collected stack gas flow and diluents data to calculate the NO_X mass emission rates in units of lb/hr (with NO_X expressed as NO_2) and lb/MMBtu.

5. Results

The results of the testing are presented in Tables 5.1 and 5.2. Any testing parameters not found in the tables may be found in *Appendix 1 - Testing Parameters / Sample Calculations* at the back of this report. Ten RATA runs were performed and nine were used to calculate RA. Stricken values do not enter into the calculations.

The following terms and abbreviations are used in the tables:

- RATA Relative Accuracy Test Audit
- ppmvd parts per million, dry volume basis
- RM reference method
- CEM continuous emission monitor
- d difference (RM CEM)
- | d| absolute value of the difference (RM CEM)
- %vd percent volume, dry
- RA relative accuracy (% of RM data unless noted otherwise)
- dscfm volumetric flow in dry standard cubic feet per minute

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- lb/hr pounds per hour
- Ib/MMBtu pounds per million British thermal units
 PS performance specification

Project Number FRO3331 Test Report, Frontier Refinery Crude Charge Heater

O ₂ (%vd)				NO _x (ppmvd)			NO _x (lb/MMBtu)		
Run	RM	CEM	d	RM	CEM	d	RM	CEM	d
1	4.1	4.1	0.0	21.7	17.5	4.2	0.027	0.023	0.0050
2	4.1	4.1	0.1	21.4	17.2	4.2	0.027	0.022	0.0050
3	4.1	4.0	0.1	21.5	17.4	4.1	0.027	0.022	0.0050
4	4.2	4.0	0.2	21.5	17.3	4.3	0.027	0.022	0.005
5	4.1	4.0	0.1	21.6	17.3	4.3	0.027	0.022	0.0053
6	4.1	4.1	0.0	21.7	17.4	4.2	0.027	0.022	0.0050
7	4.1	4.0	0.0	22.2	17.3	4.9	0.028	0.022	0.005
8	4.1	4.1	0.1	21.7	17.4	4.3	0.028	0.022	0.005
9	4.1	4.0	0.1	21.4	17.3	4.1	0.027	0.022	0.0050
10	4.1	4.0	0.1	21.6	17.3	4.3	0.027	0.022	0.0053
verage	4.1	4.0	0.1	21.6	17.3	4.2	0.027	0.022	0.005
	RA(d)	0.079		RA (%)	19.95%		RA (%)	19.08%	
	Limit	1.0	(PS3)	Limit	20%	(PS2)	Limit	20%	(PS6)

Table 5.1: RATA Results - O2 and NOX

Frontier Refining LLC: Cheyenne, Wyoming Facility Crude Charge Heater Compliance Results Summary, March 4, 2014						
Run	1	2	3	Average	Applicable Limits	
Start Time	9:46	11:31	13:02			
Stop Time	11:18	12:54	14:25			
O ₂ (%vd)	4.1	4.1	4.1	4.1		
CO ₂ (%vd)	10.3	10.4	10.3	10.3		
Gas Flow (dscfm)	30,695	31,526	29,279	30,500		
Moisture Content (%)	14.3	13.9	15.1	14.4		
NO _x (ppmvd)	21.5	21.6	21.8	21.6		
NO _x (lb/hr)	4.73	4.88	4.57	4.72	6.3	
NO _x (lb/MMBtu)	0.027	0.027	0.028	0.027	0.031	

Table 5.2: Compliance Test Results - NO_X

6. Conclusions

The results of the testing conducted by APT on March 4, 2014 at the Frontier Refining Crude Charge Heater located in Cheyenne, Wyoming indicate that the stack gas O_2 and NO_x CEMS are operating in compliance with applicable performance specifications. Additionally, the testing demonstrates that the unit is also in compliance with the permitted mass emission limits for NO_x .

Appendix 1

Test Parameters / Sample Calculations

RATA Calculations

		O ₂ (%vd)		
Run	RM	CEM	RM-CEM	Used? (Y/N)
1	4.1	4.1	0.0	Y Y
2	4.1	4.1	0.1	Y
3	4.1	4.0	0.1	Y
4				n
5	4.1	4.0	0.1	Ÿ
6	4.1	4.1	0.0	Ý
7	4.1	4.0	0.0	ÿ
8	4.1	4.1	0.1	Ý
9	4.1	4.0	0.1	Ý
10	4.1	4.0	0.1	Ý
Average	4.1	4.0	0.1	
Number of	Runs	9)	
l' value		2.306	3	
ld1		0.079	}	
Std. Dev		0.043	}	
C		0.033	}	

RATA Calculations

		NO _x (ppmvd))	
Run	RM	CEM	RM-CEM	Used? (Y/N)
1	21.7	17.5	4.2	Y
2	21.4	17.2	4.2	Y
3	21.5	17.4	4.1	Y
4	21.5	17.3	4.3	Y
5	21.6	17.3	4.3	Y
6	21.7	17.4	4.2	Y
7				N
8	21.7	17.4	4.3	Y
9	21.4	17.3	4.1	Y
10	21.6	17.3	4.3	Y
Average	21.6	17.3	4.2	
Number of R	tuns	9		
T value		2.306		
[d]		4.232		
Std. Dev		0.093		
CC		0.072		
RA (% of RM	Data)	19.95%		

RATA Calculations

	NO	x (ib/MMBa	ı) F _d	
Run	RM	CEM	RM-CEM	Used? (Y/N)
1	0.027	0.023	0.0050	Y ´
2	0.027	0.022	0.0050	y
3	0.027	0.022	0.0050	Ý
4	0.027	0.022	0.0053	Y
5	0.027	0.022	0.0053	Y
6	0.027	0.022	0.0050	Y
7				n
8	0.028	0.022	0.0052	Y
9	0.027	0.022	0.0050	Y
10	0.027	0.022	0.0053	Ÿ
Average	0.027	0.022	0.0051	
Number of R	luns	9)	
T value		2.306	3	
[d]		0.005	;	
Std. Dev		0.000)	
CC		0.000	· ·	
RA (% of RM	Data)	19.08%	•	

				Fi	old Reference M	ethod Data							
	Flum #	1	2	3	4	5	6	7			10	Average	
	Start Time	9:46	10:20	10:58	11:31	12:03	12:33	13:02	13:33	14:04	14:48	1 1	
	Stop Time	10:08	10:41	11:18	11:53	12:24	12:54	13:25	13:55	14:25	15:01		
	Sample Duration (minutes)	23	21	22	22	21	21	23	22	21	21		
											102.00	102.00	
	Stack Diameter (inches)	102.00	102,00	102.00	102.00	102.00	102.00	102.00	102.00	102.00	0.248	0 251	
aPavo	Average (Delta P)" (" H ₂ O)"	0.243	0.267	0.256	0.250	0.261	0.259	0.249	0.247		0.837	0 837	
a Ama	Pitot Tube Constant (unidoss)	0.837	0.837	0.837	0.837	0.837	0.837	0.837	0.837	0.637	324	317	
	Stack Temperature (17)	312	314	314	308	309	309	330	328	326			1
	Barometric Pressure (mber)	807	807	807	807	807	807	807	807	807	807	807 23,83	1
	Sprometric Pressure (* Hg)	23.63	23.83	23.83	23.63	23.83	23.83	23.83	23.83	23.83	23.83		l
	Stack Pressure ("H ₂ O)	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10	0.10	
	Meter Y Factor (unitless)	1.017	1.017	1.017	1.017	1.017	1.017	1.017	1.017	1.017	1.017	1,017	
	Motor Temperature (*F)	48	48	48	43	43	43	42	42	42	42	44	
	Sample Volume (It ²)	58.463	58.463	58,463	58.735	58.735	56.735	78.616	76.616	76.616	76.616	85.806	
14	Orilice Pressure Delta H (" H ₂ O)	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	1.00	
	Molature (g)	174 1	174,1	174.1	171.6	171.6	171.5	247.0	247.0	247.0	247.0	202.5	1
H -	F, value (decl/MMBtu)	8,543	8,543	8,543	8,543	8,543	8,543	8,543	8,543	8,543	8,543	8,543	
Ē	F. value (dsc/MMBtu)	1,040	1,040	1,040	1,040	1,040	1,040	1,040	1,040	1,040	1,040	1,040	
) Novel	O _s (Yord)	4.1	4.1	4.1	4.2	4.1	4.1	4.1	4.1	4,1	4.1	4.1	
4.440	O ₂ (Nivd)-3 run average		4.1			4.1			4.1			4,1	
O ₂ %vd	CO, (NWI)	10.2	10.3	10,4	10.4	10.4	10.4	10.3	10.3	10.3	10.4	10.4	
C) NITO	CO ₂ (Ned)-3 run average	7.5.0	10.3			10.4			10.3			10,3	l
Mand	N _y (Yeard)	85.7	85.5	85.4	85.4	85.5	85.6	85.6	85.6	85.6	85.5	85.5	1
2%vd		21.7	21.4	21.5	21.5	21.6	21.7	22.2	21.7	21,4	21.6	8.15	1
ry	NO _X (ppstvd)	6,5-1	21.5	4.10		21.5			21.8			21.6	1
ry	NO _x (ppmvd)-3 Run Average		210										
				Rec	erence Method	Calculations							
	Run 4	1	2	3	4	5	•	7		9	10	Average	Permit Limit
,	Sample Volume (dscf)	49,345	49.345	49,345	50.032	50.032	50.032	\$5.420	85.420	65.420	65.420	\$5.901	
Tracket Tracket	Moisture Volume (acf)	8,209	8.209	8.209	8,091	8.091	8.091	11,846	11.646	11,846	11.646	9 548	1
weekill.	Moisture Content (%/100)	0.143	0.143	0.143	0.139	0.139	0.139	0.151	0.151	0.151	0.151	0.145	
-	termenta constate I sa test												
	Malabase Pantant Miland	14.3	143	14.3	13.9	13.9	13.9	15.1	15.1	15.1	15.1	14.5	1
	Moisture Content (%vw)	14,3	14.3	14.3	13.9	13.9	13.9	15.1	15.1	15.1	15.1		
6vw	Moisture Content (%ww)-3 run avg.		14.3			13.9 13.9 29.83	13.9	15.1		29.81	15.1	14.5	
Gerer	Moisture Content (%/w/-3 run avg. Molecular Weight Dry (foft)-mole)	29.80	14.3 29.82	29.83	29.84	13.9 29.83			15.1			14.5 14.4	
Gerer	Moisture Content (Yuw)-3 run avg. Molecular Weight Dry (Ib/Ib-mole) Molecular Weight Wet (Ib/Ib-mole)	29.80 28.12	14.3 29.82 28.13	29.83 28.15	29.84 28.19	13.9 29.83 28.18	29.82 28.18	29.82	15.1 29.81	29,81	29.83	14.5 14.4 29.62	
Coror Ao An 's	Moisture Content (New)-3 run avg. Molecular Weight Dry (Ib/Ib-mole) Molecular Weight Wet (Ib/Ib-mole) Gas Velocity (Neec)	29.80 28.12 18.6	14.3 29.82 28.13 19.7	29.83 28.15 19.5	29.84 28.19 19.1	13.9 29.63 28.18 20.0	29.82 28.18 19.8	29.52 28.09	15.1 29.81 28.03	29,81 28.03	29.83 28.05	14.5 14.4 29.62 28.11	
Coror Ao Ao Taorna	Moisture Content (%/wn)-3 run evg. Molecular Weight Dry (bifb-mole) Molecular Weight Wat (fb/fb-mole) Gas Yelocity (Mesc) Gas Flow (scim)	29.80 28,12 18.6 63,404	14.3 29.82 28.13 19.7 67,148	29.83 28.15 19.6 66,861	29.84 28.19 19.1 65,082	13.9 29.83 28.18 20.0 60,099	29.82 28.18 19.8 67,581	29.82 28.03 19.4	15.1 29.81 28.03 19.2	29.81 28.03 18.3	29.83 28.05 19.2	14.5 14.4 29.52 28.11 19.3	
Coror Ao Ao Taorna	Moisture Content (%/w/-3 run avg. Molecular Weight Dry (Info-mele) Hotecular Weight Weight (Met (Bufb-mele) Gas Velocity (Mesec) Gas Flow (acim) Gas Flow (dacim)	29.80 28.12 18.6	14.3 29.82 28.13 19.7 67,148 31.301	29.83 28.15 19.5	29.84 28.19 19.1	13.9 29.53 28.18 20.0 60,099 32,078	29.82 28.18 19.8	29.82 28.03 19.4 65,065	15.1 29.81 28.03 19.2 65,324	29,81 28,63 18.3 62,423	29.83 28.05 19.2 65,407 29.810	14,5 14,4 29,62 28,11 19,3 65,741 30,431 30,500	
Good Ao Ao Is Tagnu Toecnu	Molecular Weight Dry (Brith-mole) Molecular Weight Dry (Brith-mole) Molecular Weight Weight (Brith-mole) Gas Flow (actim) Gas Flow (actim) Gas Flow (dactim) Gas Flow (dactim) Gas Flow (dactim)	29.80 28.12 18.6 63,404 29.621	14.3 29.82 28.13 19.7 67,148 31.301 30,696	29.83 28.15 19.5 66.861 31,165	29.84 28.19 19.1 65,062 30,689	13.9 29.93 28.18 20.0 60,099 32,078 31,526	29.82 28.18 19.8 67,581 31,610	29.82 28.03 19.4 65,065	15.1 29.81 28.03 19.2 85,324 29.602	29,81 28,63 18.3 62,423	29.83 28.05 19.2 65,407	14.5 14.4 29.82 28.31 19.3 85,741 30,431	
GOW As As 'e Actus 'coccus 'wactus	Motsture Content (Wavey-3 run evg. Motscudar Weight Dry (Botts-mote) Motscudar Weight Wet (Brits-mote) Gas Welcotty (Meec) Gas Row (acrim) Gas Flow (dacfm) - Gas Flow (wacfm) - Gas Flow (wacfm)	29.80 28.12 18.8 63,404 29.621	14.3 29.82 28.13 19.7 67,148 31.301 30,686 36.508	29.83 28.15 19.5 66.881 31,165	29.84 28.19 19.1 65,062 30,689	13.9 29.83 28.18 20.0 68,099 32,078 31,526 37,286	29.82 28.18 19.8 67,581 31,610	29.82 28.03 19.4 68,065 29,862	15.1 29.81 29.03 19.2 85,324 29,602 29,279	29,81 28,03 18,3 62,423 29,374	29.83 28.05 19.2 65,407 29.810	14,5 14,4 29,62 28,11 19,3 65,741 30,431 30,500	
Gover Ag Ag Te Teacher Toecher Teacher	Molecular Weight Dry (Inflo-mole) Molecular Weight Dry (Inflo-mole) Molecular Weight Weight (Inflo-mole) Gas Weight Weight (Inflo-mole) Gas Flow (actim) Gas Flow (dactim) Gas Flow (dactim) Gas Flow (wactim) Gas Flow (wactim) Gas Flow (wactim)	29.60 28.12 18.6 63,404 29.621 34,549 2,073	14.3 29.82 28.13 19.7 67,148 31.301 30,695 36,508 2,190	29.83 28.15 19.5 66.881 31.165 36.349 2,181	29.84 28.19 19.1 65,082 30,889 35,862 2,139	13.9 29.53 28.18 20.0 68,099 32,078 31,526 37,286 2,236	29.82 28.18 19.8 67,581 31,610	29.82 28.03 19.4 68,065 29,862	15.1 29.81 28.03 19.2 85,324 29,602 29,279 34,872	29,81 28,03 18,3 62,423 28,374 33,428	29.63 28.05 19.2 65,407 29.610 36.116	14.5 14.4 29.82 28.31 18.3 85,741 30,431 30,580 35,587	
Court A A A A A A A A A A A A A	Molecular Weight Dry (Inflormate) Molecular Weight Dry (Inflormate) Molecular Weight Weight (Inflormate) Gas Flow (actin) Gas Flow (doctin) Gas Flow (doctin) Gas Flow (wechn) Gas Flow (wechn) Gas Flow (mench) Gas Flow (mench) Gas Flow (mench)	29.80 28.12 18.6 63,404 29.621 34.549 2,073 35	14.3 29.82 28.13 19.7 67,148 31.301 30,696 36,508 2,190 37	29.83 28.15 19.5 66.861 31.165 36,349 2,181 36	29.64 28.19 19.1 65.062 30,689 35.852 2,139 36	13.9 29.53 28.18 20.0 68,099 32,078 31,526 37,286 2,236 37	29.82 28.18 19.8 67,581 31,610 36,854 2,217 37	29.82 28.03 19.4 68,065 29,862 36,178 2,111 35	15.1 29.81 28.03 19.2 65.324 29.602 29.279 34.872 2.092	29.81 28.03 18.3 62,423 29,374 33,425 2,006	29.83 28.05 19.2 65,407 29.810 35,116 2,107	14.5 14.4 29.82 28.11 19.3 85,741 30,431 30,580 25,587 2,135	
GOVER As AS AS ASSESSED OF THE STREET OF T	Molecular Weight Dry (Inflo-mole) Molecular Weight Dry (Inflo-mole) Molecular Weight Wei (Inflo-mole) Gas How (achm) Gas Flow (dechm) Gas Flow (dechm) Gas Flow (dechm) Gas Flow (meachn) Gas Flow (meachn) Gas Flow (meachn) Gas Flow (fineschn) Gas Flow (fineschn) Gas Flow (fineschn) Gas Flow (fineschn)	29.80 28.12 18.6 63,404 29.621 34,549 2,073 35 151,273	14.3 29.82 28.13 19.7 67,148 31.301 30,696 36,508 2,190 37 159,933	29.83 28.15 19.5 66.881 31.165 36.349 2,181 36 159,321	29.84 28.19 19.1 65,062 30,689 35,852 2,139 36 158,505	13.9 29.53 28.18 20.0 68.099 32,678 31,526 37,286 2,236 37 163,530	29.82 28.18 19.8 67,581 31,610 36.854 2,217 37 162,144	29.82 28.03 19.4 65,065 29,862 36,178 2,111 35 183,559	15.1 29.81 28.03 19.2 65,324 29,602 29,279 34,872 2,092 35	29,81 28,03 18,3 62,423 28,374 33,425 2,006 33	29.83 28.05 19.2 65,407 29.810 35,116 2,107 35	14.5 14.4 29.52 28.11 19.3 85,741 30,431 30,500 35,537 2,135 36	
GVW AG	Molesture Content (%vw)-3 run evg. Molecular Weight Dry (Brits-mole) Molecular Weight Weigh (Brits-mole) Gas Flow (actim) Gas Flow (doctim) Gas Flow (doctim) Gas Flow (doctim) Gas Flow (doctim) Gas Flow (wactim) Gas Flow (wactim) Gas Flow (wactim) Gas Flow (wactim) Gas Flow (brits) F, (unitless)	29.80 28.12 18.6 63,494 29.621 34,549 2,973 35 151,273 1,644	14.3 29.82 28.13 19.7 67,148 31.391 30,895 36.508 2,190 37 150,933 1,624	29.83 28.15 19.5 66.861 31,165 36,349 2,181 36 159,321 1,607	29.64 28.19 19.1 65,082 30,689 35,852 2,139 36 156,505 1,601	13.9 29.83 28.18 20.0 68,009 32,678 31,526 37,286 2,236 37 163,530 1.616	29.82 29.18 19.8 67,581 31,610 36.954 2,217 37 182,144 1,623	29.82 28.09 19.4 68,065 29,862 36,178 2,111 35 183,559 1,327	15.1 29.81 28.03 19.2 65.324 29.602 29.279 34.872 2.092 35 152.203	29,81 28,03 18,3 62,423 28,374 33,428 2,006 33 145,995	29.83 28.05 19.2 65,407 29.810 35.116 2,107 35 183,369	14.5 14.4 29.82 28.11 19.3 85,741 30,500 35,587 2,135 36	
GVIVI AG AG FS FACTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIVI TOROCTIV TOROCTIV TOROCTIV TOROCTIV TOROCTIV TOROCTIV TOROCTIV TOROCTIV TOROCTIV TOROCTIV TOROCTIV TORO	Moteture Content ("Movey-3 run evg. Motecular Weight Dry (Botts-mote) Motecular Weight Wei (Brits-mote) Gas Weischig (Messc) Gas Row (achth) Gas How (dachth)-3 run average Gas Row (wachth)-3 run average Gas Row (wachth) Gas Row (invachth)	29.80 28.12 18.6 63,404 29.621 34.549 2,073 35 151,273 1.644 3.5	14.3 29.82 28.13 19.7 67,148 31.301 30,696 2,190 37 159,933 1.624 3.5	29,83 28,15 19,5 66,881 31,165 36,349 2,181 36 159,321 1,607 3,8	29.84 28.19 19.1 65.082 30,889 35.862 2,139 36 156.505 1.601 3.6	13.9 29.63 29.18 20.0 60,099 32,078 31,526 37,286 2,236 37 163,530 1,616 3.8	29.82 28.18 19.8 67,581 31,810 36,854 2,217 37 162,144 1,623 3,5	29.82 28.03 19.4 65,065 29,862 35,178 2,111 35 183,559 1.827 3.5	15.1 29.81 29.03 19.2 65,324 29,602 29,279 34,872 2,992 35 152,203 1,627 3.5	29,81 28,03 18,3 62,423 28,574 33,428 2,006 33 146,895 1,627	29.83 28.05 19.2 65,407 29.810 35,116 2,107 35 153,369 1,610	14.5 14.4 29.82 28.11 18.3 85,741 30,431 30,560 35,587 2,135 38 165,773 1 821	
GVW AG AG AG AG F AGTN TOBOTH	Molesture Content (%vvv)-3 run evg. Molescular Weight Dry (Britz-mole) Molescular Weight Wei (Britz-mole) Gas How (selfm) Gas Flow (decfm) Gas Flow (forscfm) Gas Gas (form) CO ₂ (%vvv)	29.80 28.12 18.8 63,404 29.621 34.549 2,073 35 151,273 1.644 3.5 8.8	14.3 29.82 28.13 19.7 67,148 31.301 30.695 36.508 2.190 37 159.933 1.624 3.5	29.83 28.15 19.5 66.861 31.165 36.349 2.181 36 159,321 1.607 3.8	29.64 28.19 19.1 65.062 30.689 35.852 2,139 36 156.505 1.601 3.6	13.9 29.53 28.18 20.0 68,009 32,078 31,526 37,286 2,236 37 163,530 1,616 3.8	29.82 28.18 19.8 67,581 31.610 36.854 2,217 37 162,144 1,823 3,5 8,9	29.82 28.09 19.4 68,065 28,662 36,178 2,111 35 183,559 1,827 3.5 8.9	16.1 29.81 29.03 19.2 85,324 29.602 29.279 34,872 2,092 35 152,203 1,627 3,5	29.81 28.03 16.3 62,423 28,574 33,428 2,006 33 145,895 1,827 3,5	29.63 28.05 19.2 65,607 29,810 36,116 2,107 35 153,308 1,610 3.5 8.9	14.5 14.4 29.82 20.11 19.3 85,741 30,630 35,567 2,135 36 165,773 1 821 3 524	
Gover Ag Ag Fe Fectus Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche Topoche	Motesture Content (%vw)-3 run avg. Motesture Weight Dry (brits-mole) Motesture Weight Weight (brits-mole) Gas Flow (actim) Gas Flow (dactim) Gas Flow (dactim) Gas Flow (dactim) Gas Flow (dactim) Gas Flow (wastim) Gas Flow (brits) Gas Flow (brits) Gas Flow (brits) Gas Flow (brits) O ₂ (%vw) NO ₃ (ppmww)	29.80 28.12 18.6 63,404 29.621 34.549 2,073 35 151,273 1.644 3.5 6.8 18.6	14.3 29.82 28.13 19.7 67,148 31.301 30,896 36,508 2,190 37 159,333 1,524 3.5 8.6 18.4	29.83 28.15 19.5 66.861 31,165 36,349 2,181 36 159,321 1,607 3.8 8.9 18.5	29.84 28.19 19.1 65.062 30.869 35.862 2,139 36 158.505 1.601 3.6 9.0	13.9 29.53 28.18 20.0 68,009 32,678 31,526 2,236 37 163,530 1.616 3.8 8.9 18.6	29.82 28.18 19.8 67,581 31,810 36.864 2,217 37 162,144 1,523 3,5 8,9	29.82 28.03 19.4 68,065 29,862 36,178 2,111 35 183,559 1,827 3.5 8.8 18.8	16.1 29.61 29.03 19.2 85,324 29,602 29,279 34,572 2,092 35 152,203 1,827 3,5 8,7	29,81 28,03 18.3 62,423 28,374 33,425 2,005 33 145,995 1,627 3,5 8,8	29.83 28.05 19.2 65,407 29,810 35,116 2,107 35 153,308 1,610 3.5	14.5 14.4 29.52 28.91 19.3 95,741 30,431 30,500 25,537 2,135 36 165,773 1 821 3 204 8 853	
GOVER A A A A A S S S S S S S S S S S S S S	Molecure Content (%vvv)-3 run evg. Molecular Weight Dvy (Both-mole) Molecular Weight Wei (Brib-mole) Gas Weight Wei (Brib-mole) Gas Flow (contre) Gas Flow (contre) Gas Flow (contre) Gas Flow (westim) Gas Flow (forestim) Gas Flow (forestim) Gas Flow (forestim) Oas Flow (forestim) Oas Flow (forestim) Oog (Weive) NO (Sportery)	29.80 28.12 18.8 63,404 29.621 34.549 2,073 35 151,273 1.644 3.5 8.8	14.3 29.82 28.13 19.7 67,148 31,301 30,696 36,508 2,190 37 159,933 1,624 3,5 8,8 18,4 4,80	29.83 28.15 19.5 66.861 31.165 36.349 2.181 36 159,321 1.607 3.8	29.64 28.19 19.1 65.062 30.689 35.852 2,139 36 156.505 1.601 3.6	13.9 29.53 28.18 20.0 68,009 32,078 31,526 37,286 2,236 37 163,530 1,616 2,8 8,9 18.6 4,96	29.82 28.18 19.8 67,581 31.610 36.854 2,217 37 162,144 1,823 3,5 8,9	29.82 28.09 19.4 68,065 28,662 36,178 2,111 35 183,559 1,827 3.5 8.9	15.1 29.51 29.03 19.2 55.324 29.602 29.279 34.872 2.092 35 152.203 1.527 3.5 8.7 18.4 4.60	29.81 29.03 16.3 62,423 28,374 33,425 2,005 33 145,895 1,627 3,5 8,8 16.2	29.83 28.05 19.2 65,407 29.810 35.116 2,107 35 153,368 1.610 3.5 8.9 18.3	14.5 14.4 29.82 20.11 19.3 95,741 30,431 30,500 25,587 2,135 38 165,773 1 821 3 524 8 853 18.495	
Cover Ag Section Secti	Molecular Weight Dry (Inflo-mole) Molecular Weight Dry (Inflo-mole) Molecular Weight Weight (Inflo-mole) Gas How (actim) Gas Flow (actim) Oz (5/ww) NOz (5/hry-3 nu average	29.80 28.12 19.8 63,404 29.621 34.549 2,073 35 151,273 1.644 3.5 8.8 18.6 4.59	14.3 29.82 28.13 19.7 67,148 31,301 30,895 36,508 2,190 37 159,933 1,624 3.5 8.8 18.4 4,73	29.83 28.15 19.5 66.881 31,165 36,349 2,181 36 159,321 1,507 3.8 8.9 18.5 4.80	29.84 28.19 19.1 65.082 30.889 35.862 2,139 36 156.505 1.601 3.6 9.0 18.5 4.73	13.9 29.53 28.18 20.0 50.099 32,078 31,526 2,236 37 163,530 1.616 3.8 8.9 18.6 4.86	29.82 28.18 19.8 67,581 31,610 36.864 2,217 37 182,144 1,623 3.5 8.9 16.6 4.93	29.82 28.03 19.4 65.065 29.862 36,178 2,111 35 193,559 1,527 3.5 8.9 10.8 4,74	16.1 29.61 29.03 19.2 65,324 29,602 29,279 34,972 2,992 35 15,273 3.5 8.7 18.4 4.60	29.81 28.03 18.3 62,423 28,574 33,425 2,006 33 145,895 1,627 3,5 8,8 16,2 4,35	29.83 28.05 19.2 65,407 29.810 35.116 2,107 35 153,368 1.610 3.5 8.9 18.3	14.5 14.4 29.52 28.91 19.3 95,741 30,451 30,560 25,587 2,135 36 165,773 1 821 3 524 6 853 18.465 4.71	s.s
CONTRACTOR	Moteture Content ("Movey-3 run evg. Motecular Weight Dry (Both-mote) Motecular Weight Weit (Brito-mote) Gas Veilocity (Mesc) Gas Row (acrim) Gas Row (dachm) Gas Row (dachm)-3 run average Gas Row (exactim)-3 run average Gas Row (exactim) Gas Row (both) Cog ("Move") Cog ("Move") Nog (both) Nog (both) Nog (both) Nog (both) Nog (both) Nog (both) Nog (Nog (Motes)) Nog (Nog (Motes)) Nog (Nog (Motes))	29.80 28.12 18.6 63,404 29.621 34.549 2,073 35 151,273 1.644 3.5 6.8 18.6	14.3 29.82 28.13 19.7 67,148 31.301 30.656 2.190 37 150.933 1.624 3.5 8.8 18.4 4.80 4.73 0.027	29.83 28.15 19.5 66.861 31,165 36,349 2,181 36 159,321 1,607 3.8 8.9 18.5	29.84 28.19 19.1 65.062 30.869 35.862 2,139 36 158.505 1.601 3.6 9.0	13.9 29.83 28.18 20.0 68,009 32,078 31,526 37,286 2,236 37 163,530 1,616 3.8 8.9 18.6 4.96 4.96	29.82 28.18 19.8 67,581 31,810 36.864 2,217 37 162,144 1,523 3,5 8,9	29.82 28.03 19.4 68,065 29,862 36,178 2,111 35 183,559 1,527 3.5 8.8 18.8	16.1 29.61 29.03 19.2 85.324 29.602 24.279 2.992 35 152.203 1.627 3.5 8.7 19.4 4.60 4.57	29.81 29.03 16.3 62,423 28,374 33,425 2,005 33 145,895 1,627 3,5 8,8 16.2	29.83 28.05 19.2 65,407 29.810 35.116 2,107 35 153.368 1.610 3.5 8.9 18.3 4.81	14,5 14,4 23,62 28,91 19,3 95,741 30,451 30,500 25,587 2,135 36 162,773 1 821 3 524 6 853 18,495 4,71	
LOVE AND	Molecular Weight Dry (Inflo-mole) Molecular Weight Dry (Inflo-mole) Molecular Weight Weight (Inflo-mole) Gas How (actim) Gas Flow (actim) Oz (5/ww) NOz (5/hry-3 nu average	29.80 28.12 19.8 63,404 29.621 34.549 2,073 35 151,273 1.644 3.5 8.8 18.6 4.59	14.3 29.82 28.13 19.7 67,148 31,301 30,895 36,508 2,190 37 159,933 1,624 3.5 8.8 18.4 4,73	29.83 28.15 19.5 66.881 31,165 36,349 2,181 36 159,321 1,507 3.8 8.9 18.5 4.80	29.84 28.19 19.1 65.082 30.889 35.862 2,139 36 156.505 1.601 3.6 9.0 18.5 4.73	13.9 29.53 28.18 20.0 50.099 32,078 31,526 2,236 37 163,530 1.616 3.8 8.9 18.6 4.86	29.82 28.18 19.8 67,581 31,610 36.864 2,217 37 182,144 1,623 3.5 8.9 16.6 4.93	29.82 28.03 19.4 65.065 29.862 36,178 2,111 35 193,559 1,527 3.5 8.9 10.8 4,74	16.1 29.61 29.03 19.2 65,324 29,602 29,279 34,972 2,992 35 15,273 3.5 8.7 18.4 4.60	29.81 28.03 18.3 62,423 28,574 33,425 2,006 33 145,895 1,627 3,5 8,8 16,2 4,35	29.83 28.05 19.2 65,407 29.810 35.116 2,107 35 153.368 1.610 3.5 8.9 18.3 4.81	14.5 14.4 29.52 28.11 19.3 95,741 30,590 35,587 2,135 36 165,773 1 821 3 524 8 953 18.495 4.71 4.72 9 927	6,3 0,601
AND THE PROPERTY OF THE PROPER	Moteture Content ("Movey-3 run evg. Motecular Weight Dry (Both-mote) Motecular Weight Weit (Brito-mote) Gas Veilocity (Mesc) Gas Row (acrim) Gas Row (dachm) Gas Row (dachm)-3 run average Gas Row (exactim)-3 run average Gas Row (exactim) Gas Row (both) Cog ("Move") Cog ("Move") Nog (both) Nog (both) Nog (both) Nog (both) Nog (both) Nog (both) Nog (Nog (Motes)) Nog (Nog (Motes)) Nog (Nog (Motes))	29.80 28.12 19.8 63,404 29.621 34.549 2,073 35 151,273 1.644 3.5 8.8 18.6 4.59	14.3 29.82 28.13 19.7 67,148 31.301 30.656 2.190 37 150.933 1.624 3.5 8.8 18.4 4.80 4.73 0.027	29.83 28.15 19.5 66.881 31,165 36,349 2,181 36 159,321 1,507 3.8 8.9 18.5 4.80	29.84 28.19 19.1 65.062 30.889 35.862 2,139 36 156.505 1,501 3.6 9.0 18.5 4.73	13.9 29.83 20.18 20.0 60,009 32,078 31,526 37,286 2,235 37 163,530 1,616 3,8 9 10.6 4,96 4,96 4,96 0,027	29.82 28.18 19.8 67,581 31,610 36.864 2,217 37 182,144 1,623 3.5 8.9 16.6 4.93	29.82 28.03 19.4 65.065 29.862 36,178 2,111 35 193,559 1,527 3.5 8.9 10.8 4,74	16.1 29.61 29.03 19.2 85.324 29.602 24.279 2.992 35 152.203 1.627 3.5 8.7 19.4 4.60 4.57	29.81 28.03 18.3 62,423 28,574 33,425 2,006 33 145,895 1,627 3,5 8,8 16,2 4,35	29.83 28.05 19.2 65,407 29.810 35.116 2,107 35 153.368 1.610 3.5 8.9 18.3 4.81	14.5 14.4 29.52 28.11 19.3 95,741 30,590 35,587 2,135 36 165,773 1 821 3 524 8 953 18.495 4.71 4.72 9 927	
CONTRACTOR	Molecure Content (%vvv)-3 run evg. Molecular Weight Dvy (Both-mole) Molecular Weight Weigh (Brich-mole) Gas Velocity (Maec) Gas Flow (contre) Oas Flow (contre) Oas Flow (contre) Oas Flow (contre) Ober (contre) Ober (contre) Ocy (%vvv) OCy (%vvv) OCy (billet)	29.80 28.12 19.8 63,404 29.621 34.549 2,073 35 151,273 1.644 3.5 8.8 18.6 4.59	14.3 29.82 28.13 19.7 67,148 31.301 30.686 30.500 2,190 37 150.933 1.624 3.5 8.8 18.4 4.03 4.73 0.027	29.83 28.15 19.8 66.81 31.165 36.349 2.181 36 159.321 1.507 2.8 8.9 18.5 4.80	29.84 28.19 19.1 65.082 30.889 35.862 2,139 36 156.505 1.601 3.6 9.0 18.5 4.73	13.9 29.83 28.18 20.0 68,009 32,078 31,526 37,286 2,236 27 163,530 1,616 3.8 8.9 18.6 4.96 4.96	29.82 28.18 19.8 67,581 31,610 36.864 2,217 37 182,144 1,623 3.5 8.9 16.6 4.93	29.82 28.03 19.4 65.065 29.862 36,178 2,111 35 193,559 1,527 3.5 8.9 10.8 4,74	16.1 29.61 29.03 19.2 85.324 29.602 24.279 2.992 35 152.203 1.627 3.5 8.7 19.4 4.60 4.57	29.81 28.03 18.3 62,423 28,574 33,425 2,006 33 145,895 1,627 3,5 8,8 16,2 4,35	29.83 28.05 19.2 65,407 29.810 35.116 2,107 35 153.368 1.610 3.5 8.9 18.3 4.81	14.5 14.4 29.52 28.11 19.3 95,741 30,590 35,587 2,135 36 165,773 1 821 3 524 8 953 18.495 4.71 4.72 9 927	
CONTRACTOR	Molecular Weight Dry (Britz-mole) Molecular Weight Weight (Britz-mole) Molecular Weight Weight (Britz-mole) Gas How (softm) Gas Flow (sortm) Cas Flow (britz-tm) Cas (sortm) NO ₂ (sortm) NO ₃ (britz-tm) NO ₃ (britz-tm) NO ₃ (britz-tm) NO ₄ (britz-tm) NO ₅ (britz-tm) NO ₆ (britz-tm) NO ₇ (britz-tm) NO ₇ (britz-tm) NO ₈ (britz-tm) NO ₈ (britz-tm) NO ₉ (britz-tm)	29.80 28.12 18.6 63.404 29.621 34.549 2,973 35 151,273 1.644 3.5 8.8 18.6 4.39	14.3 29.82 28.13 19.7 67,148 31,301 30,695 36,508 2,190 37 159,503 1,624 3.5 8.8 18.4 4.80 4.73 0.027	29.83 28.15 19.5 66.841 31.165 36.349 2.181 36 159,321 1.607 3.8 8.9 18.5 4.80 9.027	29.84 28.19 19.1 65,082 30,689 25,862 2,139 36 156,505 1,601 3.6 9.0 18.5 4,73 0,027	13.9 29.53 28.18 20.0 60,009 32,078 31,526 37,286 2,236 37,185 3,530 1,616 3.8 8.9 18.4 4.96 4.88 0,027	29.82 28.18 19.8 67,581 31,610 36.864 2,217 37 182,144 1,623 3.5 8.9 18.6 4.93	29.82 28.03 19.4 68.065 29.862 36,178 2.111 35 133,550 1.827 2.5 8.0 10.8 4.74	16.1 29.61 28.03 19.2 85,324 29.602 29.279 34.872 2.092 35 152,203 1.627 3.5 8.7 18.4 4.60 4.57 0.028	29.81 28.03 18.3 62,423 28,574 33,425 2,006 33 145,895 1,627 3,5 8,8 16,2 4,35	29.83 28.05 19.2 65,407 29,810 35,116 2,107 35 153,308 1,610 2,5 8,9 1,83 4,81	14.5 14.4 29.52 28.11 19.3 95,741 30,590 35,597 2,135 36 165,773 1 821 3 524 8 953 18,495 4,71 4,72 0 927 0 927	
Nove Mg Mg Fe Facha Forecha Finitecha Finitecha Finitecha Finitecha Nove Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet Soviet	Moteture Content (*More)-3 run evrg. Motecular Weight Wei (britis-mote) Motecular Weight Wei (britis-mote) Gas Weight Wei (britis-mote) Gas Flow (actim) Gas Flow (dactim) Gas Flow (dactim)-3 run average Gas Flow (wactim) Gas Flow (invactin) Gas F	29.80 28.12 18.8 63.404 29.621 34.549 2,073 35 151,273 1,644 3.5 8.8 18.6 4.59	14.3 29.82 28.13 19.7 67,148 31.301 30.696 36.500 2.190 37 150.903 1.624 3.8 18.4 4.80 4.73 0.027 0.027	29.83 28.15 19.5 66.81 31.185 36,349 2.181 36 159,321 1.607 3.8 8.9 18.5 4.80	29.84 28.19 19.1 65.062 30,889 35,862 2,139 36 156,505 1,801 3.6 9.0 18.5 4.73	13.9 29.83 20.18 20.0 60.009 32.078 31.526 37.286 2.236 37 163.530 1.616 3.8 8.9 18.4 4.96 4.96 4.96 4.96	29.82 29.18 19.8 67,581 31,610 36,864 2,217 37 162,144 1,523 3,5 8,9 16,6 4,93	29.82 28.03 19.4 65,065 28,862 36,178 2,111 35 183,559 1,827 2.5 8.9 10.8 4,74	16.1 29.81 29.03 19.2 85.324 29.692 24.279 34.572 2.992 35 152.203 1.827 3.5 8.7 19.4 4.60 4.57 0.028	29,81 29,03 18,3 62,423 28,374 33,425 2,005 33 145,895 1,827 3,5 8,8 16,2 4,35 0,027	29.83 28.05 19.2 65,407 29,810 35,116 2,107 35 153,369 1,610 2,5 8.9 1,610 2,5 8.9 1,610 2,5 8.9 1,610 2,5 8.9 1,610	14.5 14.4 29.52 28.11 19.3 95,741 30,590 25,597 2,135 38 165,773 1 821 3 524 8 953 18,495 4,71 4,72 0 027 0 027	
Norm Norm Mg Mg Ng Facrus Foccins Focc	Molecular Weight Dry (Britz-mole) Molecular Weight Weight (Britz-mole) Molecular Weight Weight (Britz-mole) Gas How (softm) Gas Flow (sortm) Cas Flow (britz-tm) Cas (sortm) NO ₂ (sortm) NO ₃ (britz-tm) NO ₃ (britz-tm) NO ₃ (britz-tm) NO ₄ (britz-tm) NO ₅ (britz-tm) NO ₆ (britz-tm) NO ₇ (britz-tm) NO ₇ (britz-tm) NO ₈ (britz-tm) NO ₈ (britz-tm) NO ₉ (britz-tm)	29.80 28.12 18.6 63.404 29.621 34.549 2,973 35 151,273 1.644 3.5 8.8 18.6 4.39	14.3 29.82 28.13 19.7 67,148 31,301 30,695 36,508 2,190 37 159,503 1,624 3.5 8.8 18.4 4.80 4.73 0.027	29.83 28.15 19.5 66.841 31.165 36.349 2.181 36 159,321 1.607 3.8 8.9 18.5 4.80 9.027	29.84 28.19 19.1 65,082 30,689 25,862 2,139 36 156,505 1,601 3.6 9.0 18.5 4,73 0,027	13.9 29.53 28.18 20.0 60,009 32,078 31,526 37,286 2,236 37,185 3,530 1,616 3.8 8.9 18.4 4.96 4.88 0,027	29.82 28.18 19.8 67,581 31,610 36.864 2,217 37 182,144 1,623 3.5 8.9 18.6 4.93	29.82 28.03 19.4 68.065 29.862 36,178 2.111 35 133,550 1.827 2.5 8.0 10.8 4.74	16.1 29.61 28.03 19.2 85,324 29.602 29.279 34.872 2.092 35 152,203 1.627 3.5 8.7 18.4 4.60 4.57 0.028	29.81 28.03 18.3 62,423 28,374 33,428 2,006 33 145,995 1,827 3.5 8.8 18.2 4.35 0.027	29.83 28.05 19.2 65,407 29.810 35.116 2,107 35 133,360 1.610 3.5 8.9 18.3 4.81 0.027	14.5 14.4 23.82 28.91 19.3 95,741 30,690 25,587 2,135 36 165,773 1 821 3 524 6 853 18.495 4.71 4.72 0 927	

Run 1

Start Time	3/4/14 9:46
Run Length	23
Stop Time	10:09

		Calibration Info		
Gas		O ₂	CO ⁵	NOx
instrument		9.8	19.7	39
Span Gas	Value	4.90	10.00	18.2
allbration	h-mtlan			
Pretest Cal	Zero%	0,1	0.0	0.0
	Span%	5.0	10.1	19.0
Post Test Ca		9.4	1441	1919
1000 1000 00	Zero%	0.0	0.0	0.0
	Span%	4.8	10.0	18.0
esults				
	ule Bias (Zero)	0.0%	0.0%	0.0%
	rte Bias (Span)	2.0%	0.5%	1.5%
	lute Drift (Zero)	1.0%	0.0%	0.0%
Absol	ute Drift (Span)	2.0%	0.5%	2.6%
		Corrected O ₂ %	Corrected CO ₂ %	Corrected NO _x ppm
		4.1	10.2	21.7
Dun I annth				
Run Length (Minutes)	Time	Uncorrected O ₂ %	Uncorrected CO ₂ %	Uncorrected NO _x ppr
(Milliotes)		4.1	10.3	22.0
0.5	9:46	4.2	10.2	22.4
1	9:46	4.2	10.2	22.4
1,5	9:47	4.0	10.2	22.2
2	9:47	4.1	10.2	22.0
2.5	9:48	4.1	10.2	21.8
3	9:48	4.1	10.2	21.8
3.5	9:49	4.0	10.2	22.0
4	9:49	4.2	10.3	22.0
4.5	9:50	4.1	10.2	22.0
5	9:50	4.1	10.3	22.0 22.0
5.5	9:51	3.9	10.4 10.3	21.8
6 6.5	9:51 9:52	4.0 4.2	10.3	22.0
7	9:52	4.1	10.2	22.2
7.5	9:53	4.1	10.2	22,4
8	9:53	4.1	10.3	22.2
8.5	9:54	4.2	10.2	22.2
9	9:54	4.0	10.2	22.2
9.5	9:55	3.9	10.3	22.2
10	9:55	4.1	10.2	22.0
10.5	9:58	4.1	10.3	22.0
11	9:57	4.1	10.3	22.0
11.5	9:57	4.1	10.3 10.3	22.2 22.2
12	9:58 9:58	4.2 4.1	10.3	22.0
12.5 13	9:59	4.0	10.3	22.0
13.5	9:59	4.1	10.3	22.0
14	10:00	4.1	10.3	22.0
14.5	10:00	4.2	10.2	22.0
15	10:01	4.2	10.2	22.0
15.5	10:01	4.1	10.3	22.2
16	10:02	4.2	10.3	22.2
16.5	10:02	4.1	10.3	22.2
17	10:03	3.9	10.3	22.0
17.5	10:03	3.9	10.3	22.2
16	10:04	4.1	10.4	22.0 22.0
18.5	10:04	4.1 4.0	10.4 10.3	22.0
19 19.5	10:05 10:05	4.0	10.3	22.0
19.5	10:05	4.2	10.3	22.0
20.5	10:06	4.1	10.3	22.0
21	10:07	4.1	10.4	21.8
21.5	10:07	4.07	10.38	21.7
22	10:08	4.16	10.29	21.49
22.5	10:08	4.01	10.28	21.7

Run 2

Start Time	3/4/14 10:20
Run Length	21
Stop Time	10:41

		Calibration in		NA
Gas		O ₂	CO ₂	NO _X
Instrument I		9.8	19.7	39
Span Gas	Value	4,90	10.00	18.2
alibration				
Pretest Calil		0.0	0.0	0.0
	Zero%			
Post Test Ca	Span%	4.8	10.0	18.0
Pust 1est Ca	Zero%	-0.1	0.1	0.0
	Span%	4.9	10.0	18.2
lesults	opaira	7.0	10.0	10.6
	Bias (Zero)	1.0%	0.5%	0.0%
	Blas (Span)	1.0%	0.5%	1.0%
	e Drift (Zero)	1.0%	0.5%	0.0%
	Drift (Span)	1.0%	0.0%	0.5%
	1	Corrected O ₂ %	Corrected CO ₂ %	Corrected NO _x ppm
	- 1	4.1	10.3	21.41
Run Length				
(Minutes)	Time	Uncorrected O ₂ %	Uncorrected CO ₂ %	Uncorrected NO _x ppm
		4,1	10.3	21.3
0.5	10:20	4.0	10.2	21.0
1	10:20	4.1	10.2	21.4
1.5	10:21	4.0	10.2	21.6
2	10:21	4.0	10.2	21.4
2.5	10:22	4.2	10.3	21.4
3	10:22	4.0 4.1	10.3 10.3	21.2 21.2
3.5	10:23	4.0	10.2	21.4
4 4.5	10:23	4.1	10.3	21.4
5	10:24 10:24	4.1	10.3	21.2
5.5	10:25	4.1	10.3	21.0
6	10:25	4.1	10.3	21.0
6.5	10:28	4.2	10.2	21.0
7	10:28	4.1	10.3	21.2
7.5	10:27	4.0	10.4	21.0
8	10:27	4.1	10.3	21.0
8.5	10:28	4.2	10.3	21.4
9	10:28	4.1	10.3	21.4
9.5	10:29	3.9	10.3	21.4
10	10:29	4.1	10.4	21.4
10.5	10:30	4.2	10.4	21.0
11	10:30	4.1	10.3	21.4
11.5	10:31	3.9	10.3	21.6
12	10:31	4.0	10.4	21.4
12.5	10:32	4.2	10.4	21.2
13	10:32	4.2	10.3	21.4
13.5	10:33	4.0	10.5	21.4
14	10:33	4.0	10.4	21.0
14.5	10:34	4.2	10.4	21.0
15	10:34	4.1	10.3	21.0
15.5	10:35	4.1	10.3	21.2
16	10:35	4.1	10.4	21.4
16.5	10:36	4.3	10.3	21.6
17	10:36	4.1	10.4	21.4
17.5	10:37	3.9	10.5	21.2
	10:37	4.1	10.4	21.2
18	10:38	4.2	10.3	21.4
18.5				
18.5 19	10:39	4.2	10.3	21.6
18.5 19 19.5	10:39 10:39	4.1	10.4	21.6
18.5 19 19.5 20	10:39 10:39 10:40	4.1 4.1	10.4	21.6 21.4
18.5 19 19.5	10:39 10:39	4.1	10.4	21.6

Run 3

Start Time	3/4/14 10:56
Run Length	22
Stop Time	11:18

		Calibration In	formation	
Gas	1	O ₂	CO ₂	NOx
Instrument F	Range	9.8	19.7	39
Span Gas \	/alue	4.90	10.00	18.2
Calibration				
Pretest Calib		A4		0.0
	Zero% Span%	-0.1	0.1 10.0	18.2
Post Test Cal		4.9	10.0	10.2
Lost Lest Car	Zero%	0.0	0.1	0.2
	Span%	4.8	10.0	18.0
Results	-			
	Bias (Zero)	0.0%	0.5%	0.5%
	Blas (Span)	2.0%	0.5%	1.5%
	Drift (Zero)	1.0%	0.0%	0.5%
Absolute	Drift (Span)	1.0%	0.0%	0.5%
	- 1	Assessed A W	Corrected CO ₂ %	Corrected NO _x ppm
	1	Corrected O ₂ %		21.5
Down & country		4.1	10.4	
Run Length (Minutes)	Time	Uncorrected O ₂ %	Uncorrected CO ₂ %	Uncorrected NO _X ppm
(4.1	10.4	21.4
0.5	10:56	4.2	10.3	21.4
1	10:56	4.2	10.4	21.6
1.5	10:57	4.0	10.4	21.6
2	10:57	4.0	10.4	21.4
2.5	10:58	4.2	10.5	21.4
3	10:58	4.1 4.1	10.4 10.4	21.4 21.6
3.5 4	10:59 10:59	4.1	10.4	21.4
4.5	11:00	4.2	10.4	21.4
5	11:01	4.0	10.4	21.4
5.5	11:01	4.1	10.4	21.4
6	11:02	4.1	10.5	21.4
6.5	11:02	4.2	10.4	21,4
7	11:03	4.1	10.3	21.2
7.5	11:03	4.1	10.4	21.4
8	11:04	4.1 4.2	10.4 10.4	21.4 21.4
8.5 9	11:04 11:05	4.1	10.4	21.6
9.5	11:05	4.0	10.5	21.6
10	11:06	4.1	10.5	21.4
10.5	11:06	4.1	10.5	21.2
11	11:07	4.0	10.5	21.6
11.5	11:07	4.0	10.4	21.4
12	11:08	4.3	10.4	21.4
12.5	11:08	4.1	10.3 10.4	21.4 21.4
13 13.5	11:09 11:09	4.0 4.0	10.4	21.0
13.5	11:10	4.1	10.5	21.0
14.5	11:10	4.1	10.5	21.2
15	11:11	4.0	10.5	21.2
15.5	11:11	4.0	10.5	21.4
16	11:12	4.1	10.5	21.4
16.5	11:12	4.1	10.5	21.6
17	11:13	41	10.5	21.6
17.5	11:13	4.0	10.5	21.4
18	11:14	4.1	10.5 10.5	21.2 21.0
18.5	11:14	4.2 4.0	10.5	21.2
19 19.5	11:15 11:15	4.1	10.4	21.6
	11,10		10.4	21.4
	11:16	4.2		
20	11:16 11:16	4.2 4.2		21.4
20.5	11:16	4.2	10.5 10.5	
20			10.5	21.4

Start Time	3/4/14 11:31
Start Time Flun Length Stop Time	22
Stop Time	11:53

		Calibration in	formation	
Gas		O ₂	COs	NOx
Instrument	Range	9.8	19.7	39
Span Gas	Value	4.90	10.00	18.2
Calibration				
Pretest Cali				
	Zero% Span%	0.0	0.1	0.2
Post Test Ca		4.8	10.0	18.0
7 001 7001 00	Zero%	-0.1	0.1	0.2
	Span%	4.8	10.0	16.0
Results				
	Blas (Zero)	1.0%	0.5%	0.5%
	Bias (Span)	2.0%	0.5%	1.5%
	Drift (Zero)	1.0%	0.0%	0.0%
Absolute	Drift (Span)	0.0%	0.0%	0.0%
		Corrected O ₂ %	Corrected CO ₂ %	Corrected NO _x ppm
		4.2	10.4	21.5
Run Length				
(Minutes)	Time	Uncorrected O ₂ %	Uncorrected CO ₂ %	Uncorrected NO _x ppm
	1	4.1	10.4	21.3
0.5	11:31	4.1	10.3	21.2
1.	11:31	4.0	10.3	21.2
1.5	11:32 11:32	4.2 4.2	10.4 10.4	21.6 21.2
2 2.5	11:32	4.2	10.4	21.2
3	11:33	4.0	10.4	21.2
3.5	11:34	4.2	10.5	21.2
4	11:34	4.2	10.4	21.4
4.5	11:35	4.1	10.4	21.6
5	11:35	4.1	10.5	21.6
5.5	11:36	4.1	10.5	21.6
6	11:36	4.1	10.5	21.4
6.5 7	11:37 11:37	4.1 4.1	10.5 10.5	21.0 21.2
7.5	11:38	4.2	10.4	21.4
8	11:38	4.1	10.3	21.4
8.5	11:39	4.0	10.3	21.2
9	11:39	4.2	10.3	21.6
9.5	11:40	4.3	10.4	21.6
10	11:40	4.2	10.4	21.6
10.5 11	11:41 11:41	3.9 4.0	10.5 10.6	21.2 21.2
11.5	11:42	4.2	10.6	21.2
12	11:43	4.2	10.4	21.4
12.5	11:43	4.0	10.5	21.2
13	11:44	4.1	10.4	21.4
13.5	11:44	4.2	10.4	21.4
14	11:45	4.1	10.5	21.4
14.5	11:45	3.9	10.5	21.2
15 15.5	11:46 11:48	4.0 4.0	10.5 10.5	21.0 21.2
16.5	11:40	4.0	10.5	21.0
16.5	11:47	4.1	10.5	21.0
17	11:48	4.0	10.5	21.0
17.5	11:48	4.1	10.5	21.0
18	11:49	40	10.4	21.0
18.5	11:49	4.1	10.4	21.2
19	11:50	4.1	10.4	21.4
19.5	11:50	4.1	10.5	21.4
20	11:51	4.1	10.4	21.2
20.5	11:51	4.1	10.4	21.2
21 21.5	11:52 11:52	4.1 4.4	10.3 10.3	21.2 21.4
22	11:53	4.1	10.4	21.4
	1100	-0.0 0	4.654	-107

	Run 5
--	-------

Start Time	3/4/14 12:03
Run Length	21
Stop Time	12:24

		Calibration in	formation	
Gas		O ₂	CO2	NO _x
Instrument I	Range	9.6	19.7	39
Span Gas	Value	4.90	10.00	18.2
Calibration				
Pretest Calil				
	Zero%	-0.1	0.1	0.2
	Span%	4.8	10.0	18.0
Post Test Cal	Zero%	0.0	0.1	0.0
	Span%	4.9	10.0	18.0
Results	Sparra	7.0	10.0	10.0
Absolut	e Blas (Zero)	0.0%	0.5%	0.0%
	Blas (Span)	1.0%	0.5%	1.5%
	e Drift (Zero)	1.0%	0.0%	0.5%
Absolute	Orift (Span)	1.0%	0.0%	0.0%
	- (Corrected O ₂ %	Corrected CO ₂ %	Corrected NO _X ppm
		4.1	10.4	21.6
Run Length (Minutes)	Time	Uncorrected O ₂ %	Uncorrected CO ₂ %	Uncorrected NO _X ppn
<u>,</u>		4.1	10.4	21.3
0.5	12:03	4.0	10.4	21.6
1	12:03	4.1	10.4	21.6
1.5	12:04	42	10.3	21.4
2	12:05	4.2	10.4	21.4
2.5	12:05	4.1	10.4	21.2
3	12:06	4.2	10.4	21.2 21.2
3.5	12:08	4.3	10.3 10.4	21.2
4 4.5	12:07 12:07	4.1 4.1	10.4	21.2
5	12:08	4.2	10.4	21.0
5.5	12:08	4.4	10.4	21.4
8	12:09	4.2	10.3	21,8
6.5	12:09	4.0	10.3	21.6
7	12:10	4.2	10.4	21.4
7.5	12:10	44	10.4	21.4
8	12:11	4.1	10,4	21.2
8.5	12:11	4.0	10.4	21.2
9	12:12	4.2	10.4	21.2
9.5	12:12	43	10.3	21.4
10	12:13	4.2	10.3	21.0
10.5	12:13	4.2	10.3 10.4	20.8 21.2
11 11.5	12:14 12:14	4.2 4.4	10.4	21.2
11.5	12:14	4.1	10.4	21.2
12.5	12:15	3.8	10.4	21.4
13	12:16	39	10.4	21.2
13.5	12:18	4.0	10.4	21.2
14	12:17	3.8	10.3	21.2
14,5	12:17	4.0	10.4	21.2
15	12:18	4.0	10.3	21.6
15.5	12:18	4.0	10.4	21.4
16	12:19	3.9	10.4	21.2
16.5	12:19	4.0	10.4	21.2
17	12:20	4.1	10.3	21.0
17.5	12:20	4.0	10.4	21.4
18	12:21	3.9	10.4	21.4
18.5	12:21	3.9	10.4	21.8
19	12:22	4.0	104	21.8 22.0
19.5	12:22	4.0	10,4 10,4	21.6
20 20.5	12:23 12:23	3.8 3.9	10.4	21.6
20.5	12:23	4.1	10.4	21.4
61	16.29	7.1	107	21.4

Run 6

Start Time	3/4/14 12:33
Run Length	21
Stop Time	12:54

C		Calibration in		NO _x
Gas		O ₂	CO ₂	
instrument F		9.8	19.7	39
Span Gas \	Value	4.90	10.00	18.2
alibration				
Pretest Calib			***	
	Zero%	0.0	0.1	0.0
D T	Span%	4.9	10.0	18.0
Post Test Cal	Zero%		0.1	-0.2
		-0.1		
tesults	Span%	4.9	10.0	17.8
	Blas (Zero)	1.0%	0.5%	0.5%
	Blas (Span)	1.0%	0.5%	2.1%
	Drift (Zero)	1.0%	0.0%	0.5%
	Drift (Span)	0.0%	0.0%	0.5%
nognata	Olit (Opari)	0.076	0.076	0.070
		Corrected O ₂ %	Corrected CO ₂ %	Corrected NO _x ppm
		4.1	10.4	21.7
Run Length				
(Minutes)	Time	Uncorrected O ₂ %	Uncorrected CO ₂ %	Uncorrected NO _X ppr
		4.1	10.4	21.3
0.5	12:33	3.9	10.4	21.2
1	12:33	3.9	10.4	21.2
1.5	12:34	4.0	10.4	21.4
2	12:34	4.2	10.4	21.2
2.5	12:35	4.0	10.5	21.6
3	12:35	4.0	10.4	21.4
3.5	12:36	4.1	10,4	21.4
4	12:36	4.2	10.5	21.2
4.5	12:37	4.0	10.5	21.2
5	12:37	4.0	10.5	21.4
5.5	12:38	4.1	10.4	21.6
6	12:38	4.1	10.4	21.4
8.5	12:39	4.0	10.5	21.0
7	12:39	4.0	10.4	21.2
7.5	12:40	4.2	10.4	21.2 21.4
8	12:40	4.1	10.4 10.4	21.4
8.5	12:41	3.9	10.5	21.0
9	12:41	4.0	10.8	21.0
9.5	12:42	4.0 4.0	10.4	21.2
10	12:42	4.0	10.4	21.0
10.5	12:43	4.0	10.4	21,2
11 11.5	12:43 12:44	4.1	10.4	21.2
11.5	12:44	4.1	10.4	21.4
12.5	12:45	4.0	10.4	21.4
13	12:45	4.0	10.5	21.2
13.5	12:46	4.1	10.5	21.4
14	12:47	4.1	10.4	21.4
14.5	12:47	3.9	10.3	21.4
15	12:48	4.0	10.3	21.4
15.5	12:48	4.4	10.3	21.8
18	12:49	4.0	10.4	21.8
18.5	12:49	3.9	10.4	21.2
17	12:50	4.0	10.3	21.2
17.5	12:50	4.2	10.2	21.2
18	12:51	4.1	10.2	21.4
18.5	12:51	4.0	10.2	21.6
19	12:52	4.2	10.2	21.6
19.5	12.52	4.2	10.2	21.2
20	12:53	4.1	10.2	20.8
20.5	12.53	4.1	10.2	21.0
20.5	12:54	41	10.1	22.2
61	16.134	4.1	10.1	#e-e

Frontier Retining LLC Frontier Retinery Cheyenne, Wyoming Crude Charne Heater

Frontier Refinery	1				
Cheyenne, Wyon	ning		Start Time	3/4/14 13:02	
Crude Charge He 13/04/14	enter		Run Length Stop Time	23 13:25	
larum em			GIOD TIME	1323	
		Calibration to			
Gan		O ₂	CO2	NOx	
instrument i		9.8	19.7	39	
Span Gas \ Calibration	Value	4.90	10.00	18.2	
Protest Cali	hration				
r retout cam	Zaro%	-0.1	0.1	-0.2	
	Span%	4.9	10.0	17.8	
Post Test Ca					
	Zero%	0.0	0.1	-0.4	
Danilla	Span%	4.9	10.0	17.8	
Results Absolute	Bias (Zero)	0.0%	0.5%	1.0%	
	Bias (Span)	1.0%	0.5%	2.1%	
	Drift (Zero)	1.0%	0.0%	0.5%	
Absolute	Drift (Span)	0.0%	0.0%	0.0%	
		0	Damastad DO W	Corrected NO _x ppm	
		Corrected O ₂ %	Corrected CO ₂ %	22.2	
Dun Lameth		4.1	10.3		
Run Length (Minutes)	Time	Uncorrected O ₂ %	Uncorrected CO ₂ %	Uncorrected NO _x ppn	
(manufactura)	-	4.1	10.3	21,8	
0.5	13:02	4.2	10.2	22.0	
1	13:02	4.0	10.4	21.6	
1.5	13:03	3.9	10.4	21.4	
2	13:03	4.0	10.3	21.6	
2.5	13:04	4.2	10.3	21.8 22.0	
3 3.5	13:04 13:05	4.1 4.0	10.3 10.3	21.8	
4	13:05	4.0	10.3	22.2	
4.5	13:06	4.2	10.4	22.2	
5	13:06	4.1	10.5	22.2	
5.5	13:07	4.0	10.5	22.0	
6	13:07	4.1	10.4	22.0	
6.5	13:08	4.1	10.4	22.2 22.4	
7 7.5	13:09 13:09	4.0 3.8	10.3 10.4	22.1	
6	13:10	4.0	10.4	22.0	
8.5	13:10	4.1	10.5	21.6	
9	13:11	3.9	10.4	21.2	
9.5	13:11	4.0	10.4	21.6	
10	13:12	4.1	10.4 10.5	21.4 21.6	
10.5 11	13:12 13:13	4.3 4.0	10.4	21.2	
11.5	13:13	4.0	10.4	21.6	
12	13:14	4.1	10.3	21.8	
12.5	13:14	4.2	10.4	22.0	
13	13:15	4.0	10.3	21.4	
13.5	13:15	4.0	10.3	21.6	
14 14 E	13:16	4.1 4.2	10.3 10.3	21.6 21.8	
14.5 15	13:16 13:17	4.1	10.4	22.0	
15.5	13:17	4.1	10.3	21.4	
16	13:18	4.2	10.2	21.6	
16.5	13:18	4.2	10.3	22.0	
17	13:19	4.1	10.2	21.8	
17.5	13:19	4.1	10.3	21.8	
18	13:20	4.2 4.1	10.3 10.2	21.6 21.6	
18.5 19	13:20 13:21	4.0	10.3	21.8	
19.5	13:21	4.1	10.3	21.8	
20	13:22	4.2	10.3	21.6	
20.5	13:22	4.2	10.2	22.0	
21	13:23	4.1	10.2	21.8	
21.5	13:23	4.1	10.4	21.8	
22	13:24	4.1	10.2	21.6	
22.5 23	13:24	4.3 4.0	10.3 10.3	21.4 21.8	
43	13:25	4.0	10.3	41.0	

Run 8

Start Time	3/4/14 13:33
Run Length	22
Stop Time	13:55

	Calibration Information					
Gas		O ₂	CO ⁵	NO _X		
Instrument		9.8	19.7	39		
Span Gas	Value	4.90	10.00	18.2		
Calibration	handler 1					
Pretest Call	Zero%	0.0	0.1	-0.4		
	Span%	4.9	10.0	17.8		
Post Test Ca						
	Zero%	-0.1	0.1	-0.2		
	Span%	4.9	10.0	18.0		
Results		142	0.004	0.60		
	Blas (Zero)	1.0%	0.5%	0.5%		
	Bias (Span) Brift (Zero)	1.0%	0.0%	0.5%		
	Drift (Span)	0.0%	0.0%	0.5%		
7 - 4 - 4 - 4 - 4 - 4 - 4 - 4 - 4 - 4 -		4.576				
		Corrected O ₂ %	Corrected CO ₂ %	Corrected NO _x ppm		
		4.1	10.3	21.7		
Run Length (Minutes)	Time	Uncorrected O ₂ %	Uncorrected CO ₂ %	Uncorrected NO _X ppm		
		4.1	10.3	21.4		
0.5	13:33	4.1	10.3	21.5		
1	13:33	4.1	10.4	21.2		
1.5	13:34	4.3	10.3	21.2		
2	13:34	4.2	10.3 10.4	21.6 21.2		
2.5	13:35 13:35	4.1 4.0	10.4	21.0		
3 3.5	13:36	4.2	10.3	21.4		
4	13:36	4.2	10.3	21.8		
4.5	13:37	4.1	10.3	21.8		
5	13:37	4.2	10.3	21.6		
5.5	13:38	4.1	10.3	21.4		
6	13:38	43	10.3	21.4		
6.5	13:39	41 4.1	10.3 10.2	21.6 21.6		
7 7.5	13:39 13:40	4.2	10.2	21.8		
8	13:40	4.2	10.4	21.6		
8.5	13:41	4.1	10.3	21.4		
9	13:41	4.2	10.3	21.4		
9.5	13:42	4.3	10.3	21.4		
10	13:42	4.2	10.3	21.4		
10.5	13:43	4.2	10.3 10.3	21.4 21.4		
11 11.5	13:43 13:44	4.1 4.2	10.3	21.6		
12	13:44	4.2	10.3	21.4		
12.5	13:45	4.1	10.3	21.2		
13	13:45	4.0	10.2	21.4		
13.5	13:46	4.2	10.3	21.4		
14	13:46	4.1	10.3	21.6		
14.5	13:47	4.0	10.3	21.2		
15	13:47	4.1	10.3 10.2	21.4 21.2		
15.5 16	13:48 13:48	4.2 4.1	10.2	21.4		
16.5	13:49	4.1	10.3	21.4		
17	13:49	4.1	10.3	21.6		
17.5	13:50	4.2	10.3	21.6		
18	13:51	4.2	10.3	21.4		
18.5	13:51	4.1	10.2	21.4		
19	13:52	4.2	10.3	21.6		
19.5	13:52	4.2	10.3	21.6 21.4		
20	13:53	4.1	10.3 10.3	21.4		
20.5	13:53 13:54	4.0 4.2	10.3	21.6		
21 21.5	13:54	4.2	10.3	21.4		
22	13:55	4.2	10.3	21.0		
-	, Jane	*****				

un

Start Time	3/4/14 14:04
Run Length	21
Stop Time	14:25

		Calibration In	formation	
Gas		O ₂	CO2	NO _X
	innon F	9.8	19.7	39
Instrument Range Span Gas Value		4.90	10.00	18.2
calibration	-	7100	10:00	14.2
Pretest Calib	ration			
T Tujuni Omio	Zero%	-0.1	0.1	-0.2
	Span%	4.9	10.0	16.0
Post Test Cali				
	Zero%	0.0	0.1	-0.4
	Span%	4.9	10.0	17.8
lesults	-,			
	Blas (Zero)	0.0%	0.5%	1.0%
	Blas (Span)	1.0%	0.5%	2.1%
	Drift (Zero)	1.0%	0.0%	0.5%
	Drift (Span)	0.0%	0.0%	0.5%
	1	Corrected O ₂ %	Corrected CO ₂ %	Corrected NO _x ppm
	1	4.1	10.3	21.4
Run Length				
	Time	Uncorrected O ₂ %	Uncorrected CO ₂ %	Uncorrected NO _X ppm
(Minutes)		44	10.3	21.1
0.0	1464	4.1	10.4	21.2
0.5	14:04	4.2	10.3	21.4
1	14:04	4.1	10.3	21.4
1.5	14:05	4.2	10.4	21.8
2	14:05	4.1 4.1	10.4	21.2
2.5	14:08		10.4	21.4
3	14:06 14:07	4.2 4.1	10.3	21.0
3.5		4.1	10.3	21.8
4	14:07	4.2	10.3	21.2
4.5	14:08 14:08	4.2	10.3	21.2
5		4.0	10.3	21.2
5.5	14:09 14:09	4.1	10.3	21.0
6		4.2	10.2	21.2
6.5	14:10	4.1	10.2	21.4
7	14:10	4.1	10.3	21.2
7.5	14:11 14:11	4.2	10.3	21.2
8 8.5	14:12	4.2	10.4	21.0
9	14:13	4.0	10.3	21.2
9.5	14:13	4.1	10.3	21 2
	14:14	4.4	10.2	21.0
10 10.5	14:14	4.3	10.4	21.2
11	14:15	4.1	10.3	21.0
11.5	14:15	4.1	10.2	21.2
12	14:16	4.2	10.2	21.2
12.5	14:16	4.2	10.3	21.4
13	14:17	4.1	10.4	20.6
13.5	14:17	4.1	10.3	20.8
14	14:18	4.1	10.3	21.0
14.5	14:18	4.2	10.3	21.2
15	14:19	4.1	10.4	21.2
15.5	14:19	4.0	10.3	21.0
18	14:20	4.1	10.3	20.8
	17.20		10.3	21.2
	14-20	4.1		
16.5	14:20	4.1		21.2
16.5 17	14:21	4.1	10.3	21.2 21.2
16.5 17 17.5	14:21 14:21	4.1 4.1	10.3 10.3	21.2
16.5 17 17.5 18	14:21 14:21 14:22	4.1 4.1 4.1	10.3 10.3 10.3	21.2 21.2
16.5 17 17.5 18 18.5	14:21 14:21 14:22 14:22	4.1 4.1 4.1 4.2	10.3 10.3 10.3 10.4	21.2 21.2 21.0
16.5 17 17.5 18 18.5 19	14:21 14:21 14:22 14:22 14:23	4.1 4.1 4.1 4.2 4.0	10.3 10.3 10.3 10.4 10.3	21.2 21.2 21.0 21.0
16.5 17 17.5 18 18.5 19	14:21 14:21 14:22 14:22 14:23 14:23	4.1 4.1 4.1 4.2 4.0 4.0	10.3 10.3 10.3 10.4 10.3 10.3	21.2 21.2 21.0 21.0 21.0
16.5 17 17.5 18 18.5 19 19.5 20	14:21 14:21 14:22 14:22 14:23 14:23 14:24	4.1 4.1 4.1 4.2 4.0 4.0 4.2	10.3 10.3 10.3 10.4 10.3 10.3	21.2 21.2 21.0 21.0 21.0 21.0
16.5 17 17.5 18 18.5 19	14:21 14:21 14:22 14:22 14:23 14:23	4.1 4.1 4.1 4.2 4.0 4.0	10.3 10.3 10.3 10.4 10.3 10.3	21.2 21.2 21.0 21.0 21.0

Bun	10
23044	

Start Time	3/4/14 14:40
Run Length	21
Stop Time	15:01

		Calibration in		
Gas		O ₂	CO3	NO _X
Instrument F	Range	9.8	19.7	39
Span Gas Value		4.90	10.00	18.2
Calibration Protest Calib	ration			
1 101031 0311	Zero%	0.0	0.1	-0.4
	Span%	4.9	10.0	17.8
Post Test Cal				
	Zero%	-0.1	0.1	0.0
	Span%	5.0	10.0	17.8
esuits				
	Blas (Zero)	1.0%	0.5%	0.0%
	Blas (Span)	0.0%	0.5%	2.1%
	Drift (Zero)	1.0%	0.0%	1.0%
	Drift (Span)	1.0%	0.0%	0,0%
		Corrected O ₂ %	Corrected CO ₂ %	Corrected NO _x ppm
Don Lameth	.,	4.1	10.4	21.8
Run Length (Minutes)	Time	Uncorrected O ₂ %	Uncorrected CO ₂ %	Uncorrected NO _X ppr
		4.1	10.4	21.2
0.5	14:40	4.1	10.4	21.3
1	14:40	4.2	10.5	21.2 21.2
1.5	14:41	4.0	10.4	
2	14:41	4.0	10.5	21.0
2.5	14:42	4.2	10.5	21.0
3	14:42	4.1	10.4	21.2
3.5	14:43	4.1	10.5	21.4
4	14:43	4.1	10.4	21.6
4.5	14:44	4.2	10.5	21.8
5	14:44	4.1	10.5	21.4 21.4
5.5	14:45	40	10.5	
6	14:45	4.0	10.5	21.0 21.2
6.5	14:46	4.3	10.4	21.4
7	14:46	4.3	10.4	21.4
7.5	14:47	4.1	10.5 10.5	21.4
8	14:47	4.0	10.5	21.0
8.5	14:48	4.1	10.8	21.2
9	14:48	4.1	10.4	21.4
9.5	14:49	4.1	10.4	21.2
10	14:49	4.0 4.3	10.4	21.2
10.5	14:50		10.4	20,8
11	14:50	4.1 4.1	10.4	21.0
11.5	14:51	4.2	10.4	21.0
12 12.5	14:51 14:52	4.4	10.3	20.8
	14:52	4.2	10.5	21.0
13 13.5	14:53	4.0	10.5	21.0
13.5	14:53	4.1	10.4	21.2
14.5	14:54	4.2	10.4	21.0
15	14:55	4.2	10.4	21.2
15.5	14:55	4.0	10.5	21.0
		4.2	10.4	21.0
16 18.5	14:56 14:56	4.2	10.4	21.2
		4.2	10.4	21,2
17	14:57 14:57	4.2	10.4	21.2
17.5			10.4	20.6
18	14:58	4.0		21.0
	14:58	4.3	10.4	
18.5		A 4		
18.5 19	14:59	4.1	10.4	21.0
18.5 19 19.5	14:59 14:59	4.1	10.4	21,2
18.5 19	14:59			



EPA Methods 1-4: Determination of Stack Gas Velocity and Volumetric Flow Rate

Sample Calculations

EPA Methods 1-4: Determination of Stack Gas Velocity and Volumetric Flow Rate

Sample Calculations (continued)

gas velocity (lifesc) =
$$85.49 \, ^{\circ} \, ^{\circ$$

EPA Methods 1-4: Determination of Stack Gas Velocity and Volumetric Flow Rate

Variables and Abbreviations

Bws - moisture content of the gas (wet volume percent/100)

%CO - carbon monoxide content of the gas (dry volume percent)

%CO2 - carbon dioxide content of the gas (dry volume percent)

Co - pitot tube constant (unitiess)

D_S - diameter of the stack (inches)

ΔH - pressure differential at dry gas meter exit orifice (inches water)

Mp - molecular weight of the dry gas (grams per mol)

MA - molecular weight of the wet gas (grams per mol)

%N2 - nitrogen content of the gas (dry volume percent)

%O2 - oxygen content of the gas (dry volume percent)

Pave - average square root of the stack gas pilot differential pressure (inches water)

P_B - barometric pressure (inches mercury)

Ps - stack pressure relative to barometric presure (inches water)

P_{STD} - standard pressure (29.92 inches mercury)

T_M - average dry gas meter temperature (°F)

T₆ - average stack temperature (°F)

T_{STD} - standard temperature (528 °R)

Vic - volume of moisture collected as a liquid (milliliters)

V_M - volume indicated on dry gas meter (uncorrected actual cubic feet)

V_{MSTD} - volume of gas through dry gas meter (corrected dry standard cubic feet)

Vs - stack gas velocity (feet per second)

V_{WEID} - volume of moisture collected as a gas at standard conditions (standard cubic feet)

Y_D - dry gas meter calibration factor (unitless)

EPA Method 3A: Determination of O_2 / CO_2 Concentrations in Emissions from Stationary Sources (*Instrumental Analyzer Procedure*)

Sample Calculations

Variables and Abbreviations

cal - calibrated

conc - concentration

CO2 - Carbon Dioxide

O₂ - Oxygen

%FS_{SPAN} - average analyzer reading for span gas (percent of full scale)

%FS_{STACK} - average analyzer reading for stack gas (percent of full scale)

%FS₀ - average analyzer reading for zero gas (percent of full scale)

%vd- dry volume percent

EPA Method 7E: Determination of Nitrogen Oxides Emissions from Stationary Sources (Instrumental Analyzer Procedure)

Sample Calculations

Variables and Abbreviations

cal - calibrated

conc - concentration

FDSCFM - gas flow (dry standard cubic feet per minute, where standard = 29.92 Inches Hg and 68oF)

%FS_{SPAN} - average analyzer reading for span gas at probe tip (percent of full scale)

%FS_{STACK} - average analyzer reading for stack gas (percent of full scale)

%FS_n - average analyzer reading for zero gas at probe tip (percent of full scale)

lb/hr - pounds per hour

ppmvd - parts per million, dry volume basis

lb/MMBtu - pounds per million British thermal units

Appendix 2

Field Data

Poor Quality Source Document

The following document images have been scanned from the best available source copy.

To view the actual hard copy, contact the Region VIII Records Center at (303) 312-6473.

Air Pollution Testing, Inc.: Analyzer Calibration Datasheet

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Facility:	rate Pelin	ins acc		DOT ILL A	3.14/14	
Location :	heyenme, L	/X			CRC 3531	
Unit:	Liede Clark	f Hodel -		Page #		
	`			42		
		Analy	yzer Inform	ation		
Analyzor Typo		(0)	MOx			
Analyzer ID#	1-120 6-1	1415 6-4	421-1			
Analyzer Scale	6-25	0.20	0-200			
Celibration Range	0-9.83	0-19.7	0-38.9		<u> </u>	I
-						
	C	alibration G	as Cylinde	r Informatic	on	
	(Cylinde	er ID#Expir	ation date a	and Concer	ntration)	
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Expiration date						
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Expiration date	व्राह्म	25/21				
Mid	9.83	10.0	18.2			
CC#	162200	112200	AALO 73323			
Expiration date	12/5/21	12/5/21	10/1/110			
High	21.1	19.3	38 <u>9</u>			
CC#	ALMID 826.11	AL MUDE Z 2611	ALMO411779			
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	Delta P	Ts.	Notes	Point #	Delta P	Te	Notes	Point #	Delta P	Ts	Notes
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2	-05	312		2	.05	312		2	-05	313	
3	. 05	312	1	3	.05	313		3	.05	313	
ч	.07	312		4	-09	315		u	-07	313	1
1 - 17	.01	312		2-1	1.11	313		2-1	.10	315.	
ኔ	. 10	312		1	-09	313		1	es.	315	
3	. ০%	312		3	.03	314		3	67	315	
U	.07	312		ч	-07	314		4	-05	315	
} - 1	. o≤	312	i	3-1	.05	314		3-1	-05	315	
1	.05	3172	i	1	.05	314		2	-06	BiS	
3	.08	312	<u> </u>	3	. 67	314		3	01.	315	
4	.10	312		4	.12	314	 	4		3:5	
4.1	.05	312		4-1	1.05	314	 	4-3	-10	319	
<u> </u>	.05	512	+	1	.05	315	-		-05	1314	
3	.05	318		3	.05	315	 	3	.67	1 37.9	
<u>,</u>	.07	1312	\	4		345	+	1 4			
<u> </u>		1.01.0	<u> </u>	 	.06	72)	 	+ -	-06	314	
	<u> </u>		<u> </u>	 	+	1		 	 	+	
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	i	 	 	 	 		 	+		-	
*****	<u> </u>	1	 	 	-1	+	 		+	+	
	 	!	-	† 	 	 		<u> </u>		1	
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	1		-		<u> </u>	,	4			+	
	(A)	12.08	-	+	do actió	100 3	 		STATE:	1	
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	1.2425	•*), [—]			-				Reviewers S	-	

FRO 3331 R 4-6-

	7 150		r Poliution	Testing in	· EDA M		had Turnsmun	o Dotosho	at .		
lob#:		FRa 333			ZCH / SI				eter (Inches) :		102"
aclity:		Econie -			de Chier		•		Heturbance (in	ches): 🚗	20 (240
Date :		3-4-14	1	Points :	18.3	\$	9	Downstread	n Disturbance	(inches) : ~	1 Co Usan
Probe ID :		P. 577			215.7	6	10		of Sampling Le		180 110-0
Pitot Consta	nt ·	837			3.24.8	7	11				
	- •				438.0	8	12	,			
Run#:4				Run#:5				Run#: 6			
	COAS	CO2%:	COAS	02% :	LAGS	CO2% :	CNAS	02%:	LDAS	CO2%:	CDAS
	COAS		estimate 🚜	H20% :	LDAL	measured /		H2O%:	CDAS	measured /	
	.1		1012 807				10/2.807			Pb (mbar):	
Start Time :				Start Time :		Stop Time :		Start Time		Stop Time :	
		ck Good? : 0				ck Good? :	1.0 D 2H16		itot Leak Che		
Point #	Delta P	Ts	Notes	Point #	Delta P	Ts	Notes	Point#	Delta P	Ts.	Notes
1.	0 Y	307		- 1-1	.65	308		1-1	.05	349	
λ	,04.	307		1	.05	308		2	.06	305	
3	, 0 (,	507	Ţ	3	.05	308		3	.06	209	
ч	1.05	307	1	4	1.05	308		4	.07	309	İ
2 · 1	65	308	1	2-1	.05	308		2-1	.05	3.8	
λ	.05	308		2	.05	508		2	.05	308	1
3	.85	308		3	1.05	308		3	.07	358	
4	104	308	Ì	4	.64	307		4	105	309	
<u> </u>	.55	309		3-1	-68	309		3-1	-09	309	Ì
1	.87	368		1	-10	309		1	109	309	
<u> </u>	10	368		3	.13	309	<u> </u>	1 3	10	310	
4	.67	308	i	4	-08	309		4	• 07	760	ĺ
4 1	05	309		4-1	1.05	309		4-1	.05	310	
2	. 09	301		2	-10	709		1	-07	311	
3	1.05	309	i	3	, to	310	†	3	-07	311	
4	1.11	308	i	4	-10	310		4 4	.01	311	
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	<u> </u>			1		1					-
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					Ti Ti	1	 			†	
	i.		Ì				1			†	
	1							1		1	
	1	de	2				/ 	 			`
Averages	(D.2499)	307.9	7	Averages:	(.2613)	308.7		Averages:	(25727	367.3	
								hannahan :	-446214	1.40 1.2/	I

	0 333	Ai	r Pollution	Testing in	L : EPA Me	thod 2 - Pi	tot Travers	a Datashar	ıt		
ob#		380 333			JUH /				ter (Inches) :	·	102
acility :		5 (0 m) - 4 C					`		sturbance (in	chas): ~	20' 240
)ate :		3-61-14		Points:	18.5		9		Disturbance		150' (1400
Probe ID :		7-577			2 16-7	8	10		f Sampling Lo		-44-44-4
Pitot Consta	int .	437			3 24.8	7	11				
					4 85-0		12				
Run # : 7				Run # : 8				Run#: 9			
· ·	LDAS	CO2% .	LOAS	02% :	CDAS	CO2% :	CDAS	02%:	CDAS	CO2%:	CDA!
120% :	LAGS	measured /	estimate		LDAS	measured /	estimate	H2O%:		measured /	
Ps ("H2O) :		Pb (mbar):	10/2 807	Ps ("H2O) :		Pb (mbar):	1012 807			Pb (mbar):	
Start Time :		Stop Time:		Start Time:		Stop Time :		Start Time :		Stop Time :	
Post Test P	itot Leak Che	ck Good?:				ck Good? : o	0 D 2 H 10	Post Test P	itot Leak Che	ck Good? :	0.04211
Point #	Della P	T8	Notes	Point #	Defta P	Ts	Notes	Point#	Delta P	Ts	Notes
1. 1	1.05	330		1- 1	20	378		1-1	.03	325	
3	07	330		1	.06	128		2	که.	325	
<u> </u>	07	פננ		3	06	328		3	.04	325	
4_	06	330		4	.07	328		4	که.	יאנ	.1
4-1	. or	3 30		2.1	as	728		2.1	.05	ງນ	
λ	os -	330		2	05	3.28		2.	.05	325	
>	104	330			.09	328		3	.07	325	
Ч	1 05	330		4	1	328		7		326	
3-1	06	330		5-1	.05	3.28		3-1	.05	326.	
7	1.08	330	1	2	03	3a7		2	. a6	326	'
. }	08	330		1 5	که.	327)	.06	326	1
ч	1.07	1336		4	26	353		ч	.08	326	
61-1	10.	330	1	4-1	.04	728		4-1	ar	326	
٦	J . 1	1350		1	.04	328		l	20.	326	
>	1.08	330	1	5	.63	358		3	Qs"	326	
4	o's"	1330	1	4	.07	328		. 4	07	326	
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ERO 3331 R10-12 -

ob#:		FRO 33		Operator :	ZC#\	lethod 2 - Pi ్లు		Stack Diame		:	102
acility:	Č	564.00			is Che		•	Upstream D		inches) :	-20' (240
Date :		3.4.14	7	Points:	18.3	5	9	Downstream	n Disturbanc	e (inches) :	2 153 (1800)
Probe ID :		P-577			215.7		10	Schematic o	of Sampling	Location:	
Pitot Consta	nt :	.837			3 24.8		11				
,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,				1	4 % 0	8	12	1			
Run #: 10	·····			Run#: 1\				Run #: 12			
	COAS	CO2%:	CDAS	02% :	CDAL	CO2% :	CDAT	02%:	CDAS	CO2%:	LDAS
	LDAS	measured /		H2O% :		measured /		H20%:	CDAS		
Ps ("H2O)								Ps ("H2O) :		Pb (mbar)	
Start Time:		Stop Time :	18:67	Start Time		_Stop Time:		Start Time		Stop Time	
	tot Leak Che		11170	Post Test F	itot Leak Ci	neck Good?:	,	Post Test F	itot Leak Cl	Stop Time neck Good? :	•
Point #	Delta P	Ts	Notes	Paint#	Delta P	T8	Notes	Point #	Delta P	7 8	Notes
1- 1	04	322		1- 1		i		1- 1			
1	.05	321	<u> </u>	2	1		†	1	İ		1
	.05	322	İ.	3	 		† 	3	 		
- (.05	322		ч	İ			4			<u> </u>
2 - 1	· · · · · · · · · · · · · · · · · · ·	324		2.1	T		İ	2-1	<u> </u>		
<u> </u>	1 -06	324	1	1			1	1	<u> </u>		
5	-08	324	1	3			1	- 3	1		
4	.11	323		4	- 			1 4			
3-1	.05	323		3-1				3-1		1	
1	,67	323		1 2		- 	-	1			
3	-57	324		3			 	1-3-			-
- 1	1,09	329	<u> </u>	ų ų				4	+		
4-1	1.04	325		4-1				4-1		_	
1	1.04	325	1	1	 		-	1	1		
	1.06	1 325		3			+	13			
<u>-1</u>	1.10	325	<u> </u>	4			+	" 'u			
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	()	The state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the state of the s	L.1	procession :				WARES			

Converter Efficiency Test

40 CFR Part. 60, Appendix A, Method 7E, Seciton 16.2

16.2 - Alternative NO₂ to NO Conversion Efficiency Procedures.

16.2.2 – Add gas from the mid-level NO in N_2 calibration gas cylinder to a clean, evacuated, leak-light Tedlar bag. Dilute this gas approximately 1:1 with 20.9% O_2 , purified air. Immediately attach the bag outlet to the calibration valve assembly and begin operation of the sampling system. Operate the sampling system, recording the NO_2 response, for at least 30 minutes. If the NO_2 to NO conversion is 100%, the instrument response will be stable at the highest peak value observed. If the response at the end of 30 minutes decreases more than 2.0% of the highest peak value, the system is not acceptable and corrections must be made before repeating the check.

Date of Test:	3/4/14		
Analyzer Type:			
Analyzer S/N:	<u> 42C-1</u>		
Span Value:	38.9		
Mid-Level Gas Concentration:	18.2		
Start of Test	:	After 30 N	finutes:
Time:	1516 1511	Time:	1541
NO _x High Peak Response:	9.41	NO, Final Response:	9.40
NO Response:	9.21	NO Response:	7.01
		NO _x % Decrease:	0.1 %
40 CFR Part. 60, Appendix A,	Method 7E, Seciton	12.9, Equation 7E-9	
. % Decrease		- NO _X Final Peak	

Appendix 3
CEMS Data

Frontier Refining LLC Data for 3/4/2014 9:46 AM thru 3/4/2014 10:09 AM

Timestemp	(Crude Charge Heater) NOx ppm 1-Min	(Crude Charge Heater) NOx ppm @15% O2 1-Min	(Crude Charge Heater) NOx Ib/mmBtu 1-Min	(Crude Charge Heater) NOx lb/hr 1-Min Avg	(Crude Charge Heater) 02% 1-Min	(Crude Charge Heater) Stack Flow Rate solihr 1-Min
3/4 9:46	17,65	6,19	0.0228	2.21	4.09	1048553
3/4 9:47	17.63	6,17	0.0227	2,21	4.04	1048553
3/4 9:48	17,48	6.13	0.0225	2.19	4.08	1048553
3/4 9:49	17.38	6.09	0.0224	2.18	4.05	1048553
3/4 9:50	17.36	6.08	0.0224	2.17	4.06	1048553
3/4 9:51	17.33	6.03	0.0222	2.17	3.95	1048553
3/4 9:52	17.30	6.03	0.0221	2.17	3.96	1048553
3/4 9:53	17.41	6.11	0.0225	2.18	4.09	1048553
3/4 9:54	17.57	6.17	0.0227	2.20	4.09	1048553
3/4 9:55	17.57	6.17	0.0227	2.20	4.09	1048553
3/4 9:56	17,46	6.11	0.0224	2.19	4.03	1048553
3/4 9:57	17.42	6.10	0.0224	2.18	4.05	1048553
3/4 9:58	17.42	6.09	0.0224	2.18	4.03	1047876
3/4 9:59	17,44	6,10	0.0224	2.18	4.02	1047876
3/4 10:00	17,42	6.10	0.0224	2.18	4.06	1047876
3/4 10:01	17.45	6.15	0.0226	2.19	4.15	1048553
3/4 10:02	17.47	6,14	0.0226	2.19	4.10	1048553
3/4 10:03	17.45	6,10	0.0224	2.19	4,02	1048553
3/4 10:04	17,44	6.09	0.0224	2.18	4.01	1047876
3/4 10:05	17.45	6.10	0.0224	2.18	4.01	1047876
3/4 10:06	17,44	6.11	0.0225	2.18	4.07	1047876
3/4 10:07	17.42	6.11	0.0225	2.18	4.08	1048553
3/4 10:08	17.41	6.10	0.0224	2.18	4.07	1048553
3/4 10:09	17.44	6.12	0.0225	2.18	4.08	1047876
Average (all)	17,45	6.11	0.0225	2,19	4.05	1048356
Total (all)	47.00		-	-		4047070
Minimum (all) Maximum (all)	17.30 17.65	6.03 6.19	0,0221 0,0228	2.17 2.21	3.95 4.15	1047876 1048553
Average (valid	17.45	6.19 6.11	0.0225	2.19	4.05	1048356
values only)		****				, , , , , , , ,
Total (valid	•••	-	•••		-	_
values only) Count (valid values only)	24	24	24	24	24	24

Comment: Crude Charge Heater RATA - Run #1 Rev 1

Frontier Refining LLC Data for 3/4/2014 10:20 AM thru 3/4/2014 10:40 AM

Timestamp	(Crude Charge Heater) NOx ppm 1-Min	(Crude Charge Heater) NOx ppm @15% O2 1-Min	(Crude Charge Heater) NOx lb/mmBtu 1-Min	(Crude Charge Heater) NOx lb/hr 1-Min Avg	(Crude Charge Heater) O2% 1-Win	(Crude Charge Heater) Stack Flow Rate scift 1-Min
3/4 10:20	17.25	6.08	0.0223	2.16	4.16	1049232
3/4 10:21	17.32	6.11	0.0225	2.17	4.18	1049232
3/4 10:22	17.34	6.08	0.0223	2.17	4.07	1049232
3/4 10:23	17.24	6.04	0.0222	2.16	4.06	1049232
3/4 10:24	17.20	6.03	0.0222	2.15	4.08	1049232
3/4 10:25	17.14	6,01	0.0221	2.15	4.06	1049912
3/4 10:26	17.08	5.98	0.0220	2.14	4.08	1049912
3/4 10:27	17.10	5.96	0.0219	2.14	3.98	1049912
3/4 10:28	17.16	6.01	0.0221	2.15	4.05	1049232
3/4 10:29	17.25	6.05	0.0223	2.16	4.09	1049912
3/4 10:30	17.26	6.04	0.0222	2.16	4.05	1049912
3/4 10:31	17.31	6.09	0.0224	2.17	4.14	1049232
3/4 10:32	17.30	6.07	0.0223	2.17	4.08	1049232
3/4 10:33	17.25	6.03	0.0222	2.16	4.02	1049232
3/4 10:34	17.12	5.97	0.0219	2.14	3.97	1048553
3/4 10:35	17.01	5.96	0.0219	2.13	4.07	1048553
3/4 10:38	17.12	6.02	0.0221	2.14	4.11	1049232
3/4 10:37	17.26	6.03	0.0222	2.16	4.00	1049232
3/4 10:38	17.32	6.06	0.0223	2.17	4.04	1048553
3/4 10:39	17.41	6.12	0.0225	2.18	4.11	1048553
3/4 10:40	17.45	6.11	0.0224	2.19	4.04	1048553
Average (ali) Total (ali)	17.23	6.04	0.0222	2.16	4.07	1049232
Minimum (all)	17.01	5.98	0.0219	2.13	3.97	1048553
/laximum (all)	17.45	6.12	0.0225	2.19	4.18	1049912
verage (valid values only) Total (valid	17.23 	6.04	0.0222 	2.16 ~	4.07 	1049232
values only) Count (valid values only)	21	21	21	21	21	21

Comment: Crude Charge Heater RATA - Run #2

Frontier Refining LLC
Data for 3/4/2014 10:56 AM thru 3/4/2014 11:18 AM

Timestamp	(Crude Charge Heater) NOx ppm 1-Min	(Crude Charge Heater) NOx ppm @15% O2 1-Min	(Crude Charge Heater) NOx Ib/mmBtu 1-Min	(Crude Charge Heater) NOx ib/hr 1-Min Avg	(Crude Charge Heater) O2% 1-Min	(Crude Charge Heater) Stack Flow Rate scf/h 1-Min
3/4 10:56	17.67	6.20	0.0228	2.21	4.09	1047876
3/4 10:57	17.57	6.16	0.0226	2,20	4,06	1047876
3/4 10:58	17.51	6.11	0.0225	2.19	3.99	1047876
3/4 10:59	17.47	6.11	0.0225	2.19	4.04	1048553
3/4 11:00	17.47	6.12	0.0225	2.19	4.05	1048553
3/4 11:01	17.47	6.10	0.0224	2.19	3.99	1047876
3/4 11:02	17.42	6.07	0.0223	2.18	3.98	1047876
3/4 11:03	17.42	6.10	0.0224	2.18	4.05	1047876
3/4 11:04	17.44	6.11	0.0224	2.18	4.05	1047876
3/4 11:05	17.53	6.13	0.0225	2,20	4.03	1048553
3/4 11:06	17.56	6.10	0.0224	2.20	3.91	1048553
3/4 11:07	17.56	6.12	0.0225	2.20	3.97	1047876
3/4 11:08	17.53	6.15	0.0226	2.19	4.07	1047876
3/4 11:09	17.51	6.13	0.0226	2,19	4.06	1047876
3/4 11:10	17.38	6,05	0.0222	2,18	3.95	1048553
3/4 11:11	17.31	6,03	0.0222	2.17	3,97	1048553
3/4 11:12	17.43 <25>	6.07 <25>	0.0223 <25>	0.00 <25>	3.95 <25>	0 <25>
3/4 11:13	0.00 <25>	0.00 <25>	0.0000 <25>	0.00 <25>	18.88 <25>	0 <25>
3/4 11:14	16.00	5.69	0.0209	2.00 <25>	4.30	1047876 <25>
3/4 11:15	17.48	6.12	0.0225	2.19	4.06	1047876
3/4 11:16	17.50	6.16	0.0226	2.19	4.13	1047876
3/4 11:17	17.54	6.14	0.0226	2.19	4.05	1047876
3/4 11:18	17.52	6.15	0.0226	2.19	4.08	1047876
Average (all)	16.66	5.83	0.0214	1,99	4.68	956933
Total (all)		-			-	••
Minimum (all)	0.00	0.00	0.0000	0.00	3.91	0
Maximum (all)	17.67	6.20	0.0228	2.21	18.88	1048553
Average (valid	17.42	6.10	0.0224	2.19	4.04	1048079
values only) Total (valid values only)	-	-	-	-		-
Count (valid values only)	21	21	21	20	21	20

<25> = Backflush

Comment: Crude Charge Heater RATA - Run #3 Rev 1

Frontier Refining LLC Data for 3/4/2014 11:53 AM thru 3/4/2014 11:53 AM

Timestamp	(Crude Charge Heater) NOx ppm 1-Min	(Crude Charge Heater) NOx ppm @15% O2 1-Min	(Crude Charge Heater) NOx lb/mmBtu 1-Min	(Crude Charge Heater) NOx Ib/hr 1-Min Avg	(Crude Charge Heater) O2% 1-Min	(Crude Charge Heater) Stack Flow Rate scfihr 1-Min
3/4 11:31	17.47	6.14	0.0226	2.19	4.10	1047878
3/4 11:32	17,40	6.11	0,0225	2,18	4.11	1047876
3/4 11:33	17.29	6.05	0.0222	2.17	4,04	1048553
3/4 11:34	17.22	6.01	0.0221	2.16	4.00	1048553
3/4 11:35	17.32	6.07	0.0223	2.17	4.06	1048553
3/4 11:36	17.42	6.08	0.0224	2.18	4:00	1047876
3/4 11:37	17,32	6.05	0.0222	2.17	4.01	1047876
3/4 11:38	17.21	6.03	0.0222	2.15	4.06	1047876
3/4 11:39	17.25	6.08	0.0223	2.16	4.16	1047876
3/4 11:40	17,43	6.13	0.0225	2.18	4.13	1047876
3/4 11:41	17.43	6,08	0.0224	2.18	3.99	1047876
3/4 11:42	17.32	6.03	0.0221	2.17	3.94	1047876
3/4 11:43	17.25	6.03	0.0222	2.16	4.02	1047876
3/4 11:44	17.26	6.03	0.0222	2.16	4,00	1047876
3/4 11:45	17.26	6.03	0.0222	2.16	4.00	1047876
3/4 11:46	17.18	5.96	0.0219	2.15	3.89	1047876
3/4 11:47	17.08	6.93	0.0218	2.13	3.92	1047199
3/4 11:48	16.98	5,89	0.0216	2.12	3,89	1047199
3/4 11:49	16.97	5.92	0.0218	2.12	4.00	1047199
3/4 11:50	17.14	5.99	0.0210	2.14	4.03	1047199
3/4 11:51	17.14	6.01	0.0221	2.15	3.99	1046524
	17.23	6.05	0.0221	2.15 2.15	4.14	1046524
3/4 11:52	*		0.0222		4.14	1045178
3/4 11:53	17,21	6,06		2.15		
Average (all)	17.25	6.03	0.0222	2.16	4.03	1047612
Total (all) Minimum (all)	16.97	5.89	0.0216	2.12	3.89	1045178
Maximum (all)	17.47	6.14	0.0216	2.19	4.16	1048553
Average (valid	17,25	6.03	0.0222	2.16	4.03	1047612
values only)						
Total (valid	-	-	-	_	-	-
values only) Count (valid values only)	23	23	23	23	23	23

Comment: Crude Charge Heater RATA - Run #4 Rev 1

Frontier Refining LLC Data for 3/4/2014 12:03 PM thru 3/4/2014 12:23 PM

Timestamp	(Crude Charge Heater) NOx ppm 1-Min	(Crude Charge Heater) NOx ppm @15% O2 1-Min	(Crude Charge Heater) NOx ib/mmBtu 1-Min	(Crude Charge Heater) NOx lb/hr 1-Min Avg	(Crude Charge Heater) O2% 1-Min	(Crude Charge Heater) Stack Flow Rate scl/h 1-Min
3/4 12:03	17.33	6.09	0.0224	2.16	4.12	1041836
3/4 12:04	17.40	6.10	0.0224	2.16	4.08	1041171
3/4 12:05	17.37	6.08	0.0223	2.16	4.04	1041171
3/4 12:06	17.30	6.05	0.0222	2.15	4.03	1041171
3/4 12:07	17.24	6.04	0.0222	2.62	4.08	1274357
3/4 12:08	17.23	6.04	0.0222	2.14	4.07	1040508
3/4 12:09	17.31	6.07	0.0223	2.15	4.07	1040508
3/4 12:10	17.42	6.11	0.0224	2.16	4.07	1039848
3/4 12:11	17.34	6.06	0.0223	2.15	4.02	1039846
3/4 12:12	17.24	6.02	0.0221	2.14	4.01	1039185
3/4 12:13	17.11	5.99	0.0220	2.60	4.08	1272736
3/4 12:14	17.12	6.00	0.0220	2.60	4.06	1272736
3/4 12:15	17.15	6,01	0.0221	2.61	4,05	1272736
3/4 12:16	17.24	6.01	0.0221	2.14	3.98	1038525
3/4 12:17	17.26	6.03	0.0222	2.62	4.01	1271122
3/4 12:18	17.32	6.08	0.0223	2.15	4.09	1037867
3/4 12:19	17.36	6.07	0.0223	2.63	4.03	1271122
3/4 12:20	17.31	6.06	0.0223	2.63	4.04	1271122
3/4 12:21	17.31	6.05	0.0222	2.63	4.02	1271122
3/4 12:22	17.42	6.09	0.0224	2.64	4.01	1270317
3/4 12:23	17.43	6.07	0.0223	2.64	3.96	1270317
Average (all) Total (all)	17.30	6.05	0.0222	2.38	4.04	1150444
Minimum (all)	17.11	5.99	0.0220	2.14	3.96	1037867
Maximum (all)	17.43	6.11	0.0224	2.64	4.12	1274357
Average (valid	17.30	6.05	0.0222	2.38	4.04	1150444
values only) Total (valid values only)	8 7	. ••	••	••	40	**
Count (valid values only)	21	21	21	21	21	21

Comment: Crude Charge Heater RATA - Run #5

Frontier Refining LLC Data for 3/4/2014 12:33 PM thru 3/4/2014 12:53 PM

Timestamp	(Crude Charge Heater) NOx ppm 1-Min	(Crude Charge Heater) NOx ppm @15% O2 1-Min	(Crude Charge Heater) NOx Ib/mmBtu 1-Min	(Crude Charge Heater) NOx lb/hr 1-Min Avg	(Crude Charge Heater) 02% 1-Min	(Crude Charge Heater) Stack Flow Rate sc// 1-Min
3/4 12:33	17.28	6.04	0,0222	2.62	4.02	1268712
3/4 12:34	17.38	6.08	0.0224	2.63	4,04	1268712
3/4 12:35	17.44	6.11	0.0224	2.64	4.05	1267912
3/4 12:36	17.42	6.09	0.0224	2.64	4.03	1267912
3/4 12:37	17.36	6.05	0.0223	2.63	3.98	1267912
3/4 12:38	17.38	6.07	0.0223	2.63	4.01	1267912
3/4 12:39	17.39	6.07	0.0223	2.63	4.00	1267912
3/4 12:40	17.38	6.09	0.0224	2.63	4.05	1267114
3/4 12:41	17.37	6.09	0.0224	2.63	4.06	1267114
3/4 12:42	17.34	6.04	0.0222	2.62	3.96	1267114
3/4 12:43	17.27	6,04	0.0222	2.61	4.02	1267912
3/4 12:44	17.30	6.07	0.0223	2.62	4.08	1267912
3/4 12:45	17.44	6.11	0.0225	2.64	4.06	1267114
3/4 12:46	17.53	6.12	0.0225	2.65	3,99	1267114
3/4 12:47	17.49	6.14	0.0226	2.65	4.09	1267114
3/4 12:48	17.53	6.18	0.0227	2.17	4.17	1034594
3/4 12:49	17.53	6.14	0.0226	2.17	4.06	1035246
3/4 12:50	17.47	6.12	0.0225	2.64	4.07	1267912
3/4 12:51	17.49	6.16	0.0226	2.65	4.14	1267912
3/4 12:52	17.55	6.17	0.0227	2.17	4.13	1035246
3/4 12:53	17.45	6.12	0.0225	2.64	4.07	1268712
Average (all) Total (all)	17.42	6.10	0.0224	2.57	4.05	1234529
Ænimum (ali)	17.27	6.04	0.0222	2.17	3.96	1034594
faximum (ali)	17.55	6.18	0.0227	2.65	4.17	1268712
verage (valid values only)	17.42	6.10	0.0224	2.57	4.05	1234529
Total (valid values only)	••	••	••		••	••
Count (valid values only)	21	21	21	21	21	21

Comment: Crude Charge Heater RATA - Run #8

Frontier Refining LLC
Data for 3/4/2014 1:02 PM thru 3/4/2014 1:25 PM

Timestamp	(Crude Charge Heater) NOx ppm 1-Min	(Crude Charge Heater) NOx ppm @15% O2 1-Min	(Crude Charge Heater) NOx Ib/mmBtu 1-Min	(Crude Charge Heater) NOx Ib/hr 1-Min Avg	(Crude Charge Heater) O2% 1-Min	(Crude Charge Heater) Stack Flow Rate scf/h 1-Min
3/4 13:02	17,15	6.00	0.0221	2.60	4.04	1268712
3/4 13:03	17,10	5,94	0.0218	2.59	3.91	1268712
3/4 13:04	18.99	5.94	0.0218	2.57	4.02	1268712
3/4 13:05	17.03	5.97	0.0219	2.58	4.08	1268712
3/4 13:06	17.18	6.03	0.0222	2.12	4.08	1035246
3/4 13:07	17,25	6,01	0,0221	2.61	3.96	1267114
3/4 13:08	17,25	6.02	0.0221	2.61	4.00	1267114
3/4 13:09	17.31	6.08	0.0224	2.62	4.11	1267912
3/4 13:10	17.36	6.08	0.0224	2.63	4.08	1267912
3/4 13:11	17.32	6.04	0.0222	2,62	3.99	1267912
3/4 13:12	17.24	6.04	0.0222	2.61	4.06	1267114
3/4 13:13	17,21	6.02	0.0221	2.13	4.02	1035246
3/4 13:14	17,21	6.03	0.0222	2.13	4.05	1035246
3/4 13:15	17,22	6,01	0.0221	2,61	4.00	1268712
3/4 13:16	17.23	6.04	0.0222	2.13	4.06	1035899
3/4 13:17	17,29	6.04	0.0222	2.62	4,02	1268712
3/4 13:18	17.32	6.08	0.0224	2.62	4.10	1268712
3/4 13:19	17,38	6.11	0.0225	2.15	4,11	1035899
3/4 13:20	17,43	6.10	0.0224	2.16	4.04	1036554
3/4 13:21	17.38	6.10	0.0224	2.64	4.09	1269514
3/4 13:22	17.34	6.06	0.0223	2.63	4.03	1289514
3/4 13:23	17.39	6.10	0.0224	2.15	4.08	1038554
3/4 13:24	17,32	6.05	0.0222	2.63	4.00	1269514
3/4 13:25	17,29	6.06	0.0223	2.62	4.08	1270317
Average (all)	17,26	6,04	0,0222	2,47	4,04	1200649
Total (all)	-	••	_		-	
Minimum (ail)	16.99	5.94	0.0218	2:12	3.91	1035246
Maximum (all)	17.43	6.11	0.0225	2.64	4.11	1270317
Average (valid	17.26	6.04	0.0222	2.47	4.04	1200649
values only) Total (valid		_	_		-	
values only)		_	_		_	•
Count (valid values only)	24	24	24	24	24	24

Comment: Crude Charge Heater RATA - Run #7 Rev 1

CeDAR 1-Minute Data

Frontier Refining LLC
Data for 3/4/2014 1:33 PM thru 3/4/2014 1:55 PM

Timestamp	(Crude Charge Heater) NOx ppm 1-Min	(Crude Charge Heater) NOx ppm @15% O2 1-Min	(Crude Charge Heater) NOx ib/mmBtu 1-Min	(Crude Charge Heater) NOx (b/hr 1-Min Avg	(Crude Charge Heater) 02% 1-Min	(Crude Charge Heater) Stack Flow Rate softh 1-Min
3/4 13:33	17,32	6.05	0.0222	2.63	4.01	1269514
3/4 13:34	17,29	6.06	0,0223	2,62	4.07	1270317
3/4 13:35	17.17	5,99	0.0220	2.60	4.00	1270317
3/4 13:36	17.27	6.05	0.0222	2.62	4.05	1289514
3/4 13:37	17.41	6.11	0.0225	2.64	4.10	1289514
3/4 13:38	17.48	6.12	0.0225	2.65	4,05	1269514
3/4 13:39	17.38	6.11	0.0225	2.15	4.12	1038554
3/4 13:40	17.37	6.10	0.0224	2.15	4.11	1036554
3/4 13:41	17,38	6.07	0.0223	2.84	4.00	1269514
3/4 13:42	17.34	6.09	0.0224	2,63	4.09	1269514
3/4 13:43	17.31	6.06	0.0223	2.62	4.06	1270317
3/4 13:44	17.39	6.09	0.0224	2.64	4.05	1270317
3/4 13:45	17.39	6.08	0.0223	2.64	4.02	1270317
3/4 13:46	17.42	6.11	0.0225	2,64	4,08	1269514
3/4 13:47	17,40	6,09	0.0224	2.64	4.04	1270317
3/4 13:48	17.36	6.06	0.0223	2.63	4.01	1270317
3/4 13:49	17.37	6.09	0.0224	2.63	4.07	1270317
3/4 13:50	17.46	6.11	0.0225	2,65	4.05	1269514
3/4 13:51	17.48	6.12	0.0225	2.65	4.07	1269514
3/4 13:52	17.46	6.12	0.0225	2.65	4.06	1269514
3/4 13:53	17.42	6.10	0.0224	2.64	4.04	1269514
3/4 13:54	17.43	6.10	0.0224	2.64	4.05	1269514
3/4 13:55	17.44	6.11	0.0224	2.64	4.05	1269514
Average (all)	17,38	6.09	0.0224	2.59	4.05	1249536
Total (all)	-	-	-	••	••	_
Minimum (ell)	17.17	5.99	0.0220	2.15	4.00	1036554
Maximum (all)	17.48	6.12	0.0225	2.65	4.12	1270317
Average (valid values only)	17.38	6.09	0.0224	2.59	4.05	1249536
Total (valid	_	_	-	_	_	-
values only)	_	-				
Count (valid values only)	23	23	23	23	23	23

Comment: Crude Charge Heater RATA - Run #8 Rev 1

CeDAR 1-Minute Data

Frontier Refining LLC Data for 3/4/2014 2:04 PM thru 3/4/2014 2:24 PM

Timestamp	(Crude Charge Heater) NOx ppm 1-Min	(Crude Charge Heater) NOx ppm @15% O2 1-Min	(Crude Charge Heater) NOx lb/mmBtu 1-Min	(Crude Charge Heater) NOx Ib/hr 1-Min Avg	(Crude Charge Heater) O2% 1-Min	(Crude Charge Heater) Stack Flow Rate sciith 1-Min
3/4 14:04	17.41	6.06	0.0223	2.64	3.96	1268712
3/4 14:05	17.44	8.10	0.0224	2.64	4.03	1267912
3/4 14:08	17.43	6.09	0.0224	2.64	4.00	1267114
3/4 14:07	17.37	6.06	0.0223	2.63	4.00	1267114
3/4 14:08	17.33	6.06	0.0223	2.62	4.02	1267912
3/4 14:09	17.33	6.06	0.0223	2.62	4.03	1267912
3/4 14:10	17.33	6.07	0.0223	2.62	4.05	1267114
3/4 14:11	17.37	6.10	0.0224	2.63	4.09	1267114
3/4 14:12	17.35	6.05	0.0223	2.62	3.99	1268316
3/4 14:13	17.27	6.03	0.0221	2.61	3.99	1268316
3/4 14:14	17.28	6.08	0.0223	2.61	4.12	1268316
3/4 14:15	17.35	6.08	0.0223	2.62	4.06	1266316
3/4 14:16	17.42	6.12	0.0225	2.63	4.11	1286316
3/4 14:17	17.38	6.06	0.0223	2.63	3.98	1265521
3/4 14:18	17,31	6.05	0.0222	2.62	4.02	1265521
3/4 14:19	17.28	6.03	0.0221	2.61	3.98	1266316
3/4 14:20	17.21	6.00	0.0221	2.60	3.98	1268316
3/4 14:21	17,25	6.02	0,0221	2.61	3.98	1265521
3/4 14:22	17.38	6.05	0.0223	2.63	3.96	1265521
3/4 14:23	17.35	6.04	0.0222	2.62	3.96	1265521
3/4 14:24	17.20	5,99	0.0220	2.60	3.96	1265521
Average (all) Total (all)	17,34	6.08	0.0223	2.62	4.01	1266583
Winimum (all)	17.20	5.99	0.0220	2.60	3.96	1265521
Aaximum (ali)	17.44	6.12	0.0225	2.64	4.12	1268712
verage (valid values only)	17.34	6.06	0.0223	2.62	4.01	1266583
Total (valid values only)	•• ••	••	••		•• 24	**
Count (valid values only)	21	21	21	21	21	21

Comment: Crude Charge Heater RATA Data - Run #9

CeDAR 1-Minute Data

Frontier Refining LLC Data for 3/4/2014 2:40 PM thru 3/4/2014 3:00 PM

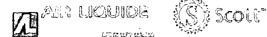
Timestamp	(Crude Charge Heater) NOx ppm 1-Min	(Crude Charge Heater) NOx ppm @15% O2 1-Min	(Crude Charge Heater) NOx lb/mmBtu 1-Min	(Crude Charge Heater) NOx Ib/hr 1-Min Avg	(Crude Charge Heater) 02% 1-Min	(Crude Charge Heater) Stack Flow Rate scifft 1-Min
3/4 14:40	17.30	6.01	0.0221	2.61	3.91	1263143
3/4 14:41	17.18	5.96	0.0219	2.59	3.91	1262353
3/4 14:42	17.14	5.95	0.0219	2.58	3.91	1262353
3/4 14:43	17.29	6.01	0.0221	2.61	3.94	126235 3
3/4 14:44	17.46	6.07	0.0223	2.63	3.93	1262353
3/4 14:45	17.43	6.03	0.0222	2.63	3.85	1262353
3/4 14:46	17.36	6.06	0.0223	2.62	3.99	1261565
3/4 14:47	17.40	6.09	0.0224	2.62	4.05	1261565
3/4 14:48	17.41	6.05	0.0222	2.62	3.91	1262353
3/4 14:49	17.35	6.01	0.0221	2.61	3.87	1261565
3/4 14:50	17.28	6.01	0.0221	2.60	3.94	1261565
3/4 14:51	17.19	5.99	0.0220	2.59	3.98	1261565
3/4 14:52	17.09	5.98	0.0220	2,57	4.04	1281565
3/4 14:53	17.12	5.96	0.0219	2.58	3.94	1262353
3/4 14:54	17.18	5.99	0.0220	2.59	3.99	1261565
3/4 14:55	17.19	6.00	0.0220	2.59	3.99	1261565
3/4 14:56	17.18	6.00	0.0221	2.59	4.01	1261565
3/4 14:57	17.20	6.01	0.0221	2.59	4.01	1261565
3/4 14:58	17.18	5.98	0.0220	2.59	3.96	1261565
3/4 14:59	17.22	6.02	0.0221	2.59	4.01	1261565
3/4 15:00	17.31	6.04	0.0222	2.61	4.00	1260778
Average (ali) Total (ali)	17.26	6.01	0.0221	2.60	3.98	1261665 —
Minimum (all)	17.09	5.95	0.0219	2.57	3.85	1260778
Maximum (all)	17.46	6.09	0.0224	2.63	4.05	1263143
Average (valid values only)	17.26	6.01	0.0221	2.60	3.96	1261865
Total (valid values only)	-	-	-	-		-
Count (valid values only)	21	21	21	21	21	21

Comment: Crude Charge Heater RATA Data - Run #10

Fuel Gas BTU content Crude Charge Heater 3/4/14

9 WebBLISS. Ad a	Tota
11.1	Sa
Hydrogen (mal W)	21.7
Methane (mol%)	43,25,
Ethane (mol%)	9.65
Ethylene (mol%)	3.41
Propene (mot%)	6.10 .
Freeylese (mo(%)	6.18 .
scbotane-(mol%)	0.77 .
ti-Butana (mol%)	0.82 •
1-Butens (mol%)	0.23 *
isobutene (mol%)	0.21
t-2-Butene (mol*)	0.25
c-2-Butene (mol%)	0.16 ·
1,3-Butadiene (mol%)	0.00 '
Isecentana (mol%)	0.35
N-Pentana (mol56)	0.13 -
C6+ (mel%)	0.00 4
HZS (mol%)	0.00
02 (mel#6)	0.52 •
N2 (mol%)	1.66 •
CO2 (mol%)	0.17.
CO (mol†s) 1	4.50
Gas Specific Gravity (mol%)	0.7002
Ideal Gross BTUs (mol%)	1,141.63
Avg Molecular Weight (mol%)	20.24

Appendix 4 Calibration Data and Certificates





500 WEAVER PARK RD, LONGMONT, CO 80501 Phone: 888-253-1635 Fax: 303-772-7673

RATA CLASS

Guaranteed +/- 1% Accuracy

CERTIFICATE OF ACCURACY: EPA Protocol Gas

Assay Laboratory - PGVP Vendor ID: A42013

AIR LIQUIDE AMERICA SPECIALTY GASES LLC

500 WEAVER PARK RD LONGMONT, CO 60501

P.O. No.: DOOFC

Document #: 83048587-014

Folio 6:5% CO2, 5% O2/N2

Customer

AIR POLLUTION TESTING INC 5830 MARSHALL STREET

ARVADA CO 60002

110

ANALYTICAL INFORMATION

Gas Type: CO2,O2,BALN

This certification was performed eccording to EPA Traceability Protocol For Assay & Certification of Gasecus Calibration Standards; Procedure G-1. EPA/600/R-12/531; May 2012. Do not use this standard if pressure is tess than 100 psig.

Cylinder Number: ALMO00809 Cylinder Pressure: 1900 PSIG Certification Date: 04Dec2013

Exp. Date: 05Dec2021

Betch No: LGM0104492

COMPONENT

CERTIFIED CONCENTRATION (Moles)

ACCURACY (ABSOLUTE/ RELATIVE)

CARBON DIOXIDE

4.98 %

0.03 % / 0.6 %

OXYGEN

4.90

0.04 % / 0.8 %

NITROGEN

OXYGEN

BALANCE

TRACEABILITY

REFERENCE STANDARD

COMPONENT

CARBON DIOXIDE

CONCENTRATION 4.8540 % 10.0300 %

UNCERTAINTY 0.0250 % 0.0700 %

CYLINDER KD14722 10012176

TYPEISRM SAMPLE

NTRM 2000 NÎTRM 2858 ECP. DATE 25Nov 2017 01 Feb2016

ANALYTICAL METHOD

tet Analysis: 04Dec2013

COM PONENT

CARBON DIOXOE

INSTRUMENT

MKB ONLINE/2030/0928082

ANALYTICAL/PRINCIPLE

FTIR 1st Analysis: 26Nov2013

CALIBRATED 13Nov2018

CONCENTRATION

4.980 %

4.RDD %

COMPONENT

INSTRUMENT

ANALYTICAL/PRINCIPLE

CALIBRATED

CONCENTRATION

PARAMAGNETIC OXYMAT/6E/W5-951 11Nov 2013 OXYGEN

QUALITY ASSURANCE

APPROVED BY: JON WITZAK

(aignature on file)



500 WEAVER PARK RD. LONGMONT, CO 80501 Phone: 888-253-1835 Fax: 303-772-7873

RATA CLASS

Guaranteed +/- 1% Accuracy

CERTIFICATE OF ACCURACY: EPA Protocol Gas

Absey Leberatory - PGVP Vender ID: A42013 AIR LIQUIDE AMERICA SPECIALTY GASES LLC

500 WEAVER PARK RD LONGMONT, CO 80501

P.O. No.: DOOFC Document # : 53048587-001 Follo #:10% CO2, 10% OZ/N2 Customer AIR POLLUTION TESTING INC 6850 MARSHALL STREET ARVADA CO 80002

ANALYTICAL INFORMATION Gas Type : CO2,O2,BALN

This certification was performed eccording to EPA Tracoability Protocol For Assay & Certification of Gaseous Celibration Standards; Procedure G-1. EPA/600/R-12/631; May 2012. Do not use this standard if pressure is less than 100 pag.

Cylinder Number: 1L2200 Cylinder Pressure: 1800 P81G Certification Date: 040ec2013

Exp. Date: 050002021 Batch No: LGM0104489

COMPONENT CARBON DIOXIDE CERTIFIED CONCENTRATION (Moles)

ACCURACY (ABSOLUTE/ RELATIVE)

OXYGEN NITROUEN 10.00 € 9.83 % BALANCE

0.08 \$ 7 0.8 \$ 0.07 % / 0.7 %

TRACEABILITY

REFERENCE STANDARD

COMPONENT CARBON DIOXIDE OXY GEN

CONCENTRATION UNCERTAINTY 17.8700 % 10.0300 %

0.1100 % 0.0700 %

CYLINDER KD22438 K012176

TYPERM SAMPLE NTRM 1800 NTRM 2658

ECP. DATE 01Mpr2019 01Feb2018

ANALYTICAL METHOD

1st Analysis: 04Dec2013

COMPONENT CARBON DIOXDE

INSTRUMENT MKB ONLINE/2030/0929082 ANALYTICAL/PRINCIPLE FTIR

CALIBRATED 13Nov 2013

CONCENTRATION 10.00 %

1st Analysis: 25Nov2013

COMPONENT OXYGEN

INSTRUMENT OXYMAT/8E/WS-851 ANALYTICAL/PRINCIPLE PARAMAGNETIC

CALIBRATED 11Nov 2013

CONCENTRATION 9.830 %

QUALITY ASSURANCE

APPROVED BY: JON WITZAK

(eignature on file)

AM LICUICE .

S. 3000

RATA CLASS

Dual-Analyzed Calibration Standard

500 WEAVER PARK RD, LONGMONT, CO 80501

Phone: 868-263-1635

Fax: 303-772-7673

CERTIFICATE OF ACCURACY: Interference Free Multi-Component EPA Protocol Gas

Assay Laboratory - PGVP Vendor ID: A42013

P.O. No.: DOOFC

Customer AIR POLLUTION TESTING INC

المتنا القاليف والتراكية في المجاولة ويصيف الما المجاولة الما المجاولة

A'R LIQUIDE AMERICA SPECIALTY GASES LLC

500 WEAVER PARK RD LONGMONT, CO 80501

Document # : 60761111-003

5530 MARSHALL STREET

ARVADA CO 80002

ANALYTICAL INFORMATION Gas Type: CO2.O2,BALN
This curtification was performed occurring to EPA Tracontainty Protocol For Assay & Cartification of Gaseous Calibration Standards;

Procedure G-1; September, 1997.

Cylinder Number: ALMO08261

Certification Date:

Cylinder Number: Cylinder Pressure***: 1993 PSIG

22May2013

Exp. Date: 23May2021 Batch No: LGM0088835

COMPONENT CARBON DIOXIDE OXYGEN

CERTIFIED CONCENTRATION (Moles)

TRACEABILITY Direct NIST and VSL

NITROGEN

BALANCE

*** Do not use when cylindar pressure is below 150 paig.

** Analytical accuracy is based on the requirements of EPA Protocol Procedure G1, September 1997.

K012178

REFERENCE STANDARD TYPE/8RM NO. EXPIRA EXPIRATION DATE

01Mar2018 NTRM 1800 NTRM 2658

01Feb2016

CYLINDER NUMBER K022438

CONCENTRATION 17.87 %

COMPONENT CARBON DIOXIDE

OXYGEN

INSTRUMENTATION INSTRUMENT/MODEL/SERIAL# FT:R!/0929062

OXYMAT/BEAMS-951

DATE LAST CALIBRATED

10.03 %

18May2013

20May2013

ANALYTICAL PRINCIPLE

FTIR PARAMAGNETIC

ANALYZER READINGS

IZ=Zoro Gas R Releigence Gas T=Test Gas r Correlation Coefficient)

First Triad Analysis

Second Triad Analysis

Calibration Curva

CARBON DIOXIDE

Date: 21May2013 Response Unit:%

21=-0.00091 R1=17.86919 T1=19.67284 R2=17.88036 Z2=0.00008 T2=19.87789

23-0.00294 T3-19.68646 R3-17.88415

Avg. Concentration:

18.67

Concentration = A + 8x + Cx2 + Dx3 + Ex4 r=8.99999E-1

Constants:

A = -4.53571E+1 8 = 1.38847E+0 C=0.00000E+0

D=0.00000E+0 E=0.00000E+0

OXYGEN

Date: 22May2013 Response Unit: VOLTS

Z1=0.00000 R1=10.06000 T1=21.09000

R2=10.04000 Z2=0.00000 T2-21.08000 Z3=0.00000 T3=21.09000 R3=10.04000

Avg. Concentration: 21.05

Concentration = A + 8x + Cx2 + Dx3 + Ex4 -C 999999 Constants:

A = 0.00327224

B=0.998213631 C=

D-£-

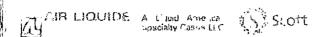
APPROVED BY:

ADAM HANLEY

ار میرورد با از برای موسور برسور باشدانیم آزاد <u>روافت ماکری فافت توانیخ</u>

Page

1 of 1



RATA CLASS

Guaranteed +/- 1% Accuracy

500 WEAVER PARK RD. LONGMONT. CO 80501

Phone: 888-263-1636

Fax: 303-772-7673

CERTIFICATE OF ACCURACY: EPA Protocol Gas

Assny Laboratory - PGVP Vandor ID: A42013 AIN LIQUIDE AMERICA SPECIALTY GASES LLC 500 WEAVER PARK RD

LONGMONT, CO 80501

P.O. No.: DOOFC

Document # : 52075783-003 Folio #:18.2PPM NO/N2

Customer AIR POLLUTION TESTING INC 5530 MARSHALL STREET ARVADA CO 80002 US

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ANALYTICAL INFORMATION

Gas Type: NO.BALN

This contilication was performed according to EPA Tracealistic Procedure G-1. EPA/600/R-12/631; May 2012. Do not use this standard if pressure is less than 100 pag.

Cylinder Number: Cylinder Pressure:

AAL073323 2000 PSIG

Certification Date:

30Sep2013

Exp. Date: 010ct2016 Batch No: LGM0099323

COMPONENT NITRIC OXIDE

NITROGEN - OXYGEN FREE

CERTIFIED CONCENTRATION (Moles)

18.1 BALANCE

PPM

ACCURACY (ABSOLUTE / RELATIVE)

TOTAL OXIDES OF NITROGEN

18.2

Reference Value Only

TRACEABILITY REFERENCE STANDARD

COMPONENT NITRIC OXIDE CONCENTRATION 10.1100

UNCERTAINTY 0.1200

CYLINDER_ KAL004118

TYPE/SRM SAMPLE

NTRM 2828

EXP. DATE

ANALYTICAL METHOD

1st Analysis:

238ep2013

COMPONENT

NITRIC OXIDE

INSTRUMENT NONOX/CLA-220/41528760062 CHEMILUMINESCENT

ANALYTICAL/PRINCIPLE CALIBRATED CONCENTRATION 18.20 PPM 17Sep 2013

2nd Analysis: 308ep2013

COMPONENT

NITRIC OXIDE

INSTRUMENT

NONOX/CLA-220/41528750082

ANALYTICAL/PRINCIPLE CALIBRATED CONCENTRATION CHEMILUMINESCENT

176ep2013

16.06 PPM

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500 WEAVER PARK RD. LONGMONT, CO 80501 Phone: 888-263-1635 Fax: 303-772-7673

RATA CLASS

Guaranteed +/- 1% Accuracy

CERTIFICATE OF ACCURACY: EPA Protocol Gas

Assay Laboratory - PGVP Vendor ID: A42013 AIR LIQUIDE AMERICA SPECIALTY GASES LLC 600 WEAVER PARK RD

LONGMONT, CO 80501

P.O. No.: DOOFC Document # : 62075783-904 Fallo #:39,2PPM NO/N2

Customer AIR POLLUTION TESTING INC 6830 MARSHALL STREET ARVADA CO 80002 UB

ANALYTICAL INFORMATION Gas Type: NO,BALN

This certification was performed according to EPA Traceability Protocol For Assay & Certification of Gaseous Calibration Standards; Procedure G-1. EPA/600/R-12/531; May 2012. Do not use this standard if pressure is less than 100 psig.

Cylinder Number: ALMO46779 Cylinder Pressure: 1900 PSIG Certification Date: 308ep2013

Exp. Date: 010ct2018 Batch No: LGM0098324

COMPONENT

CERTIFIED CONCENTRATION (Moles)

ACCURACY (ABSOLUTE/ RELATIVE)

NITRIC OXIDE

38.8 PPM

0.5 PPM / 1.2 %

NITROGEN - OXYGEN FREE

BALANCE

TOTAL OXIDES OF NITROGEN 38.9 PPM

Reference Value Only

TRACEABILITY

REFERENCE STANDARD

COMPONENT NITRIC ONDE

CONCENTRATION UNCERTAINTY 20.3800 PPM

0.2500 PPM

CYLINDER KAL004313

TYPESRM SAMPLE

NTRM 2829

EXP. DATE 31May 2018

ANALYTICAL METHOD

1st Anatysła: 23Sep2013

COMPONENT NITRIC OXIDE

INSTRUMENT

MICS ONLINE/2030/0929082

ANALYTICAL/PRINCIPLE

CALIBRATED DEReo2013

CONCENTRATION 38.76 PPM

ETIR 2nd Analysis: 308ep2013

COMPONENT NITRIC OXDE

INSTRUMENT MKS ONLINE/2030/0929062 FTIR

ANALYTICAL/PRINCIPLE

CALIBRATED 08Sep2013

CONCENTRATION

38.66 PPM

QUALITY ASSURANCE

APPROVED BY: JON WITZAK

(algnature on file)



Wind Tunnel Pitot Calibration

S-type Pitot ID: P-577 Date: 13-Feb-13

Standard Pitot ID: 001 Personnel: DH

Cp(std): 0.99 Cp(actual): 0.837
Part Number: PPS12-Y-007.5 Pber(In Hg): 29.09

Test Velocity (fps): 50 T(°F): 47

44.6	i - ΔΡ _ε	ΔP, (In. H ₂ 0)	Cp(s)	Deviation*
A-SIDE	0.579	0.814	0.835	-0.003
S	0.589	0.811	0.843	0.005
K	0.581	0.815	0.836	-0.003
	0.584	0.811	0.840	0.001
		AVERAGE	0.839	0.003
			Std deviation	0.004

ш	ΔΡ ₂ ! (in. H ₂ 0)	ΔP, (In H ₂ 0)	Cp(s) (Deviation*
SIDE	0.581	0.820	0.833	-0.003
	0.584	0.819	0.836	0.000
ά	0.588	0.819	0.838	0.003
	0.581	0.816	0.836	0.000
		AVERAGE	0.836	0.001
			Std deviation	0.002

$$Cp(s) = Cp(std)\sqrt{\frac{\Lambda P(std)}{\Delta P(s)}}$$

$$Cp(A) - Cp(B) = 0.003$$
 {must be <0.010}

*Deviation = $\{Cp(s) - AVGCp(s)\}\$ {must be <0.010}

Standard deviation of the deviations must be less than 0.02 for both sides.

Pitot tube S/N P-577 was calibrated in accordance with the CFR 40, Part 60 Appendix A, Method 2, Section 10.

Signature

2-/3-/3



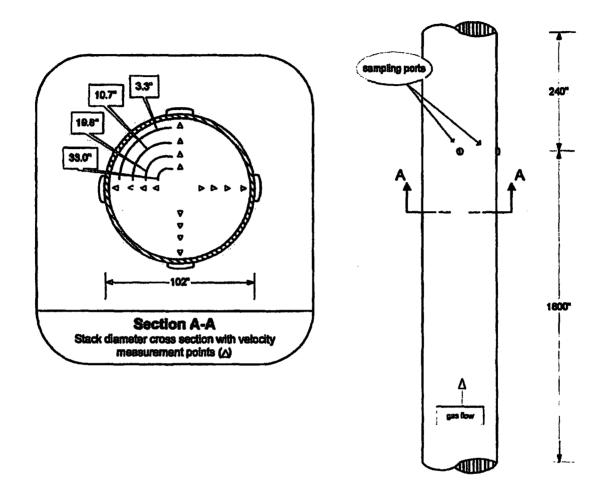
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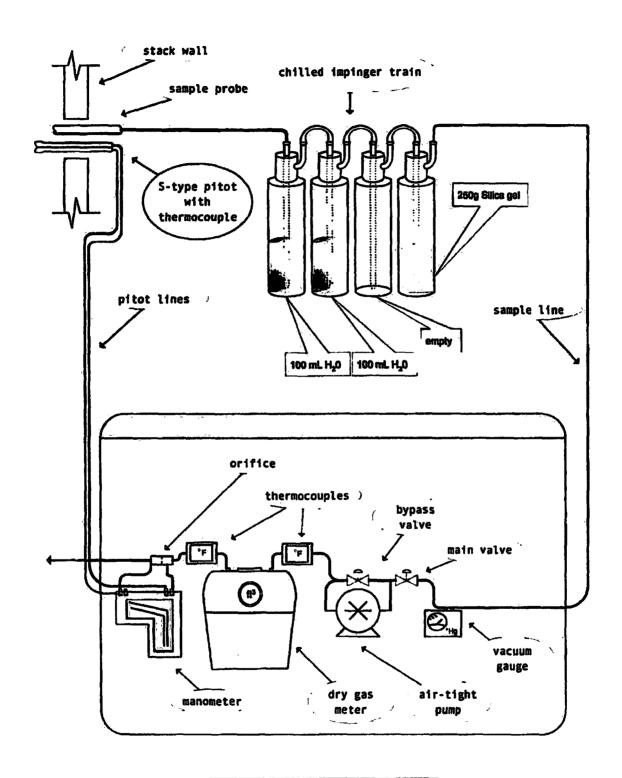
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Appendix 5

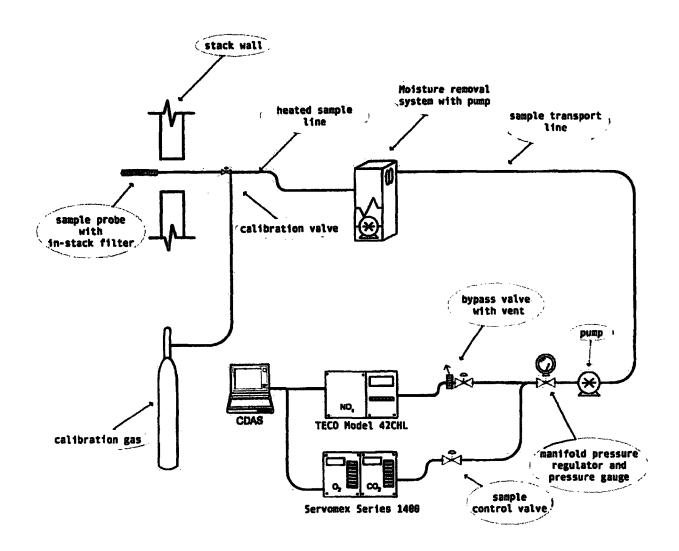
Schematics



Frontier Refinery
Crude Charge Heater
Stack Sampling Location Schematic
(not to scale)



EPA Methods 1,2, & 4 sampling train schematic



EPA Methods 3A & 7E sampling train schematic

Crude Charge Heater

7-Day Drift Test

January 21 – 27, 2014

Frontier Refining LLC 7-Day Drift Test Crude Charge Heater NOx ppm

	Instrument	Zero	Zero	Zero	Zero	Span	Span	Span	Span	
Time	Span	Reference	Measured	Drift	Drift Limit	Reference	Measured	Drift	Drift Limit	Status
01/21/14 06:10 AM	100	0.00	0.28	0.28	2.50	89.90	89.27	-0.63	2.50	On-Line
01/22/14 06:10 AM	100	0.00	1.24	1.24	2.50	89.90	89.35	-0.55	2.50	On-Line
01/23/14 06:10 AM	100	0.00	1.22	1.22	2.50	89.90	89.13	-0.77	2.50	On-Line
01/24/14 06:10 AM	100	0.00	1.19	1.19	2.50	89.90	89.06	-0.84	2.50	On-Line
01/25/14 06:10 AM	100	0.00	1.68	1.68	2.50	89.90	88.40	-1.50	2.50	On-Line
01/26/14 06:10 AM	100	0.00	1.56	1.56	2.50	89.90	87.77	-2.13	2.50	On-Line
01/27/14 06:10 AM	100	0.00	0.85	0.85	2.50	89.90	88.85	-1.05	2.50	On-Line

The 7-Day Drift Test has been passed.

Frontier Refining LLC

7-Day Drift Test
Crude Charge Heater O2%

	Instrument	Zero	Zero	Zero	Zero	Span	Span	Span	Span	
Time	Span	Reference	Measured	Drift	Drift Limit	Reference	Measured	Drift	Drift Limit	Status
01/21/14 06:10 AM	25	0.000	0.006	0.006	0.500	20.900	20.919	0.019	0.500	On-Line
01/22/14 06:10 AM	25	0.000	0.176	0.176	0.500	20.900	20.845	-0.055	0.500	On-Line
01/23/14 06:10 AM	25	0.000	0.159	0.159	0.500	20.900	20.928	0.028	0.500	On-Line
01/24/14 06:10 AM	25	0.000	0.173	0.173	0.500	20.900	20.937	0.037	0.500	On-Line
01/25/14 06:10 AM	25	0.000	0.267	0.267	0.500	20.900	20.966	0.066	0.500	On-Line
01/26/14 06:10 AM	25	0.000	0.281	0.281	0.500	20.900	20.989	0.089	0.500	On-Line
01/27/14 06:10 AM	25	0.000	0.137	0.137	0.500	20.900	20.981	0.081	0.500	On-Line

The 7-Day Drift Test has been passed.

Frontier Refining LLC

7-Day Drift Test
Crude Charge Heater Stack Flow Delta P

Time	Instrument Span	Zero Reference	Zero Measured	Zero Drift	Zero Drift Limit	Span Reference	Span Measured	Span Drift	Span Drift Limit	Status
01/21/14 06:25 AM	0.25	0.000	0.000	0.000	0.008	0.100	0.105	0.005	0.008	On-Line
01/21/14 09:17 AM	0.25	0.000	0.000	0.000	0.008	0.100	0.106	0.006	0.008	On-Line
01/21/14 11:03 AM	0.25	0.000	0.000	0.000	0.008	0.125	0.137	0.012	0.008	On-Line
01/21/14 11:06 AM	0.25	0.000	0.000	0.000	0.008	0.125	0.149	0.024	0.008	On-Line
01/21/14 11:08 AM	0.25	0.000	0.000	0.000	0.008	0.125	0.137	0.012	0.008	On-Line
01/21/14 11:12 AM	0.25	0.000	0.000	0.000	0.008	0.125	0.143	0.018	0.008	On-Line
01/21/14 11:13 AM	0.25	0.000	0.000	0.000	0.008	0.125	0.131	0.006	0.008	On-Line
01/21/14 12:58 PM	0.25	0.000	0.000	0.000	0.008	0.125	0.133	0.008	0.008	On-Line
01/22/14 06:25 AM	0.25	0.000	0.000	0.000	0.008	0.125	0.128	0.003	0.008	On-Line
01/23/14 06:25 AM	0.25	0.000	0.000	0.000	0.008	0.125	0.127	0.002	0.008	On-Line
01/24/14 06:25 AM	0.25	0.000	0.000	0.000	0.008	0.125	0.130	0.005	0.008	On-Line
01/25/14 06:25 AM	0.25	0.000	0.000	0.000	0.008	0.125	0.127	0.002	0.008	On-Line
01/26/14 06:25 AM	0.25	0.000	0.000	0.000	0.008	0.125	0.128	0.003	0.008	On-Line
01/27/14 06:25 AM	0.25	0.000	0.000	0.000	0.008	0.125	0.130	0.005	0.008	On-Line

The 7-Day Drift Test has been passed

Crude Charge Heater

Linearity Test

March 6, 2014

Data Sheet for Crude Charge Heater CEM System Linearity Check

1. Date Audit Commenced:	6-Mar-14	Time Audit Commenced:	10:25 AM
			

2. Audit Gases Used for Test (All gases to be Protocol 1 Certified):

Acceptable Audit Gas Ranges	Cylinder Number and Expiration Date	Audit Gas Concentrations		+/- of Audit Gas Range
NO _x Low:	AAL073323	18.20		18.20%
20 - 30 ppm	1-Oct-16	10.20	ppm	10.20%
NO _x Mid:	ALMO39664	39.40		39.40%
50 - 60 ppm	21-May-14	38.40	ppm	39.40%
NO _x High:	ALMO48270	89.90		89.90%
90 - 100 ppm	20-Aug-21	09.80	ppm	09.9076
O ₂ Low:	CC420681	4.96	%	4.96%
4 - 6% by volume	4-Mar-21	4.50	70	4.90%
O ₂ Mid:	CC2603	0.05	%	0.050
8 - 12% by volume	5-Mar-21	9.95	70	9.95%
O₂ High:	CC100519	47.04	%	47.040/
18 - 21% by volume	30-Sep-21	17.84	70	17.84%

Data Sheet for Crude Charge Heater CEM System Linearity Check

3. CEM System Response:

	Low-Span NO _x		Mid-Sp	an NO _x	High-Span NO _x		
	Analyzer	CeDAR5	Analyzer	CeDAR5	Analyzer	CeDAR5	
Run 1	18.20	17.79	38.65	37.66	90.10	87.75	
Run 2	18.26	17.78	38.56	37.56	89.95	87.60	
Run 3	18.38	17.91	38.61	37.62	89.85	87.42	
Avg. (d _m)	18.28	17.83	38.61	37.61	89.97	87.59	
Α	0.44	-2.05	-2.01	-4.53	0.07	-2.57	
Pass?	Yes	Yes	Yes	Yes	Yes	Yes	

	Low-Span O₂		Mid-S	pan O ₂	High-Span O₂		
	Analyzer	CeDAR5	Analyzer	CeDAR5	Analyzer	CeDAR5	
Run 1	5.00	5.00	9.97	9.97	17.95	17.96	
Run 2	5.03	5.03	10.02	10.02	17.97	17.97	
Run 3	5.03	5.03	10.03	10.03	17.97	17.98	
Avg. (d _m)	5.02	5.02	10.01	10.01	17.96	17.97	
Α	1.21	1.21	0.57	0.57	0.69	0.73	
Pass?	Yes	Yes	Yes	Yes	Yes	Yes	

4. Signature of Technician(s) performing Test:

Ron Anderson, Kevin Marschner and/or Tad Milliken

Calculation of A:

 $A = (d_m - c_a) / c_a \times 100$

A must be +/-5% to pass.

where:

A = accuracy of CEM

 d_m = average of reponses

 c_a = certified audit value of gas

DEPARTMENT OF ENVIRONMENTAL QUALITY AIR QUALITY DIVISION CONTINUOUS EMISSION MONITORING REPORT

FORM A

I. GENERAL INFORMATION

- A. Facility Name: FRONTIER REFINING LLC
- B. Process Unit/Pollutant Monitored: Nox MONITOR CRUDE CHARGE HEATER
- C. Applicable Permit Number or Regulation: Consent Decree
- D. Applicable Emission Limit: 0.031 lb/mmbtu (1-hr average): 6.3 lb/hr (1-hr average)

II. MONITOR INFORMATION

- A. Date of Original Monitor Installation: December 20, 2013 (New Installation)
- B. Date of Latest Monitor Certification: March 6, 2014
- C. Pollutant/Opacity Monitor
 - 1. Manufacturer: Teledyne Advanced Pollution Instrumentation
 - 2. Model Number: T200H/M
 - 3. Serial Number Main Chassis: 154
 - 4. Basis of Measurement (If Applicable Wet or Dry): Dry
 - 5. Instrument Span, Range Value (Specify Units): 0-100 ppm NO.

D. Diluent Monitor

- 1. Type of Monitor: O2
- 2. Manufacturer: Teledyne Advanced Pollution Instrumentation
- 3. Model Number: T200H/M
- 4. Serial Number Main Chassis: 154
- 5. Basis of Measurement (If Applicable Wet or Dry): Dry
- 6. Instrument Span, Range Value (Specify Units): 0-25 percent (%)

E. Flow Monitor

- 1. Type of Instrument: Microprocessor Based Delta P Pressure "Smart" Transmitter
- 2. Manufacturer: Air Monitor Corporation
- 3. Model Number: Veltron II
- 4. Serial Number Main Chassis: 81983A

Flow Monitor Probe

- 1. Type of Instrument (i.e. S-type Pitot Tube): Pitot Traverse
- 2. Manufacturer: Air Monitor Corporation
- 3. Model Number: Drawing No. W81983AA
- 4. Serial Number Main Chassis: 81983

F. Quality Assurance Data

- 1. QA Plan Date: To be Submitted
- 2. QA Plan Approval Date:

III. Operating/Monitoring Data

A. Quarter: 2 Year: 2014

B Total Hours in Reporting Period: 2184

C. Hours Unit Operated During the Reporting Period: 2184

Note: Include <u>all</u> unit operating time for the quarter including operating time associated with Startup/Shutdown and Chapter 1 Section 5 (Emergency/Abnormal) Operations. Report time in hours to one decimal place, i.e. 1902.8.

IV. Quarterly Audits/Monitoring System Modifications

A. Quarterly Audits
Type Audit: <u>CGA</u>

	Date Conducted	Pass Pass
Pollutant/Opacity Monitor:	6/4/2014	Yes
Diluent Monitor	<u>6/4/2014</u>	<u>Yes</u>

Note: A copy of the quarterly audits shall be included with the corresponding quarterly excess emission report.

B. Equipment Replaced During Reporting Period: <u>Changed NO. Span Calibration Bottle:</u> <u>Changed out Calibration Flow Regulator.</u>

Note: Only equipment replacements or modifications to the system that could affect the ability of the continuous monitoring system to comply with the associated Performance Specification shall be reported.

V. Report Contact

A. Name: David Weeks, Environmental Engineer

B. Phone Number: (307) 771-8827

EXCESS EMISSION SUMMARY REPORT Crude Charge Heater NO_x (lb/mmbtu) CEMS 1-hr average = 0.031 lb/mmbtu

FORM B

Emission Data Summary (12-hour average	ge ppm)	CMS Performance Report I. CMS Downtime in Reporting Period Due to:			
I. Duration of Excess Emission in Reporting Per	riod Due to:				
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	2.0		
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	0.0		
C. Process Problem	0.0	C. Quality Assurance Calibration	1.0		
D. Other Known Causes	41.0	D. Other Known Causes	0.0		
E. Unknown Causes	0.0	E. Unknown Causes	0.0		
II. Total Duration of Excess Emission	41.0	II. Total CMS Downtime	3.0		
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	1.9%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	0.1%		

Total time of excess emission events due to emergency/abnormal operations: ____0_. NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2. Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)
- 4. New CEMS installation on December 20, 2013. Data not valid until March 6, 2014 after 7-Day Drift Test, RATA and Linearity Test was successfully completed.

Crude Charge Heater Excess Emissions Summary Frontier Refining LLC NOx Ib/mmBtu 1-Hr Excess Emissions for 4/1/2014 thru 6/30/2014

Reason	Duration
Crude Charge Heater Placed on Circulation in Natural Draft Mode	19 hours
Forced Draft Fan off-line for Maintenance, Hester went to Natural Draft operation. This caused the Excess O2 to be elevated.	6 hours
NOx (b/mmbtu Emission Exceedance - High Excess O2	14 hours
Process O2 was not Reading Correctly. Put into Natural Draft Mode.	1 hour
The FD and ID fans were running with the output of the FD fan running higher than normal. The Process O2 on the TDC were incorrect.	1 hour
Total duration of NOx lb/mmBtu 1-Hr excess emissions	41 hours
Total operating time	2184 hours
Operating time with excess emissions	1.9%

Comment: Form C - Excess Emissions Summary

Crude Charge Heater Excess Emissions

Frontier Refining LLC
NOx lb/mmBtu 1-Hr Excess Emissions for 4/1/2014 thru 6/30/2014

Parameter	Start	End	Duration	Value	Min	Max	Limit	Reason	Action
łOx lb/mmBtu 1-Hr	5/7/2014 7:00 AM	12:59 PM	6 hours	0.0326	0.0324	0.0330	0.031	Forced Draft Fan off-line for Maintenance, Heater went to Natural Draft operation. This caused the Excess O2 to be elevated.	Adjusted air registers to lower Excess O2.
IOx Ib/mmBtu 1-Hr	5/19/2014 7:00 AM	7:59 AM	1 hour	0.0338	0.0338	0.0338	0.031	Process O2 was not Reading Correctly. Put into Natural Draft Mode,	Adjusted Air Registers to Lower Excess O2. Returned to Forced Draft Mode.
iOx ib/mmBtu 1-Hr	5/21/2014 3:00 AM	3:59 AM	1 hour	0.0315	0.0315	0.0315	0.031	The FD and ID fans were running with the output of the FD fan running higher than normal. The Process O2 on the TDC were incorrect.	Operator tried to manipulate the controllers at the fans from the TDC to get some air flow out the stack that helped get heat out. For safety, the unit charge was reduced and went to Natural Draft Mode.
IOx ib/mmBtu 1-Hr	5/27/2014 3:00 AM	3:59 AM	1 hour	0.0311	0.0311	0.0311	0.031	NOx fb/mmbtu Emission Exceedance - High Excess O2	Adjusted Excess O2
łOx ib/mmBtu 1-Hr	6/14/2014 12:00 AM	2:59 AM	3 hours	0.0321	0.0318	0.0327	0.031	NOx ib/mmbtu Emission Exceedance - High Excess O2	Adjusted Excess O2
IOx Ib/mmBtu 1-Hr	6/14/2014 8:00 PM	11:59 PM	4 hours	0.0317	0.0316	0.0317	0.031	NOx lb/mmbtu Emission Exceedance - High Excess O2	Adjusted Excess O2
lOx ib/mmBtu 1-Hr	6/15/2014 12:00 AM	5:59 AM	6 hours	0.0316	0.0314	0.0318	0.031	NOx ib/mmbtu Emission Exceedance - High Excess O2	Adjusted Excess O2
lOx ib/mmBtu 1-Hr	6/23/2014 2:00 AM	8:59 PM	19 hours	0.0462	0.0418	0.0504	0.031	Crude Charge Heater Placed on Circulation in Natural Draft Mode	Adjusted Air Registers and Returned to Forced Draft Mode
Total	duration		41 hours						

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Parameter	SIBIT	End	Duration	Value	win	Max	Limit	Reason	ACTION
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Comment: Form C - Excess Emissions Summary

Crude Charge Heater CEMS Downtime Summary Frontier Refining LLC NOx lb/mmBtu CEMS Downtime for 4/1/2014 thru 6/30/2014

Reason	Duration
Cylinder Gas Audit (CGA)	1 hour
Failed Moming NOx ppm Span Calibration Check - OOC	2 hours
Total duration of NOx ib/mmBtu CEMS downtime	3 hours
Total operating time	2184 hours
Operating time with CEMS downtime	0.1%

Comment: Form D - Downtime Summary

Crude Charge Heater CEMS Downtime

Frontier Refining LLC NOx Ib/mmBtu CEMS Downtime for 4/1/2014 thru 6/30/2014

Parameter	Start	End	Duration	Reason	Action
NOx ib/mmBtu	5/31/2014 6:00 AM	7:59 AM	2 hours	Failed Morning NOx ppm Span Calibration Check - OOC	Ran Manual Calibration
NOx lb/mmBtu	6/4/2014 9:00 AM	9:59 AM	1 hour	Cylinder Gas Audit (CGA)	Ran CGA on NOx and O2
	Total duration		3 hours		<u></u>

Comment: Form D - Downtime Summary

EXCESS EMISSION SUMMARY REPORT Crude Charge Heater NO_x (lb/hr) CEMS 1-hr average = 6.3 lb/hr

FORM B

Emission Data Summary (lb/hr)	:	CMS Performance Report			
I. Duration of Excess Emission in Reporting Pe	riod Due to:	I. CMS Downtime in Reporting Period Due to:			
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	29.0		
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	0.0		
C. Process Problem	0.0	C. Quality Assurance Calibration	1.0		
D. Other Known Causes	0.0	D. Other Known Causes	3.0		
E. Unknown Causes	0.0	E. Unknown Causes	0.0		
II. Total Duration of Excess Emission	0.0	II. Total CMS Downtime	33.0		
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.0%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	1.5%		

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2. Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)
- 4. New CEMS installation on December 20, 2013. Data not valid until March 6, 2014 after 7-Day Drift Test, RATA and Linearity Test was successfully completed.

Crude Charge Heater Excess Emissions Summary Frontier Refining LLC NOx lbs 1-Hr Excess Emissions for 4/1/2014 thru 6/30/2014

Reason	Duration		
There are no excess emissions for this report.	·		
Total duration of NOx ibs 1-Hr excess emissions	0		
Total operating time	2184 hours		
Operating time with excess emissions	0.0%		

Crude Charge Heater CEMS Downtime Summary
Frontier Refining LLC
NOx lbs CEMS Downtime for 4/1/2014 thru 6/30/2014

Reason	Duration	
Cylinder Gas Audit (CGA)	1 hour	
Falled Moming NOx ppm Span Calibration Check - OOC	2 hours	
Falled Morning Stack Flow Delta P Span Calibration Check	22 hours	
Falled Morning Stack Flow Delta P Span Calibration Check - OOC	1 hour	
Maintanance - Stack Flow	1 hour	
Maintenance - Stack Flow System	2 hours	
Stack Flow Delta P Transmitter Malfunction	4 hours	
Total duration of NOx lbs CEMS downtime	33 hours	
Total operating time	2184 hours	
Operating time with CEMS downtime	1.5%	

Comment: Form D - Downtime Summary

Crude Charge Heater CEMS Downtime

Frontier Refining LLC NOx ibs CEMS Downtime for 4/1/2014 thru 6/30/2014

Parameter	Start	End	Duration	Reason	Action
NOx lbs	4/1/2014 6:00 AM	7:59 AM	2 hours	Failed Morning Stack Flow Delta P Span Calibration Check	Passed Manual Calibration
NOx ibs	4/2/2014 6:00 AM	7:59 AM	2 hours	Failed Morning Stack Flow Delta P Span Calibration Check	Passed Manual Calibration
NOx ibs	4/3/2014 7:00 AM	9:59 AM	3 hours	Failed Morning Stack Flow Delta P Span Calibration Check	Passed Manual Calibration
NOx lbs	4/13/2014 5:00 AM	4:59 PM	12 hours	Failed Morning Stack Flow Delta P Span Calibration Check	Passed Manual Calibration
NOx ibs	4/28/2014 6:00 AM	8:59 AM	3 hours	Failed Morning Stack Flow Delta P Span Calibration Check	Passed Manual Calibration
NOx ibs	4/28/2014 10:00 AM	11:59 AM	2 hours	Maintenance - Stack Flow System	Rebuilt Regulator and found obstruction in Needle Valve
NOx ibs	5/31/2014 6:00 AM	7:59 AM	2 hours	Failed Morning NOx ppm Span Calibration Check - OOC	Ran Manual Calibration
NOx lbs	6/4/2014 9:00 AM	9:59 AM	1 hour	Cylinder Gas Audit (CGA)	Ran CGA on NOx and O2
NOx lbs	6/5/2014 5:00 AM	5:59 AM	1 hour	Failed Morning Stack Flow Delta P Span Calibration Check - OOC	Calibrated stack flow, adjusted span, ran validation.
NOx fbs	6/21/2014 6:00 AM	9:59 AM	4 hours	Stack Flow Delta P Transmitter Malfunction	Adjusted and Ran Manual Calibration
NOx lbs	6/24/2014 1:00 PM	1:59 PM	1 hour	Maintenance - Stack Flow	Replaced Stack Flow Regulator. Made Adjustments on Regulator and Needle Valve.
	Table desiles		22 haven		on Regulator and Needle Va

Total duration 33 hours

Comment: Form D - Downtime Summary

Data Sheet for Crude Charge Heater CEM System Cylinder Gas Audit

1.	Date Audit Commenced:	6/4/2014	Time Audit Commenced:	9:45 AM

2. Audit Gases Used for CGA (All gases to be Protocol 1 Certified):

Acceptable Audit Gas Ranges	Cylinder Number and Audit Gas Expiration Date Concentrations		ns	+/- of Audit Gas Range
NOx Low:	CC90737	26.20 ppm		26 200/
20 - 30 ppm	26-Mar-22	– 26.20 ppm		26.20%
NOx Mid:	CC143970	SE 07		55.67%
50 - 60 ppm	2-Apr-22	55.67 ppm		55.0776
O2 Low:	EB0042977	400	0,	
4.18 - 6.27% by volume	23-Mar-22	4.99 %		23.88%
O2 Mid:	CC189312	10.01 %		
10.45 - 12.54% by volume	23-Mar-22			47.89%

3. CEM System Response:

	Low-Sp	oan NO _x	Mid-Span NO _x		Low-S	pan O ₂	Mid-S	oan O ₂
	Analyzer	Cisco	Analyzer	CISCO	Analyzer	CISCO	Analyzer	CISCO
Run 1	25.33	25.33	55.38	55.38	5.00	5.01	9.98	9.98
Run 2	25.28	25.28	55.47	55.47	5.00	5.00	9.99	9.99
Run 3	25.33	25.33	55.48	55.48	5.01	5.01	9.99	9.99
Avg. (d _m)	25.31	#DIV/0I	55.44	#DIV/0!	5.01	5.01	9.99	9.99
Α	3.39	#DIV/0!	0.41	#DIV/01	0.32	0.33	0.24	0.23
Pass?	Yes	Yes	Yes	Yes	Yes	Yes	Yes	Yes

4. Signature of Technician(s) performing CGA:

Calculation of A:

 $A = (d_m - c_a) / c_a \times 100$

A must be +/-15% to pass.

where:

A = accuracy of CEM

d_m = average of reponses

c_a = certified audit value of gas



Calibration Gases & Equipment

EPA Protocol Standard Gas Mixture

To: Norco, Inc Cheyenne Warehouse 100 S. Greeley HWY Cheyenne, WY 82007 Report of Analysis and Certification Manufactured at/by: EPA Protocol Vendor ID P12014

NorLab Order#

34175499

Date Certified:

03/27/14

Customer PO#

N/A

Cylinder Pressure:

2000

psig @, 70 F

Part Number

SPG 5E166025PN

Lat Number: Cylinder Number 4-072-522

CC90737

Expiration Date:

03/26/22

Component(s)	Cone V/V	t EPA Uncertainty	Analyzer1 NO, Nox	MTO 60a FTIR			
Nitrie Oxide, ppm	26,15	0.174	Calibrated:	Assay 1, 2, 3	3/21/2014	3/21/2014	
Total Nax, ppm	26.20			SREF!			
			Analyzer 2				
			Calibrated:	Assay 1; 2; 3		#REFI	#REF
Nitrogen, O2 Free	Balance						

		Refere	nce Standard	Data		,		
Comp	tonent	Lot# and XP Date (MMYR)	10	Cyt#	Conc.	U		
Nitric	Oxide	2-094-170 XP 8x15		CC 138737	na.	25.61	0.16	
Treceable	Std if GMIS	8-023-600 XP 2x14	SRM 2628a	CAL 016489	49-11-84	9.89	0.11	
		Replic	ate Analysis	Data				
	Assay I		Assay 2		Assay 3			
NO		NO						
3/21/2014		3/27/2014						
26.05		26.08						
26.11	I	26.17						
26,22		26.19						
26,18		26,20						
26,14		26.21						
26.06		26,18						
26.13		26.17						

The analysis listed in this report was performed in accordance with the Procedure G1 of the EPA Traceability Protocol, EPA 600/R-12/531 May 2012.

The contents	of this cul	indor must not	be used if the pres	stura le lore than	a IAA nelo.
THE WHENIS	VI IIII CY	STUMBE TUMBA TEUR	US MAGU II IIIG DI G.	1304 E 13 SL33 IMU	i iuu daim.

Analysi: A

Approved:

Aaron Schwenken, Lab Technician

Charles Eckman, Quality Assurance Unit

Page 1 of 1

4-072-522 cheyenne 34175499



Calibration Gases & Equipment

EPA Protocol Standard Gas Mixture

To: Norco, Inc Cheyenne Warehouse 100 S. Greeley HWY Cheyenne, WY 82007 Report of Analysis and Certification Manufactured at/by: **EPA Protocol Vendor ID P12014**

NorLab Order #

34175499

Date Certified:

04/03/14

Customer PO# NA

Cylinder Pressure:

2000

psig @ 70 F

Part Number Lot Number: Cylinder Number SPG 5E166055PN 4-072-521

CC143970

Expiration Date:

04/02/22

_			-							
Component(s)	Cons. V/V	± EPA Uncertainty	Analyzeri NO, Nox		MTO	MTO 60a FTIR				
Nitrie Oxide, ppm	55.15	0.37	Calibrated	Assay 1, 2, 3	3/18/2014					
Total Nox, ppm	ppm 55.67 #REF*					ek:				
			Analyzer 2							
			Calibrated:	Assay 1; 2; 3		#REF!	arefi			
Nitrogen, O2 Free	Balance									
		Refere	nce Standard	Data						
Component (Lots and XP Date (MMYR)) ID Cyts Sam# Conc. U										
Nitric Oxide	3-084-17	71 XP 6x15	GMIS 1684b	CC 127510	na .	60.88	0.21			
Toronto ALLEGALIA	4 666 8	W VD Cuto	COMMON	ICAL DEFOOR	44 51 66	A4 38	7.77			

Cons		LOT and XP Date (MW/TK)	10	CYB	Sama	Conc.		
	Oxide	3-084-171 XP 6x15		CC 127610	na .	60.88	0.21	
Traceabla	Traceable Std If GMIS 1-082-60		SRM1684b	CAL 015080	44-8-92	97.45	0,41	
		Repli	cate Analysis	Data				
	Assey I		Assay 2		Atsay 3			
МО		NO						
3/20/2014		4/2/2014			N		** /	
35.15		55.19						
55.25		55.10						
55.16		55.06						
55.15		55.12						
						,		
55.18		55.12						

The analysis listed in this report was performed in accordance with the Procedure GI of the EPA Traceability Protocol, EPA 600/R-12/531 May 2012.

The contents of this cylinder must not be used if the pressure is less than 100 psig.

Analyst:

Approved:

Aaron Schwenken, 1.ab Technician

Charles Eckman, Quality Assurance Unit

Page 1 of 1

4-072-521 cheyenne 34175499





Calibration Gases & Equipment EPA Protocol Standard Gas Mixture

Report of Analysis and Certification Manufactured at/by: EPA Protocol Vendor ID P12013

To: Norco Inc.

Cheyenne Whse. 100 S. Greeley Hwy.

Cheyenne, WY. 341'

NorLab Order #

34175499

Date Certified:

03/24/14

Customer PO#

13.0

Cylinder Pressure:

2000

psig @ 70 F

Part Number

Cylinder Number

SPG 5E10725VN

Lot Number:

4-072-524

EB0042977

Expiration Date:

03/23/22

Component(s)	Conc. V/V	.t RPA Analyzer1 Uncertainty (O2)		Servomer Paramagnetic Analyzer MTO 97A				
Oxygen, %	4.999	0.029	Calibrated.	Assay 1, 2, 3	3/24/2014			
Nitrogen. O2 Free	Balance							

Reference Standard Data								
Component ht and XP Date (MM/Y) ID Cyll Samt Conc. U								
Oxygen, %	3-079-161 XP 6	X18 GMIS 2858A	CC 53742		9.913	0.043		
Traceable Std if GMIS	0-130-600 6x1	7 SRM 2658a	CAL 016948	72-D-46	9 918	0.022		

	Replica	te Analysis Data		
Assay	1	Assay 2		Азвау 3
Охудап, %	Oxygen	,%	()xygen. %	
Охудел, % 3/24/2014				
4.98				
5.00				
5.01				
5,00				
U 00 U				
0 00				
5.00				

The analysis listed in this report was performed in accordance with the Procedure G1 of the EPA Traceability Protocol, EPA 600/R-12/531 May 2012.

The contents of this cylinder, must not be used if the pressure is less than 100 psig.

Analyst:

orn, Lab Technician

Approved:

Charles Eckman, Quality Assurance Unit

Page 1 of 1

4-072-524 CHE 34175499



Calibration Gases & Equipment

EPA Protocol Standard Gas Mixture

Report of Analysis and Certification Manufactured at/by: EPA Protocol Vendor ID P12013

To:

Norco Inc.

Cheyenne Whse.

100 S. Greeley Hwy.

Cheyenne, WY. 341'

NorLab Order #

34175499

Date Certified:

03/24/14

Customer PO#

na

Cylinder Pressure:

2000

psig @ 70 F

Part Number Lot Number:

4-072-523

Cylinder Number C

CC 189312

SPG 5E107210VN

Expiration Date:

03/23/22

Component(s)	Conc. V/V	± FPA Uncertainty	Analyzeri (O2)	Servomex Paramagnetic Analyzer MT(197A			ATO 97A
Oxygen, %	10.01	0.047	Calibrated:	Assay 1, 2; 3	3/24/2014		
Nitrogen, O2 Free	Balance						

	Refer	ence Stand	dard Data			
Component	# and XP Date (MMY	ID	Cy#	Sam#	Conc.	U
Oxygen, %	3-079-161 XP 6X18	GMIS 2858A	CC 53742		9,913	0.043
Traceable Std if GMIS	0-130-600 6x17	SRM 2658a	CAL 016946	72-D-46	9.918	0.022

	Replicate Analysis Data				
Assay I	Assay 2		Assay 3		
Oxygen, %	Oxygen, %	Oxygen, %			
3/24/2014					
10 00					
10.02					
10.01					
1001					
0.00					
0 00					
10 01					

The analysis listed in this report was performed in accordance with the Procedure G1 of the EP.4 Traceability Protocol, EPA 600/R-12/531 May 2012.

The contents of this cylinder paust not be used if the pressure is less than 100 psig.

Analyst: ¿

Mil Korok Kab Technician

.tpproved:

Charles Eckman, Quality Assurance Unit

Page 1 of 1

4-072-523 CHE 34175499





Department of Environmental Quality

To protect, conserve and enhance the quality of Wyoming's environment for the benefit of current and future generations.



Todd Parfitt, Director

August 13, 2014

Mr. David Weeks **Environmental Engineer** Frontier Refining, LLC P.O. Box 1588 Cheyenne, WY 82003-1588



Re: 2014 Frontier Refining Crude Charge Heater CEMS Certification Report.

Dear Mr. Weeks:

The Wyoming Department of Environmental Quality, Air Quality Division (Division) has completed its review of the continuous emission monitoring system (CEMS) certification reports submitted by Frontier Refining, LLC (Frontier) on the crude charger heater outlet stack. Frontier conducted the CEMS certification testing at the Cheyenne plant located near Cheyenne, Wyoming during the week of March 4, 2014. Testing performed was to determine exhaust gas flow rates, concentrations, and mass emission rate of nitrogen oxides (NOx) and oxygen (O₂).

Air Pollution Testing compared the reference method testing results with the results from the Frontier facility's CEMS to decide the relative accuracy. I am happy to inform Frontier that the Division recognizes that the CEMS cited above, based on the RATA reports submitted, has demonstrated compliance with the CEMS performance specification outlined in 40 CFR 60.

If you have any questions, please feel free to contact me at (307) 777-7351.

Sincerely.

Mark Gagen

CEMS Coordinator

John Loger

Enclosure (1)

cc: Glenn Spangler, DEQ District Engineer

CEMS

File



Frontier Refining
Crude Charge Heater Certification
03/27/ 2014

Summary of Frontier Refining Crude Charge Heater

Parameter	Units	RM Value	CEMS Value	%RA Reported		% RA Limit
Nox ppm	ppm	21.6	17.3	19.95	19.88	20.0
Nox	lbs/mmBtu	0.027	0.022	19.08	19.19	20.0
02	%	4.1	4.0	0.08	0.08	1.0

Compliance

Paramter	Units		Reviewed RM Value	
Nox	ppm	21.6	21.6	N/A
Nox	lb/hr	4.7	4.7	6.3
Nox	lb/mmBtu	0.027	0.027	0.031

Section E - LDAR

LDAR Corrective Action Plan

Frontier Refining LLC
P.O. Box 1588 • Cheyenne, WY 82003-1588

Paragraph	Attachment E - LDAR	Comments
216e	Any additional items required by any other Paragraph of this Consent Decree to be submitted with a semi- annual report including but not limited to reports required under Paragraphs 137, 152, 170, and 205.	See Below
152	Implementation of Actions Necessary to Correct Non-Compliance. If the results of any of the audits conducted pursuant to Paragraphs 147 - 150 identify any areas of non-compliance, FRI and FEDRC, as applicable, shall implement all steps necessary to correct the area(s) of non-compliance as soon as possible and to prevent a recurrence of the cause of the non-compliance. For purposes of this Paragraph, a ratio of the process unit valve leak percentage established through a comparative monitoring audit conducted under Paragraphs 147 through 150 to determine the average valve leak percentage reported for the process unit for the four quarters immediately preceding the audit in excess of 3.0 shall be cause for corrective action and shall be subject to stipulated penalties as provided in Paragraph 294. If the calculated ratio yields an infinite result, FRI and FEDRC shall assume 1 leaking valve was found during the 4-quarter period and shall recalculate the ratio. Until two years after termination of this Consent Decree FRI and FEDRC shall retain the audit reports generated pursuant to Paragraphs 147 through 150 and shall maintain a written record of the corrective actions taken at each of the Covered Refineries in response to any deficiencies identified in any audits. In the semi-annual report submitted pursuant to the provisions of Paragraph 216 of this Consent Decree (Reporting and Record Keeping) for the first calendar half of each year, FRI and FEDRC shall submit the audit reports and corrective action records for audits performed and actions taken during the previous calendar year.	A Consent Decree required LDAR audit was conducted in August of 2011. The next audit was completed in August of 2013. The final report and the summary of the corrective actions taken was included in the 2nd half 2013 semi-annual report.
170	Record Keeping and Reporting. Consistent with the requirements of Section XI. (Reporting and Record Keeping), FRI and FEDRC shall maintain records to demonstrate compliance with the requirements of Section VI.M. of this Consent Decree, and shall include the information set forth below in the designated semi-annual progress report(s):	See Below
170a	First Semi-Annual Progress Report Due under this Consent Decree. At the later of the first semi-annual progress report due under this Consent Decree, or the first semi-annual progress report in which the requirement becomes due, for their respective Covered Refinery, FRI and FEDRC shall include the following:	See Below
170a.i	Copies of the written Refinery-wide LDAR Program required by Paragraph 144;	Initial plan submitted Feb. 26, 2010.
170a.ii	A certification of the implementation of the lower leak definitions and monitoring frequencies in Paragraphs 153, 154, 155, 158, and 159;	Certification submitted Aug. 31, 2009.
170a.iii	A certification of the implementation of the "initial attempt at repair" or "optical imaging" program of Paragraphs 156 and 157;	Certification submitted Apr. 15, 2009.
170a.lv	A certification of the implementation of QA/QC procedures for review of data generated by LDAR technicians as required by Paragraph 162;	Certification submitted Aug. 31, 2009.
170a.v	An identification of the individual at each of the Covered Refineries responsible for LDAR performance as required by Paragraph 144. g.;	Certification submitted Aug. 31, 2009.

Paragraph	Attachment E - LDAR	Comments
170a.vi	A certification of the development of a tracking program for new valves and pumps added during maintenance and construction as required by Paragraph 164;	Certification submitted Aug. 31, 2009.
170a.vii	A certification of the implementation of the calibration drift assessment procedures of Paragraph 166;	Certification submitted Aug. 31, 2009.
170a.viii	A certification of the implementation of the "delay of repair" procedures of Paragraph 167; and	Certification submitted Aug. 31, 2009.
170a.ix	report of the implementation of the "chronic leaker" program of Paragraph 169.	Report submitted on Feb. 26, 2010.
170b	that FRI and FEDRC submit pursuant to Section XI. (Reporting and Record Keeping) for the first calendar half of each year, they shall include an identification of each audit that was conducted pursuant to the requirements of Paragraphs 147 - 150 in the previous calendar year including an identification of the auditors, a summary of the audit results, and a summary of the actions that each took or intends to take to correct all deficiencies identified in the audits.	A Consent Decree required LDAR audit was conducted in August of 2011. The next audit was completed in August of 2013. The final report and the summary of the corrective actions taken was included in the 2nd half 2013 semi-annual report.

Section F - SEP

Frontier Refining LLC
P.O. Box 1588 • Cheyenne, WY 82003-1588

Paragraph	Attachment F - Supplemental Environmental Projects/Environmentally Beneficial Projects	Comments
216c	A description of all Supplemental Environmental Projects and implementation activity in accordance with this Consent Decree;	Per paragraph 189, geodesic domes were installed on tanks TK 2-70 and TK 2-71. The project was completed on Feb. 18, 2010.
216e	Any additional items required by any other Paragraph of this Consent Decree to be submitted with a semi- annual report including but not limited to reports required under Paragraphs 137, 152, 170, and 205.	See below.
205	FRI and FEDRC shall include in each Report required by Paragraph 216 of this Consent Decree a progress report for each SEP being performed under Paragraphs 188 through 199 of this Consent Decree. In addition to the information required by Paragraph 216 of this Consent Decree, for the reporting period in which any SEP identified in Paragraphs 188 through 199 of this Consent Decree is completed, the following information with respect to each completed SEP shall be included in the report required by Paragraph 216:	See below.
205a	A report containing a detailed description of the SEP as implemented;	Per paragraph 189, geodesic domes were installed on tanks TK 2-70 and TK 2-71. The project was completed on Feb. 18, 2010.
205b	A brief description of any significant operating problems encountered, including any that had an impact on the environment, and the solutions for each problem;	
205c	Certification, in the form required by Paragraph 219 of this Consent Decree, that the SEP has been fully implemented pursuant to the provisions of this Consent Decree together with a statement of the total SEP cost upon completion; and	Certification previously submitted Aug. 31, 2010.
205d	A description of the environmental and public health benefits resulting from implementation of each project (including quantification of the benefits and pollutant reductions, if feasible).	Per paragraph 189, installation of the geodesic domes resulted in an expected reduction of 49,490 pounds per year.

Section G - SRP

CEMS Data

Frontier Refining LLC
P.O. Box 1588 • Cheyenne, WY 82003-1588

Paragraph	Attachment G - SRPs	Comments
2424	502 - initian from all Sulfus December Diente in term non vene	Emissions information contained in
217d	SO2 emissions from all Sulfur Recovery Plants in tons per year;	this section.
	for each of the estimates or calculations in Subparagraphs 217.a. through 217.g. above, the basis for the	Basis for the emission estimate or
1 717h		calculation is included with the
ļ	emissions estimate or calculation (i.e. stack tests, CEMS, emission factor, etc.).	emission information.
240-	for operating units emissions limits that are required by this Consent Decree and monitored with CEMS, for	CEM monitoring data is included in
218a	each CEMS:	this section.

DEPARTMENT OF ENVIRONMENTAL QUALITY AIR QUALITY DIVISION CONTINUOUS EMISSION MONITORING REPORT

FORM A

I. GENERAL INFORMATION

- A. Facility Name: FRONTIER REFINING LLC
- B. Process Unit/Pollutant Monitored: <u>SO₂ MONITOR NO. 1 AND NO. 2 SULFUR RECOVERY UNITS (COMMON STACK)</u>
- C. Applicable Permit Number or Regulation: NSPS Subpart J. CT-84A2, MD-188, MD-1115A
- D. Applicable Emission Limit: 250 ppmyd @ 0% 02 (12-hr rolling average): 18.6 lb/hr (1-hr average)

II. MONITOR INFORMATION

- A. Date of Original Monitor Installation: June 28, 2000
- B. Date of Latest Monitor Certification: August 21, 2000
- C. Pollutant/Opacity Monitor
 - 1. Manufacturer: Brimstone Instrumentation LTD.
 - 2. Model Number: BRM 991-CEM
 - 3. Serial Number Main Chassis: CEM-00002-00003
 - 4. Basis of Measurement (If Applicable Wet or Dry): Wet
 - 5. Instrument Span, Range Value (Specify Units): 0-500 ppm SO₂
- D. Diluent Monitor
 - 1. Type of Monitor: Q2
 - 2. Manufacturer: AMETEK Process & Analytical Division
 - 3. Model Number: Series 2000
 - 4. Serial Number Main Chassis: 10202890
 - 5. Basis of Measurement (If Applicable Wet or Dry): Wet
 - 6. Instrument Span, Range Value (Specify Units): 0 25 percent (%)
- **E.** Flow Monitor
 - 1. Type of Instrument (i.e. S-type Pitot Tube): Pitot Tube
 - 2. Manufacturer:
 - 3. Model Number:
- 4. Serial Number Main Chassis:
- F. Quality Assurance Data
 - 1. QA Plan Date: January 7, 2013
 - 2. QA Plan Approval Date: August 29, 2013

III. Operating/Monitoring Data

A. Quarter: 1 Year: 2014

B Total Hours in Reporting Period: 2160

C. Hours Unit Operated During the Reporting Period: 2160 (Hours with one or both SRU's operating)

Note: Include <u>all</u> unit operating time for the quarter including operating time associated with Startup/Shutdown and Chapter 1 Section 5 (Emergency/Abnormal) Operations. Report time in hours to one decimal place, i.e. 1902.8.

IV. Quarterly Audits/Monitoring System Modifications

A. Quarterly Audits
Type Audit: CGA

	Date Conducted	Pass
Pollutant/Opacity Monitor:	<u>3/26/2014</u>	Yes
Diluent Monitor	<u>3/26/2014</u>	<u>Yes</u>

Note: A copy of the quarterly audits shall be included with the corresponding quarterly excess emission report.

B. Equipment Replaced During Reporting Period: <u>Changed filters and steel wool: Changed SO₂ Span Calibration Bottle: Replaced Sample Line: Changed Probe: Replaced WTC DAS to CiSCO CeDAR5.</u>

Note: Only equipment replacements or modifications to the system that could affect the ability of the continuous monitoring system to comply with the associated Performance Specification shall be reported.

V. Report Contact

A. Name: David Weeks, Environmental Engineer

B. Phone Number: (307) 771-8827

EXCESS EMISSION SUMMARY REPORT Incinerator SO2 (ppm) CEMS 12-hr rolling average = 250 ppm @ 0 % O2

FORM B

Emission Data Summary (12-hour average ppm)		CMS Performance Report		
I. Duration of Excess Emission in Reporting Per	iod Due to:	I. CMS Downtime in Reporting Period Due to:		
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	491.0	
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	60.0	
C. Process Problem	28.0	C. Quality Assurance Calibration	0.0	
D. Other Known Causes	0.0	D. Other Known Causes	13.0	
E. Unknown Causes	0.0	E. Unknown Causes	0.0	
II. Total Duration of Excess Emission	28.0	II. Total CMS Downtime	564.0	
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	1.7%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	26.1%	

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2. Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)

1Q14 TGTU Incinerator CEMS

Incinerator SO2 ppm (12-Hour)

Form C - Excess Emissions Summary

No.	Start Time	End Time	Max	Periods	Reason	Action
1	2/17/2014 6:00:00 AM	2/17/2014 3:00:00 PM	312.5	9	SRU #2 shut down	Restarted unit
2	3/4/2014 2:00:00 AM	3/4/2014 4:00:00 AM	254.1	2	Process Upset - DHDS Rate Increase	Adjused Unit Rates to Bring into Compliance
3	3/4/2014 9:00:00 PM	3/5/2014 2:00:00 PM	421.5	17	Process Upset - DHDS Rate Increase	Adjused Unit Rates to Bring Into Compliance
	Ta	tal Periods Excess Emis	esions	28		

Monday, April 28, 2014

TGTU Incinerator Excess Emissions Summary

Frontier Refining LLC SO2 ppm (dry) @0% O2 12-Hr Rolling Excess Emissions for 3/26/2014 thru 3/31/2014

Reason	Duration
There are no excess emissions for this report.	
Total duration of SO2 ppm (dry) @0% O2 12-Hr Rolling excess emissions	0
Total operating time	144 hours
Operating time with excess emissions	0.0%

Incinerator SO2 ppm (1-Hour)

No.	Start Time	End Time	Hours	Reason	Action
1	1/5/2014 4:00:00 AM	1/8/2014 10:00:00 AM	30	Failed daily CD check (excessive drift)	Ran Manual Calibration
2	1/8/2014 4:00:00 AM	1/8/2014 6:00:00 AM	2	Sample system fallure	Cleaned Sample Cell
3	1/8/2014 10:00:00 AM	1/8/2014 11:00:00 AM	1	Sample system failure	Cleaned Sample Cell
4	1/8/2014 10:00:00 PM	1/8/2014 11:00:00 PM	1	Sample system failure	Replaced Sample Line
5	1/9/2014 9:00:00 AM	1/9/2014 1:00:00 PM	4	Sample system failure	Replaced Sample Line
6	1/10/2014 8:00:00 AM	1/10/2014 10:00:00 AM	2	Sample system failure	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
7	1/11/2014 4:00:00 AM	1/11/2014 6:00:00 AM	2	Sample system failure	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
8	1/13/2014 12:00:00 PM	1/13/2014 3:00:00 PM	3	Sample system fallure	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
9	1/14/2014 10:00:00 AM	1/14/2014 11:00:00 AM	1	Sample system failure	Leak Checked Sample Line - Reptaced Sample Line
10	1/20/2014 10:00:00 AM	1/20/2014 11:00:00 AM	1	Sample system failure	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
11	1/21/2014 1:00:00 AM	1/21/2014 2:00:00 AM	1	Sample system failure	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
12	1/22/2014 8:00:00 AM	1/22/2014 1:00:00 PM	5	Sample system failure	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
13	1/22/2014 6:00:00 PM	1/22/2014 8:00:00 PM	2	Sample system failure	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
14	1/22/2014 9:00:00 PM	1/22/2014 10:00:00 PM	1	Sample system failure	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
15	1/23/2014 3:00:00 AM	1/23/2014 7:00:00 AM	4	Sample system fallure	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
16	1/23/2014 10:00:00 AM	1/23/2014 1:00:00 PM	3	Sample system fallure	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
17	1/23/2014 9:00:00 PM	1/25/2014 4:00:00 AM	31	SO2 Analyzer issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer

Incinerator SO2 ppm (1-Hour)

No.	Start Time	End Time	Hours	Reason	Action
18	1/28/2014 4:00:00 AM	1/28/2014 6:00:00 AM	2	SO2 Analyzer issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
19	1/28/2014 8:00:00 AM	1/28/2014 10:00:00 AM	2	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
20	1/28/2014 1:00:00 PM	1/28/2014 5:00:00 PM	4	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
21	1/29/2014 4:00:00 AM	1/29/2014 2:00:00 PM	10	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
22	1/30/2014 2:00:00 AM	1/30/2014 3:00:00 AM	1	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
23	1/30/2014 5:00:00 AM	1/30/2014 6:00:00 AM	1	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
24	1/31/2014 4:00:00 PM	1/31/2014 6:00:00 PM	2	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
25	1/31/2014 9:00:00 PM	1/31/2014 10:00:00 PM	1	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
26	<i>2/1/</i> 2014	2/1/2014 2:00:00 AM	2	SQ2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
27	2/1/2014 4:00:00 AM	2/4/2014 4:00:00 AM	72	Failed daily CD check (excessive drift)	Passed Morning Cal
28	2/5/2014 4:00:00 AM	2/12/2014 2:00:00 PM	178	Falled daily CD check (excessive drift)	OEM Service Technician Troubleshooting
29	2/13/2014 4:00:00 AM	2/13/2014 10:00:00 AM	6	Failed daily CD check (excessive drift)	Ran Manual Calibration
30	2/13/2014 6:00:00 PM	2/14/2014 2:00:00 PM	20	SO2 Analyzer issues	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
31	2/25/2014 4:00:00 AM	2/25/2014 9:00:00 AM	5	Failed daily CD check (excessive drift)	Ran Manual Calibration
32	2/27/2014 2:00:00 AM	2/27/2014 3:00:00 AM	1	SO2 Analyzer Issues	Worked on Analyzer - Pulling Draegers every Hour
33	2/27/2014 5:00:00 AM	2/27/2014 6:00:00 PM	13	SO2 Analyzer issues	Worked on Analyzer - Pulling Draegers every Hour
34	2/27/2014 7:00:00 PM	2/27/2014 9:00:00 PM	2	SO2 Analyzer Issues	Worked on Analyzer - Pulling Draegers every Hour

Incinerator SO2 ppm (1-Hour)

No.	Start Time	End Time	Hours	Reason	Action
35	2/27/2014 10:00:00 PM	3/1/2014 6:00:00 PM	44	SO2 Analyzer issues	Worked on Analyzer - Pulling Draegers every Hour
36	3/2/2014 1:00:00 AM	3/2/2014 2:00:00 AM	1	SO2 Analyzer issues	Worked on Analyzer - Pulling Draegers every Hour
37	3/2/2014 3:00:00 AM	3/2/2014 5:00:00 AM	2	SO2 Analyzer issues	Worked on Analyzer - Pulling Draegers every Hour
38	3/2/2014 10:00:00 AM	3/2/2014 6:00:00 PM	8	SO2 Analyzer Issues	Worked on Analyzer - Pulling Draegers every Hour
39	3/2/2014 8:00:00 PM	3/3/2014 1:00:00 PM	17	SO2 Analyzer issues	Worked on Analyzer - Pulling Draegers every Hour
40	3/14/2014 11:00:00 AM	3/14/2014 12:00:00 PM	1	Sulfur Unit problems caused high SO2, knocking CEMS out of calibration	Cleared probe and sample line, changed liters and steel wool. Ran Manual Cal.
41	3/14/2014 9:00:00 PM	3/14/2014 10:00:00 PM	1	Suffur Unit problems caused high SO2, knocking CEMS out of calibration	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
42	3/14/2014 11:00:00 PM	3/15/2014 1:00:00 AM	2	Suffur Unit problems caused high SO2, knocking CEMS out of calibration	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
43	3/15/2014 4:00:00 AM	3/17/2014 4:00:00 AM	48	Failed daily CD check (excessive drift)	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
44	3/17/2014 11:00:00 PM	3/18/2014	1	SO2 Analyzer Issues	No Action Taken - Self Corrected
45	3/22/2014 5:00:00 AM	3/22/2014 8:00:00 AM	3	SO2 Analyzer Issues	Cleared Probe, changed Filters and Steel Wool
46	3/22/2014 9:00:00 AM	3/22/2014 3:00:00 PM	6	SO2 Analyzer Issues	Cleared Probe, changed Filters and Steel Wool
47	3/25/2014 2:00:00 PM	3/25/2014 3:00:00 PM	1	SO2 Analyzer Issues	No Action Taken - Self Corrected
	Total Ho	urs Monitor Unavailable	551		

TGTU Incinerator CEMS Downtime Summary

Frontier Refining LLC SO2 ppm CEMS Downtime for 3/26/2014 thru 3/31/2014

Reason	Duration
Data Acquisition System (DAS) Conversion from WTC to CISCO CeDAR5 - Start-Up Issues	13 hours
Total duration of SO2 ppm CEMS downtime	13 hours
Total operating time	144 hours
Operating time with CEMS downtime	9.0%

Comment: Data Acquisition System (DAS) Conversion from WTC to CISCO CeDAR5 on 26-Mar-14

TGTU Incinerator CEMS Downtime

Frontier Refining LLC SO2 ppm CEMS Downtime for 3/26/2014 thru 3/31/2014

Parameter	Start	End	Duration	Reason	Action
SO2 ppm	3/26/2014 1:00 PM	4:59 PM	4 hours	Data Acquisition System (DAS) Conversion from WTC to CISCO CeDAR5 - Start-Up Issues	Troubleshoot DAS Conversion Start-Up lasues
SO2 ppm	3/27/2014 11:00 AM	11:59 AM	1 hour	Data Acquisition System (DAS) Conversion from WTC to CISCO CeDAR5 - Start-Up Issues	Troubleshoot DAS Conversion Start-Up Issues
SO2 ppm	3/28/2014 3:00 AM	6:59 AM	4 hours	Data Acquisition System (DAS) Conversion from WTC to CISCO CeDAR5 - Start-Up Issues	Troubleshoot DAS Conversion Start-Up issues
SO2 ppm	3/31/2014 6:00 AM	9:59 AM	4 hours	Data Acquisition System (DAS) Conversion from WTC to CiSCO CeDAR5 - Start-Up tssues	Troubleshoot DAS Conversion Start-Up Issues
	Total duration		13 hours		

Comment: Data Acquisition System (DAS) Conversion from WTC to CiSCO CeDAR5 on 26-Mar-14

EXCESS EMISSION SUMMARY REPORT Incinerator SO2 (lb/hr) CEMS 1-hr average = 18.6 lb/hr

FORM B

Emission Data Summary (lb/hr))	CMS Performance Report		
I. Duration of Excess Emission in Reporting Pe	riod Due to:	I. CMS Downtime in Reporting Period Due to:		
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	168.0	
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	151.0	
C. Process Problem	5.0	C. Quality Assurance Calibration	0.0	
D. Other Known Causes 0.0		D. Other Known Causes	43.0	
E. Unknown Causes	0.0	E. Unknown Causes	0.0	
II. Total Duration of Excess Emission	5.0	II. Total CMS Downtime	362.0	
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.1%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	16.8%	

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2. Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)

1Q14 TGTU Incinerator CEMS

Incinerator SO2 lbs/hr (1-Hour)

Form C - Excess Emissions Summary

No.	Start Time	End Time	Max	Periods	Reason	Action
1	2/17/2014 11:00:00 PM	2/18/2014 1:00:00 AM	19.5	2	SRU #2 shut down	Restarted unit
2	3/4/2014 7:00:00 PM	3/4/2014 9:00:00 PM	20.7	2	Process Upset - DHDS Rate Increase	Adjused Unit Rates to Bring into Compliance
3	3/4/2014 10:00:00 PM	3/4/2014 11:00:00 PM	22.1	1	Process Upset - DHDS Rate Increase	Adjused Unit Rates to Bring Into Compliance
Total Periods Excess Emissions						

TGTU Incinerator Excess Emissions Summary

Frontier Refining LLC SO2 lbs 1-Hr Excess Emissions for 3/26/2014 thru 3/31/2014

Reason	Duration
There are no excess emissions for this report.	
Total duration of SO2 ibs 1-Hr excess emissions	0
Total operating time	144 hours
Operating time with excess emissions	0.0%

Comment: Data Acquisition System (DAS) Conversion from WTC to CISCO CeDAR5 on 26-Mar-14

Incinerator SO2 lbs/hr (1-Hour)

No.	Start Time	End Time	Hours	Reason	Action
1	1/8/2014 5:00:00 AM	1/8/2014 6:00:00 AM	1	Sample system failure	Cleaned Sample Cell
2	1/8/2014 10:00:00 AM	1/8/2014 11:00:00 AM	1	Sample system fallure	Cleaned Sample Call
3	1/8/2014 10:00:00 PM	1/8/2014 11:00:00 PM	1	Sample system fallure	Replaced Sample Line
<u>,</u>	1/9/2014 9:00:00 AM	1/9/2014 1:00:00 PM	4	Sample system fallure	Replaced Sample Line
5	1/13/2014 12:00:00 PM	1/13/2014 3:00:00 PM	3	Sample system failure	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
6	1/14/2014 10:00:00 AM	1/14/2014 11:00:00 AM	1	Sample system failure	Leak Checked Sample Line - Replaced Sample Line
7	1/20/2014 10:00:00 AM	1/20/2014 11:00:00 AM	1	Sample system failure	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
8	1/20/2014 3:00:00 PM	1/20/2014 4:00:00 PM	1	Sample system faiture	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
9	1/21/2014	1/21/2014 2:00:00 AM	2	Sample system failure	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
10	1/21/2014 9:00:00 AM	1/21/2014 10:00:00 AM	1	Sample system fallure	Cleared probe and sample line, changed filters and steel wool. Ran Manuel Cal.
11	1/22/2014 8:00:00 AM	1/22/2014 1:00:00 PM	5	Sample system fallure	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
12	1/22/2014 6:00:00 PM	1/22/2014 8:00:00 PM	2	Sample system failure	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
13	1/22/2014 9:00:00 PM	1/22/2014 10:00:00 PM	1	Sample system failure	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
14	1/23/2014 3:00:00 AM	1/23/2014 7:00:00 AM	4	Sample system failure	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
15	1/23/2014 10:00:00 AM	1/23/2014 1:00:00 PM	3	Sample system failure	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
16	1/23/2014 9:00:00 PM	1/24/2014 8:00:00 PM	23	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
17	1/28/2014 5:00:00 AM	1/28/2014 6:00:00 AM	1	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer

incinerator SO2 ibs/hr (1-Hour)

No.	Start Time	End Time	Hours	Reason	Action
18	1/28/2014 8:00:00 AM	1/28/2014 10:00:00 AM	2	SO2 Analyzar Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
19	1/28/2014 1:00:00 PM	1/28/2014 5:00:00 PM	4	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
20	1/29/2014 11:00:00 AM	1/29/2014 12:00:00 PM	1	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
21	1/30/2014 2:00:00 AM	1/30/2014 3:00:00 AM	1	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
22	1/30/2014 5:00:00 AM	1/30/2014 6:00:00 AM	1	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
23	1/31/2014 4:00:00 PM	1/31/2014 6:00:00 PM	2	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - installed a Parallel SO2 Analyzer
24	1/31/2014 9:00:00 PM	1/31/2014 10:00:00 PM	1	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
25	2/1/2014	2/1/2014 7:00:00 AM	7	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
26	2/1/2014 11:00:00 AM	2/1/2014 1:00:00 PM	2	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
27	2/1/2014 5:00:00 PM	2/1/2014 8:00:00 PM	3	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
28	2/2/2014 9:00:00 AM	2/2/2014 10:00:00 AM	1	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - installed a Parallel SO2 Analyzer
29	2/2/2014 11:00:00 AM	2/2/2014 12:00:00 PM	1	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
30	2/2/2014 3:00:00 PM	2/2/2014 4:00:00 PM	1	SO2 Analyzer issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
31	2/3/2014 3:00:00 PM	2/3/2014 5:00:00 PM	2	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
32	2/3/2014 7:00:00 PM	2/3/2014 11:00:00 PM	4	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
33	2/7/2014 9:00:00 AM	2/7/2014 2:00:00 PM	5	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - installed a Parallel SO2 Analyzer

Incinerator SO2 lbs/hr (1-Hour)

No.	Start Time	End Time	Hours	Reason	Action
34	2/7/2014 3:00:00 PM	2/7/2014 11:00:00 PM	8	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
35	2/8/2014 2:00:00 AM	2/8/2014 9:00:00 AM	7	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parellel SO2 Analyzer
36	2/8/2014 11:00:00 AM	2/8/2014 7:00:00 PM	8	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
37	2/8/2014 8:00:00 PM	2/8/2014 9:00:00 PM	1	SO2 Analyzer issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
38	2/8/2014 10:00:00 PM	2/9/2014 3:00:00 AM	5	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
39	2/9/2014 11:00:00 AM	2/9/2014 3:00:00 PM	4	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - installed a Parallel SO2 Analyzer
40	2/9/2014 6:00:00 PM	2/9/2014 8:00:00 PM	2	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
41	2/9/2014 9:00:00 PM	2/9/2014 10:00:00 PM	1	SO2 Analyzer issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parellel SO2 Analyzer
42	2/10/2014 10:00:00 AM	2/10/2014 7:00:00 PM	9	SO2 Analyzer Issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
43	2/10/2014 10:00:00 PM	2/10/2014 11:00:00 PM	1	SO2 Analyzer Issues - Appears to be Amine Contemination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
44	2/11/2014	2/11/2014 2:00:00 PM	14	SO2 Analyzer issues - Appears to be Amine Contamination	Worked on Analyzer - Installed a Parallel SO2 Analyzer
45	2/11/2014 3:00:00 PM	2/11/2014 9:00:00 PM	6	SO2 Analyzer Issues - Appears to be Amine Contamination	OEM Service Technician Troubleshooting
46	2/12/2014 11:00:00 AM	2/12/2014 1:00:00 PM	2	SO2 Analyzer Issues - Appears to be Amine Contamination	OEM Service Technician Troubleshooting
47	2/13/2014 6:00:00 PM	2/14/2014 12:00:00 PM	18	SO2 Analyzer Issues	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
48	2/27/2014 1:00:00 AM	3/3/2014 1:00:00 PM	108	SO2 Analyzer Issues	Worked on Analyzer - Pulling Draegers every Hour
49	3/14/2014 11:00:00 AM	3/14/2014 12:00:00 PM	1	Sulfur Unit problems caused high SO2, knocking CEMS out of calibration	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.

incinerator SO2 lbs/hr (1-Hour)

No.	Start Time	End Time	Hours	Reason	Action
50	3/14/2014 9:00:00 PM	3/14/2014 10:00:00 PM	1	Suffur Unit problems caused high SO2, knocking CEMS out of calibration	Cleared probe and sample line, changed filters and steel wool, Ran Manual Cal.
51	3/14/2014 11:00:00 PM	3/15/2014 1:00:00 AM	2	Sulfur Unit problems caused high SO2, knocking CEMS out of calibration	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
52	3/15/2014 1:00:00 PM	3/15/2014 2:00:00 PM	1	Sulfur Unit problems caused high SO2, knocking CEMS out of calibration	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
53	3/15/2014 3:00:00 PM	3/15/2014 10:00:00 PM	7	Suffur Unit problems caused high SO2, knocking CEMS out of calibration	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
54	3/15/2014 11:00:00 PM	3/16/2014	1	Sulfur Unit problems caused high SO2, knocking CEMS out of calibration	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
65	3/16/2014 1:00:00 AM	3/16/2014 2:00:00 AM	1	Suffur Unit problems caused high SO2, knocking CEMS out of calibration	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
56	3/16/2014 3:00:00 AM	3/16/2014 4:00:00 AM	1	Sulfur Unit problems caused high SO2, knocking CEMS out of calibration	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cai.
57	3/16/2014 6:00:00 AM	3/16/2014 9:00:00 AM	3	Sutfur Unit problems caused high SO2, knocking CEMS out of calibration	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
58	3/16/2014 12:00:00 PM	3/16/2014 3:00:00 PM	3	Sulfur Unit problems caused high SO2, knocking CEMS out of calibration	Cleared probe and sample line, changed filters and steel wool. Ran Manual Cal.
59	3/17/2014 11:00:00 PM	3/18/2014	1	SO2 Analyzer Issues	No Action Taken - Self Corrected
60	3/22/2014 5:00:00 AM	3/22/2014 8:00:00 AM	3	SO2 Analyzer Issues	Cleared Probe, changed Filters and Steel Wool
61	3/22/2014 9:00:00 AM	3/22/2014 3:00:00 PM	6	SO2 Analyzer issues	Cleared Probe, changed Filters and Steel Wool
62	3/25/2014 2:00:00 PM	3/25/2014 3:00:00 PM	1	SO2 Analyzer Issues	No Action Taken - Self Corrected
	Total Ho	urs Monitor Unavailable	319		

TGTU Incinerator CEMS Downtime Summary

Frontier Refining LLC SO2 lbs CEMS Downtime for 3/26/2014 thru 3/31/2014

Reason	Duration
Data Acquisition System (DAS) Conversion from WTC to CISCO CaDAR5 - Stack Flow Start-Up Issues	35 hours
Data Acquisition System (DAS) Conversion from WTC to CiSCO CeDAR5 - Start-Up issues	8 hours
Total duration of SO2 lbs CEMS downtime	43 hours
Total operating time	144 hours
Operating time with CEMS downtime	29.9%

Comment: Data Acquisition System (DAS) Conversion from WTC to CISCO CeDAR5 on 28-Mar-14

TGTU Incinerator CEMS Downtime

Frontier Refining LLC SO2 lbs CEMS Downtime for 3/26/2014 thru 3/31/2014

Parameter	Start End Duration Reason		Action		
SO2 lbs	3/26/2014 1:00 PM	11:59 PM	11 hours	Data Acquisition System (DAS) Conversion from WTC to CISCO CeDAR5 - Stack Flow Start-Up Issues	Troubleshoot DAS Conversion Start-Up Issues
SO2 ibs	3/27/2014 12:00 AM	11:59 PM	24 hours	Data Acquisition System (DAS) Conversion from WTC to CISCO CeDAR5 - Stack Flow Start-Up Issues	Troubleshoot DAS Conversion Start-Up Issues
SO2 lbs	3/28/2014 3:00 AM	6:59 AM	4 hours	Data Acquisition System (DAS) Conversion from WTC to CISCO CeDAR5 - Start-Up Issues	Troubleshoot DAS Conversion Start-Up issues
SO2 ibs	3/31/2014 6:00 AM	9:59 AM	4 hours	Data Acquisition System (DAS) Conversion from WTC to CISCO CeDAR5 - Start-Up lasues	Troubleshoot DAS Conversion Start-Up issues
	Total duration		43 hours		

Comment: Data Acquisition System (DAS) Conversion from WTC to CiSCO CeDAR5 on 26-Mar-14

Data Sheet for TGTU Incinerator CEM System Cylinder Gas Audit

1. Date Audit Commenced: 26-Mar-14 Time Audit Commenced: 9:50 a.m.

2. Audit Gases Used for CGA (All gases to be Protocol 1 Certified):

Acceptable Audit Gas Ranges	Cylinder Number and Expiration Date	Audit Gas Concentration	+/- of Audit Gas Range	
SO ₂ Low:	EB0038571	127.20		39.75%
100 - 150 ppm	3-Mar-22	127.20	ppm	38.7576
SO₂ Mid: ∂50 - 300 ppm	CC420619 300.70 p		ppm	93.97%
	28-Feb-21	300.70	53.51 70	
O₂ Low: 4 - 6% by volume	CC420681	4.96	%	19.85%
	4-Mar-21	4.50	18.0376	
O ₂ Mid:	CC2603	9,95	%	39.82%
8 - 12% by volume	5-Mar-21	70 08.8		39.02%

3. CEM System Response:

	Low-Span NO _x		Mid-Span NO _x		Low-Span O ₂		Mid-Span O ₂	
	Analyzer	CeDAR	Analyzer	CeDAR	Analyzer	CeDAR	Analyzer	CeDAR
Run 1	130.00	NA	301.00	NA	4.88	NA	9.84	NA
Run 2	118.00	NA	306.00	NA	4.88	NA	9.83	NA
Run 3	127.00	NA	308.00	NA	4.88	NA	9.83	NA
Avg. (d _m)	125.00	#DIV/0I	305.00	#DIV/0!	4.88	#DIV/0!	9.83	#DIV/0!
Α	1.73%	#DIV/0!	1.43%	#DIV/0I	1.67%	#DIV/0!	1.21%	#DIV/0!
Pass?	Yes	#DIV/01	Yes	#DIV/01	Yes	#DIV/01	Yes	#DIV/0!

4. Signature of Technician(s) performing CGA:

Matt Hobbs, Kevin Marschner and/or Tad Milliken

Calculation of A:

 $A = (d_m - c_a) / c_a \times 100$

A must be +/-15% to pass.

where:

A = accuracy of CEM

d_m = average of reponses

c_a = certified audit value of gas



Calibration Gases & Equipment

EPA Protocol Standard Gas Mixture

To:

Norco, Inc

Cheyenne Warehouse 100 S. Greeley HWY Cheyenne, WY 82007 Report of Analysis and Certification
Manufactured at/by:

EPA Protocol Vendor ID P12013

NorLab Order #

34020710

Date Certified:

03/04/14

Customer PO#

N/A

Cylinder Pressure:

2000

psig @ 70 F

Part Number Lot Number: SPG 5E1079125PN

Cylinder Number

4-049-521 EB0038571

8571 Expiration Date:

03/03/22

Component(s)	Component(s) Conc. V/V			MTO 6	On FTIR		
Sulfur Dioxide, ppm	127.2	1.2	Calibrated:	Assay 1; 2; 3	2/12/2014	2/12/2014	
Nitrogen, O2 Free			1				
		Refere	nce Standard	l Data			
Component	Lot# and XP	Date (MM/YR	i iD	Cy#	Sam#	Conc.	U
Sulfur Dioxide, ppm		75 XP 3X16	GMIS1661A	CC 32121	NA	101.9	0.82
Traceable Std If GM		10 XP 1X17	SRM 1661A	FF28137	94-H-18	490.9	3.0
		Repli	cate Analysis	Data			
Assay			Assny 2			Assay 3	
SO2		SO2					
2/25/2014		3/4/2014					
127.2							
127.4		L					
127.1							
J27 3		1-15					
00		00					
0.0		0.0			· · · · · · · · · · · · · · · · · · ·		
127 2		127.2	1	 			

The analysis listed in this report was performed in accordance with the Procedure GI of the EPA Traceability Protocol, EPA 600/R-12/331 May 2012.

The contents of this cylinder must not be used if the pressure is less than 190 psig.

dunkati

Aaron Schwenken, Lab Technician

Anneounds

Laft Many One How Advantage Class

Page 1 of 1

4-049-521 CHEYENNE 34020710 EB0038571

898 W. GOWEN ROAD • BOISE, IDAHO 83705 Phone (208) 336-1643 • Fax (208) 331-3038 • 800-657-6672

DEPARTMENT OF ENVIRONMENTAL QUALITY AIR QUALITY DIVISION CONTINUOUS EMISSION MONITORING REPORT

FORM A

L GENERAL INFORMATION

- A. Facility Name: FRONTIER REFINING LLC
- B. Process Unit/Pollutant Monitored: <u>SO₂ MONTTOR NO. 1 AND NO. 2 SULFUR RECOVERY UNITS (COMMON STACK)</u>
- C. Applicable Permit Number or Regulation: NSPS Subpart J. CT-84A2, MD-188, MD-1115A
- D. Applicable Emission Limit: 250 ppmvd @ 0% 02 (12-hr rolling average): 18.6 lb/hr (1-hr average)

II. MONITOR INFORMATION

- A. Date of Original Monitor Installation: <u>June 28, 2000</u>
 B. Date of Latest Monitor Certification: August 21, 2000
- C. Pollutant/Opacity Monitor
 - 1. Manufacturer: Brimstone Instrumentation LTD.
 - 2. Model Number: BRM 991-CEM
 - 3. Serial Number Main Chassis: CEM-00002-00003
 - 4. Basis of Measurement (If Applicable Wet or Dry): Wet
 - 5. Instrument Span, Range Value (Specify Units): 0-500 ppm SO₂
- D. Diluent Monitor
 - 1. Type of Monitor: O2
 - 2. Manufacturer: AMETEK Process & Analytical Division
 - 3. Model Number: Series 2000
 - 4. Serial Number Main Chassis: 10202890
 - 5. Basis of Measurement (If Applicable Wet or Dry): Wet
 - 6. Instrument Span, Range Value (Specify Units): 0-25 percent (%)
- E. Flow Monitor
 - 1. Type of Instrument (i.e. S-type Pitot Tube): Pitot Tube
 - 2. Manufacturer:
 - 3. Model Number:
- 4. Serial Number Main Chassis:
- P. Quality Assurance Data
 - 1. QA Plan Date: January 7, 2013
 - 2. QA Plan Approval Date: August 29, 2013

III. Operating/Monitoring Data

A. Quarter: 2 Year: 2014

B Total Hours in Reporting Period: 2184

C. Hours Unit Operated During the Reporting Period: 2184 (Hours with one or both SRU's operating)

Note: Include <u>all</u> unit operating time for the quarter including operating time associated with Startup/Shutdown and Chapter 1 Section 5 (Emergency/Abnormal) Operations. Report time in hours to one decimal place, i.e. 1902.8.

IV. Quarterly Audits/Monitoring System Modifications

A. Quarterly Audits

Type Audit: CGA

Date Conducted Pass
Pollutant/Opacity Monitor: 6/6/2014 Yes
Diluent Monitor 6/6/2014 Yes

Note: A copy of the quarterly audits shall be included with the corresponding quarterly excess emission report.

B. Equipment Replaced During Reporting Period: <u>Changed Sample Filters: Changed SO</u>
Span Calibration Bottle: Replaced RTD.

Note: Only equipment replacements or modifications to the system that could affect the ability of the continuous monitoring system to comply with the associated Performance Specification shall be reported.

V. Report Contact

A. Name: David Weeks, Environmental Engineer

B. Phone Number: (307) 771-8827

EXCESS EMISSION SUMMARY REPORT Incinerator SO2 (ppm) CEMS 12-hr rolling average = 250 ppm @ 0 % O2

FORM B

Emission Data Summary (12-hour averag	e ppm)	CMS Performance Report				
I. Duration of Excess Emission in Reporting Peri	od Due to:	I. CMS Downtime in Reporting Period Due to:				
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	130.0			
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	0.0			
C. Process Problem	7.0	C. Quality Assurance Calibration	0.0			
D. Other Known Causes	0.0	D. Other Known Causes	2.0			
E. Unknown Causes	0.0	E. Unknown Causes	0.0			
II. Total Duration of Excess Emission	7.0	II. Total CMS Downtime	132.0			
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.3%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	6.0%			

Total time of excess emission events due to emergency/abnormal operations: _____0_. NOTE:

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2. Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)

TGTU Incinerator Excess Emissions Summary Frontier Refining LLC SO2 ppm (dry) @0% O2 12-Hr Rolling Excess Emissions for 4/1/2014 thru 6/30/2014

Reason	Duration
Process Upset - SWS Temperature and Pressure Issues	7 hours
Total duration of SO2 ppm (dry) @0% O2 12-Hr Rolling excess emissions	7 hours
Total operating time	2184 hours
Operating time with excess emissions	0.3%

Comment: Form C - Excess Emission Summary

TGTU Incinerator Excess Emissions

Frontier Refining LLC SO2 ppm (dry) @0% O2 12-Hr Rolling Excess Emissions for 4/1/2014 thru 6/30/2014

Parameter	Start	End	Duration	Value	Min	Max	Limit	Reason	Action
SO2 ppm (dry) @0% O2 12-Hr Rolling	5/8/2014 4:00 AM	10:59 AM	7 hours	287.7	250.8	305.6	250	Process Upset - SWS Temperature and Pressure Issues	Made Louver Adjustments

7 hours

Comment: Form C - Excess Emission Summary

Total duration

TGTU Incinerator CEMS Downtime Summary Frontier Refining LLC SO2 ppm CEMS Downtime for 4/1/2014 thru 6/30/2014

Reason	Duration
Analyzer Out of Control - During startup of SRU2 they were running the start gasses thru the incinerator. This was leaving a light coating on the lenses which caused the analyzer to drift towards a negitive number.	16 hours
Failed Morning O2% & SO2 ppm Span Calibration Checks - OOC	2 hours
Falled Morning SO2 ppm Zero & Span Calibration Check	9 hours
Falled Morning SO2 Span Calibration Check	2 hours
Failed Morning SO2 Zero Calibration Check	2 hours
Maintenance	2 hours
Sample Filters Plugged after Unit Excursion	3 hours
Sample Interface Malfunction	53 hours
Sample Interface Malfunction - Zinc Cell Heater	17 hours
Sample Interface Malunction - Zinc Cell Heater	1 hour
Sample System Malfunction	22 hours
SO2 Analyzer Out-of-Range - Result of Prior Upsets caused by Boilers #1 & #2 Shutdown	3 hours
Total duration of SO2 ppm CEMS downtime	132 hours
Total operating time	2184 hours
Operating time with CEMS downtime	6.0%

Comment: Form D - Downtime Summary

TGTU Incinerator CEMS Downtime

Frontier Refining LLC SO2 ppm CEMS Downtime for 4/1/2014 thru 6/30/2014

Parameter	Start	End	Duration	Reason	Action
SO2 ppm	4/1/2014 2:00 AM	4:59 AM	3 hours	Sample System Malfunction	Passed Moming Calibration Check
SO2 ppm	4/1/2014 9:00 AM	9:59 AM	1 hour	Maintenance	Replaced RTD going to SO2 incinerator.
SO2 ppm	4/2/2014 5:00 AM	8:59 AM	4 hours	Sample System Malfunction	Self Corrected
SO2 ppm	4/10/2014 9:00 AM	9:59 AM	1 hour	Maintenance	Took unit out of service to zero and clean probe. Probe was partially plugged.
SO2 ppm	4/11/2014 5:00 PM	7:59 PM	3 hours	Sample Interface Malfunction	Self Corrected
SO2 ppm	4/12/2014 7:00 AM	11:59 AM	5 hours	Sample Interface Matfunction	Self Corrected
SO2 ppm	4/13/2014 7:00 AM	11:59 PM	17 hours	Sample Interface Malfunction	Passed Manual Calibration
SO2 ppm	4/14/2014 12:00 AM	1:59 PM	14 hours	Sample Interface Malfunction	Passed Manual Calibration
SO2 ppm	4/14/2014 10:00 PM	11:59 PM	2 hours	Sample Interface Malfunction	Self Corrected
SO2 ppm	4/15/2014 12:00 AM	1:59 AM	2 hours	Sample Interface Matfunction	Self Corrected
SO2 ppm	4/17/2014 5:00 AM	6:59 AM	2 hours	Falled Moming SO2 Zero Calibration Check	Adjusted zero on incinerator SO2 enalyzer. Ren validation.
SO2 ppm	4/20/2014 10:00 AM	2:59 PM	5 hours	Sample Interface Malfunction - Zinc Cell Heater	Zinc Cell heater was reading low and causing readings to be invalid. Adjusted heater and started working again on 27-Apr-14.
SO2 ppm	4/20/2014 4:00 PM	6:59 PM	3 hours	Sample Interface Malfunction - Zinc Cell Heater	Zinc Cell heater was reading low and causing readings to be invalid. Adjusted heater and started working again on 27-Apr-14.
SO2 ppm	4/22/2014 5:00 PM	6:59 PM	2 hours	Sample Interface Malfunction - Zinc Cell Heater	Zinc Cell heater was reading low and causing readings to be invalid. Adjusted heater
SO2 ppm	4/26/2014 8:00 AM	2:59 PM	7 hours	Sample Interface Matfunction - Zinc Cell Heater	Zinc Cell heater was reading low and causing readings to be invalid. Adjusted heater
SO2 ppm	4/27/2014 11:00 AM	11:59 AM	1 hour	Sample Interface Matunction - Zinc Ceil Heater	Zinc Cell heater was reading low and causing readings to be invalid. Adjusted heater.

Parameter	Start	End	Duration	Reason	Action
SO2 ppm	4/29/2014 12:00 AM	9:59 AM	10 hours	Sample Interface Malfunction	Changed out sample filter and cleared the alarm on the analyzer.
SO2 ppm	4/29/2014 6:00 PM	11:59 PM	6 hours	Sample System Malfunction	Took SO2 out of service to perform testing of the flow system. Waiting on part to fix flow.
SO2 ppm	4/30/2014 12:00 AM	8:59 AM	9 hours	Sample System Malfunction	Took SO2 out of service to perform testing of the flow system. Waiting on part to fix flow.
SO2 ppm	5/7/2014 7:00 AM	8:59 AM	2 hours	Failed Morning SO2 Span Calibration Check	Ran zero and span calibration and manually adjusted settings. Performed maintenance on unit as well changing out filter.
SO2 ppm	5/29/2014 4:00 PM	6:59 PM	3 hours	Sample Filters Plugged after Unit Excursion	Changed Filters
SO2 ppm	6/14/2014 12:00 AM	1:59 AM	2 hours	SO2 Analyzer Out-of-Range - Result of Prior Upsets caused by Bollers #1 & #2 Shutdown	Pulled and cleaned filters and tubing.
SO2 ppm	6/14/2014 4:00 AM	4:59 AM	1 hour	SO2 Analyzer Out-of-Range - Result of Prior Upsets caused by Bollers #1 & #2 Shutdown	Pulled and cleaned filters and tubing.
SO2 ppm	6/14/2014 5:00 AM	1:59 PM	9 hours	Failed Morning SO2 ppm Zero & Span Calibration Check	Changed sample probe filter. Ran Manual Calibration
SO2 ppm	6/15/2014 5:00 AM	6:59 AM	2 hours	Falled Morning O2% & SO2 ppm Span Calibration Checks - OOC	Changed sample probe filter. Ran validation on both analyzers.
SO2 ppm	6/30/2014 8:00 AM	11:59 PM	16 hours	Analyzer Out of Control - During startup of SRU2 they were running the start gasses thru the incinerator. This was leaving a light coating on the lenses which caused the analyzer to drift towards a negitive number.	Cleaned the lenses multiple times and purged the lines but still had problems with the lenses being contaminated. Switching SRU2 to tailgas eliminated the contamination of the lenses.

Total duration

132 hours

Comment: Form D - Downtime Summary

EXCESS EMISSION SUMMARY REPORT Incinerator SO2 (lb/hr) CEMS 1-hr average = 18.6 lb/hr

FORM B

Emission Data Summary (lb/hr)	CMS Performance Report				
I. Duration of Excess Emission in Reporting Pe	riod Due to:	I. CMS Downtime in Reporting Period Due to:				
A. Startup/Shutdown	0.0	A. Monitor Equipment Malfunction	130.0			
B. Control Equipment Problems	0.0	B. Non-Monitor Equipment Malfunctions	0.0			
C. Process Problem	1.0	C. Quality Assurance Calibration	0.0			
D. Other Known Causes	0.0	D. Other Known Causes	2.0			
E. Unknown Causes	0.0	E. Unknown Causes	0.0			
II. Total Duration of Excess Emission	1.0	II. Total CMS Downtime	132.0			
III. Total Duration of Excess Emissions x 100 divided by Total Source Operating Time minus Total CMS Downtime	0.0%	III. Total CMS Downtime x 100 divided by Total Source Operating Time	6.0%			

- 1. Only report excess emissions which occur when the unit/process is operating. Include all excess emissions in the Emission Data Summary including those excess emissions associated with startup/shutdown and those excess emissions associated with Chapter 1 Section 5 (Emergency/Abnormal) operations. Report times in hours for gaseous monitors and in tenths of an hour for opacity monitors. Include detailed excess emission information and causes in the Excess Emission Table (Form C).
- 2. Only report CEM downtime which occurs while the unit/process is operating. Report time in hours to one decimal point. Include detailed CEM downtime and causes in the Monitor Outage Table (Form D).
- 3. Include an explanation of what corrective actions were taken for total excess emissions or monitor downtime for the quarter (Emission Data Summary and CMS Performance Summary, Item III) greater than 5%. (See Instructions for further details.)

TGTU Incinerator Excess Emissions Summary

Frontier Refining LLC SO2 lbs 1-Hr Excess Emissions for 4/1/2014 thru 6/30/2014

Reason	Duration
Process Upset - SWS Temperature and Pressure Issues	1 hour
Total duration of SO2 lbs 1-Hr excess emissions	1 hour
Total operating time	2184 hours
Operating time with excess emissions	0.0%

Comment: Form C - Excess Emission Summary

TGTU Incinerator Excess Emissions

Frontier Refining LLC SO2 ibs 1-Hr Excess Emissions for 4/1/2014 thru 6/30/2014

Parameter	Start	End	Duration	Value	Min	Max	Limit	Reason	Action
SO2 lbs 1-Hr	5/7/2014 11:00 PM	11:59 PM	1 hour	19.10	19.10	19.10	18.6	Process Upset - SWS Temperature and Pressure Issues	Made Louver Adjustments
	otal duration	-	1 hour						

Comment: Form C - Excess Emission Summary

TGTU Incinerator CEMS Downtime Summary Frontier Refining LLC SO2 lbs CEMS Downtime for 4/1/2014 thru 6/30/2014

Reason	Duration
Analyzer Out of Control - During startup of SRU2 they were running the start gasses thru the incinerator. This was leaving a light coating on the lenses which caused the analyzer to drift towards a negitive number.	16 hours
Falled Morning 02% & S02 ppm Span Calibration Checks - OOC	2 hours
Failed Moming SO2 ppm Zero & Span Calibration Check	9 hours
Falled Morning SO2 Span Calibration Check	2 hours
Failed Morning SO2 Zero Calibration Check	2 hours
Maintenance	2 hours
Sample Filters Plugged after Unit Excursion	3 hours
Sample Interface Malfunction	53 hours
Sample Interface Malfunction - Zinc Cell Heater	17 hours
Sample Interface Malunction - Zinc Cell Heater	1 hour
Sample System Malfunction	22 hours
SO2 Analyzer Out-of-Range - Result of Prior Upsets caused by Boilers #1 & #2 Shutdown	3 hours
Total duration of SO2 lbs CEMS downtime	132 hours
Total operating time	2184 hours
Operating time with CEMS downtime	6.0%

Comment: Form D - Downtime Summary

TGTU Incinerator CEMS Downtime

Frontier Refining LLC SO2 lbs CEMS Downtime for 4/1/2014 thru 6/30/2014

Parameter	Start	End	Duration	Reason	Action
502 lbs	4/1/2014 2:00 AM	4:59 AM	3 hours	Sample System Maifunction	Passed Morning Calibration Check
SO2 ibs	4/1/2014 9:00 AM	9:59 AM	1 hour	Maintenance	Replaced RTD going to SO2 incinerator.
SO2 lbs	4/2/2014 5:00 AM	8:59 AM	4 hours	Sample System Malfunction	Self Corrected
602 lbs	4/10/2014 9:00 AM	9:59 AM	1 hour	Maintenance	Took unit out of service to zero and clean probe. Probe was partially plugged.
SO2 lbs	4/11/2014 5:00 PM	7:59 PM	3 hours	Sample interface Maifunction	Self Corrected
\$02 lbs	4/12/2014 7:00 AM	11:59 AM	5 hours	Sample Interface Malfunction	Self Corrected
SO2 lbs	4/13/2014 7:00 AM	11:59 PM	17 hours	Sample Interface Malfunction	Passed Manual Calibration
SO2 lbs	4/14/2014 12:00 AM	1:59 PM	14 hours	Sample Interface Malfunction	Passed Manual Calibration
SO2 lbs	4/14/2014 10:00 PM	11:59 PM	2 hours	Sample Interface Malfunction	Self Corrected
602 lbs	4/15/2014 12:00 AM	1:59 AM	2 hours	Sample Interface Maifunction	Self Corrected
SO2 lbs	4/17/2014 5:00 AM	6:59 AM	2 hours	Failed Morning SO2 Zero Calibration Check	Adjusted zero on incinerator SO2 analyzer. Ran validation.
SO2 ibs	4/20/2014 10:00 AM	2:59 PM	5 hours	Sample Interface Maifunction - Zinc Cell Heater	Zinc Cell heater was reading low and causing readings to be invalid. Adjusted heater and started working again on 27-Apr-14.
SO2 lbs	4/20/2014 4:00 PM	6:59 PM	3 hours	Sample Interface Malfunction - Zinc Cell Heater	Zinc Cell heater was reading low and causing readings to be invalid. Adjusted heater and started working again on 27-Apr-14.
\$02 lbs	4/22/2014 5:00 PM	6:59 PM	2 hours	Sample Interface Malfunction - Zinc Cell Heater	Zinc Cell heater was reading low and causing readings to be invalid. Adjusted heater
SO2 ibs	4/26/2014 8:00 AM	2:59 PM	7 hours	Sample Interface Malfunction - Zinc Cell Heater	Zinc Cell heater was reading low and causing readings to be invalid. Adjusted heater
SO2 lbs	4/27/2014 11:00 AM	11:59 AM	1 hour	Sample Interface Malunction - Zinc Cell Heater	Zinc Cell heater was reading low and causing readings to be invalid. Adjusted heater.

Parameter	Start	End	Duration	Reason	Action
SO2 ths	4/29/2014 12:00 AM	9:59 AM	10 hours	Sample Interface Malfunction	Changed out sample filter and cleared the alarm on the analyzer.
SO2 lbs	4/29/2014 6:00 PM	11:59 PM	6 hours	Sample System Malfunction	Took SO2 out of service to perform testing of the flow system. Waiting on part to fix flow.
SO2 lbs	4/30/2014 12:00 AM	8:59 AM	9 hours	Sample System Malfunction	Took SO2 out of service to perform testing of the flow system. Waiting on part to fix flow.
SO2 lbs	5/7/2014 7:00 AM	8:59 AM	2 hours	Failed Morning SO2 Span Calibration Check	Ran zero and span calibration and manually adjusted settings. Performed maintenance on unit as well changing out filter.
SO2 lbs	5/29/2014 4:00 PM	6:59 PM	3 hours	Sample Filters Plugged after Unit Excursion	Changed Filters
SO2 lbs	6/14/2014 12:00 AM	1:59 AM	2 hours	SO2 Analyzer Out-of-Range - Result of Prior Upsets caused by Boilers #1 & #2 Shutdown	Pulled and cleaned filters and tubing.
SO2 ibs	6/14/2014 4:00 AM	4:59 AM	1 hour	SO2 Analyzar Out-of-Range - Result of Prior Upsets caused by Bollers #1 & #2 Shutdown	Pulled and cleaned filters and tubing.
SO2 ibs	6/14/2014 5:00 AM	1:59 PM	9 hours	Failed Morning SO2 ppm Zero & Span Calibration Check	Changed sample probe filter. Ran Manual Calibration
SO2 ibs	6/15/2014 5:00 AM	6:59 AM	2 hours	Failed Morning 02% & SO2 ppm Span Calibration Checks - OOC	Changed sample probe filter. Ran validation on both analyzers.
SO2 ibs	6/30/2014 8:00 AM	11:59 PM	16 hours	Analyzer Out of Control - During startup of SRU2 they were running the start gasses thru the incinerator. This was leaving a light coating on the lenses which caused the analyzer to drift towards a neglitive number.	Cleaned the lenses multiple times and purged the lines but still had problems with the lenses being contaminated. Switching SRU2 to tailgas eliminated the contamination of the lenses.

Total duration

132 hours

Comment: Form D - Downtime Summary

Data Sheet for TGTU Incinerator CEM System Cylinder Gas Audit

1. Date Audit Commenced: 6-6-2014 Time Audit Commenced: 1100

2. Audit Gases Used for CGA (All gases to be Protocol 1 Certified):

Acceptable Audit Gas Ranges	Cylinder Number and Expiration Date	Audit Gas Concentratio	+/- of Audit Gas Range		
SO ₂ Low:	EB0038571	127.20		39.75%	
84 - 99 ppm 	3-Mar-22	127,20	ppm	35./376	
SO ₂ Mid:	CC274015	270.50		84.53%	
4 60 ~ 492 ppm 2 50 ~ 300	28-Apr-22	270.50 ppm		04.5376	
O ₂ Low:	EB0042977	4.99	%	19.96%	
4 - 6% by volume	23-Mar-22	4.99 76		18.50%	
O ₂ Mid:	CC189312	10.01	%	40.04%	
8 - 12% by volume	23-Mar-22	10.01	70	40.0476	

3. CEM System Response:

	Low-Sp	oan NO _x	Mid-Span NO _x		Low-Span O₂		Mid-Span O ₂	
	Analyzer	CeDAR	Analyzer	CeDAR	Analyzer	CeDAR	Analyzer	CeDAR
Run 1	122.00		268.00		5.64		9.88	
Run 2	121.00		270.00		5.68		10.00	
Run 3	120.00		266.00		5.83		9.99	
Avg. (d _m)	121.00	#DIV/0!	268.00	#DIV/0!	5.72	#DIV/0!	9.96	#D!V/0!
Α	4.87%	#DIV/01	0.92%	#DIV/0!	14.56%	#DIV/0!	0.53%	#DIV/01
Pass?	Yes	#DIV/0!	Yes	#DIV/01	Yes	#DIV/01	Yes	#D(V/0)

4. Signature of Technician(s) performing CGA:	Und land
	Matt Hobbs, Kevih Marschner and/or Tad Milliken
Calculation of A:	

1 21

 $A = (d_m - c_a) / c_a \times 100$

A must be +/-15% to pass.

where:

A = accuracy of CEM

d_m = average of reponses

c_a = certified audit value of gas



Calibration Gases & Equipment

EPA Protocol Standard Gas Mixture

To:

Norco, Inc

Cheyenne Warehouse 100 S. Greeley HWY Cheyenne, WY 82007 Report of Analysis and Certification

Manufactured at/by: EPA Protocol Vendor ID P12013

NorLab Order #

34020710

Date Certified:

03/04/14

Customer PO#

N/A

Cylinder Pressure:

2000

psig /at 70 F

Part Number

SPG 5E1079125PN 4-049-521

Lot Number: Cylinder Number

EB0038571

Expiration Date:

03/03/22

Component(s)	Cons. V/V	± EPA Analyz Uncertainty (802)		Cone V/V			MTO 6	Oa FTIR	
Sulfur Dioxide, ppm	127.2	1.2	Calibrated:	Assay 1; 2; 3	2/12/2014	2/12/2014			
Nitrogen, O2 Free									
		Refere	ence Standard	i Data					
Component	Lot# and XP	Date (MM/YF	(I) ID	Cy#	Sam#	Conc.	U		
Sulfur Dicodde, ppr	n 6-035-17	75 XP 3X18	GMIS1681A	CC 32121	N/A	101.9	0.82		
Traceable Std If GIV	IS 9-126-60	20 XP 1X17	SRM 1881A	FF28137	94-H-18	490.9	3.		
		Repli	cate Analysis	Data					
Assay			Assay 2			Assay 3			
SO2		SO2							
2/25/2014		3/4/2014							
127.2									
127.4		L.,							
127.1		· · · · · · · · · · · · · · · · · · ·							
1273		1- 5							
0.0		0.0	<u> </u>						
0.0		0.0	 			 _			
127 2		127 2	+	 		 			

The analysis listed in this report was performed in accordance with the Procedure G1 of the EPA Traceability Protocal, EPA 600/R-12/531 May 2012.

The contents of this c	ylinder must not be used .	if the pressure is	less than 100 psig

Analyst:

Approved: 🚅

Aaron Schwenken, Lab Technician

Jeff Korn, Quality/Assurance Linit

Page 1 of 1

4-049-521 CHEYENNE 34020710 EB0038571



Calibration Gases & Equipment

EPA Protocol Standard Gas Mixture

To:

Norco, Inc

Cheyenne Warehouse 100 S. Greeley HWY Cheyenne, WY 82007 Report of Analysis and Certification Manufactured at/by:

EPA Protocol Vendor ID P12013

NorLab Order #

34376087

Date Certified:

04/29/14

Customer PO#

N/A

Cylinder Pressure:

2000

psig @ 70 F

Part Number

SPG 5E1079270PN 4-105-522

Lot Number: Cylinder Number

CC 274015

Expiration Date:

04/28/22

Compone	nt(s)	Conc. V/V	± EPA Uncertainty	Analyzer1 (802)		MTO 6	Oa FTIR	
Sulfur Dioxide, p	om	270.5	1.8	Calibrated:	Assay 1; 2; 3	4/17/2014	4/17/2014	
Nitrogen, O2 Free	· · · · · · · · · · · · · · · · · · ·							
			Refere	nce Standard	i Data			
Compon	ent	Lot# and XP	Date (MM/YR	I ID	Cyl#	Sam#	Conc.	U
Sulfur Dioxic	le, ppm		O XP 8x15	GMIS 1661a	CC 45427	0	252.5	1.3
Traceable Sto	I If GMIS	9-126-60	00 XP 1x17	SRM 1661a	FF28137	94-H-18	490.9	3.
			Replic	cate Analysis	Data			
	Assay i			Assay 2			Assay 3	
SO2			SO2					
4/22/2014			4/29/2014					
270.6			270.5					
271.1			270.5					
270.2			271.1					
269.7			270.4					
								
270.4			270.8					

The analysis listed in this report was performed in accordance with the Procedure GI of the FPA Traceability Protocol, EPA 600/R-12/531 May 2012.

The contents of this cylinder must not be used if the pressure is less than 100 psig.

Aaron Schwenken, Lab Technician

Charles Eckman, Quality Assurance Unit

Page 1 of 1

4-105-522 cheyenne 34376087



Calibration Gases & Equipment EPA Protocol Standard Gas Mixture

Report of Analysis and Certification Manufactured at/by: EPA Protocol Vendor ID P12013

To:

Norco Inc.

Chevenne Whse.

100 S. Greeley Hwy.

Cheyenne, WY. 341

NorLab Order #

34175499

Date Certified:

03/24/14

Customer PO#

D4

Cylinder Pressure:

2000

psig @ 70 F

Part Number

SPG 5E10725VN

Lot Number:

4-072-524

Cylinder Number

EB0042977

Expiration Date:

03/23/22

Component(s)	Conc. V/V	± EPA Uncertainty	Analyzer1 (O2)	Servomex Paramagnetic Analyzer MTO 97A
Oxygen, %	4.999	0.029	Calibrated:	Assity 1; 2; 3 3/24/2014
Nitrogen, O2 Free	Balance			

Reference Standard Data								
Component	## and XP Date (MM/		Cy##	Sam#	Conc.	U		
Oxygen, %	3-079-161 XP 6X18	GMIS 2658A	CC 53742		9.913	0.043		
Traceable Std if GMIS	0-130-600 6x17	SRM 2658a	CAL 016948	72-D-46	9.918	0.022		

Replicate Analysis Data								
Assay I		Assay 2		Assay 3				
Oxygen, %	Oxygen, %		Oxygen, %					
3/24/2014								
4.98								
5.00								
5.01								
5.00								
0.00								
0.00								
5.00								

The analysis listed in this report was performed in accordance with the Procedure G1 of the EPA Traceability Protocol, EPA 600/R-12/531 May 2012.

The contents of this cylinder, must not be used if the pressure is less than 100 psig.

Analyst:

Approved: ___

Charles Eckman, Quality Assurance Unit

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Calibration Gases & Equipment EPA Protocol Standard Gas Mixture

Report of Analysis and Certification Manufactured at/by: EPA Protocol Vendor ID P12013

To: Norco Inc. Cheyenne Whse. 100 S. Greeley Hwy. Cheyenne, WY. 341'

NorLab Order #

34175499

Date Certified:

03/24/14

Customer PO#

na

Cylinder Pressure:

2000

psig @ 70 F

Part Number

SPG 5E107210VN

Lot Number:

4-072-523

Cylinder Number

CC 189312

Expiration Date:

03/23/22

Component(s)	Conc. V/V	± EPA Uncertainty	Analyzer1 (O2)	Servom	ex Paramagn	tic Analyzer N	TTO 97A
Oxygen, %	10.01	0,047	Calibrated:	Assay 1; 2; 3	3/24/2014		
Nitrogen, O2 Free	Balance						

Reference Standard Data								
Component	it# and XP Date (MM/Y)		Cy##	Sam#	Conc.	U		
Oxygen, %	3-079-161 XP 6X18	GMIS 2658A	CC 53742		9.913	0.043		
Traceable Std if GMIS	0-130-600 6x17	SRM 2658a	CAL 018948	72-D-46	9.918	0.022		

Replicate Analysis Data									
Assay	Assay 2	Assay 3							
Oxygen, % 3/24/2014	Oxygen, %	Oxygen, %							
3/24/2014									
10.00									
10.02									
10.01									
10.01									
0.00									
0.00									
10.01									

The analysis listed in this report was performed in accordance with the Procedure G1 of the EPA Traceability Protocol, EPA 600/R-12/531 May 2012.

The contents of this cylinder past not be used if the pressure is less than 100 psig.

Approved:

Analyst: 6

Jeff Koro Lab Technician

Charles Eckman, Quality Assurance Unit

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Attachment G - SRP

Paragraph 217d - SRP Emission Data

	Actual Emissions tons/yr	Method of Determination
SO2	17.0	CEMS

Section H – Additional Miscellaneous Requirements

Additional Miscellaneous Requirements

Frontier Refining LLC
P.O. Box 1588 • Cheyenne, WY 82003-1588

Paragraph	Attachment H - Miscellaneous	Comments
11	FRI and FEDRC shall implement programs to reduce NOx emissions from the FCCUs at their respective Covered Refineries, as specified in this Section VI.A. FRI and FEDRC shall incorporate lower NOx emission limits established for their respective Covered Refineries under this Consent Decree into federally enforceable permits and shall each demonstrate future compliance with the lower emission limits through the use of CEMS.	Frontier has submitted a permit application to incorporate Consent Decree conditions.
12	FRI FCCU NOx Emission Limits. By no later than one hundred and eighty (180) days from the Date of Entry of this Consent Decree, FRI shall notify EPA and the Applicable Intervenor as to which one of the following two options that it shall comply with: a. Paragraph 13 of this Consent Decree; or b. Paragraph 14 of this Consent Decree.	Frontier chose to comply with Paragraph 14.
14	If FRI elects to comply with Paragraph 12.b above, then FRI shall:	
14a	By no later than one hundred and eighty (180) days from the Date of Entry, comply with interim FCCU NOx concentration emission limits of 60 ppmvd on a 365-day rolling average basis, and 120 ppmvd on a 7-day rolling average basis, both at 0% oxygen; and	Periods of non-compliance with these requirements are found in Attachment B CEMs Data.
14b	By no later than December 31, 2015, comply with FCCU NOx concentration emission limits of 40 ppmvd on a 365-day rolling average basis, and 80 ppmvd on a 7-day rolling average basis, both at 0% oxygen.	Frontier anticipates meeting this requirement at the required time.
17	At FRI and/or FEDRC, NOx emissions during periods of Startup, Shutdown, or Malfunction of an FCCU controlled by catalyst additives, or NOx emissions during periods of Malfunction of an FCCU, or during periods of Malfunction of a NOx Control Technology used to meet NOx emissions limits required by this Consent Decree, shall not be used in determining compliance with the seven (7)-day rolling average NOx emission limits established pursuant to Paragraphs 11 - 16, provided that during such periods FRI or FEDRC, as appropriate, implements good air pollution control practices to minimize NOx emissions.	Frontier manages the CEMs data appropriately.
18	Demonstrating Compliance With FCCU Emissions Limits. For each FCCU at FRI and FEDRC, beginning no later than the Date of Entry, FRI and FEDRC shall each use NOx, SO2, CO and O2 CEMS to monitor the performance of their respective FCCUs and to report upon compliance with the terms and conditions of this Consent Decree. CEMS shall be used to demonstrate compliance with the respective NOx emission limits established pursuant to Paragraphs 11 - 16 of this Decree, the SO2 emission limits established pursuant to Paragraphs 19 - 25 of this Decree, and CO emission limits established pursuant to Paragraphs 32 - 35 of this Decree. FRI and FEDRC shall, upon request, each make all CEMS data available to EPA and the Applicable Intervenor.	CEMs have been installed to monitor Nox, SO2, CO and O2.
18 a	FRI and FEDRC each shall install, certify, calibrate, maintain, and operate all CEMS required by Paragraph 18 in accordance with the provisions of 40 C.F.R. § 60.13 that are applicable to CEMS (excluding those provisions applicable only to Continuous Opacity Monitoring Systems), 40 C.F.R. Part 60 Appendices A and F, and the applicable performance specification tests of 40 C.F.R. Part 60 Appendix B.	Frontier recently voluntarily disclosed audit findings indicating the QA/QC manuals for the FCCU and SRU CEMs were out-of-date. These manuals have since been updated and submitted to WDEQ.

Paragraph	Attachment H - Miscellaneous	Comments
18b	Unless 40 C.F.R. Part 60 Appendix F requirements are specifically mandated by Subpart J or the applicable Intervenor, in lieu of the requirements of 40 C.F.R. Part 60, Appendix F §§ 5.1.1, 5.1.3 and 5.1.4, FRI or FEDRC may opt to conduct either a Relative Accuracy Audit ("RAA") or a Relative Accuracy Test Audit ("RATA") on each CEMS at least once every three (3) years. If FRI or FEDRC elect such an option, they must conduct a Cylinder Gas Audit ("CGA") each calendar quarter during which an RAA or RATA is not performed.	RATA tests are conducted annually on the CEMs.
В.	SO2 Emissions Reductions From FCCUs	
19	FRI and FEDRC shall implement those programs identified under this Section VI.B. of this Consent Decree to reduce SO2 emissions from the FRI and FEDRC FCCUs. FRI and FEDRC each shall incorporate lower SO2 emission limits into federally enforceable permits and each shall demonstrate future compliance with the lower emission limits through the use of CEMS.	Frontier has submitted a permit application to incorporate Consent Decree conditions.
	FRI FCCU SO2 Emission Limits. By no later than one hundred and eighty (180)days from the Date of Entry, FRI shall notify EPA and the Applicable Intervenor of which one of the following two options that FRI shall comply with: a. Paragraph 21 of this Consent Decree; or b. Paragraph 22 of this Consent Decree.	Frontier chose to comply with Paragraph 22.
22	If FRI elects to comply with Paragraph 20.b above, then FRI shall:	
22a	By no later than one hundred and eighty (180) days from the Date of Entry, and continuing until FRI begins to comply with Paragraph 22.b., infra, FRI shall add an EPA approved SO2 reducing additive at a rate of 396 pounds per day (based on 10% of total catalyst added to the FCCU for a period from August 2006 to September 2008); and	Catalyst injection rates were less than 396 lbs on 7 days during the reporting period. Also, during the reporting period there was a loss of data capture from 2/4/2014 through 5/5/2014. the FCCU was shut down 11 days during this period and there were no catalyst injections during the outage.
22b	By no later than September 30, 2015, comply with FCCU SO2 concentration emission limit of 25 ppmvd on a 365-day rolling average basis and a FCCU SO2 concentration emission limit of 50 ppmvd on a 7-day rolling average basis, both at 0% oxygen.	Frontier anticipates meeting this requirement at the required time.
22a	If the SO2 Reducing Catalyst Additive addition rate required by this Paragraph 22.a. limits the processing rate or the conversion capability of the FRI FCCU in a manner that cannot be reasonably compensated for by adjustment of other parameters, FRI may, up until 12 months from the Date of Entry, submit a request to EPA to reduce the SO2 Reducing Catalyst Additive addition rate to a level at which the additive no longer causes such limits or effects. Such a request shall include all data that demonstrates the limit on processing rate or conversion capability with evidence that links these limits to the SO2 Reducing Catalyst Additive and that documents all efforts made to compensate by adjustment of other parameters. If EPA provides written approval, FRI may reduce the SO2 Reducing Catalyst Additive addition rate required by this Paragraph 22.a. to the level that EPA allows in its approval.	Frontier did not elect to adjust the catalyst injection rate under this Paragraph.

Paragraph	Attachment H - Miscellaneous	Comments
24	Startup, Shutdown, or Malfunction. At FRI and/or FEDRC, SO2 emissions during periods of Startup, Shutdown, or Malfunction of an FCCU or during periods of a Malfunction of an FCCU catalyst additive system or other SO2 emission control device shall not be used by FRI or FEDRC in determining compliance with the 7-day rolling average SO2 emission limits established pursuant to Paragraphs 20 - 25, provided that during such periods FRI and FEDRC, as applicable, implement good air pollution control practices to minimize SO2 emissions.	Frontier manages the ŒMs data appropriately.
C.	Particulate Matter Emissions Reductions From FCCUs	
26	FRI and FEDRC shall maintain particulate matter ("PM") emissions from their FCCUs in accordance with the requirements of this Section VI.C. of this Consent Decree and shall incorporate those requirements into federally enforceable permits.	Frontier has submitted a permit application to incorporate Consent Decree conditions.
28	By the second turnaround of the FRI FCCU or December 31, 2015, whichever occurs first, FRI shall accept and comply with an emission limit of 1.0 pounds of PM per 1,000 pounds of coke burned on a 3-hour average basis. By the second turnaround of the FRI FCCU or December 31, 2015, whichever occurs first, upon prior written notice to EPA pursuant to Section XIX (General Provisions) Paragraph 356 (Notice), FRI may choose to accept and comply with an emission limit of 0.50 pounds of PM per 1,000 pounds of coke burned, in which case FRI shall receive the release from liability provided in Paragraph 331.	Frontier anticipates meeting this requirement at the required time.
29	PM Testing. To measure PM emissions from their FCCUs, FRI and FEDRC shall each follow the test protocol specified in 40 C.F.R. § 60.106(b)(2) and use EPA Reference Method 5B or 5F to measure PM emissions identified in Paragraphs 26 - 28 from each of their FCCUs. FEDRC shall conduct its first stack test by June 30, 2010 and submit a stack test protocol to the Applicable Intervenor for approval no later than sixty (60) days prior to the stack test. FRI shall conduct its first stack test one hundred and eighty (180) days from the second FCCU turnaround after entry of this Consent Decree but no later than June 30, 2016. FRI shall submit a stack test protocol to the Applicable Intervenor for approval no later than sixty (60) days prior to the stack test. FRI and FEDRC shall thereafter conduct annual stack tests for their FCCUs and include stack test results in the semi-annual reports required under Paragraph 216, Section XI. (Reporting and Record Keeping) of this Consent Decree for the period in which such stack test(s) occurred. Not less than forty-five (45) days before the conduct of any stack test, FRI or FEDRC, shall give notice to EPA and the Applicable Intervenor pursuant to Section XIX.(General Provisions), Paragraph 356 (Notice) of the time and date upon which the test shall be conducted. Within sixty (60) days of completion of any stack test, test reports shall be sent to EPA and the Applicable Intervenor. Upon demonstrating through at least three (3) annual tests that a particular FCCU's PM limits are not being exceeded, FRI or FEDRC, as appropriate, may request EPA approval to conduct these stack tests less frequently than annually at such FCCU.	This requirement does not apply until after the Dec. 31, 2015 compliance deadline for the FCCU PM emission reductions.
30	Neither FRI nor FEDRC shall use PM emissions during periods of Startup, Shutdown, or Malfunction of an FCCU or Malfunction of a PM control device to determine compliance with the emission limits established in Paragraphs 27 and 28 provided that during such periods FRI or FEDRC, as applicable, implement good air pollution control practices to minimize PM emissions.	This requirement does not apply until after the Dec. 31, 2015 compliance deadline for the FCCU PM emission reductions.

Paragraph	Attachment H - Miscellaneous	Comments
31	Opacity Monitoring At FCCUs. FRI, by June 30, 2015, and FEDRC, by December 31, 2009, shall each install and operate a Continuous Opacity Monitoring System ("COMS") to monitor opacity at each of the Covered Refineries' FCCUs. If Wet Gas Scrubber(s) are installed at either Covered Refinery, FRI and FEDRC, as applicable, shall operate the Wet Gas Scrubber(s) pursuant to an EPA-approved Alternative Monitoring Plan for opacity. FRI and FEDRC, as appropriate, shall install, certify, calibrate, maintain, and operate all COMS required by this Consent Decree in accordance with 40 C.F.R. §§ 60.11, 60.13 and Part 60 Appendix A, and the applicable performance specification test of 40 C.F.R. Part 60 Appendix B.	This requirement does not apply unt June 30, 2015. A PM CEM is current in place on the FCCU stack, and an AMP is in place addressing the PM CEM use in place of the COM.
D	CO Emissions Reductions From FCCUs	
32	ishall reduce emissions further at each ECU in accordance with the requirements of this Section VLD of this	Frontier has submitted a permit application to incorporate Consent Decree conditions.
	emission limit of 500 ppmvd CO corrected to 0% O2 on a 1-hour block average basis and 100 ppmvd CO	Periods of non-compliance with thes requirements are found in Attachment B CEMs Data.
35	CO emissions during periods of Startup, Shutdown, or Malfunction of an FCCU or Malfunction of a CO control	Frontier manages the CEMs data
	NSPS Applicability to FCCU Regenerators.	
36	FRI FCCU Catalyst Regenerators. By no later than the dates specified below for each pollutant, the FRI FCCU Catalyst Regenerator shall be an "affected facility," as defined in 40 C.F.R.§ 60.2, under NSPS Subpart J, and shall comply with the applicable requirements of NSPS Subparts A and J for each of the following pollutants by the specified dates: SO2 September 30, 2015; PM September 30, 2015; and CO Date of Entry.	Frontier has submitted a permit application to incorporate Consent Decree conditions.
38	For FCCU Catalyst Regenerators that become "affected facilities," as defined in 40 C.F.R. § 60.2, under NSPS Subpart J pursuant to this Section VI.E., entry of this Consent Decree and compliance with the relevant monitoring requirements of this Consent Decree at the Covered Refineries' FCCUs shall satisfy the notice requirements of 40 C.F.R. § 60.7(a) and the initial performance test requirement of 40 C.F.R. § 60.8(a). a. If prior to the termination of this Consent Decree, the FCCU becomes subject to NSPS Subpart Ja for a particular pollutant due to a "modification" (as that term is defined in the final Subpart Ja rule), the modified affected facility shall be subject to and comply with NSPS Subpart Ja in lieu of NSPS, Subpart J for that regulated pollutant to which a standard applies as a result of the modification. b. If prior to the termination of this Consent Decree, the FCCU becomes subject to NSPS Subpart Ja due to a "reconstruction" (as that term is defined in the final Subpart Ja rule), the reconstructed facility shall be subject to and comply with NSPS Subpart Ja for all pollutants in lieu of Subpart J.	The FCCU has not triggered NSPS Ja.
F	NOx Emission Reductions From Heaters and Boilers	

Paragraph	Attachment H - Miscellaneous	Comments
40	FRI and FEDRC shall each implement programs to reduce NOx emissions from refinery heaters and boilers at their respective Covered Refineries to meet the requirements of Paragraphs 42, 45 and 46 through the installation of NOx controls and the acceptance of federally enforceable permit emission limits on the units controlled, or the shut down of certain units. Further, at their respective Covered Refineries, FRI and FEDRC shall monitor compliance with the emission limits through stack testing, use of CEMS, or PEMS.	Per the Nox Control Plan, the CO Boiler was permanently shut down on Dec. 22, 2013. Frontier has met this requirement.
41	Installation of NOx Control Technology. For each Covered Refinery, FRI and FEDRC shall select one or any combination of the following "Qualifying Controls" to satisfy the requirements of Paragraphs 42, 45 and 46: a. SCR or SNCR; b. Current Generation or Next Generation Ultra-Low NOx Burners; c. Other technologies or combination of technologies which FRI or FEDRC, as appropriate, demonstrates to EPA's satisfaction shall reduce NOx emissions to 0.040 lbs. per mmBTU or lower; or d. Permanent shutdown of a heater or boiler with revocation of its federally enforceable operating permit.	Per the Nox Control Plan, the CO Boiler will be permanently shut down and the permit revoked by Dec. 31, 2013. Frontier has met this requirement.
42	On or before December 31, 2013, for each Covered Refinery, FRI and FEDRC shall use Qualifying Controls to reduce the aggregate NOx emissions (i.e. combined NOx emissions of both Covered Refineries) from the Heaters and Boilers listed in Appendix A by at least 649 tons per year, so as to satisfy the following inequality: n 3 [(E actual)i - (E allowable)i] \$ 649 tons of NOx per year i = 1 Where: (E allowable)i = [(The permitted allowable pounds of NOx per million BTU for heater or boiler i, or, the requested portion of the permitted reduction pursuant to Paragraph 213(a) /(2000 pounds per ton)] x [(the lower of permitted or maximum heat input rate 33 capacity in million BTU per hour for heater or boiler i) x (the lower of 8760 or permitted hours per year)]; (E actual)i = The tons of NOx per year prior actual emissions during calendar years 2003 and 2004 (unless prior actual emissions exceed allowable emissions, then use allowable) as shown in Appendix A for heater or boiler i and n = The number of heaters and boilers with Qualifying Controls from those listed in Appendix A that are selected by FRI or FEDRC, as appropriate, to satisfy the requirements of the equation set forth in this Paragraph 42 of this Consent Decree. Federally enforceable permit limits established to implement this Paragraph 42 may use a 365 - day rolling average for heaters and boilers that use a CEMS or PEMS to monitor compliance.	Per the Nox Control Plan, the CO Boiler will be permanently shut down and the permit revoked by Dec. 31, 2013. Frontier has met this requirement.
45	By December 31, 2009, FRI and FEDRC each shall install at their respective Covered Refineries Qualifying Controls and have by December 31, 2009 also applied for emission limits from the appropriate permitting authority sufficient to achieve, in the aggregate, two-thirds of the NOx emissions reductions required by Paragraph 42. No later than March 31, 2010, FRI and FEDRC shall each provide to EPA and the Applicable Intervenor a report showing how they have satisfied the requirement of this Paragraph 45 at their respective Covered Refineries.	The Nox Control Plan identifies dates of Nox emission reductions and identifies how the aggregate two-thirds reduction was accomplished by Dec. 31, 2009.
46	By no later than December 31, 2013, heaters and boilers with Qualifying Controls shall represent at least 30% of the total maximum heat input capacity or, if less, the allowable heat input capacity, as shown in Appendix A, of all heaters and boilers greater than 40 mmBTU/hr at each Covered Refinery. Any Qualifying Controls can be used to satisfy this requirement, regardless of when the Qualifying Controls were installed.	The Nox Control Plan identifies dates of Nox emission reductions and identifies how the 30% reqiurement was accomplished by Dec. 31, 2013.

Paragraph	Attachment H - Miscellaneous	Comments
47	Beginning no later than one hundred and eighty (180) days after installing Qualifying Controls on and commencing operation of a heater or boiler that shall be used to satisfy the requirements of Paragraphs 42, 45, and 46, at each Covered Refinery FRI and FEDRC shall monitor the heaters or boilers as follows:	See below
47a	For heaters and boilers with a capacity greater than 150 mmBTU/hr (HHV), install or continue to operate a NOx CEMS;	No applicable sources.
47b	For heaters and boilers with a capacity greater than 100 mmBTU/hr (HHV) but less than or equal to 150 mmBTU/hr (HHV), install or continue to operate a NOx CEMS, or monitor NOx emissions with a predictive emissions monitoring system ("PEMS") developed and operated pursuant to the requirements of Appendix B (Predictive Emissions Monitoring Systems for Heaters and Boilers with Capacities Between 100 and 150 Mmbtu/hr) of this Consent Decree:	No applicable sources.
47 c	For heaters and boilers with a capacity of less than or equal to 100 mmBTU/hr (HHV), conduct an initial performance test and any periodic tests that may be required by EPA or by the applicable State or local permitting authority under other applicable regulatory authority. FRI and FEDRC shall report the results of the initial performance testing at their respective Covered Refinery to EPA and the Applicable Intervenor;	No applicable sources.
47d	FRI and FEDRC shall use Method 7E in conjunction with Method 19 or an EPA-approved alternative test method to conduct initial performance testing for NOx emissions required by Subparagraph 47.c. Monitoring with a PEMS that is required by this Paragraph shall be conducted in accordance with the requirements of Appendix B. Units with Qualifying Controls installed before the Date of Entry that are subject to this Paragraph shall comply with this Paragraph by Date of Entry; and	No applicable sources.
47e	Any heater or boiler included in Appendix A that (i) already had Qualifying Controls installed prior to January 1, 2003, and (ii) is used solely to meet the heat input capacity requirement in Paragraph 46, shall install CEMS by December 31, 2013.	The Crude Charge Heater is covered by this requirement. Frontier has met this requirement by the required date.
48	Beginning no later than one hundred and eighty (180) days after installing Qualifying Controls and commencing operation of a heater or boiler that shall be monitored by use of a NOx CEMS that is required by Paragraph 47, at their respective Covered Refineries, FRI and FEDRC shall each install, certify, calibrate, maintain, and operate these CEMS in accordance with the provisions of 40 C.F.R. § 60.13 that are applicable to CEMs (excluding those provisions applicable only to Continuous Opacity Monitoring Systems) and Part 60 Appendices A and F, and the applicable performance specification test of 40 C.F.R. Part 60 Appendix B. Unless Appendix F requirements are specifically required by NSPS or state regulations, with respect to 40 C.F.R. Part 60, Appendix F, in lieu of the requirements of 40 C.F.R. Part 60, Appendix F §§ 5.1.1, 5.1.3 and 5.1.4, FRI and/or FEDRC, as appropriate, must conduct either a Relative Accuracy Audit ("RAA") or a Relative Accuracy Test Audit ("RATA") on each CEMS at least once every three (3) years. At their respective Covered Refinery, FRI and FEDRC each shall conduct a Cylinder Gas Audit ("CGA") each calendar quarter during which a RAA or a RATA is not performed.	Frontier currently has no sources subject to this and anticipates meeting this requirement at the required time.

Paragraph	Attachment H - Miscellaneous	Comments
50	For their respective Covered Refineries, FRI and FEDRC shall retain all records required to support their reporting requirements under this Section VI.F. this Consent Decree 3B until termination of this Consent Decree, Section XX. (Termination). Upon request, FRI and FEDRC shall submit said records to EPA or the Applicable Intervenor.	Records required to support this section are maintained as required.
G	SO2 Emissions Reductions from and, NSPS Applicability to, Heaters and Boilers and Other Specified Equipment.	
53	NSPS Applicability to Heaters and Boilers and Other Specified Equipment.	
53 a	Upon the Date of Entry, all heaters and boilers at each Covered Refinery shall be "affected facilities" as defined by 40 C.F.R. § 60.2 under NSPS Subpart J, and shall comply with the applicable requirements of NSPS Subparts A and J for fuel gas combustion devices, except for those heaters and boilers listed in Appendix C, which shall be "affected facilities" as defined by 40 C.F.R. § 60.2, and shall be subject to and comply with the applicable requirements of NSPS Subparts A and J for fuel gas combustion devices by the dates listed in Appendix C.	All heaters and boilers listed in Appendix C are affected facilities under NSPS Subparts A and J.
5 3 b	Upon the Date of Entry all equipment listed in Appendix D shall be "affected facilities" as defined by 40 C.F.R. § 60.2, under NSPS Subpart J, and shall comply with the applicable requirements of NSPS Subparts A and J for fuel gas combustion devices by the dates listed in Appendix D.	All heaters and boilers listed in Appendix D are affected facilities under NSPS Subparts A and J.
53c	Where Appendix C or D specifies an alternative monitoring plan ("AMP") submittal date (rather than a final NSPS Subpart J compliance date), FRI and FEDRC shall submit to EPA and the Applicable Intervenor a timely and complete AMP application. Such an AMP may be based on alternative monitoring for H2S or SO2. If an AMP is not approved, FRI and/or FEDRC, as appropriate, shall, within ninety (90) days of receiving notice of such disapproval submit to EPA for approval, and send a copy to the Applicable Intervenor, a plan and schedule that provide for compliance with the monitoring requirements of NSPS Subpart J in accordance with the schedules contained in Appendices C and D. The plan may include a revised AMP application, physical or operational changes to the equipment, or additional or different monitoring.	An AMP for an inherently-low sulfur stream at the Butamer unit was filed prior to the revisions to J/Ja exempting those streams. No action has been taken by EPA on this AMP at this time. A different AMP was filed and approved for flares in Appendix D.
53f	If prior to the termination of this Consent Decree, any heater, boiler or other specified equipment becomes subject to NSPS Subpart Ja for a particular pollutant due to a "modification" (as that term is defined in the final Subpart Ja rule), the modified affected facility shall be subject to and comply with NSPS Subpart Ja in lieu of NSPS Subpart J for that regulated pollutant to which a standard applies as a result of the modification.	No heaters or boilers identified in Appendix C have triggered NSPS Ja.
53g	If prior to the termination of this Consent Decree, any heater, boiler or other specified equipment becomes subject to NSPS Subpart Ja due to a "reconstruction" (as that term is defined in the final Subpart Ja rule), the reconstructed facility shall be subject to and comply with NSPS Subpart Ja for all pollutants in lieu of Subpart J.	No heaters or boilers identified in Appendix C have triggered NSPS Ja.



Paragraph	Attachment H - Miscellaneous	Comments
54	Elimination/Reduction of Fuel Oil Burning. Effective on the Date of Entry, neither FRI nor FEDRC shall burn Fuel Oil in any Combustion Unit at their respective Covered Refineries except that: a. Either FRI or FEDRC may burn Fuel Oil at their respective Covered Refineries during periods of Natural Gas Curtailment, test runs, and operator training; and b. Either FRI or FEDRC may burn Torch Oil in FCCU regenerators at their respective Covered Refineries to assist in starting, restarting, hot standby, or to maintain regenerator heat balance.	No fuel oils burning occurs other than those identified in 54a and 54b.
Н	Sulfur Recovery Plants	
56	Claus Sulfur Recovery Plant NSPS Applicability. Upon the Date of Entry of this Consent Decree, the FRI SRP and the FEDRC SRP shall continue to be "affected facilities," as defined by 40 C.F.R. § 60.2, under NSPS, 40 C.F.R. Part 60, Subparts A and J and shall, except as provided below in Paragraphs 57, 57.a. and 57.b., comply with all provisions applicable to such an "affected facility" as defined in 40 C.F.R. Part 60, Subparts A and J.	The SRP is an affected facility under NSPS Subparts A and J.
56a	Except as provided in Paragraph S8 of this Consent Decree, the FRI SRP shall fully comply with all provisions under NSPS, 40 C.F.R. Part 60, Subparts A and J, in effect on the Date of Entry, including periods of TGTU maintenance turnarounds; and	Excess emissions are included in Attachment G CEMs information.
56c	If prior to the termination of this Consent Decree, a SRP becomes subject to NSPS Subpart Ja for a particular pollutant due to a "modification" (as that term is defined in the final Subpart Ja rule), the modified affected facility shall be subject to and comply with NSPS Ja in lieu of NSPS Subpart J for that regulated pollutant to which a standard applies as a result of the modification.	The SRP has not triggered NSPS Ja.
56d	If prior to the termination of this Consent Decree, a SRP becomes subject to NSPS Subpart Ja due to a	The SRP has not triggered NSPS Ja.
57	Claus Sulfur Recovery Plant NSPS Compliance. Except as provided for the two scheduled tail gas unit maintenance turnarounds set forth in Paragraphs 58 and 59 below, the FRI and FEDRC SRPs shall comply with all applicable provisions of NSPS set forth at 40 C.F.R. Part 60, Subparts A and J, including, but not limited to, the following:	See below
57a		Excess emissions are included in Attachment G CEMs information.

Paragraph	Attachment H - Miscellaneous	Comments
57b	Monitoring. At their respective refineries, FRI and FEDRC shall monitor tail gas emissions points (stacks) for tail gas emissions and shall report excess emissions from each of these emissions points as required by 40 C.F.R. §§ 60.7(c), 60.13, and 60.105(a)(5), (6) or (7). FRI and FEDRC shall monitor emissions from their respective SRPs with CEMS at all of the emission points, unless an SO2 alternative monitoring procedure has been approved by EPA, per 40 C.F.R. § 60.13(i.), for any of the emission points. The requirement for continuous monitoring of the SRP emission points is not applicable to the Acid Gas Flaring Devices used to flare the Acid Gas or Sour Water Stripper Gas diverted from the SRPs.	Monitoring of the tail gas emissions is conducted per these requirements.
58	Interim SRP Requirements For The FRI TGTU Maintenance Turnarounds. FRI shall implement the following interim measures at the FRI SRP for any two maintenance turnarounds of the existing TGTU scheduled between June 30, 2008 and March 31, 2016:	Frontier has one of the maintenance turnarounds to date. Frontier anticipates complying with this when required.
58 a	FRI shall monitor the emissions from the FRI Claus Trains during the TGTU maintenance turnaround in accordance with 40 C.F.R. Part 60, Subpart A, § 60.13 or other EPA approved alternative monitoring plan.	Frontier has had one of the maintenance turnarounds to date. Frontier anticipates complying with this when required.
58b	By no later than one hundred and eighty (180) days after Date of Entry, FRI shall complete an optimization study, or submit a copy of a recent optimization study, to identify ways to minimize emissions and maximize sulfur recovery efficiencies at FRI SRU No.1 and SRU No.2 and shall submit a copy of that study to EPA and WDEQ. This study shall meet the requirements set forth in Paragraph 60 (Optimization). FRI shall promptly implement the physical improvements and operating parameters recommended in the study to optimize performance of FRI SRU No. 1 and SRU No. 2 during TGTU maintenance turnarounds in accordance with the schedule submitted under Paragraph 58.c, as applicable.	Optimization study has been completed. The study reccomendations have been completed
58c	By no later than ninety (90) days after completion of the optimization study in Paragraph 58.b above, FRI shall submit a report to EPA and WDEQ that proposes an appropriate interim performance standard (percent recovery efficiency and/or emission limitation) and, if necessary, a schedule for implementing related optimization study recommendations that are necessary to comply with FRI's proposed interim standard. Beginning with the date of such submission, FRI shall comply with its proposed interim performance standard and, if necessary, its proposed optimization study implementation schedule during TGTU turnarounds.	Optimization study has been completed. The study recommendations have been completed.





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58d	If, within thirty (30) days of receipt of the report required under Subparagraph 58.c., EPA, after consultation with WDEQ, determines that a more stringent interim performance standard and/or a different implementation schedule is appropriate and can be achieved with a reasonable certainty of compliance, EPA shall notify FRI of its determination. Unless FRI disputes EPA's determination(s) within ninety (90) days of FRI's receipt of EPA's notice, FRI shall, within that ninety (90) day period, comply with such new interim performance standard and/or a different implementation schedule or, if necessary, such other period as may be established by EPA based upon the approved implementation schedule. FRI shall comply with the appropriate interim performance standard for the two scheduled TGTU maintenance turnarounds that occur prior to March 31, 2016.	Optimization study has been completed. The study recommendations have been completed.
60	Optimization. Each optimization study required for SRPs at FRI or FEDRC under Paragraph 58.b. or Paragraph 59.b of this Consent Decree shall: a. contain a detailed evaluation of plant design and capacity, operating parameters and efficiencies - including catalytic activity, and material balances; b. contain an analysis of the composition of the acid gas and sour water stripper gas resulting from the processing of crude slate actually used, or expected to be used, in those Claus trains; c. contain a review of each critical piece of process equipment and instrumentation within the Claus train that is designed to correct deficiencies or problems that prevent the Claus train from achieving its optimal sulfur recovery efficiency and expanded periods of operation; d. establish baseline data through testing and measurement of key parameters throughout the Claus train; e. establish a thermodynamic process model of the Claus train; f. for any key parameters that have been determined to be at less than optimal levels, identify each change necessary to move such parameters toward their optimal values and a schedule for the implementation of those change(s); g. verify through testing, analysis of continuous emission monitoring data or other means, of incremental and cumulative improvements in sulfur recovery efficiency, if any; h. establish new operating procedures, if needed, for long-term efficient operation; and i. be conducted to optimize the performance of the Claus trains in light of the actual characteristics of the feeds to the trains.	The optimization plan contained the necessary information.
61	Sulfur Pit Emissions. FRI and FEDRC shall continue to route or re-route all sulfur pit emissions at their respective refineries so that sulfur pit emissions are eliminated, controlled, or included and monitored as part of the SRPs' emissions subject to the NSPS Subpart J limit for SO2, 40 C.F.R. § 60.104(a)(2).	Sulfur pit vents are routed to the TGTU incinerator.

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62	62. Good Operation and Maintenance. By no later than two hundred and seventy (270) days after the Date of Entry of this Consent Decree, FRI and FEDRC shall submit to EPA and the Applicable Intervenor a summary of the plans, implemented or to be implemented, at the their respective refineries for enhanced maintenance and operation of the FRI and FEDRC SRPs and the appropriate Upstream Process Units. The plans shall be entitled "Preventive Maintenance and Operation Plan" ("PMO Plan"). The PMO Plan shall be a compilation of approaches for exercising good air pollution control practices and for minimizing SO2 emissions from sulfur processing through applying good operating practices at the sulfur processing equipment and other production processes at the Covered Refineries. PMO Plans shall have as their goals the elimination of Acid Gas Flaring and the minimization of emissions from SRPs between scheduled maintenance turnarounds. The PMO Plan shall include as appropriate, but not be limited to: a. sulfur shedding procedures; b. Startup and Shutdown procedures for SRPs; c. control devices and Upstream Process Units; d. emergency procedures and schedules to coordinate maintenance turnarounds of the SRPs' Claus trains; and e. any control devices to coincide with scheduled turnarounds of major Upstream Process Units.	The PMO plan was developed and submitted as required.
62	At their respective Covered Refineries, FRI and FEDRC shall implement the PMO Plans at all times, including periods of Startup, Shutdown, upset, and Malfunction of its SRPs. Changes to a PMO Plan related to minimizing Acid Gas Flaring and/or SO2 emissions shall be summarized and reported by FRI and FEDRC to EPA and the Applicable Intervenor in the semi-annual report required under Paragraph 216.	The PMO plan was implemented at all times during the reporting period.
ı	Hydrocarbon Flaring	
65	NSPS Applicability to Hydrocarbon Flaring Devices. FRI and FEDRC, at their respective Covered Refineries, own and operate the Hydrocarbon Flaring Devices identified in Appendix G to this Consent Decree. FRI and FEDRC agree that each Hydrocarbon Flaring Device identified in Appendix G shall be an "affected facility," as that term is used in NSPS, 40 C.F.R. Part 60, and shall be subject to and required to comply with, the requirements of 40 C.F.R. Part 60, Subparts A and J, for fuel gas combustion devices used as emergency control devices for the quick and safe release of gases. FRI and FEDRC shall by the dates specified in Appendix G meet the NSPS Subparts A and J requirements for each Hydrocarbon Flaring Device identified in Appendix G. FRI and FEDRC shall achieve compliance with Subparts A and J requirements for each Hydrocarbon Flaring Device identified in Appendix G through the use of one or any combination of the following methods identified in Subparagraphs 65.a 65.e.:	See below
65a	Operating and maintaining a flare gas recovery system to prevent continuous or routine combustion in the Hydrocarbon Flaring Device. Use of a flare gas recovery system on a flare obviates the need to continuously monitor emissions as otherwise required by 40 C.F.R. § 60.105(a)(4);	Flare gas recovery compressors are utilized on portions of the flares. Those streams which are managed by the compressors are considered to be covered by this requirement.

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65b	Eliminating the routes of continuous or intermittent, routinely-generated refinery fuel gases to an Hydrocarbon Flaring Device and operating the Flaring Device such that it receives only non-routinely generated gases, process upset gases, fuel gas released as a result of relief valve leakage or gases released due to other Malfunctions;	Frontier is currently conducting a voluntary audit of sources to the flare and has preliminarily identified some minor intermittent or low flow streams which potentially may not be characterized as process upset gases.
65c	Operating the Hydrocarbon Flaring Device as a fuel gas combustion device, monitoring it for the continuous or intermittent, routinely-generated refinery fuel gas streams put into the flare header, with a CEMS as required by 40 C.F.R. § 60.105(a)(4) or with a parametric monitoring system approved by EPA as an alternative monitoring system under 40 C.F.R. § 60.13(i.) and complying with emission limits when and as required by Paragraph 68.a.; or	Frontier operates the Main Plant Flare as a fuel gas combustion device, however all of the streams which require monitoring which are covered by an AMP arecurrently being reviewed
65d	d. During the term of this Consent Decree eliminate to the extent practicable routes of continuous or intermittent routinely generated fuel gases to a Flaring Device and monitor the mass flow of sulfur dioxide emitted by use of a CEMS and flow meter; provided however, that this compliance method may not be used unless FRI and/or FEDRC, as appropriate: i. demonstrates to EPA and the Applicable Intervenor that the Flaring Device in question emits less than 500 pounds per day of SO2 under normal conditions; and by the dates specified in Appendix G;ii. secures EPA and the Applicable Intervenor's approval for use of this method as the selected compliance method; and iii. uses this compliance method for only one of the Flaring Devices listed in Appendix G at each Covered Refinery;	Frontier does not utilize this option.
65e	FRI and/or FEDRC may submit to EPA and the Applicable Intervenor a timely and complete application for an Alternative Monitoring Plan ("AMP") for a Flaring Device listed in Appendix E and Appendix G, by the applicable date listed in those appendices (rather than a final NSPS Subpart J compliance date). Such an AMP may be based on alternative monitoring for H2S or SO2. If an AMP is not approved by EPA, FRI and/or FEDRC, as appropriate, shall, within ninety (90) days of receiving notice of such disapproval submit to EPA for approval, with a copy to the Applicable Intervenor, a plan and schedule that provide for compliance with the monitoring requirements of NSPS Subpart J in accordance with the schedules contained in Appendices E and G. Such plan may include a revised AMP application, physical or operational changes to the equipment, or additional or different monitoring.	Frontier does not utilize this option.

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65f	For Flaring Devices that combust low-flow VOC streams from vents, pump seals, and other sources, it is anticipated that some of the AMP applications shall rely in part on calculating a weighted average H2S concentration of all VOC and fuel gas streams that are burned in a single Flaring Device and demonstrating with alternative monitoring that either the SO2 emissions from the Flaring Device shall not exceed 20 ppm or that the weighted average H2S concentration is not likely to exceed 162 ppm H2S. EPA shall not reject an AMP solely due to the AMP's use of one of these approaches to demonstrating compliance with NSPS Subpart J.	Frontier does not utilize this option.
65g	If prior to the termination of this Consent Decree, a Flaring Device becomes subject to NSPS Subpart Ja for a particular pollutant due to a "modification" (as that term is defined in the final Subpart Ja rule), the modified affected facility shall be subject to and comply with NSPS Subpart Ja in lieu of NSPS, Subpart J for that regulated pollutant to which a standard applies as a result of the modification.	The flares are now subject to NSPS Ja as modified flares.
65h	If prior to the termination of this Consent Decree, a Flaring Device becomes subject to NSPS Subpart Ja due to a "reconstruction" (as that term is defined in the final Subpart Ja rule), the reconstructed facility shall be subject to and comply with NSPS Subpart Ja for all pollutants in lieu of Subpart J.	The flares did not trigger the reconstruction definition of NSPS Ja.
66	At their respective Covered Refineries, FRI and FEDRC shall implement the compliance option chosen for each Hydrocarbon Flaring Device according to the schedule in Appendix G and identify the option that was implemented for each Hydrocarbon Flaring Device in the first Semi-Annual Report due under Paragraph 216 after such compliance option is chosen. The Parties recognize that periodic maintenance may be required for properly designed and operated flare gas recovery systems. At their respective Covered Refineries, FRI and FEDRC shall take all reasonable measures to minimize emissions while such periodic maintenance is being performed on any flare gas recovery system installed. FRI may request from WDEQ permission to temporarily operate the Old Flare (identified in Appendix G) at the FRI Refinery for only those periods of maintenance scheduled for the Main Flare. During such periods of operation, FRI must operate the Old Flare in compliance with NSPS Subpart J.	The Old Flare was not utilized during this reporting period.
67	Within one hundred and eighty (180) days after bringing an Hydrocarbon Flaring Device into compliance with 40 C.F.R. Part 60, Subparts A and J, at their respective Covered Refineries, FRI and FEDRC shall conduct a flare performance test pursuant to 40 C.F.R. § 60.18, or an EPA-approved equivalent method. In lieu of conducting the velocity test required in 40 C.F.R. § 60.18, FRI and FEDRC may submit velocity calculations to EPA and the Applicable Intervenor which demonstrate that the NSPS Hydrocarbon Flaring Device meets the performance specification required by 40 C.F.R. § 60.18. Operation of an adequately sized flare gas recovery unit that recovers all routine continuous and intermittent gases sent to the flare obviates the need to conduct a performance test pursuant to methods in 40 C.F.R. 60.18(f) on the associated flare(s).	The required information has previously been submitted.

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68	Compliance With the Emissions Limit at 40 C.F.R. § 60.104(a)(1). a. Continuous or Intermittent, Routinely-Generated Refinery Fuel Gases. For continuous or intermittent, routinely-generated refinery fuel gases that are combusted in any of the NSPS Hydrocarbon Flaring Devices at their respective Covered Refineries, FRI and FEDRC shall comply with the emission limit at 40 C.F.R. § 60.104(a)(1) by the dates specified in Appendix G. b. Non-Routinely Generated Gases. The combustion of gases generated by the Startup, Shutdown, or Malfunction of a refinery process unit or released to an NSPS Flaring Device as a result of relief valve leakage or other Malfunction is exempt from the requirement to comply with 40 C.F.R. § 60.104(a)(1).	Frontier is currently conducting a voluntary audit of sources to the flare and has preliminarily identified some minor intermittent or low flow streams which potentially may not be characterized as process upset gases.
J	Control of Acid Gas Flaring and Tail Gas Incidents	
71	Investigation and Reporting. Commencing upon the Date of Entry and thereafter, no later than sixty (60) days following the end of any Acid Gas Flaring Incident, at their respective Covered Refineries, FRI and FEDRC shall conduct an investigation into the root cause(s) of the incident and record the findings of the investigation in a report (the "Incident Report"). Each Incident Report shall be included in the Semi-Annual Report required by Paragraph 84. The Incident Report for each incident shall include the following:	Incident Reports have been completed for all acid gas and tail gas flaring incidents during the reporting period.
72	Corrective Action. In response to any AG Flaring Incident occurring after the Date of Entry, at their respective Covered Refineries, FRI and FEDRC shall take, as expeditiously as practicable, such interim and/or long-term corrective actions, if any, as are consistent with good engineering practice to minimize the likelihood of a recurrence of the Root Cause and all significant contributing causes of that AG Flaring Incident.	Information on corrective actions is included in the incident Reports.
72a	After a review of any report required to be prepared by Paragraph 71 and submitted to EPA and the Applicable Intervenor as required by Paragraph 84, EPA shall notify FRI and/or FEDRC, as applicable, in writing of (1) any deficiencies in the corrective action(s) listed in the findings and/or (2) any objections to the schedule(s) of implementation, and explain the basis for EPA's objection(s). FRI and/or FEDRC, as applicable, will implement an alternative or revised corrective action or implementation schedule based on EPA's comments. If a corrective action that EPA has identified as deficient is already completed, then FRI and/or FEDRC, as applicable, is not obligated to implement the corrective action identified by EPA for that Flaring Incident. However, FRI and/or FEDRC, as applicable, will be put on notice that such corrective action is deficient and not acceptable for remedying any subsequent, similar root cause(s) of any incident.	No deficiencies have been identified by EPA/WDEQ on incident reports

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78	In the event a dispute under Paragraphs 74 through 77 is brought to the Court pursuant to the Dispute Resolution provisions of this Consent Decree, Section XVII. (Retention of Jurisdiction/Dispute Resolution), FRI and/or FEDRC, as appropriate, may also assert a Startup, Shutdown and/or upset defense (including an individual sulfur recovery unit within an SRP), but the United States shall be entitled to assert that such defenses are not available. If FRI, or FEDRC, as appropriate, prevails in persuading the Court that the defenses of Startup, Shutdown and/or upset are available for AG Flaring Incidents under 40 C.F.R. § 60.104(a)(1), FRI, or FEDRC, as appropriate, shall not be liable for stipulated penalties for emissions resulting from such Startup, Shutdown and/or upset. If the United States prevails in persuading the Court that the defenses for Startup, Shutdown and/or upset are not available, FRI or FEDRC, as appropriate, shall be liable for such stipulated penalties.	No disputes arose during the reporting period.
79	Other than for a Malfunction or force majeure, if no Acid Gas Flaring Incident occurs at either the FEDRC or FRI Refinery for a rolling 36-month period, then the stipulated penalty provisions of Paragraph 254 of Section XIII. (Stipulated Penalties) shall no longer apply to that refinery. EPA may elect to reinstate the stipulated penalty provision if such refinery has an Acid Gas Flaring Incident that would otherwise be subject to stipulated penalties. EPA's decision shall not be subject to dispute resolution. Once reinstated, the stipulated penalty provision shall continue for the remaining life of this Consent Decree for that Covered Refinery.	Frontier is not utilizing this option.
80	Emissions Calculations.	See below
80a	Calculation of the Quantity of Sulfur Dioxide Emissions Resulting from AG Flaring. For purposes of this Consent Decree, FRI and FEDRC shall calculate the quantity of SO2 emissions resulting from an AG Flaring Incident by applying the following formula: Tons of SO2 = [FR][TD][ConcH2S][8.44 x 10-5] The quantity of SO2 emitted shall be rounded to one decimal point. (Thus, for example, for a calculation that results in a number equal to 10.050 tons, the quantity of SO2 emitted shall be rounded to 10.1 tons.) For purposes of determining the occurrence of, or the total quantity of SO2 emissions resulting from, an AG Flaring Incident that consists of intermittent AG Flaring, the quantity of SO2 emitted shall be equal to the sum of the quantities of SO2 flared during each 24-hour period starting when the Acid Gas was first flared.	
80b	Calculation of the Rate of SO2 Emissions During AG Flaring. For purposes of this Consent Decree, the rate of SO2 emissions resulting from an AG Flaring Incident shall be expressed in terms of pounds per hour and shall be calculated by the following formula: ER = [FR][ConcH2S][0.169] The emission rate shall be rounded to one decimal point. (Thus, for example, for a calculation that results in an emission rate of 19.95 pounds of SO2 per hour, the emission rate shall be rounded to 20.0 pounds of SO2 per hour; for a calculation that results in an emission rate of 20.05 pounds of SO2 per hour, the emission rate shall be rounded to 20.1.)	Acid gas flaring events are calculated and reported in Attachment C Flaring

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82	Tail Gas Incidents: Investigation, Reporting, Corrective Action and Stipulated Penalties. For Tail Gas Incidents, FRI and/or FEDRC, as appropriate, shall follow the same investigative, reporting, corrective action and assessment of stipulated penalty procedures as those set forth in Paragraphs 71 through 79 for Acid Gas Flaring Incidents. Those procedures shall be applied to TGTU shutdowns, bypasses of a TGTU, or other events which result in a Tail Gas Incident, including unscheduled Shutdowns of a Claus Sulfur Recovery Plant. Notwithstanding the foregoing, during the interim periods identified in Paragraphs 58 and 59, stipulated penalties shall not apply to a Tail Gas Incident attributable to the scheduled Startup or Shutdown of an individual train at the FRI SRP or at the FEDRC SRP, provided that FRI and/or FEDRC, as appropriate, demonstrate in their Tail Gas Incident Report that they have implemented good air pollution control practices. This Paragraph 82 shall apply without the exemption from stipulated penalties for all Tail Gas Incidents that occur after the effective dates of full NSPS applicability for SRPs, as provided in Paragraph 56 above.	Tail Gas incidents are investigated and reported in Attactment C Flaring
	Calculation of the Quantity of SO2 Emissions Resulting From A Tail Gas Incident. For the purposes of this Consent Decree, the quantity of SO2 emissions resulting from a Tail Gas Incident shall be calculated by one of the following methods, based on the type of event: a. If Tail Gas is combusted in a flare, the SO2 emissions are calculated using the methods outlined in Paragraph 80; or b. If Tail Gas exceeding the 250 ppmvd (NSPS J limit) is emitted from a monitored SRP incinerator, then the following formula applies: ERTGI = [FRInc.]i [Conc. SO2 – 250]i [0.169 x 10-6] TD i TGI Σ = 1 209 209 . % 2 . O Where: ERTGI = Emissions from Tail Gas Unit at the SRP incinerator, pounds of SO2 over a 24 hour period TDTGI = Hours when the incinerator CEM was exceeding 250 ppmvd SO2 on a rolling twelve hour average, corrected to 0% O2, in each 24 hour period of the Incident i = Each hour within TDTGI FRInc. = Incinerator Exhaust Gas Flow Rate (standard cubic feet per hour, dry basis) (actual stack monitor data or engineering estimate based on the acid gas feed rate to the SRP) for each hour of the Incident Conc. SO2 = The average SO2 concentration (CEMS data) that is greater than 250 ppm in the incinerator exhaust gas, ppmvd corrected to 0% O2, for each hour of the Incident % O2 = O2 concentration (CEMS data) in the incinerator exhaust gas in volume % on dry basis for each hour of the Incident 0.169 x 10-6 = [1.0 lb mole of SO2 / 379 SO2] [64 lbs SO2 / 1.0 lb mole SO2] [1 x 10-6] Standard conditions = 60 degree F; 14.7 lbforce/sq.in. absolute In the event the concentration SO2 data point is inaccurate or not available or a flow meter for FRInc does not exist or is inoperable, then either FRI or FEDRC, as applicable, shall estimate emissions based on best engineering judgment.	Emissions are calculated using the pounds/hour output from the CEM and subtracting the SRP SO2 permit limit. Going forward, Frontier will utilize the equations in paragraph 83
К	Control of Hydrocarbon Flaring Incidents	
L	Benzene Waste NESHAP Program Enhancements	

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86	At each of the Covered Refineries, FRI and FEDRC agree to comply with all applicable requirements of 40 C.F.R. Part 61, Subpart FF ("Benzene Waste Operations NESHAP" or "Subpart FF" or "BWON") and to undertake the measures set forth in this Section VI.L. for ensuring future compliance with Subpart FF and minimizing or eliminating fugitive benzene waste emissions.	Frontier recently voluntarily disclosed audit findings indicating various deficiencies in the BWON program. The specific issues related to Consent Decree items are identified below.
88	88. FRI Refinery Compliance Status Changes. FRI has reported a Total Annual Benzene ("TAB") of less than 10 Mg/yr. If at any time from the Date of Entry of this Consent Decree through its termination, FRI is determined to have a TAB equal to or greater than 10 Mg/yr, FRI shall utilize the appropriate compliance option specified below. a. If the TAB exceeds 10 Mg/yr based on errors, omissions, or mischaracterization of waste streams existing at the refinery as of the Date of Entry, FRI shall utilize the compliance option set forth at 40 C.F.R. § 61.342(e) (the "6 BQ compliance option"). b. If the TAB exceeds 10 Mg/yr based on increased throughput/capacity expansion, FRI may select either the 2 Mg or 6 BQ compliance option.	Frontier determined the facility TAB was over 10 Mg/yr, and is complying with the 68Q compliance option.
89	FRI shall consult with EPA and the Applicable Intervenor before making any change in compliance strategy required by Paragraph 88. All changes must be undertaken in accordance with the regulatory provisions of the BWON.	No change in compliance status occurred during this reporting peroid.
90	90. One-Time Review and Verification of Each Covered Refinery's TAB: Phase One of the Review and Verification Process. By no later than 12 months after the Date of Entry, FRI and FEDRC shall complete a Phase One review and verification of each Covered Refinery's TAB and compliance with the 2 Mg compliance option at the FEDRC Refinery. For each Covered Refinery, the Phase One review and verification process shall include, at a minimum: a. an identification of each waste stream as defined in Subpart FF that is required to be included in the Covered Refinery's TAB; b. a review and identification of the calculations and/or measurements used to determine the flows of each waste stream for the purpose of ensuring the accuracy of the annual waste quantity for each waste stream; c. an identification of the benzene concentration in each waste stream. FRI and FEDRC shall be required to sample for benzene concentration at no less than ten (10) waste streams per Covered Refinery consistent with the requirements of 40 C.F.R. § 61.355(c)(1) and (3). FRI and FEDRC may use previous analytical data or documented knowledge of waste streams in accordance with 40 C.F.R. § 61.355(c)(2) for any remaining waste streams not sampled; and d. an identification of whether or not the waste stream is controlled consistent with the requirements of Subpart FF.	Previously submitted.
91	Phase One Report. By no later than fifteen (15) months after Date of Entry FRI and FEDRC shall submit to EPA and the Applicable Intervenor a BWON Compliance Review and Verification Report for their respective Covered Refinery that sets forth the results of Phase One, including but not limited to the items identified in (a) through (d) of Paragraph 90.	Previously submitted.

Paragraph	Attachment H - Miscellaneous	Comments
92	One-Time Review and Verification of Each Covered Refinery's TAB: Phase Two of the Review and Verification Process. Based on EPA's review of the BWON Compliance Review and Verification Reports and after an opportunity for consultation with the Applicable Intervenor, EPA may select up to twenty (20) additional waste streams at each Covered Refinery for sampling for benzene concentration. At their respective Covered Refinery, FRI and FEDRC shall conduct the required sampling and submit the results to EPA within sixty (60) days of receipt of EPA's request. FRI and FEDRC shall use the results of this additional sampling to reevaluate the TAB and the uncontrolled benzene quantity and to amend the BWON Compliance Review and Verification Report, as needed. To the extent that EPA requires FRI and FEDRC to sample a waste stream as part of the Phase Two review that FRI and/or FEDRC sampled and included as part of its Phase One review, each may average the results of such sampling at their respective Covered Refinery. FRI and FEDRC shall submit an amended BWON Compliance Review and Verification Report within one-hundred twenty (120) days following the date of the completion of the required Phase Two sampling, if Phase Two sampling is required by EPA. This amended BWON Compliance Review and Verification Report. If Phase Two sampling is not required by EPA, the originally-submitted BWON Compliance Review and Verification Report.	Previously submitted.
93	Amended TAB Reports. If the results of the BWON Compliance Review and Verification Report indicate that a Covered Refinery's TAB report filed most recently before this Consent Decree does not satisfy the requirements of Subpart FF, the Covered Refinery shall submit, by no later than one-hundred twenty (120) days after completion of the BWON Compliance Review and Verification Report, an amended TAB report to EPA. The BWON Compliance Review and Verification Report submitted by FRI and/or FEDRC, as appropriate, shall be deemed an amended TAB report for purposes of Subpart FF reporting to EPA.	Previously submitted.
94	Implementation of Actions Necessary to Correct Non-Compliance: FRI. If the results of the BWON Compliance Review and Verification Report indicate that FRI has a TAB of over 10 Mg/yr, FRI shall submit to EPA, by no later than one-hundred eighty (180) days after completion of the BWON Compliance Review and Verification Report, a Compliance Plan that identifies with specificity: a. the actions it shall take to ensure that the FRI's TAB remains below 10 Mg/yr for 2009 and each calendar year thereafter; or b. a compliance strategy and schedule that FRI shall implement to ensure that FRI complies with the 6 BQ or the 2Mg compliance option as soon as practicable but by no later than December 31, 2010, if it cannot ensure a consistent TAB below 10 Mg/yr.	Previously submitted.

Paragraph	Attachment H - Miscellaneous	Comments
96	Implementation of Actions Necessary to Correct Non-Compliance: Review and Approval of Plans. Any plans submitted pursuant to Paragraphs 94 and 95 shall be subject to the approval of, disapproval of, or modification by EPA, after an opportunity for consultation with the Applicable Intervenor. Within sixty (60) days after receiving any notification of disapproval or request for modification from EPA, FRI and/or FEDRC, as appropriate, shall submit to EPA and the Applicable Intervenor a revised plan that responds to all identified deficiencies. Unless EPA disapproves or requests modifications of the revised plan within sixty (60) days, FRI and/or FEDRC, as appropriate, shall implement its proposed plan.	EPA did not disapprove or request a modification of the plan.
97	Implementation of Actions Necessary to Correct Non-Compliance: Certification of Compliance. By no later than thirty (30) days after completion of the implementation of all actions, if any, required pursuant to Paragraphs 94 and 95 to come into compliance with the applicable compliance option, FRI and FEDRC shall for their respective Covered Refinery submit, pursuant to Paragraph 139 of this Consent Decree, their certifications and a report, pursuant to Section XIX (General Provisions), Paragraph 356 (Notice), to EPA and the Applicable Intervenor that such refinery complies with the BWON.	Previously submitted.
101	Prohibition of Use of Single Canisters. Except as expressly allowed in Paragraph 105, FRI and FEDRC shall not use single carbon canisters for any new units or installations that require vapor control pursuant to the BWON at any of their Covered Refineries.	Frontier does not currently utilize single canisters.
102	Definition of "Breakthrough" In Dual Canister Systems. For dual carbon canister systems in series and depending upon the parameter that FRI and/or FEDRC decide to monitor, "breakthrough" between the primary and secondary canister shall be defined as any reading equal to or greater than either 50 ppm VOC or 5 ppm benzene.	Frontier utilizes a breakthrough definition of 50 ppm VOC.
103	Monitoring for Breakthrough in Dual Canister Systems. By the later of either the Date of Entry or seven (7) days after the installation of any new dual canister, FRI and FEDRC shall start to monitor for Breakthrough between the primary and secondary carbon canisters at times when there is actual flow into the carbon canister, in accordance with the frequency specified in 40 C.F.R. § 61.354(d), and shall monitor the outlet of the secondary canister on a monthly basis or at its design replacement interval (whichever is less) to verify the proper functioning of the system.	Frontier recently voluntarily disclosed audit findings indicating monitoring had not been conducted per these requirements. Monitoring is now conducted per this requirement.
104	Replacing Canisters in Dual Canister Systems. FRI and FEDRC shall replace each original primary carbon canister (or route the flow to an appropriate alternative control device) immediately when any Breakthrough is detected. The original secondary carbon canister shall become the new primary carbon canister and a fresh carbon canister shall become the secondary canister unless both the primary and secondary carbon canisters are replaced. For purposes of this Paragraph, "immediately" shall mean within twenty-four (24) hours. As an alternative, FRI and FEDRC may continue to operate the dual carbon canister system after Breakthrough is detected provided VOC monitoring is conducted at the outlet of the secondary carbon canister on a daily basis. If any VOC reading is detected at the outlet of the secondary carbon canister, both canisters must be replaced within twelve (12) hours.	Frontier recently voluntarily disclosed audit findings indicating replacement had not been conducted per these requirements. Replacement of dual canisters now occurs per this requirement.

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Paragraph	Attachment H - Miscellaneous	Comments
105	Limited Use of Single Canisters. FRI and FEDRC may utilize properly sized single canisters for short-term operations such as with temporary storage tanks or as temporary control devices. For canisters operated as part of a single canister system, Breakthrough is defined for purposes of this Decree as any reading of VOC or benzene above background. Beginning no later than the Date of Entry, FRI and FEDRC shall monitor for Breakthrough from each single carbon canister each day there is actual flow to the carbon canister.	Frontier does not currently utilize single canisters.
106	Replacing Canisters in Single Canister Systems. FRI and FEDRC shall replace each single carbon canister with a fresh carbon canister, discontinue flow, or route the stream to an alternate, appropriate device immediately when any Breakthrough is detected. For this Paragraph, "immediately" shall mean within eight (8) hours for canisters of 55 gallons or less and within twenty-four (24) hours for canisters greater than 55 gallons. If flow to a single canister is discontinued under this Paragraph, such canister may not be placed back into BWON vapor control service until it has been appropriately regenerated or replaced.	Frontier does not currently utilize single canisters.
107	Maintaining Canister Supplies. At their respective Covered Refineries, FRI and FEDRC shall maintain a supply of fresh activated carbon canisters at all times.	Frontier maintains a supply of fresh activated carbon at all times.
108	Records Relating to Canisters. FRI and FEDRC shall maintain records for the requirements of Paragraphs 98 - 107 in accordance with 40 C.F.R. § 61.356(j)(10). Additionally, all VOC and/or benzene measurements used to calculate removal efficiencies through control carbon canisters shall be maintained in a logbook or electronic database. The date, time, monitoring instrument type, instrument reading, and canister location shall be maintained in the logbook or database.	Frontier recently voluntarily disclosed audit findings indicating records had not been maintained as required. Records are now maintained as directed by this requirement.
109	Annual Review. By no later than sixty (60) days after Date of Entry, at their respective Covered Refineries, FRI and FEDRC shall modify existing Management of Change ("MOC") procedures or develop a new program to annually review process and project information for each Covered Refinery, including but not limited to construction projects, to ensure that all new benzene waste streams are included in each Covered Refinery's waste stream inventory during the life of this Consent Decree.	Frontier recently voluntarily disclosed audit findings indicating previous reviews were not as comprehensive as they could have been. An annual review was conducted prior to the submission of the BWON annual report this year.
112	Until this Consent Decree is terminated, FRI and FEDRC shall conduct subsequent audits of each of their respective laboratories used for BWON analyses at least once every two years.	Audits are conducted every two years. The last audit was completed August 2013.
114	Benzene Spills. Beginning no later than the Date of Entry, at their respective Covered Refineries, FRI and FEDRC shall continue to review spills to determine whether more than ten (10) pounds of benzene waste was generated in any twenty-hour (24) hour period at either Covered Refinery. FRI and FEDRC shall continue to include the benzene generated by such spills in the TAB and in the uncontrolled benzene quantity calculations for each Covered Refinery in accordance with the applicable compliance option as required by Subpart FF.	Benzene spills are evaluated per this requirement.

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118	Wastes Subject to Subpart FF: Schematics. By no later than one hundred and eighty (180) days after the Date of Entry, FRI and FEDRC shall each submit to EPA and the Applicable Intervenor schematics for their respective Covered Refineries that: a. depict the waste management units (including sewers) that handle, store, and transfer wastes subject to Subpart FF; b. identify the control status of each waste management unit; and c. show how such waste is transferred within the Covered Refinery. FRI and FEDRC shall include with the schematics a quantification of all uncontrolled wastes subject to Subpart FF. If requested by EPA, FRI and/or FEDRC, as appropriate, shall submit to EPA within ninety (90) days of the request, revised schematics regarding the characterization of these wastes and the appropriate control standards.	Previously Submitted. As part of the recent audit and work following, Frontier has done a thorough review of the BWON system and is in the process of determining how the schematic needs to be updated. After it is determined how to update the schematic to properly reflect operations, it will be submitted.
119	Wastes Subject to Subpart FF: Non-Aqueous Benzene Waste Streams. By Date of Lodging, all waste management units at each Covered Refinery handling non-exempt, non-aqueous benzene wastes, as defined in Subpart FF, shall meet the applicable control standards of Subpart FF.	Frontier recently voluntarily disclosed audit findings indicating that this requirement was not being met. Non-Aqueous Benzene Wastes are now managed per this requirement.
120	Wastes Subject to Subpart FF: Aqueous Benzene Waste Streams. For purposes of calculating each Covered Refinery's TAB pursuant to the requirements of 40 C.F.R. § 61.342(a), FRI and FEDRC shall include all wastes subject to Subpart FF that become "aqueous" until such streams are recycled to a process or put into a process feed tank (unless the tank is used primarily for the storage of wastes). Appropriate adjustments shall be made to such calculations to avoid the double-counting of benzene. For purposes of complying with the 2 Mg or 6 BQ compliance option, by Date of Lodging, all waste management units at each Covered Refinery handling BWON waste streams either shall meet the applicable control standards of Subpart FF or shall have their uncontrolled benzene quantity count toward the applicable 2 Mg or 6 BQ limit.	Aqueous Benzene Wastes are managed per this requirement.
121	BWON Sampling Plans: General. By no later than the completion of the BWON training specified in Paragraph 115, FRI and FEDRC shall each submit to EPA and the Applicable Intervenor, for approval, BWON Sampling Plans for their respective Covered Refineries to describe the sampling of BWON streams that FRI and FEDRC shall undertake to estimate quarterly and annual TABs (for FRI) or quarterly and annual uncontrolled benzene quantities for Covered Refineries with a TAB greater than or equal to 10 Mg/yr (for FEDRC and FRI if and when FRI's TAB exceeds 10 Mg/yr).	A plan was previously submitted. As part of the recent audit and work following, Frontier has done a thorough review of the BWON Sampling Plan and is in the process of determining how the plan needs to be updated. After it is determined how to update the plan, it will be submitted and implemented.

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122	Sampling Plan shall identify: a. annually, each waste stream that has contributed 0.05 Mg/yr or more at the	A plan was previously submitted. As part of the recent audit and work following, Frontier has done a thorough review of the BWON Sampling Plan and is in the process of determining how the plan needs to be updated. After it is determined how to update the plan, it will be submitted and implemented.
127	BWON Sampling Plans: Timing for Implementation. At their respective Covered Refineries, FRI and FEDRC shall implement the sampling required under their Sampling Plan during the first full calendar quarter after they submit that plan. FRI and FEDRC shall, at their respective Covered Refinery, continue to implement the Sampling Plan: a. unless and until EPA disapproves the plan; or b. unless and until FRI and/or FEDRC modifies a plan, with EPA's approval, under Paragraph 128.	Implemented as required.
128	BWON Sampling Plans: Modifications.	
128a	Changes in Processes, Operations, or Other Factors. If changes in processes, operations, or other factors lead FRI and/or FEDRC to conclude that a Sampling Plan for a Covered Refinery may no longer provide an accurate basis for estimating that Covered Refinery's quarterly or annual TABs or benzene quantities under Paragraph 129, then by no later than ninety (90) days after FRI and/or FEDRC, as appropriate, determine that the plan no longer provides an accurate measure, they shall submit to EPA and the Applicable Intervenor a revised Sampling Plan for EPA approval. In the first full calendar quarter after submitting the revised plan, FRI and/or FEDRC, as appropriate shall implement the revised plan. FRI and/or FEDRC, as appropriate, shall continue to implement the revised plan unless and until EPA disapproves the revised plan after an opportunity for consultation with the Applicable Intervenor.	As part of the recent audit and work following, Frontier has done a thorough review of the BWON Sampling Plan and is in the process of determining how the plan needs to be updated. After it is determined how to update the plan, it will be submitted and implemented.
128b	Requests for Modifications. After two (2) years of implementing a Sampling Plan, FRI and/or FEDRC, as appropriate, may submit a request to EPA for approval, with a copy to the Applicable Intervenor, to revise a Covered Refinery's sampling plan, including sampling frequency. EPA shall not unreasonably withhold its consent. FRI and FEDRC shall not implement any proposed revisions under this Subparagraph until EPA provides its approval after an opportunity for consultation with the Applicable Intervenor.	Frontier has not requested a modification to the sampling plan requirements.
129	Quarterly and Annual Estimations of TABs and Uncontrolled Benzene Quantities. At the end of each calendar quarter and based on sampling results and approved flow calculations, FRI and FEDRC shall calculate a quarterly and projected annual: a. TAB for each Covered Refinery with a TAB less than 10 Mg/yr; and b. uncontrolled benzene quantity for each Covered Refinery with a TAB greater than or equal to 10 Mg/yr.	Frontier calculates these values and reports them as required. See Attachment A for details.

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131	Corrective Measures: Basis. Except as set forth in Paragraph 132, FRI and FEDRC shall implement corrective measures specified in Paragraph 133 of this Consent Decree at the applicable Covered Refinery if:	No corrective measures are required to be reported during this reporting period.
131c	For any Covered Refinery with a TAB greater than or equal to 10 Mg/yr and electing the 6 BQ compliance option, the quarterly uncontrolled benzene quantity equals or exceeds 1.5 Mg or the projected annual uncontrolled benzene quantity equals or exceeds 6 Mg for the then-current compliance year.	No corrective measures are required to be reported during this reporting period.
132	Exception to Implementing Corrective Measures. If, at their respective Covered Refineries, FRI and/or FEDRC can identify the reason(s) in any particular calendar quarter that the quarterly and projected annual calculations result in benzene quantities in excess of those identified in Paragraph 133 and state that they do not expect such reason or reasons to recur, then FRI and/or FEDRC, as appropriate, may exclude the benzene quantity attributable to the identified reason(s) from the projected calendar year quantity. EPA and the Applicable Intervenor may dispute any determination made by FRI or FEDRC. If that exclusion results in no potential violation of the BWON, FRI and/or FEDRC, as appropriate, shall not be required to implement corrective measures under Paragraph 131, and may exclude the uncontrolled benzene attributable to the identified reason(s) in determining the applicability of Paragraph 133. At any time that either FRI or FEDRC proceeds under this Paragraph, they shall describe how they have satisfied the conditions in this Paragraph in the reports due under Section XI. (Reporting and Record Keeping) of this Decree.	No corrective measures are required to be reported during this reporting period.
133	Compliance Assurance Plan - Corrective Measures. If at their respective Covered Refineries, FRI and/or FEDRC meets one or more conditions in Paragraph 131 (except as provided under Paragraph 132), then by no later than sixty (60) days after the end of the calendar quarter in which one or more of the conditions were met, FRI and/or FEDRC, as appropriate, shall submit a Compliance Assurance Plan to EPA for approval, with a copy to the Applicable Intervenor. In that Compliance Assurance Plan, FRI and/or FEDRC shall identify the quantity and cause(s) of the potentially-elevated benzene quantities, all corrective measures that they have taken or plan to take to ensure that the cause(s) shall not recur, and the schedule of actions that they shall take to ensure that the subject refinery complies with the BWON for the calendar compliance year. At their respective Covered Refinery, FRI and/or FEDRC shall implement the plan unless and until EPA disapproves after an opportunity for consultation with the Applicable Intervenor.	No corrective measures are required

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134	Third-Party Assistance. If the projected annual benzene quantity under Paragraph 129 exceeds, in two consecutive quarters, 10 Mg/yr for a Covered Refinery subject to Paragraph 131.a, 2 Mg/yr for a Covered Refinery subject to Paragraph 131.b, or 6 Mg/yr for a Covered Refinery subject to Paragraph 131.c., and FRI and/or FEDRC cannot identify the reason for the exceedances as allowed under Paragraph 132, they shall within thirty (30) days retain a third-party contractor during the following quarter to undertake a TAB study and compliance review at that Covered Refinery. By no later than ninety (90) days after they receive the results of the third-party TAB study and compliance review, FRI and/or FEDRC, as appropriate, shall submit such results and a plan and schedule for remedying any deficiencies identified in the third-party study and compliance review to EPA and the Applicable Intervenor. At their respective Covered Refinery, FRI and FEDRC shall implement their proposed plan unless and until EPA disapproves after an opportunity for consultation with the Applicable Intervenor. By no later than thirty (30) days after completion of the implementation of all actions, if any, required to come into compliance with the applicable compliance option, FRI and FEDRC shall submit their respective certifications, pursuant to Paragraph 139 of this Consent Decree, and a report, pursuant to Section XIX (General Provisions), Paragraph 356 (Notice), to EPA and the Applicable Intervenor that such Covered Refinery complies with the BWON.	No corrective measures are required to be reported during this reporting period.
135	Miscellaneous Measures.	
135a	For the FRI Refinery, by no later than the date FRI submits a Compliance Plan under Paragraph 94.a, FRI shall:	
135a.i	Conduct monthly visual inspections of all Subpart FF water traps within the FRI Refinery's individual drain systems;	Frontier recently voluntarily disclosed audit findings indicating these inspections previously were not complete. Monthly visual inspection of all Subpart FF water traps are now being conducted.
135a.ii	On a weekly basis, visually inspect all Subpart FF conservation vents on process sewers for detectable leaks; reset any vents where leaks are detected; and record the results of the inspections. After two (2) years of weekly inspections, and based upon an evaluation of the recorded results, FRI may submit a request to the Applicable EPA Region to modify the frequency of the inspections. EPA shall not unreasonably withhold its consent. Nothing in this Subparagraph shall require FRI to monitor conservation vents on fixed roof tanks. Alternatively, for conservation vents with indicators that identify whether flow has occurred, FRI may elect to visually inspect such indicators on a monthly basis and, if flow is then detected, FRI shall then visually inspect that indicator on a weekly basis for four (4) weeks. If flow is detected during any two (2) of those four (4) weeks, FRI shall install a carbon canister on that vent until appropriate corrective action(s) can be implemented to prevent such flow;	Frontier recently voluntarily disclosed audit findings indicating these inspections previously were not complete. Monthly visual inspection of all Subpart FF water traps are now being conducted.

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135a.iii	Conduct quarterly monitoring of the controlled oil-water separators in benzene service in accordance with the "no detectable emissions" provision in 40 C.F.R. § 61.347, or quarterly measurements of the oil-water separator seal gap if using the alternative control requirements allowed under 40 C.F.R. § 61.352, if the separator is a control device under Subpart FF; and	Frontier recently voluntarily disclosed audit findings indicating these inspections previously were not complete. Quarterly inspection of controlled oil-water separators in benzene service are now being conducted.
135a.iv	Continue to manage all groundwater remediation wastes that are covered by Subpart FF at the FRI Refinery in appropriate waste management units under and as required by the BWON.	As part of the recent voluntary audit and work following, Frontier has determined the groundwater remediation sump is not a controlled WMU. Frontier included the uncontrolled emissions in the 6BQ calculations. An action plan is currently being developed to control the groundwater remediation wastes.
136	Reporting and Record Keeping Requirements for this Section VI.L. Outside of the Reports Required under 40 C.F.R. § 61.357 or under the Progress Report Procedures of Section XI (Reporting and Record Keeping). At the times specified in the applicable provisions of this Section VI.L. for their respective Covered Refineries, FRI and FEDRC shall submit, as and to the extent required, copies of the following reports to EPA and the Applicable Intervenor:	Previously submitted.
136a	A BWON Compliance Review and Verification Report, Paragraph 90, as amended, if necessary, by Paragraph 92;	Previously submitted.
	An Amended TAB Report, if necessary (Paragraph 93);	Previously submitted.
136c	A Plan for the FRI Refinery to come into compliance with the 6 BQ or the 2Mg compliance option if and when FRI discovers that its TAB equals or exceeds 10 Mg/yr through the BWON Compliance Review and Verification Report (Paragraph 94), or through sampling (Paragraph 133);	Previously submitted.
136d	A compliance certification, if necessary (Paragraph 97);	Previously submitted.
136f	Schematics of Subpart FF waste movements (Paragraph 118), as revised, if necessary;	Previously submitted.
136g	Sampling Plans (Paragraph 121), and revised Sampling Plans, if necessary (Paragraph 128); and	Previously submitted.
136h	A Compliance Assurance Plan to ensure that uncontrolled benzene does not equal or exceed, as applicable, 6 BQ or 2 Mg/yr (Paragraph 133).	Not required.

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138	At any time after two years of reporting pursuant to the requirements of Paragraphs 136 and 137, FRI or FEDRC may submit a request to EPA to modify the reporting frequency for any or all of the reporting categories. This request may include a request to report the previous year's projected calendar year TAB and uncontrolled benzene quantity in the Part XI report due on February 28th of each year, rather than semi-annually on February 28th and August 31st of each year. FRI and FEDRC shall not change the due dates for their reports under Paragraphs 136 and 137 unless and until EPA approves their request after an opportunity for consultation with the Applicable Intervenor.	Frontier has not requested a modification of the reporting requirements.
139	Certifications Required in Section VI.L. Certifications required under this Section shall include the following statement: I certify under penalty of law that this information was prepared under my direction or supervision in accordance with a system designed to assure that qualified personnel properly gather and evaluate the information submitted. Based on my directions and my inquiry of the person(s) who manage the system, or the person(s) directly responsible for gathering the information, the information submitted is, to the best of my knowledge and belief, true, accurate, and complete	Certifications are included as required.
M	Leak Detection and Repair ("LDAR") Program Enhancements	
142	FRI - Affected Facilities. Upon the Date of Entry, all equipment, as defined by 40 C.F.R. § 60.591, within each process unit and all compressors at FRI shall become "affected facilities" for purposes of 40 C.F.R. Part 60, Subpart GGG, and shall become subject to and comply with the requirements of 40 C.F.R. Part 60, Subpart GGG, and the requirements of Section VI.M. of this Consent Decree.	All process units are affected facilities under NSPS Subparts A and GGG.

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144	ensure that components subject to LDAR requirements that are added to each facility during scheduled maintenance and construction activities are integrated into the LDAR program; f. A process for evaluating new and replacement LDAR equipment that includes active consideration of equipment or techniques that shall minimize leaks and/or eliminate chronic leakers; and g. A definition of "LDAR Personnel" and a process for accountability, identifying for each facility the person or position that shall be the "LDAR Coordinator." Consistent with FRI and FEDRC management authorities, this person shall have the responsibility to implement improvements to the LDAR program.	Frontier recently voluntarily disclosed audit findings indicating the written LDAR plan had not been kept up-to-date. The plan was updated in December 2012 to address this.
145	FRI and FEDRC shall submit a copy of each Covered Refinery's initial written LDAR Program to EPA and to the Applicable Intervenor with the first Semi-Annual Progress Report required by Paragraph 170(a). EPA shall review and may comment on the written program after an opportunity for consultation with the Applicable Intervenor. FRI and/or FEDRC, as appropriate, shall address EPA's comments (if any). A description of program changes shall be maintained on-site during the term of this Consent Decree but need not be submitted to the agencies.	Previously submitted.
146	Training. If not already in place, FRI and FEDRC shall commence implementation of the following training programs at each Covered Refinery:	Training is conducted as required and records are maintained.
146a	As of the Date of Entry of this Consent Decree, for any employee newly-assigned to LDAR responsibilities, FRI and FEDRC shall require that each such employee satisfactorily complete LDAR training prior to beginning any LDAR work;	Training is conducted as required and records are maintained.
146b	By no later than the Date of Entry, for all FRI and FEDRC employees assigned specific LDAR responsibilities as a primary job function, such as monitoring technicians, database users, quality assurance/quality control ("QA/QC") personnel and the LDAR Coordinator, FRI and FEDRC shall provide and require completion of annual LDAR refresher training and initial training before the employee begins LDAR responsibilities;	Training is conducted as required and records are maintained.
146c	By no later than the Date of Entry, for all other FRI and FEDRC employee operations and maintenance personnel, FRI and FEDRC shall provide and require completion of an initial training program that includes instruction on aspects of LDAR that are relevant to the person's duties. Refresher training for these personnel shall be performed every three years;	Training is conducted as required and records are maintained.

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146d	if contract employees are performing LDAR work, FRI and/or FEDRC, as appropriate, shall maintain all training records, as required under this Paragraph, for the contract employees; and e. Training records shall be kept for a period of five (5) years.	Training is conducted as required and records are maintained.
147	LDAR Audits. At their respective Covered Refineries, FRI and FEDRC shall implement the refinery-wide audits set forth in Paragraphs 147 - 150 to ensure each Covered Refinery's compliance with all applicable LDAR requirements. The LDAR audits shall include but not be limited to, comparative monitoring, observation of the LDAR technicians' calibration and monitoring techniques, records review to ensure monitoring and repairs were completed in the required periods, a field audit to ensure affected equipment has been identified and included in the facility LDAR program, and a review to ensure records and reports have been maintained and submitted as required. During the LDAR audits, leak rates shall be calculated for each process unit where comparative monitoring was performed. Each LDAR audit shall be conducted by personnel with expertise in LDAR regulations.	LDAR audit program was implemented. See below for details.
148	148. Initial Compliance Audit. By no later than the Date of Entry, at their respective Covered Refineries, FRI and FEDRC shall engage a third-party contractor to undertake a refinery-wide audit of its compliance with the LDAR regulations at each of the Covered Refineries, including, at a minimum, each of the audit requirements set forth in Paragraph 147. No later than sixty (60) days after completion of each audit, FRI and FEDRC shall report to EPA and the Applicable Intervenor any areas of non-compliance identified as a result of its refinery-wide audits and submit in writing proposed compliance schedule for correcting any non-compliance. If the proposed compliance schedule(s) extends for more than sixty (60) days beyond the audit completion date, FRI and/or FEDRC, as applicable, must seek approval of the compliance schedule from EPA. At their respective Covered Refineries, FRI and FEDRC shall implement the compliance schedule as proposed until the schedule is approved or disapproved by EPA. Unless the request for a schedule extension is approved by EPA, within ninety (90) days of completing each audit and by no later than two hundred and forty (240) days after the Date of Entry, FRI and FEDRC shall certify to EPA that each Covered Refinery: a. is in compliance; b. has completed related corrective action (if necessary) and/or is on a compliance schedule; and c. specifically certify that all affected equipment has been identified and included in the facility LDAR program to the extent of the program as of the Date of Entry.	Previously completed.
149	Third-Party Audits. FRI and FEDRC shall retain one or more independent contractor(s) to perform a third-party audit of each of the Covered Refineries' LDAR programs, including compliance with LDAR regulations and the LDAR requirements under Section VI.M. of this Consent Decree, at least once every four (4) years.	Third-Party audits are conducted as required.

Paragraph	Attachment H - Miscellaneous	Audits are conducted by third-parties every 2 years. The last audit was completed in August 2013.	
	Internal Audits. FRI and FEDRC shall conduct internal audits of each of the Covered Refineries' LDAR programs by sending personnel from one Covered Refinery to audit the other Covered Refinery's LDAR program. The audits, among other things, shall include a review of compliance with LDAR regulations and the LDAR requirements under Section VI.M. of this Consent Decree. FRI and FEDRC shall complete the first internal LDAR audit at each Covered Refinery by no later than two years after the initial third-party audit for the Covered Refinery was conducted according to Paragraph 148. Internal audits of each of the Covered Refineries shall be conducted at least once every four years thereafter. FRI and/or FEDRC may elect to retain third-parties to undertake these internal audits, provided that an audit of each of the Covered Refineries occurs every two (2) years.		
151	Audit Every Two Years. To ensure that an audit at each of the Covered Refineries occurs every two years, third- party and internal audits shall be separated by two years.	Internal audits are conducted by thin parties every 2 years. The last audit was completed in August 2013.	
153	Internal Leak Definition for Valves and Pumps. Except as provided in Subparagraph 153.c., on and after the Date of Entry, for the Covered Refineries FRI and FEDRC shall utilize the following internal leak definitions for valves and pumps in light liquid and/or gas/vapor service, unless other permit(s), regulations, or laws require the use of lower leak definitions:	Implemented as required.	
1535	Leak Definition for Valves. 500 ppm VOCs for all the Covered Refinery's valves, excluding pressure relief devices; and	Implemented as required.	
153b	Leak Definition for Pumps. 2,000 ppm VOCs for all of the Covered Refinery's pumps.	Implemented as required.	
154	Reporting of Valves and Pumps Based on the Internal Leak Definitions. For regulatory reporting purposes, FRI and FEDRC may continue to report leak rates in valves and pumps against the applicable regulatory leak definition or use the lower, internal leak definitions specified in Paragraph 153. FRI and FEDRC shall identify in the report which definition is being used.	Frontier includes in applicable regulatory reports both the applicable regulatory leak definition and the internal leak definition.	
155	Recording, Tracking, Repairing and Re-Monitoring Leaks Based on the Internal Leak Definitions. By no later than the date FRI and FEDRC implement the lower leak definitions under Paragraph 153, each shall record, track, repair and re-monitor all leaks in excess of the internal leak definitions in Paragraph 153. FRI and FEDRC shall have five (5) days to make an initial repair attempt and re-monitor the component under Paragraph 157.a and thirty (30) days either to make repairs and re-monitor leaks that are greater than the internal leak definitions but less than the applicable regulatory leak definitions or to place the component on the delay of repair list according to Paragraph 167. All records of repairs, repair attempts, and re-monitoring shall be maintained for the life of this Consent Decree.	Implemented as required.	

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156	Election of Compliance for Initial Attempt at Repair or Use of IR Camera. Within thirty (30) days of the Date of Entry of this Consent Decree, for each Covered Refinery, FRI and FEDRC shall notify EPA and the Applicable Intervenor as to which one of the following options it shall comply with: a. FRI and/or FEDRC shall comply with Paragraph 157.a. of this Consent Decree; or b. FRI and/or FEDRC shall comply with Paragraph 157.b. of this Consent Decree. If either FRI or FEDRC elects the option in Paragraph 156.a., above, at any time after the Date of Entry of this Consent Decree, either may, at its option, conduct a study of the efficacy of reducing VOC emissions from utilizing the 200 ppm of VOCs leak level for the initial attempt at repair. FRI or FEDRC may submit the results of such study to EPA with a request for EPA approval to change its election to the option in Paragraph 156.b. above.	Frontier elected to comply with 156b The program to conduct initial attempt at repair has been implemented as required.	
157	Additional VOC Monitoring. Upon the election of the compliance option under Paragraph 156, FRI and FEDRC shall comply with at least one of the following additional VOC monitoring requirements:	Frontier elected to comply with 156b The program to conduct initial attempt at repair has been implemented as required.	
157a	Initial Attempt at Repair. No later than sixty (60) days after the Date of Entry, FRI and FEDRC shall promptly make an "initial attempt" at repair on all valves that have a reading greater than 200 ppm of VOCs, excluding control valves. FRI and FEDRC, shall re-monitor the leaking valve within five (5) days of identification. i. If the re-monitored leak rate is below the applicable leak definition, Paragraph 153, no further action shall be necessary. ii. If the re-monitored leak reading is greater than the applicable leak definition, Paragraph 153, repair the leaking valve according to the requirements under Paragraph 155. All records of repairs, repair attempts, and re-monitoring shall be maintained for the life of this Consent Decree. iii. If FRI or FEDRC can demonstrate with sufficient monitoring and repair data that this "initial attempt" at repair requirement at 200 ppm does not reduce emissions, after two (2) years of implementing the "initial attempt" requirement, either may request that the EPA reconsider or amend this requirement;	Frontier elected to comply with 156b The program to conduct initial attempt at repair has been Implemented as required.	
158	LDAR Monitoring Frequency: Pumps. Unless more frequent monitoring is required by a federal or state regulation when the lower internal leak definition for pumps becomes applicable pursuant to the provisions of Paragraph 153, FRI and FEDRC shall begin monitoring pumps in light liquid service, other than dual-mechanical seal pumps or pumps vented to a control device, at the lower leak definition on a monthly basis.	Pumps are monitored as required.	
159	LDAR Monitoring Frequency: Valves. Unless more frequent monitoring is required by a federal or state regulation when the lower internal leak definition for valves becomes applicable pursuant to the provisions of Paragraph 153, FRI and FEDRC shall monitor valves, other than difficult-to-monitor or unsafe-to-monitor valves, on a quarterly basis.	Valves are monitored as required.	
160	Electronic Storing and Reporting of LDAR Data. FRI and FEDRC have and shall continue to maintain an		

Paragraph	Attachment H - Miscellaneous	Comments		
161	Electronic Data Collection During LDAR Monitoring and Transfer. Beginning no later than the Date of Entry, FRI and FEDRC shall use data loggers and/or electronic data collection devices during LDAR monitoring. FRI and FEDRC, or their respective designated contractor(s), shall use their best efforts to transfer, on a daily basis, electronic data from electronic data logging devices to the electronic database required by Paragraph 160. For all monitoring events in which an electronic data collection device is used, the collected monitoring data shall include a time and date stamp, and instrument and operator identification. FRI and FEDRC may use paper logs where necessary or more feasible (e.g., small rounds, remonitoring, or when data loggers are not available or broken), and shall record, at a minimum, the identification of the technician undertaking the monitoring, the date, the daily start and end time for monitoring, and the identification of the monitoring equipment. FRI and FEDRC shall transfer any manually recorded monitoring data to the electronic database required by Paragraph 160 within seven (7) days of monitoring. FRI and FEDRC shall maintain the LDAR information required by this Paragraph for the life of this Consent Decree.			
162	QA/QC of LDAR Data. If not already in place, beginning no later than the Date of Entry, FRI and FEDRC shall develop and implement a procedure to ensure a QA/QC review of all data generated by LDAR monitoring technicians. At their respective Covered Refineries, FRI and FEDRC shall ensure that monitoring collected by monitoring technicians is reviewed for QA/QC by the technician daily. At least once per calendar quarter, FRI and FEDRC shall QA/QC the monitoring data collected during the quarter which shall include, but not be limited to, an evaluation of the number of components monitored per technician, time between monitoring events, and abnormal data patterns. Results from LDAR monitoring indicating any leaks requiring a first-attempt repair shall be reported to unit supervisors daily.	QA/QC program is in place.		
163	LDAR Personnel. By no later than one-hundred and eighty (180) days after the Date of Entry, at their respective Covered Refineries, FRI and FEDRC shall establish a program that shall hold LDAR personnel accountable for LDAR performance. FRI and FEDRC shall maintain a position responsible for LDAR management, with authority to implement improvements, ("LDAR Coordinator") at each Covered Refinery.	Contained in the LDAR sitewide monitoring plan.		
164	Adding New Valves and Pumps. By no later than one-hundred and eighty (180) days after the Date of Entry, FRI and FEDRC shall establish a tracking program for maintenance records (e.g., a Management of Change program) to ensure that new valves and pumps added to each of the Covered Refineries during maintenance and construction are integrated into the LDAR program.	The MOC program at the facility is utilized to track new valves and pumps. Frontier recently voluntarily disclosed audit findings indicating some valves and pumps were not caught by this program. The program has been updated.		
165	Calibration. FRI and FEDRC shall conduct all calibrations of LDAR monitoring equipment using methane as the calibration gas, in accordance with 40 C.F.R. Part 60, Appendix A, EPA Reference Test Method 21, and shall maintain records of the calibrations for the life of this Consent Decree.	Calibrations are conducted as required.		

Paragraph	Attachment H - Miscellaneous	Comments
156	Calibration Drift Assessment. Beginning no later than the Date of Entry, FRI and FEDRC shall, at each Covered Refinery, at a minimum conduct calibration drift assessments of LDAR monitoring equipment at the end of each monitoring shift. FRI and FEDRC shall conduct the calibration drift assessment using, at a minimum, a 500 ppm calibration gas. If any calibration drift assessment after the initial calibration shows a negative drift of more than 10% from the previous calibration, FRI and FEDRC shall re-monitor all valves that were monitored since the last calibration that had a reading greater than 100 ppm and shall re-monitor all pumps that were monitored since the last calibration that had a reading greater than 500 ppm.	Calibration drift assessments are conducted as required. Frontier recently voluntarily disclosed audit findings indicating that these requirements may have been missed on a few monitoring events. Details are in the disclosure.
167	Delay of Repair. Beginning no later than the Date of Entry, at their respective Covered Refinery, FRI and FEDRC shall implement the following requirements:	Program previously implemented.
167a	For all equipment: i. Require sign-off by the unit supervisor that the piece of equipment is technically infeasible to repair without a process unit shutdown, before the component is eligible for inclusion on the "delay of repair" list; and ii. Include equipment that is placed on the "delay of repair" list in regular LDAR monitoring.	Program previously implemented.
167b	For valves: For valves (other than control valves) leaking at a rate of 10,000 ppm or greater that cannot otherwise be repaired, FRI and FEDRC shall use "drill and tap" or similarly effective repair methods to repair such leaking valves unless they can document that there is a safety, mechanical, or major environmental concern posed by repairing the leak in this manner. FRI and FEDRC shall make two repair attempts (if necessary) using "drill and tap" or similarly effective repair method within thirty (30) days of identification of the leak.	Program previously implemented.
168	New Method of Repair for Leaking Valves. If a new valve repair method not currently in use by the refining industry is planned to be used by FRI or FEDRC, they shall advise EPA pursuant to Section XIX (General Provisions), Paragraph 356 (Notice) prior to implementing such a method or, if prior notice is not practicable, as soon as practicable after implementation.	No new methods of repair are being utilized or proposed.
169	Chronic Leaker Program. FRI and FEDRC shall replace, re-pack, or perform similarly effective repairs on all chronically leaking non-control valves at the next process unit turnaround. A chronic leaker shall be defined as any component that leaks above 10,000 ppm twice in any consecutive four (4) quarters. If a component has not leaked above 10,000 ppm for a period of twelve (12) consecutive quarters or more prior to a turnaround, it is exempt from the requirements in this Paragraph.	Program previously implemented.

Paragraph	Attachment H - Miscellaneous	Information included in reports. See those reports for details.	
171	171. Reports due under 40 C.F.R. § 63.654. In each report due under 40 C.F.R. § 63.654, FRI and FEDRC shall include: a. Training. Information identifying the measures implemented to comply with the provisions of Paragraphs 146 and 163; and b. The following information on LDAR monitoring and repairs: i. the number of valves and pumps present in each process unit during the quarter; ii. the number of valves and pumps monitored in each process unit; iii. an explanation for missed monitoring if the number of valves and pumps present exceeds the number of valves and pumps monitored during the quarter; iv. the number of valves and pumps found leaking via Method 21; v. the number of leaks identified through optical imaging (if performing); vi. the number of "difficult to monitor" pieces of equipment monitored; vii. a list of all equipment currently on the "delay of repair" list and the date each component was placed on the list; viii. the number of repair attempts not completed promptly according to Paragraph 155 or completed within five (5) days pursuant to Paragraph 157; ix. the number of repairs not completed within thirty (30) days or placed on the delay of repair list according to Paragraph 155 and/or Paragraph 167; x. the number of chronic leakers that do not get repaired according to the requirements of Paragraph 169; and xi. the number of repairs to leaks identified through optical imaging which are not performed within five (5), or fifteen (15), or forty-five (45) days, respectively, according to Paragraphs 157.b.		
N	CERCLA/EPCRA Reviews		
172	CERCLA/EPCRA Compliance Review. FRI and FEDRC shall each conduct a CERCLA/EPCRA Compliance Review at their respective Covered Refinery of the five (5) year period prior to the Date of Entry of this Consent Decree to identify any releases that may have been reportable under Section 103(a) of CERCLA, 42 U.S.C. § 9603(a), and Section 304 of EPCRA, 42 U.S.C. § 11004, or similar or corresponding state reporting regulations. Upon completion of this review, FRI and FEDRC shall resolve their respective liability for potential violations of Section 103(a) of CERCLA and Section 304 of EPCRA, or similar or corresponding state reporting regulations, with respect to the events identified in its Compliance Review by completing the following activities no later than one hundred and twenty (120) days after the Date of Entry:	Previously completed.	
172	For all releases for which FRI and FEDRC seek a resolution of liability, submit a CERCLA/EPCRA Compliance Review Report to EPA and the Applicable Intervenor that identifies potential violations of Section 103(a) of CERCLA and Section 304 of EPCRA, or similar or corresponding state reporting regulations;	Previously completed.	
172b	Based on the Compliance Review Report, correct and/or update release reporting procedures and identify specific steps FRI and FEDRC shall take to ensure compliance in the future. FRI and FEDRC shall submit a copy of the corrected reporting procedures to EPA and the Applicable Intervenor; and	Previously completed.	
172c	Conduct training for the environmental compliance staffs at FRI and FEDRC to instruct them on the reporting requirements of Section 103(a) of CERCLA, 42 U.S.C. § 9603(a), and Section 304 of EPCRA, 42 U.S.C. § 11004, or similar or corresponding state reporting regulations, and to acquaint the compliance staffs with the procedures adopted by FRI and FEDRC to meet those requirements.	Most recent training completed August 2013.	

Paragraph	Attachment H - Miscellaneous Comments					
VII	ENVIRONMENTALLY BENEFICIAL PROJECTS					
188	isnali at its Chevenne. Wyoming Ketinery spend no less than 5405 URU to implement and complete the	SEP project to install two geodesic domes completed in Feb 2010.				
189	FRI shall install a geodesic dome fixed roof on two 70 foot diameter finished gasoline storage tank which are designated Tank 2-70 and 2-71. Installing the geodesic dome roofs will convert the current external floating roof tank to an internal floating roof tank which FRI represents will reduce the amount of VOC and other hazardous air pollutants from the converted tank by approximately 49,490 pounds per year ("lb/yr").					
190	FRI shall submit a detailed description of the SEP, a work plan, and SEP implementation schedule to EPA and WDEQ for review and approval within one hundred and eighty (180) days of the Date of Entry of this Consent Decree. Installing the fixed roofs requires that the tanks be taken out of service for approximately four to six weeks. This has the potential to impact gasoline supplies in the area. FRI shall develop a work plan to minimize any such impacts. Within thirty (30) days of final approval by EPA, FRI shall implement the SEP in accordance with the approved work plan and schedule. FRI shall complete implementation of the project in accordance with the election made under Paragraph 220 unless an alternative schedule is approved in writing by EPA and WDEQ.	SEP project to install two geodesic domes completed in Feb 2010.				
200	SEP Performance. SEPs described in this Section VII. shall conform to the requirements of EPA's "EPA Supplemental Projects Policy" (effective May 1, 1998). SEP work plans submitted under this Section VII are incorporated by reference herein and are enforceable as part of this Consent Decree.	SEP project to install two geodesic domes completed in Feb 2010.				
201	If at any time prior to the completion of the projects identified in Paragraphs 188 through 199, either FEDRC or FRI is required to perform any of those projects pursuant to a federal, state, or local statute, regulation, or permit, then FEDRC and/or FRI, as applicable, shall not receive SEP credit for the amounts expended on that project. Within one hundred and twenty (120) days of any event that invalidates a specific SEP: a. For FEDRC, FEDRC shall propose for approval by EPA and KDHE an additional SEP of equal or greater value to be performed at FEDRC or in the same community as the invalidated SEP; and b. For FRI, FRI shall propose for approval by EPA and WDEQ an additional SEP of equal or greater value to be performed at FRI or in the same community as the invalidated SEP.	SEP project to install two geodesic domes completed in Feb 2010.				

Paragraph	Attachment H - Miscellaneous	Comments	
202	FRI and FEDRC are responsible for the satisfactory completion of the SEPs identified in Paragraphs 188 through 199 of this Consent Decree. Upon completion of each SEP, FEDRC and/or FRI, as applicable, shall submit to EPA and the Applicable Intervenor a SEP construction completion and cost report (documenting SEP expenditures and including copies of invoices, receipts, purchase orders, etc.) accompanied by a certification by a responsible corporate official in the form required pursuant to Paragraph 219 of this Consent Decree. a. If FRI and/or FEDRC do not expend the entire projected cost of any SEP, then FRI and/or FEDRC, as applicable, shall pay a stipulated penalty equal to the difference between the amount expended as demonstrated in the certified cost report and the projected cost with one half of that amount payable to EPA and the remaining half payable to the Applicable Intervenor. The stipulated penalty shall be paid as provided in Section XIII (Stipulated Penalties) of this Consent Decree. b. If FRI and/or FEDRC withdraw a SEP, or otherwise do not implement a SEP required under this Consent Decree, then FRI and/or FEDRC, as applicable, shall either: (i.) Notwithstanding the election in Paragraph 220, pay a stipulated penalty equal to one hundred and ten percent (110%) of the full cost of the withdrawn SEP. This stipulated penalty shall apply in lieu of stipulated penalties under Paragraph 298 of this Consent Decree. One half of the foregoing amount shall be payable to EPA and the remaining half payable to the Applicable Intervenor; or (ii.) Propose for approval by EPA and the Applicable Intervenor a substitute SEP or SEPs of equal or greater value to be performed at the Covered Refinery or in the same community as the withdrawn SEP.	SEP project to install two geodesic domes completed in Feb 2010.	
203	Should FEDRC or FRI, as applicable, fail to implement any SEP in accordance with the schedule approved by EPA and the Applicable Intervenor, FEDRC or FRI, as applicable, shall be liable for the payment of stipulated penalties in accordance with the provisions of Section XIII. (Stipulated Penalties) of this Consent Decree as specified in Paragraph 298 of this Consent Decree.	SEP project to install two geodesic domes completed in Feb 2010.	
204	By signing this Consent Decree, FRI and FEDRC each certifies for its respective refinery that it is not required, and has no liability under any federal, state or local law or regulation or pursuant to any agreement or order of any court, to perform or develop any of the SEP projects identified in Paragraphs 188 through 199 of this Consent Decree. Further, FRI and FEDRC each certifies for its respective refinery that it has not applied for or received, and will not in the future apply for or receive credit as a SEP or other penalty offset in any other enforcement action for any project set forth in Paragraphs 188 through 199 of this Consent Decree and, except as otherwise specifically provided in this Consent Decree, credit for any emissions reduction resulting from any SEP project set forth in Paragraphs 188 through 199 of this Consent Decree in any federal, state or local emissions netting, trading, or early reduction program, or similar emissions compliance program. For federal income tax purposes, FRI and FEDRC each agree for its respective refinery that it will neither capitalize into inventory or basis nor deduct any costs or expenditures incurred in performing SEPs.	SEP project to install two geodesic domes completed in Feb 2010.	
206	FRI and FEDRC each agree that in any public statements regarding these SEPs, FRI and FEDRC shall clearly indicate that these projects are being undertaken as part of the settlement of an enforcement action for alleged violations of the CAA and corollary state statutes.	Frontier does not issue public statements regarding the SEPs.	

Paragraph	Attachment H - Miscellaneous	Comments
VII	INCORPORATION OF CONSENT DECREE REQUIREMENTS INTO FEDERALLY ENFORCEABLE PERMITS.	
207	Obtaining Permit Limits for Consent Decree Emission Limits That Are Effective Upon Entry. By no later than one hundred and twenty (120) days after the Date of Entry of this Consent Decree, FRI and FEDRC shall submit applications to the Applicable Intervenor(s) to incorporate the emission limits and standards required by this Consent Decree that are effective as of the Date of Entry into federally enforceable minor or major new source review permits or other permits (other than CAA Title V permits). Following submission of the permit applications, FRI and FEDRC shall cooperate with the Applicable Intervenor by promptly submitting to the Applicable Intervenor all information that the Applicable Intervenor seeks following their receipt of the permit applications. Upon issuance of such permits or in conjunction with such permitting, FRI and FEDRC shall file any applications necessary to incorporate the requirements of those permits into the CAA Title V permit for the relevant Covered Refinery.	
208	Obtaining Permit Limits for Consent Decree Emission Limits That Become Effective After Date of Entry. As soon as practicable, but in no event later than ninety (90) days after the effective date or establishment of any emission limits and/or standards under Section VI. (Affirmative Relief) of this Consent Decree, FRI and FEDRC, as appropriate, shall submit applications to the Applicable Intervenor to incorporate those emission limits and/or standards, identified in Appendix J, into federally enforceable minor or major new source review permits or other permits, other than CAA Title V permits, which are federally enforceable. Following submission of the permit application(s), FRI and FEDRC, as appropriate, shall cooperate with the Applicable Intervenor by promptly submitting to the Applicable Intervenor all information that the Applicable Intervenor seeks following its receipt of the permit application. Upon issuance of such permit or in conjunction with such permitting, FRI and FEDRC, as applicable, shall file any applications necessary to incorporate the requirements of that permit into the Title V permit of the appropriate Covered Refinery.	Frontier has applied for the limits and is working with WDEQ to incorporate them as needed.
209	be in accordance with the applicable state or local CAA Title V rules.	Frontier has applied for the limits and is working with WDEQ to incorporate them as needed.
210	Construction Permits. FRI and FEDRC each agree to use best efforts to obtain all required, federally enforceable permits for the construction of the pollution control technology and/or the installation of equipment necessary to implement the affirmative relief and environmental projects set forth in Section VI. (Affirmative Relief) and Section VII (Environmentally Beneficial Projects) of this Consent Decree. To the extent that FRI and/or FEDRC must submit permit applications for this construction or installation to the Applicable Intervenor(s), they each shall cooperate with the Applicable Intervenor by promptly submitting to the Applicable Intervenor all information that the Applicable Intervenor seeks following its receipt of the permit application.	Frontier has applied for the limits and is working with WDEQ to incorporate them as needed.

Attachment H - EMISSIONS SUMMARY

P217F - Summary of All Other Emission Sources

	PM	SO2	NOx	CO	
Grand Total	292	153	22	16	CEMs, Emission Factors,
Grand Total					Stack Tests, Various